

JAERI-M
83-002

BASE INPUT FOR LARGE BREAK LOCA
ANALYSIS OF COMMERCIAL PWR WITH
PUBLISHED VERSION OF THYDE-P1
(THYDE-P1 SAMPLE CALCULATION RUN 21)

January 1983

Masashi HIRANO and Seiji KOSUGI

日本原子力研究所
Japan Atomic Energy Research Institute

JAERI-M
83-002

BASE INPUT FOR LARGE BREAK LOCA
ANALYSIS OF COMMERCIAL PWR WITH
PUBLISHED VERSION OF THYDE-P1
(THYDE-P1 SAMPLE CALCULATION RUN 21)

January 1983

Masashi HIRANO and Seiji KOSUGI

日本原子力研究所
Japan Atomic Energy Research Institute

JAERI-M レポートは、日本原子力研究所が不定期に公刊している研究報告書です。

入手の問合わせは、日本原子力研究所技術情報部情報資料課（〒319-11 茨城県那珂郡東海村）あて、お申しこしください。なお、このほかに財団法人原子力弘済会資料センター（〒319-11 茨城県那珂郡東海村 日本原子力研究所内）で複写による実費頒布をおこなっております。

JAERI-M reports are issued irregularly.

Inquiries about availability of the reports should be addressed to Information Section, Division of Technical Information, Japan Atomic Energy Research Institute, Tokai-mura, Naka-gun, Ibaraki-ken 319-11, Japan.

© Japan Atomic Energy Research Institute, 1983

編集兼発行 日本原子力研究所
印刷 日立高速印刷株式会社

Base Input for Large Break LOCA Analysis of Commercial PWR
with Published Version of THYDE-P1
(THYDE-P1 Sample Calculation Run 21)

by

Masashi HIRANO and Seiji KOSUGI

Division of Nuclear Safety Evaluation
Tokai Research Establishment

(Received January 6, 1982)

This report describes input data to be used with the THYDE-P1 interim version SVO2LO3, which has been published through NEA DATA BANK in April, 1982, and its calculated results. The input data consist of three input data sets, one is for steady state and the following transients and the other two are for restarting, and they are successively used for a through calculation of a large break loss-of-coolant accident (LOCA) of a 1,100 MWe commercial pressurized water reactor (PWR) with "best estimate" (BE) options. The major purposes to set up the input data are not only to provide users sample data in publishing THYDE-P1 but also to demonstrate the ability of the published version of THYDE-P1 without any modification to perform a through calculation of a large break LOCA. The results from the present calculation will also be widely utilized as a bench mark in performing sensitivity calculations and further code modifications. In this sense, the input can be called a base input for the published version of THYDE-P1.

This report also contains the results from several sensitivity calculations, which show high capability of the version of THYDE-P1 to analyse large break LOCAs.

Keywords : THYDE-P1, LOCA, Large Break, 1,100 MWe Commercial PWR, Through Calculation, Base Input

公開版 THYDE-P1 による商用 PWR
大破断 LOCA 解析用ベースインプット
(THYDE-P1 サンプル計算 Run21)

日本原子力研究所東海研究所安全解析部
平野 雅司・小杉 誠司

(1983年1月6日受理)

1982年4月に、NEAデータ・バンクを通して公開されたTHYDE-P1コード(SV02L03)用インプットデータ、及びその計算結果を報告する。本インプットデータは、3個のインプットデータセットにより構成され、1個は、定常及びそれに続く過渡計算用で、他の2個は、再スタート用であり、これらのデータセットで、最適評価モデルによる1,100MWe商用PWR大破断冷却材喪失事故(LOCA)の一貫解析を行う。本インプットデータは、THYDE-P1の公開に際して、利用者にサンプルデータを提供すると共に、公開版THYDE-P1の大破断LOCA一貫解析性能を検証する目的で作成された。また、本解析結果は、今後、感度解析や、コードの修正を実施する際のベンチマークとして広範に利用可能である。その意味から、本インプットデータは、公開版THYDE-P1のベースインプットと呼び得る。

また、本報告では、いくつかの感度解析の結果も含まれており、それらは、公開版THYDE-P1の高い解析性能を示している。

Contents

1.	Introduction	1
2.	Description of Base Input Data	3
2.1.	Usage of Base Input Data	3
2.2.	Input Data Presentation	3
2.3.	Deviation from Run 20	7
3.	Results and Discussions from Base Calculation, Run 21	11
3.1.	Pressure Transient	11
3.2.	Fuel and Core	11
3.3.	Downcomer and Lower Plenum	12
3.4.	Break	12
3.5.	ECC Injection	12
3.6.	Reflooding	13
4.	Sensitivity Calculations	29
4.1.	Pump On and Off	29
4.2.	CHF Correlations	30
4.3.	Minimum Stable Film Boiling Temperature Model	36
5.	Conclusion	43
	Acknowledgement	43
	References	44
	Appendix A Input data list	47
	Appendix B Figures showing results from base calculation	59

目 次

1	序	1
2	ベースインプットデータの記述	3
2.1	ベースインプットデータの使用法	3
2.2	インプットデータの記述	3
2.3	Run 20 との相違点	7
3	ベース計算Run21の結果, 及び議論	11
3.1	圧力の過渡変化	11
3.2	燃料, 及び炉心	11
3.3	ダウンカマ, 及び下部プレナム	12
3.4	破断点	12
3.5	ECC注入	12
3.6	再冠水	13
4	感度解析	29
4.1	ポンプ作動, 及び停止	29
4.2	臨界熱流束相関式	30
4.3	最小安定膜沸騰温度モデル	36
5	結 論	43
	謝 辞	43
	参考文献	44
	付録 A インプットデータリスト	47
	付録 B ベース計算の結果	59

List of Figures

No.	Title	Page
2-1	Nodalization of base input data	8
3-1-1	Intact loop hot leg and pressurizer pressures	15
3-1-2	SG primary and secondary pressures at intact loop	15
3-1-3	SG primary and secondary pressures at broken loop	16
3-2-1	Cladding surface temperatures in average channel	17
3-2-2	Cladding surface temperatures in hot channel	17
3-2-3	Fuel centre temperatures in average channel	18
3-2-4	Fuel centre temperatures in hot channel	18
3-2-5	Core inlet flows	19
3-2-6	Core outlet flow	19
3-2-7	Heat transfer coefficients in average channel	20
3-2-8	Heat transfer coefficients in hot channel	20
3-3-1	Mass fluxes at inlet and outlet of downcomer	21
3-3-2	Equilibrium node average densities at downcomer and lower plenum	21
3-3-3	Differential pressure through downcomer	22
3-4-1	Pressures at break point	23
3-4-2	Hot leg side of break flow	23
3-4-3	Cold leg side of break flow	24
3-4-4	Equilibrium coolant qualities at break points	24
3-5-1	ECC injection mass fluxes	25
3-5-2	Coolant temperatures at ECC injection ducts	25
3-6-1	Differential pressure through core	26
3-6-2	Differential pressure through intact loop	26
3-6-3	Differential pressure through broken loop	27
3-6-4	Differential pressure through broken loop cold leg	27
3-6-5	Mass flow rates through hot legs of intact and broken loops	28
4-1-1	Experimental cladding surface temperatures in LOFT Large Break Experiments L2-3 and L2-5	31
4-1-2	Normalized pump speeds	31
4-1-3	Pump heads	32
4-1-4	Normalized pump hydraulic torques	32

List of Figures (continued)

No.	Title	Page
4-1-5	Normalized pump flows	33
4-1-6	Cladding surface temperatures at middle of hot channel	33
4-1-7	Core inlet mass fluxes	34
4-1-8	Hot leg side of break flows	34
4-1-9	Cold leg side of break flows	35
4-1-10	Intact loop hot leg pressures	35
4-2-1	Cladding surface temperatures at middle of hot channel	37
4-2-2	Fuel centre temperatures at middle of hot channel	37
4-2-3	Heat transfer coefficients at middle of hot channel	38
4-3-1	Boiling curve in present MSFBI model	40
4-3-2	Cladding surface temperatures at bottom of hot channel	41
4-3-3	Cladding surface temperatures at middle of hot channel	41
4-3-4	Cladding surface temperatures at top of hot channel	42
B-1	Normalized power	59
B-2-1	Upper plenum pressure (short range)	60
B-2-2	Break pressures (short range)	60
B-2-3	Accumulator pressures (short range)	61
B-2-4	Pressures during reflooding (broken loop)	61
B-2-5	Pressures during reflooding (intact loop)	62
B-2-6	Gap pressures	62
B-3-1	Mass flow rates at cross flow area	63
B-3-2	Mass flow rates at core bypass	63
B-3-3	Mass flow rate at pressurizer surge line	64
B-4-1	Coolant temperatures at SG primary system of intact loop ..	65
B-4-2	Coolant temperatures at SG primary system of broken loop ..	65
B-4-3	Coolant temperatures at upper plenum and lower plenum	66
B-4-4	Coolant temperatures at intact loop hot leg and downcomer ..	66
B-4-5	Coolant temperatures at middle of core	67
B-5-1	Differential pressure through core (short range)	68
B-5-2	Differential pressure through broken loop (short range) ...	68

List of Figures (continued)

No.	Title	Page
B-5-3	Differential pressure through intact loop (short range) ...	69
B-5-4	Differential pressures through pumps (short range)	69
B-6-1	Equilibrium densities at intact loop	70
B-6-2	Equilibrium densities at broken loop	70
B-7-1	Pressurizer water level	71
B-7-2	Water levels at SG secondary systems	71
B-7-3	Accumulator water levels	72
B-8-1	Equilibrium coolant qualities at average channel	73
B-8-2	Equilibrium coolant qualities at hot channel	73
B-9-1	Normalized pump speeds	74
B-9-2	Pump heads	74
B-9-3	Normalized pump hydraulic torques	75
B-9-4	Normalized pump volumetric flows	75
B-10-1	Wall temperatures at SG primary system of intact loop	76
B-10-2	Wall temperatures at SG secondary system of intact loop ...	76
B-10-3	Heat transfer coefficients at SG primary system of intact loop.	77
B-10-4	Heat transfer coefficients at SG secondary system of intact loop	77
B-10-5	Heat inputs to coolant per unit volume at SG of intact loop .	78
B-10-6	Heat inputs to coolant per unit volume at SG of broken loop .	78

List of Tables

No.	Title	Page
2-1	Node geometrical data	9
2-2	Loss coefficients of nodes	10
3-1	Chronology of events	14

1. Introduction

The THYDE-P1 code^(1,2) is a computer code to analyse transient thermal-hydraulic responses of pressurized water reactors (PWRs) to postulated loss-of-coolant accidents (LOCAs). Extensive verification calculations⁽³⁻⁹⁾ have been performed so far and the THYDE-P1 interim version SV02L03 has been published through NEA DATA BANK in April, 1982.

A through calculation of a large break LOCA of a 1,100 MWe 4-loop commercial PWR has been carried out using the published version of THYDE-P1 without any modification not only to provide a complete set of input data being called a base input, which is used as sample data for published THYDE-P1, but also to demonstrate the ability of the code to analyse large break LOCAs. This report contains the description of the set of input data, the base data, and the results from the calculation. The base data consist of three input data sets. The first data set is used for the steady state and the following blowdown analysis until 15 sec and the second and the third data sets are used for restarting from 15 sec until 30 sec and from 30 sec to the end of the problem, respectively. The second and the third data sets are the same except the input data for the time constants of the relaxation model⁽⁴⁻⁹⁾.

The base input data have been made based on those used in Sample Calculation Run 20⁽⁴⁾, which is one of a series of THYDE-P1 verification calculations, where the plant geometrical data are almost identical with the RELAP4/MOD5 sample problem⁽¹⁰⁾. The present calculation has been performed also as Sample Calculation Run 21. The major models and assumptions applied in Run 21 are summarized as follows:

- (1) Double-ended guillotine break at the cold leg,
- (2) Discharge coefficient 0.6,
- (3) Pump coastdown just after rupture,
- (4) "Best estimate" (BE) calculation, and
- (5) Two core channel calculation with a single cross flow.

This report also contains the results from several sensitivity calculations using the data which deviates from the base data with respect to pump condition, CHF correlations and a minimum stable film boiling

temperature (MSFBT) correlation, for the sake of future usability. As for the MSFBT correlation, a model has been tentatively developed and studied. The calculated results from the pump on and off of a commercial PWR are shown to be qualitatively consistent with the experimental results from LOFT large break experiments L2-3⁽¹¹⁾ and L2-5^(12,13). By applying the present MSFBT model, the history of the cladding surface temperature at high elevation during the reflooding is shown to be markedly improved.

2. Description of Base Input Data

2.1. Usage of Base Input Data

The THYDE-P1 input requirement has been described in detail in Ref.2). There are two kinds of input data sets in THYDE-P1. One is for starting from an initial steady state and another is for restarting from a restart dump point in a previous run. In the base data, the data for restarting are further divided into two data sets. Therefore the base data for the published version of THYDE-P1 consist of three data sets named Data 1, Data 2 and Data 3 :

- (1) The first data set Data 1 is used for the steady state and the following blowdown until 15 sec,
- (2) The second data set Data 2 is used for restarting from 15 sec to 30 sec, and
- (3) The third data set Data 3 is used for restarting from 30 sec to the end of the problem (250 sec).

In the first data set Data 1, the relaxation model for density change is not taken into account for any nodes and mixing junctions. Therefore, an equilibrium model is applied during the period. In the second data set Data 2, the relaxation model is firstly taken into account in order to avoid the large pressure drop due to very rapid vapor condensation at the duct nodes near the ECC injection points. The time constants τ_{ps} are set in Data 2 to be 4 sec for the ECC duct nodes and the cold leg nodes from 15 sec after rupture. In Data 3, those for the downcomer and lower plenum nodes are set to be 40 sec and those for the core nodes and upper plenum node are set to be 4 sec and 40 sec, respectively, from 30 sec after rupture. The input data sets Data 1, Data 2 and Data 3 are listed in Appendix A.

2.2. Input Data Presentation

The input data of THYDE-P1 Sample Calculation Run 21, the base data, are made based on those used in THYDE-P Sample Calculation Run 20⁽⁴⁾. The major parts of them are summarized in this subsection.

A nodalization scheme in the present calculation is shown in Fig.2-1. The main parts of the plant are expressed by the following nodes:

Average core channel	Nodes 23 to 28
Hot core channel	Nodes 29 to 34
Lower plenum	Node 22
Upper plenum	Node 37
Downcomer	Node 21
S.G. Secondary	Nodes 46 and 47
Accumulator	Nodes 48 and 49
Pressurizer	Node 45
Upperhead	Node 38.

The geometrical data and loss coefficients for each node are shown in Tables 2-1 and 2-2, respectively.

(1) Steam Generator Data

U-tube pitch	3.0×10^{-2} m
Number of U-tubes of one unit	3265
Initial secondary system pressure	62atm
Initial specific enthalpy of feedwater	222 kcal/kg
Initial feedwater mass flow rate	474.0 kg/sec
Initial subcooled water level	4.0 m
Initial void fraction of saturated region	0.95

Initial heat flux

Node No.	Heat flux (kcal/m.sec)
14	65.65
15	49.24
16	41.03

The feedwater is assumed to be shut off at 0.4 sec after LOCA initiation.

(2) Core Data

The core is divided radially into two channels, i.e. an average channel and a hot bundle average channel. The radial peaking factor of the hot channel is assumed to be a value of 1.30. The input data are shown as follows:

Initial heat flux and number of fuel rods

	Hot channel region		Average channel region	
	node no.	heat flux (kcal/m.sec)	node no.	heat flux (kcal/m.sec)
initial heat flux	29	non-heated	23	non-heated
	30	203.0	24	156.0
	31	304.0	25	234.0
	32	304.0	26	234.0
	33	203.0	27	156.0
	34	non-heated	28	non-heated
number of rod	200		39170	

Reactor thermal power	3,479 MWt
Fuel length	3.66 m
Plenum gas volume	1.235×10^{-5} m
Clad outer diameter	1.0732×10^{-2} m
Clad thickness	6.187×10^{-4} m
Pellet diameter	9.3146×10^{-3} m
Fuel rod pitch	1.42×10^{-2} m,

where the last four values are those at a full power operating condition.

(3) Pressurizer Data

Cross-sectional area	3.58 m
----------------------	--------

Height 15.56 m
 Stand pipe length 0.1 m
 Initial subcooled water level 9.0 m
 Initial void fraction of saturated region 0.99

(4) ECCS Data

Accumulator data

Initial water volume 23.3 m
 Initial nitrogen volume 10.0 m
 Specific enthalpy of water 30 kcal/kg
 Initial pressure 44 atm

Pumped injection data

Specific enthalpy of water 30 kcal/kg for each loop
 Mass flow rate 220 kg/sec for each loop

(5) Container pressure

Time(sec)	0.0	7.5	15.0	30.0	1000.0
Pressure(atm)	1.0	2.7	4.0	4.0	4.0

(6) Time constants of relaxation model for density change

After 15 sec:

4 sec for the duct nodes 7, 8, 9, 10, 18, 19, 20, 41, 42, 43 and 44,
 and
 4 sec for all the mixing junctions.

After 30 sec:

40 sec for the nodes 8, 21(downcomer), 22(lower plenum) and
 37(upper plenum),
 4 sec for all the core nodes 23 to 36, and
 10 sec for all the other nodes and all the mixing junctions.

2.3. Deviation from Run 20

The deviation of the base input data from those used in Run 20 is summarized in this subsection.

- (1) The values of diameter and length for pump nodes are modified in order to avoid the large pressure drops at the pump nodes during the early stage of the blowdown.
- (2) The temperature coefficients in the reactivity data BB17 of the sample calculation Run 20 are greater by a factor of about twenty than those of the RELAP4/MOD5 sample problem⁽¹⁰⁾. These data are revised based on the RELAP4/MOD5 sample problem.
- (3) The pump trip index is altered from pump rotor locking into pump coastdown.

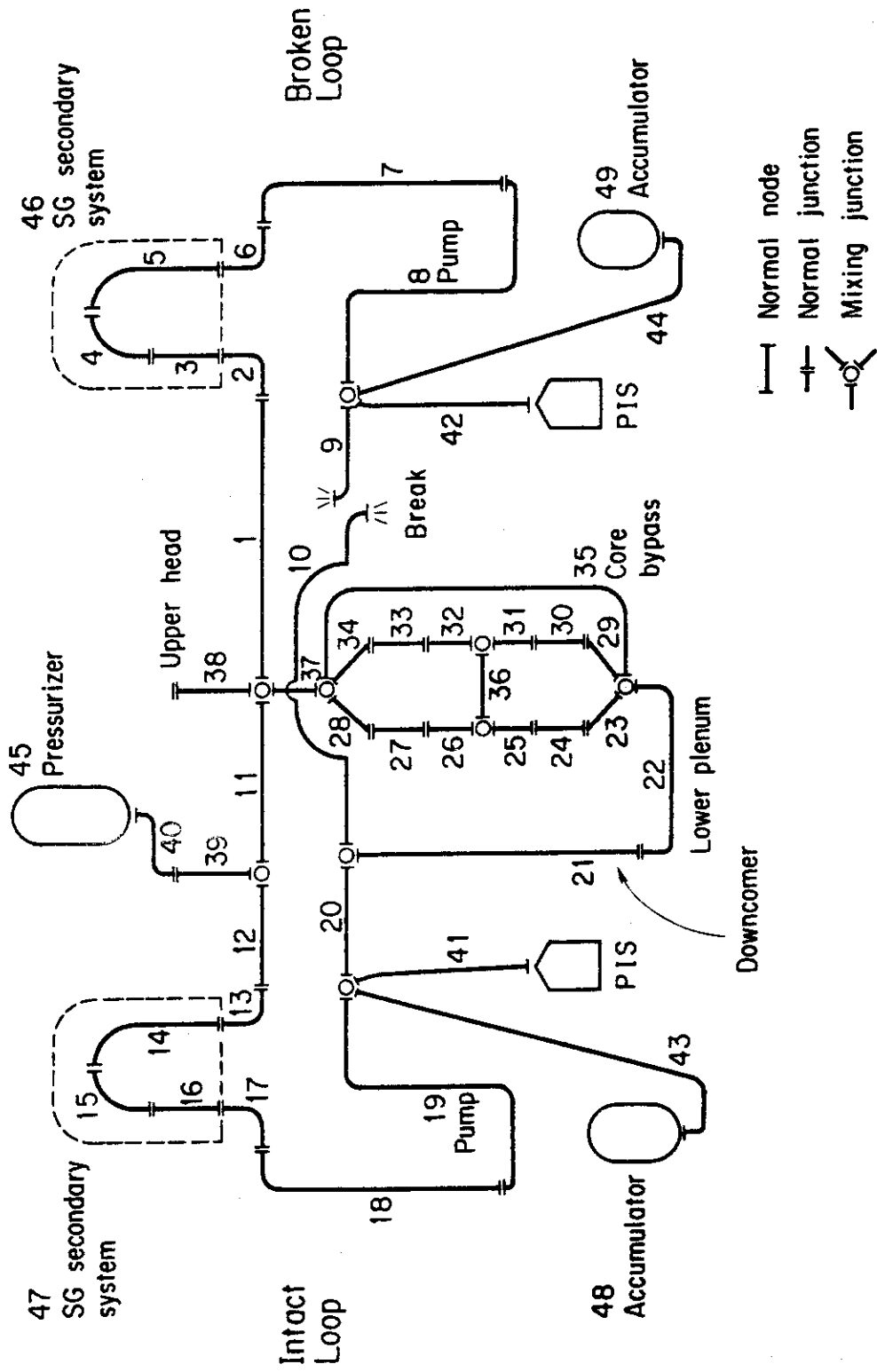


Fig.2-1 Nodalization of base input data

Table 2-1 Node geometrical data

Node No.	Description	Flow Area		Node Length	Node Volume
		A (m ²)	L (m)	L (m)	V (m ³)
1	Broken loop hot leg	0.4266	5.240		2.235
2	SG inlet plenum	2.8953	1.665		4.821
3	SG U-tube	0.9952	5.000		4.976
4	SG U-tube	0.9952	5.460		5.434
5	SG U-tube	0.9952	10.460		10.410
6	SG outlet plenum	2.8953	1.665		4.821
7	Broken loop cold leg	0.4865	7.340		3.571
8	Pump	0.4266	12.412		2.379
9	Broken loop cold leg	0.3837	2.825		1.084
10	Broken loop cold leg	0.3837	3.130		1.201
11	Intact loop hot leg	1.2798	2.000		2.560
12	Intact loop hot leg	1.2798	3.240		4.147
13	SG inlet plenum	8.6859	1.665		14.462
14	SG U-tube	2.9856	5.460		14.928
15	SG U-tube	2.9856	5.460		16.301
16	SG U-tube	2.9856	10.460		31.229
17	SG outlet plenum	8.6859	1.665		14.462
18	Intact loop cold leg	1.4594	7.340		10.712
19	Pump	0.5750	12.412		7.137
20	Intact loop cold leg	1.2798	5.955		6.855
21	Downcomer	2.7435	7.248		19.885
22	Lower plenum	4.8578	6.075		29.511
23	non-Active core in average	4.3552	0.230		1.002
24	Active core in average	4.3552	0.800		3.484
25	Active core in average	4.3552	0.800		3.484
26	Active core in average	4.3552	0.800		3.484
27	Active core in average	4.3552	0.800		3.484
28	non-Active core in average	4.3552	0.230		1.002
29	non-Active core in hot	0.0222	0.230		5.11-3
30	Active core in hot	0.0222	0.800		1.78-2
31	Active core in hot	0.0222	0.800		1.78-2
32	Active core in hot	0.0222	0.800		1.78-2
33	Active core in hot	0.0222	0.800		1.78-2
34	non-Active core in hot	0.0222	0.230		5.11-3
35	Core bypass	0.2419	3.660		0.885
36	Core cross area	9.079-4	0.100		9.08-5
37	Upper plenum	9.2941	4.341		40.346
38	Upper head	3.8568	3.658		14.108
39	Pressurizer surge line	0.0661	15.00		0.992
40	Pressurizer surge line	0.0661	14.30		0.945
41	Pumped injection duct	0.2192	12.00		2.630
42	Pumped injection duct	0.0731	12.00		0.877
43	Accumulator duct	0.1161	120.00		13.932
44	Accumulator duct	0.0387	120.00		4.644

Table 2-2 Loss coefficients of nodes

Node No.	K	K ^{Af}	K ^{Ar}	K ^{Ef}	K ^{Er}
1	0.023	0.043	0.084	0.0	0.0
2	0.021	3.73	1.97	0.0	0.0
3	0.011	0.033	0.048	0.0	0.0
4	0.008	0.0	0.0	0.0	0.0
5	0.017	0.0	0.0	0.033	0.048
6	0.030	0.0	0.0	3.73	1.97
7	0.019	0.042	0.077	0.0	0.0
8	0.303	0.273	0.367	0.203	0.203
9	3.958	0.055	0.015	0.0	0.0
10	0.019	0.0	0.0	0.0	0.0
11	0.024	0.043	0.083	0.0	0.0
12	0.028	0.0	0.0	0.0	0.0
13	0.013	3.73	1.97	0.0	0.0
14	0.025	0.033	0.048	0.0	0.0
15	0.021	0.0	0.0	0.0	0.0
16	0.027	0.0	0.0	0.033	0.048
17	0.029	0.0	0.0	3.73	1.97
18	0.022	0.042	0.077	0.0	0.0
19	3.961	0.055	0.015	0.203	0.203
20	0.011	0.0	0.0	0.0	0.0
21	1.032	0.0	0.0	0.0	0.0
22	1.398	0.0	0.0	0.0	0.0
23	6.416	0.74	0.74	0.0	0.0
24	6.161	0.0	0.0	0.0	0.0
25	6.072	0.0	0.0	0.0	0.0
26	6.218	0.0	0.0	0.0	0.0
27	6.045	0.0	0.0	0.0	0.0
28	6.737	0.0	0.0	0.0	0.0
29	5.295	1.284	2.482	0.0	0.0
30	5.642	0.0	0.0	0.0	0.0
31	5.570	0.0	0.0	0.0	0.0
32	5.574	0.0	0.0	0.0	0.0
33	4.662	0.0	0.0	0.0	0.0
34	6.104	0.76	0.34	0.0	0.0
35	47.857	0.77	0.83	0.87	0.78
36	12.354	0.0	0.0	0.0	0.0
37	2.08-2	0.0	0.0	0.0	0.0
38	5.0	1.491+4	1.491+4	0.0	0.0
39	5.0	0.41	0.87	0.0	0.0
40	5.0	0.0	0.0	0.0	0.0
41	10.0	0.0	0.0	0.0	0.0
42	10.0	0.0	0.0	0.0	0.0
43	10.0	0.109	0.049	0.0	0.0
44	10.0	0.109	0.049	0.0	0.0

3. Results and Discussions from Base Calculation, Run 21

In this section, the calculated results from Run 21 are presented along with the brief discussions on them. The chronology of events is shown in Table 3-1. The other calculated results from Run 21 than those shown in this section are presented in Appendix B without explanation.

3.1. Pressure Transient

The pressures calculated at pressurizer and the intact loop hot leg are shown in Fig. 3-1-1. The hot leg pressure shows that the end of blowdown is about 30 sec after rupture. The calculated SG primary system and secondary system pressures of the intact and broken loop loops are shown in Figs. 3-1-2 and 3-1-3, respectively. As shown in these figures, the maximum pressure at the SG secondary system of the broken loop is higher than that of the intact loop and the depressurization rate of the SG secondary system is also higher in the broken loop than in the intact loop.

3.2. Fuel and Core

The calculated cladding surface temperatures of the average and hot channels are shown in Figs. 3-2-1 and 3-2-2, respectively. The fuel center temperatures are presented in Figs. 3-2-3 and 3-2-4. Rewetting phenomenon during the early portion of the blowdown observed in the LOFT large break experiments⁽¹¹⁾ is calculated to occur only at the bottom of the core as shown in Figs. 3-2-1 and 3-2-2. The cladding surface temperature at the middle of the hot channel reaches a peak at about 50 sec during the very early stage of the reflooding, and then rapidly decreases owing to the effects of ECC water. The mass fluxes at the core inlet and outlet are shown in Figs. 3-2-5 and 3-2-6, respectively. From the figures, it is found that the core flow has large effects on the behavior of the cladding surface temperature. The core flow becomes almost stagnant at 30 sec and then the surface temperatures increase gradually until the reflooding begins. After the reflooding starts, the core nodes become successively quenched from the lower part to the upper one. The quenching in the hot channel is delayed in comparison with the average channel. The time when all the core nodes in the

average channel become quenched is about 170 sec and in the case of the hot channel the time is about 230 sec. The behavior of the cladding surface temperature in the uppermost node seems to be unrealistic in that the quench does not occur even when the surface temperature decreases below 300 C. This point will be discussed later in Subsec. 4.3 .

The histories of the calculated heat transfer coefficients at the average and hot channels are shown in Figs.3-2-7 and 3-2-8, respectively.

3.3. Downcomer and Lower Plenum

Figure 3-3-1 shows the mass fluxes at the inlet and the outlet of the downcomer. At about 47 sec, ECC water begins to enter into the downcomer and after that the flows remain almost positive. The calculated equilibrium densities at the downcomer and the lower plenum are shown in Fig. 3-3-2. It shows that the equilibrium states at the downcomer and the lower plenum become subcooled almost simultaneously at about 50 sec. Fig. 3-3-3 shows the differential pressure through the downcomer, which indicates the collapsed water level of the node. The figure shows the non-equilibrium mixture density of the downcomer gradually approaches to the equilibrium value according to the relaxation model. The time when the downcomer is actually filled with subcooled water is about 200 sec after rupture.

3.4. Break

The histories of the break pressures are presented in Figs. 3-4-1. Figures 3-4-2 and 3-4-3 show the break flows of the hot leg side and the cold leg side, respectively. Figure 3-4-4 shows the equilibrium coolant qualities at the break points. The Figures 3-4-2 and 3-4-3 indicate that the hot leg side of the break flow remains positive throughout the problem. At the hot leg side, on the other hand, the reverse flow occurs twice at about 70 sec and 110 sec, which is due to the rapid system depressurization caused by ECC injection.

3.5. ECC Injection

The mass fluxes and coolant temperatures at the ECC ducts are shown in Figs. 3-5-1 and 3-5-2, respectively. The accumulator at the intact loop is actuated at about 15 sec and terminated at about 70 sec. The pumped injections to the intact and broken loops are actuated by trips at about 25 sec simultaneously with a constant mass flow rate of 220 kg/sec.

3.6. Reflooding

The calculated differential pressure through the core is shown in Fig. 3-6-1. The figure shows that the total amount of mass accumulation in the core increases rather rapidly during the early portion of the reflooding but decreases or remains almost constant during the later portion. The calculated differential pressures through the intact loop, through the SG side of the broken loop and through the vessel side of the broken loop are shown in Figs. 3-6-2, 3-6-3 and 3-6-4, respectively. Differential pressures through the intact loop and the broken loop (hot leg side) have similar trends to each other but the former is larger than the latter. The reason is that the mass flow rate through the broken loop is higher than that through the intact loop especially during the early portion of the reflooding as shown in Fig. 3-6-5.

The reason for the negative values of the differential pressure through the vessel side of the broken loop cold leg (see Fig. 3-6-4) is that the reverses flows are calculated to occur due to the system depressurization.

Table 3-1 Chronology of events

Time (sec)	Events
0.01	Rupture took place.
0.01	Pumps were tripped off.
0.15	Voiding started at top of hot channel.
0.22	Voiding started at intact loop hot leg.
0.3	Voiding started at upperhead.
0.4	SG feed waters were tripped off.
3.5	Voiding started at lower plenum.
9.0	Accumulator injection to broken loop started.
16.0	Accumulator injection to intact loop started.
22.0	Pressurizer emptied.
22.5	Pumped injections started by trips.
47.0	ECC water started to penetrate downcomer(end of bypass).
48.0	Reflooding started(bottom of core recovery).
63.0	Accumulator injection to broken loop ended.
66.0	Accumulator injection to intact loop ended.
170.0	Reflooding ended at average channel.
230.0	Reflooding ended at hot channel.

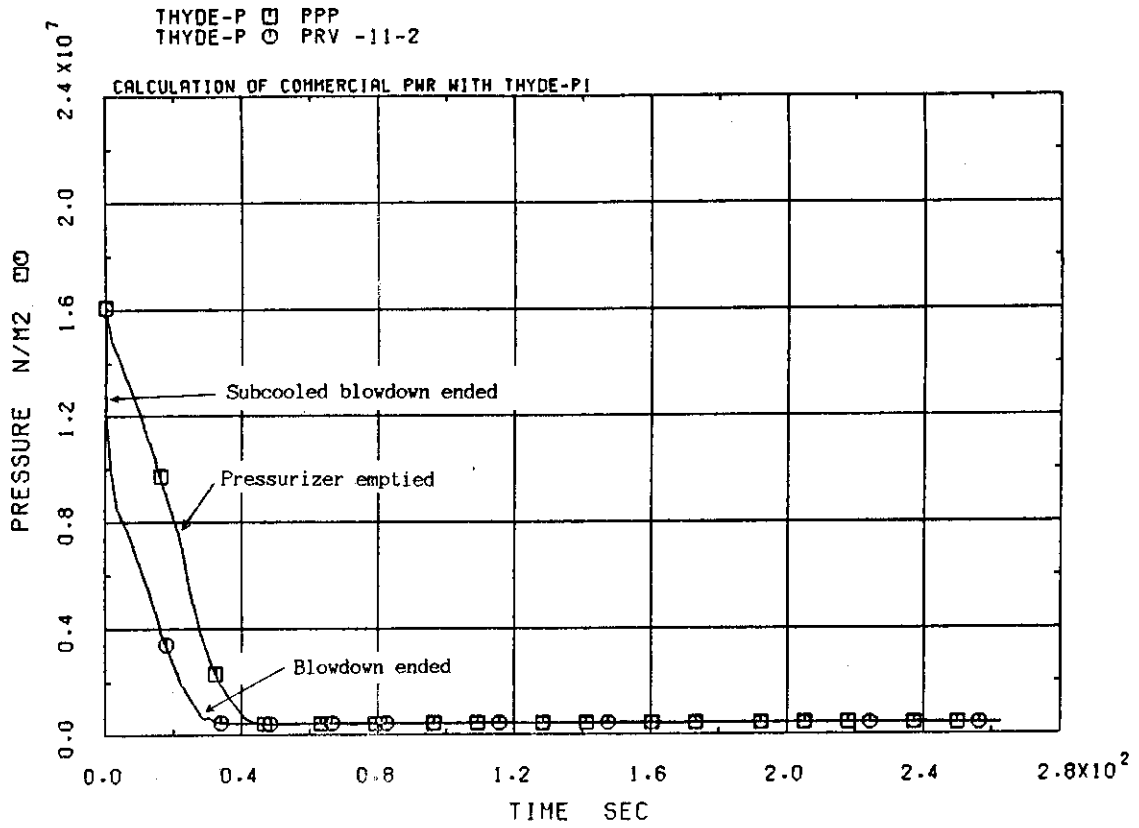


Fig.3-1-1 Intact loop hot leg and pressurizer pressures

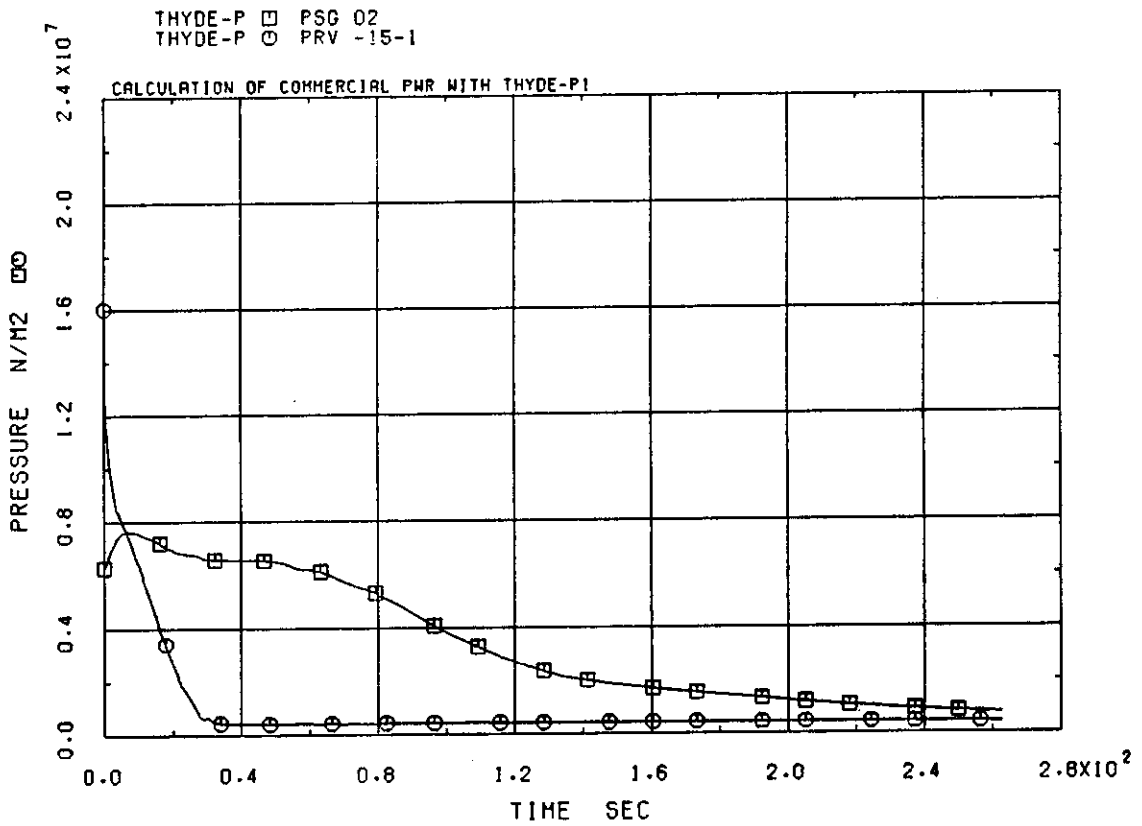


Fig.3-1-2 SG primary and secondary pressures at intact loop

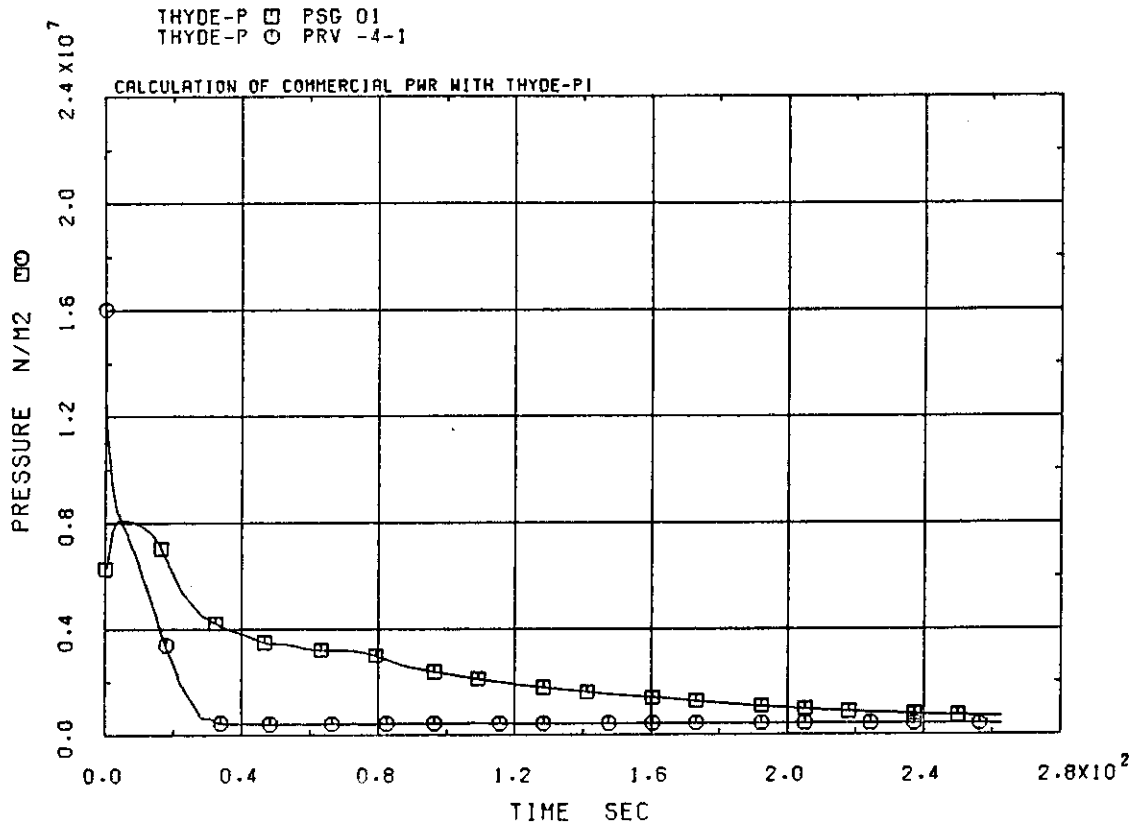


Fig.3-1-3 SG primary and secondary pressures at broken loop

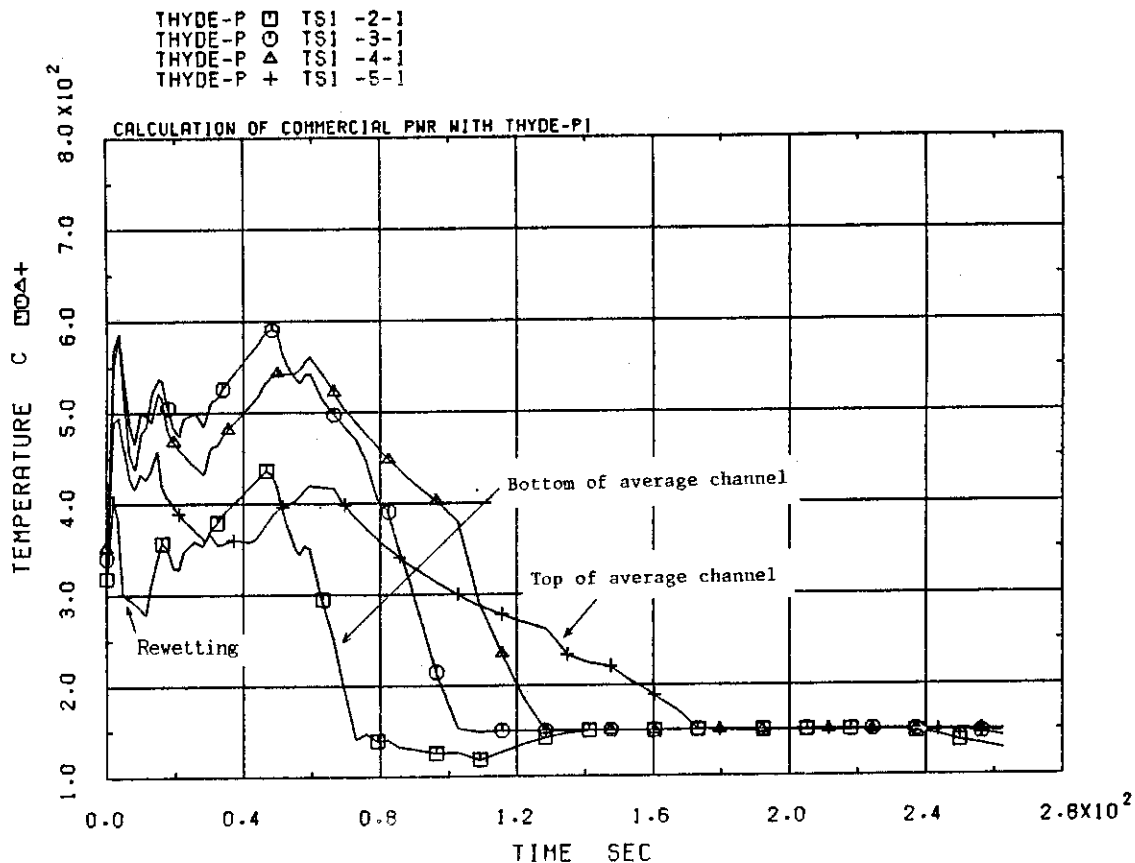


Fig.3-2-1 Cladding surface temperatures in average channel

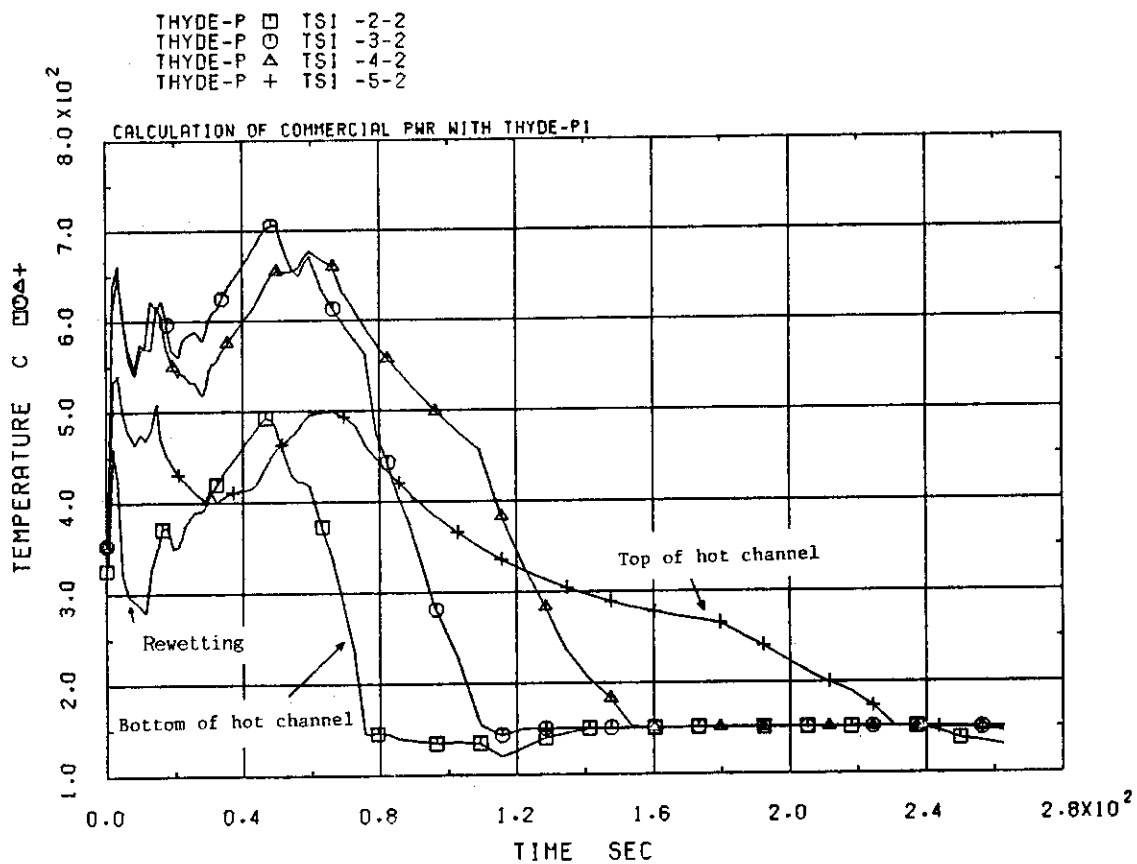


Fig.3-2-2 Cladding surface temperatures in hot channel

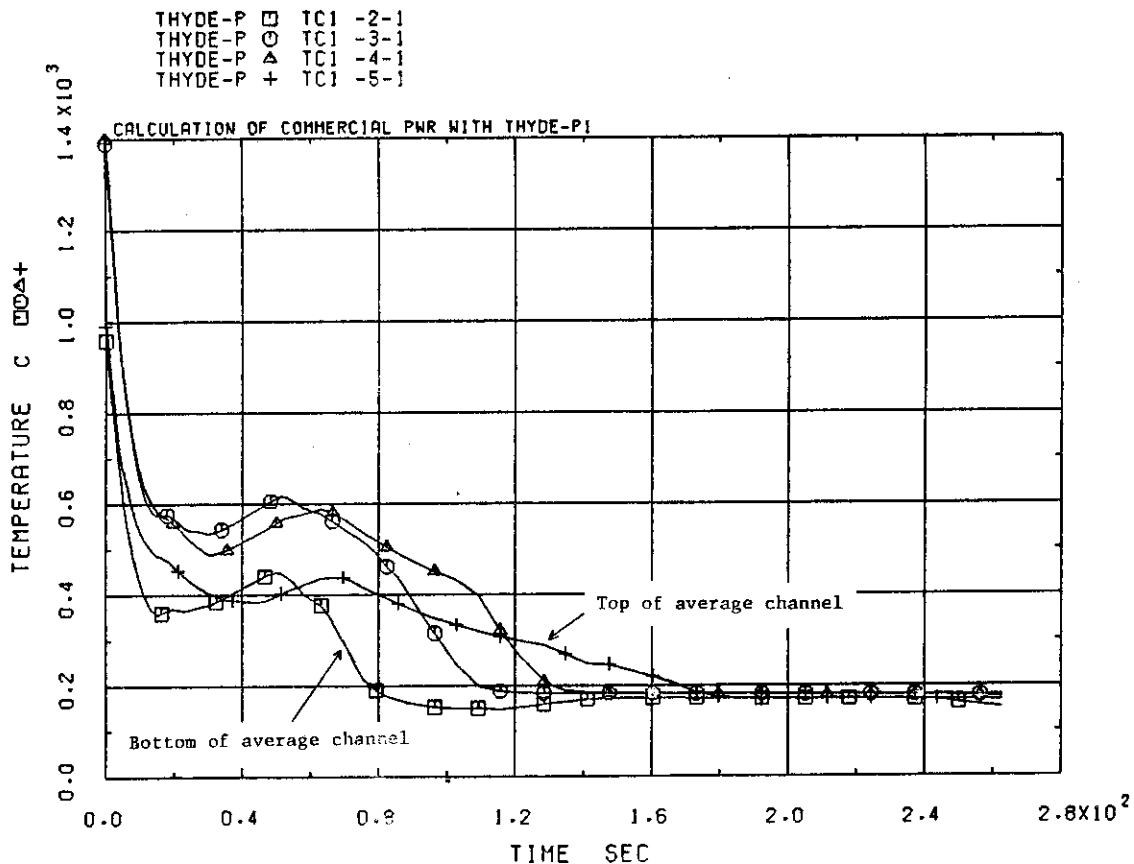


Fig.3-2-3 Fuel centre temperatures in average channel

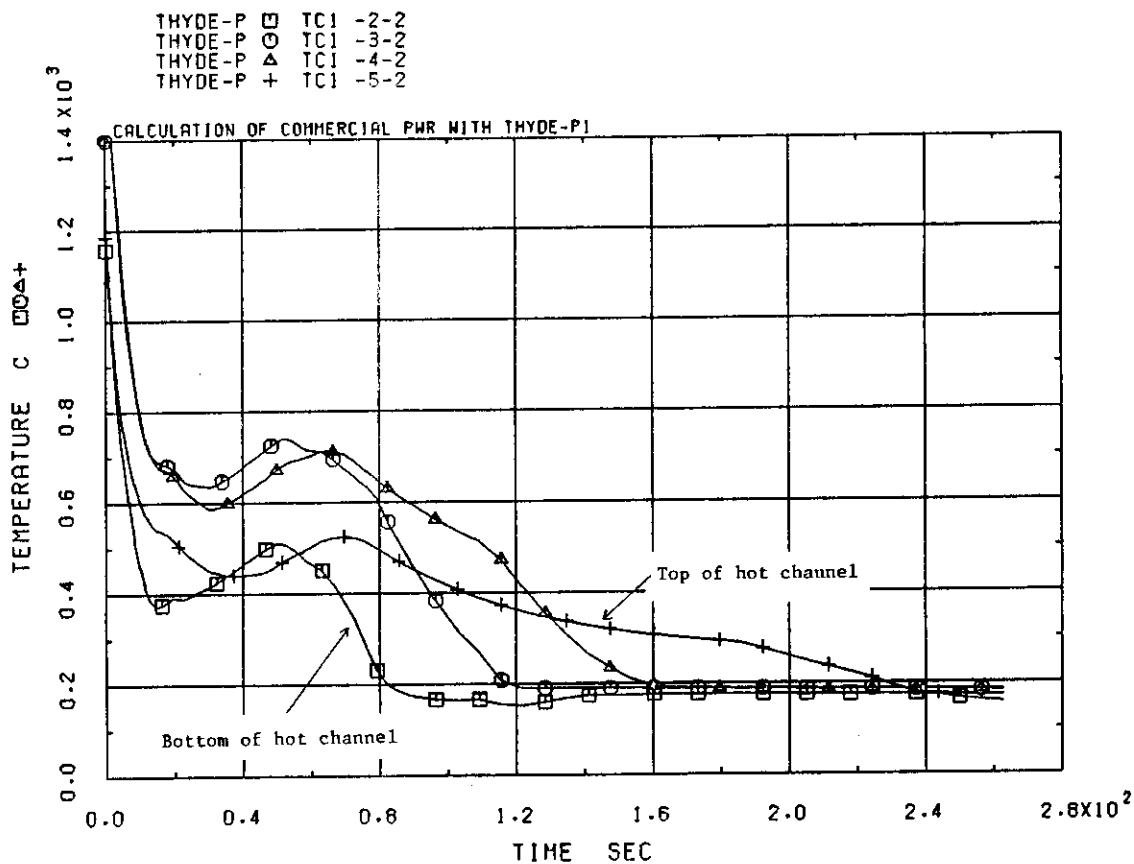


Fig.3-2-4 Fuel centre temperatures in hot channel

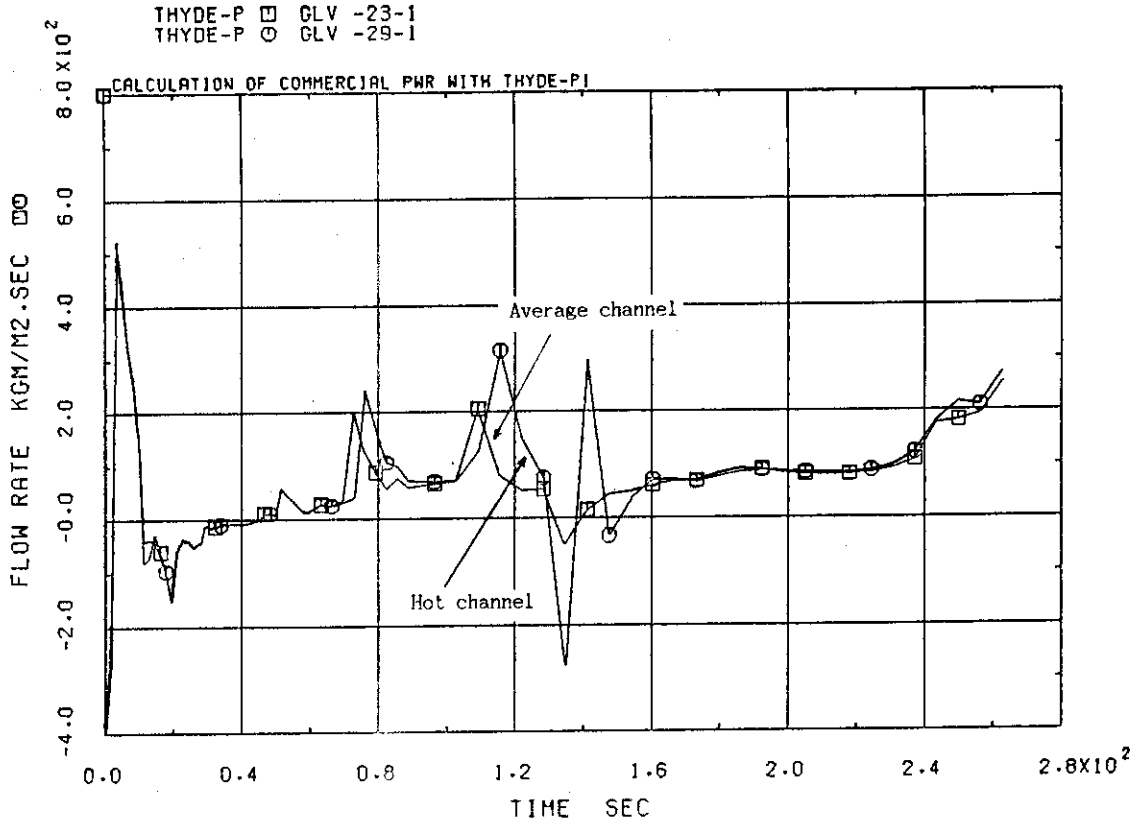


Fig.3-2-5 Core inlet flows

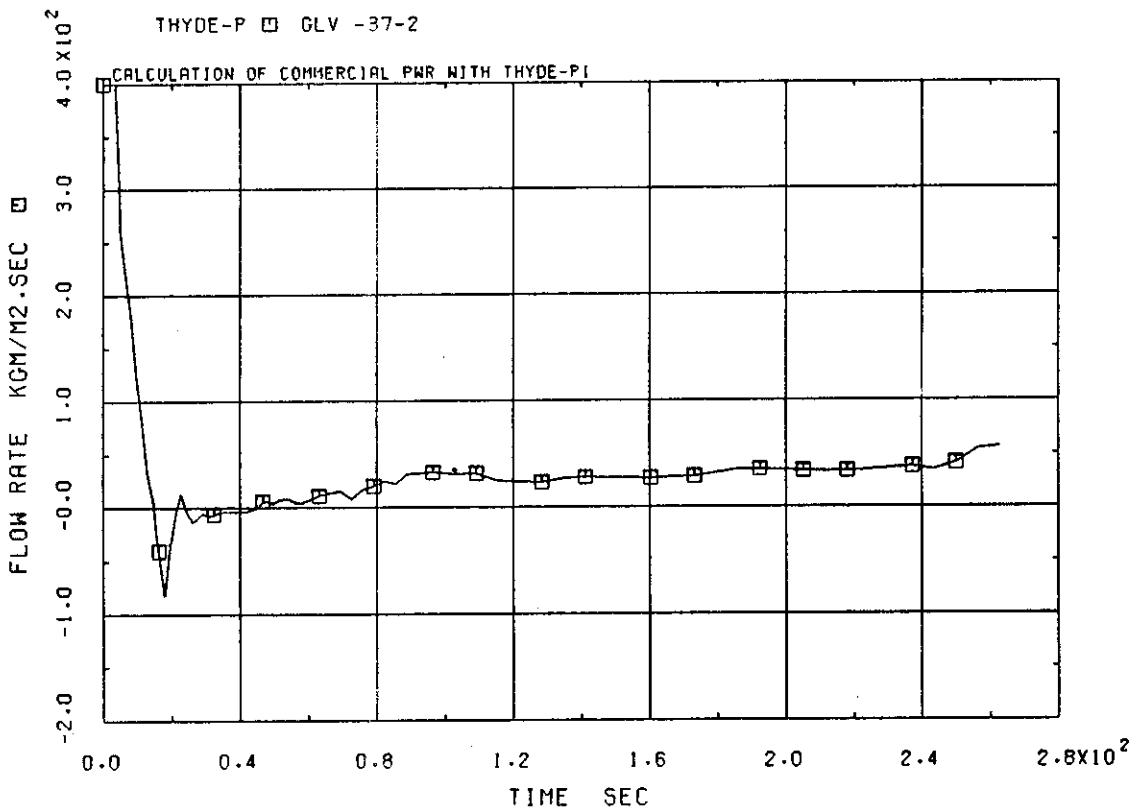


Fig.3-2-6 Core outlet flow

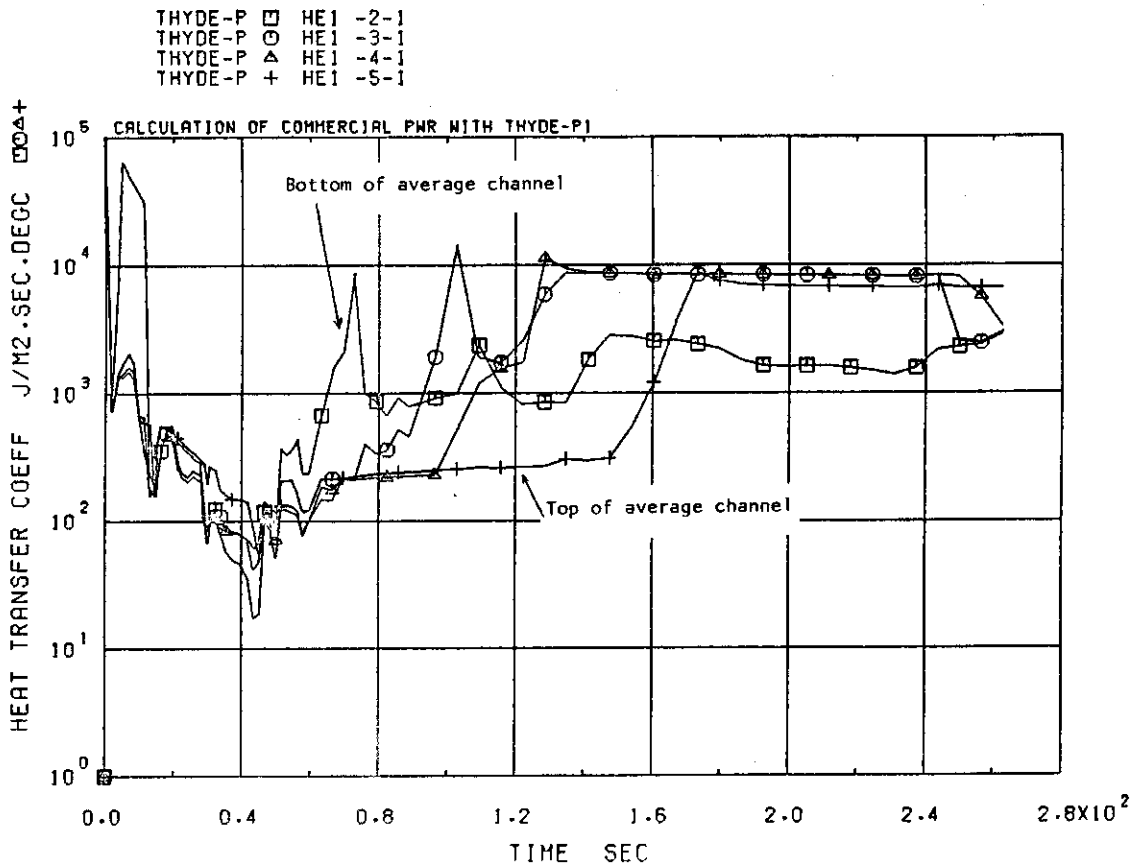


Fig.3-2-7 Heat transfer coefficients in average channel

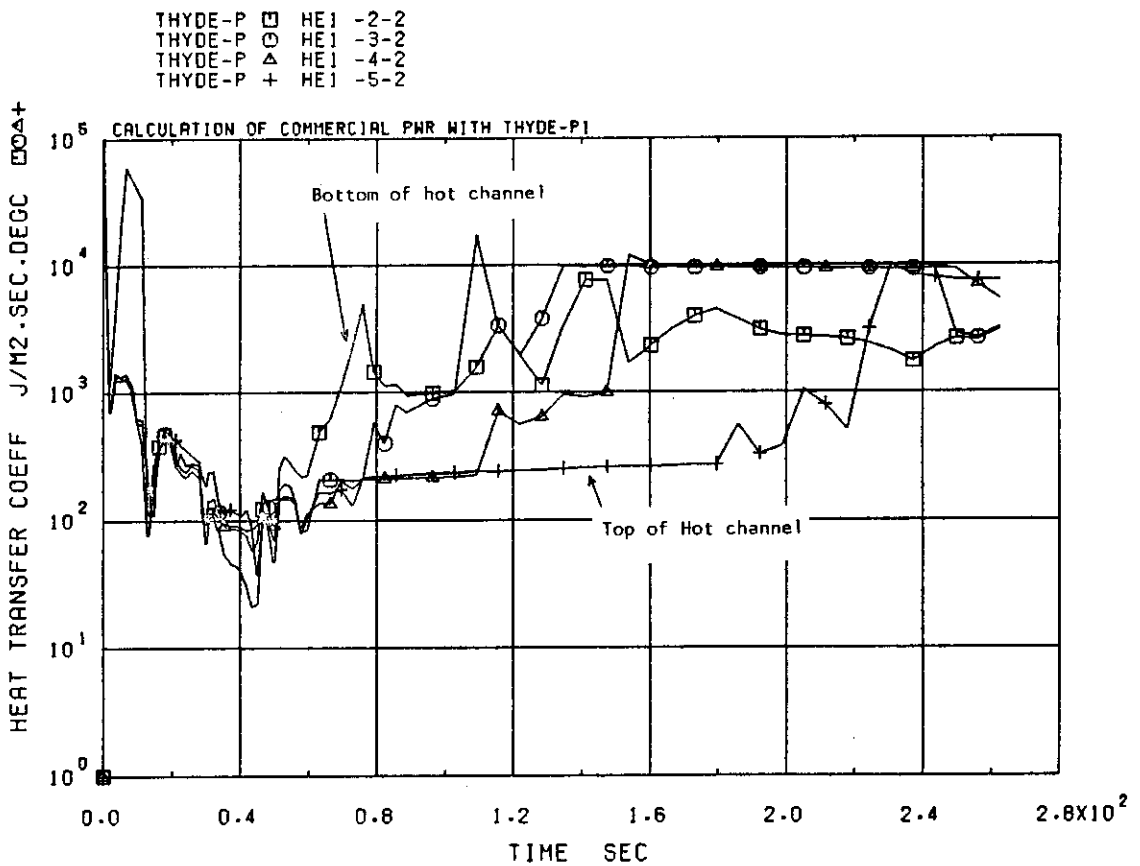


Fig.3-2-8 Heat transfer coefficients in hot channel

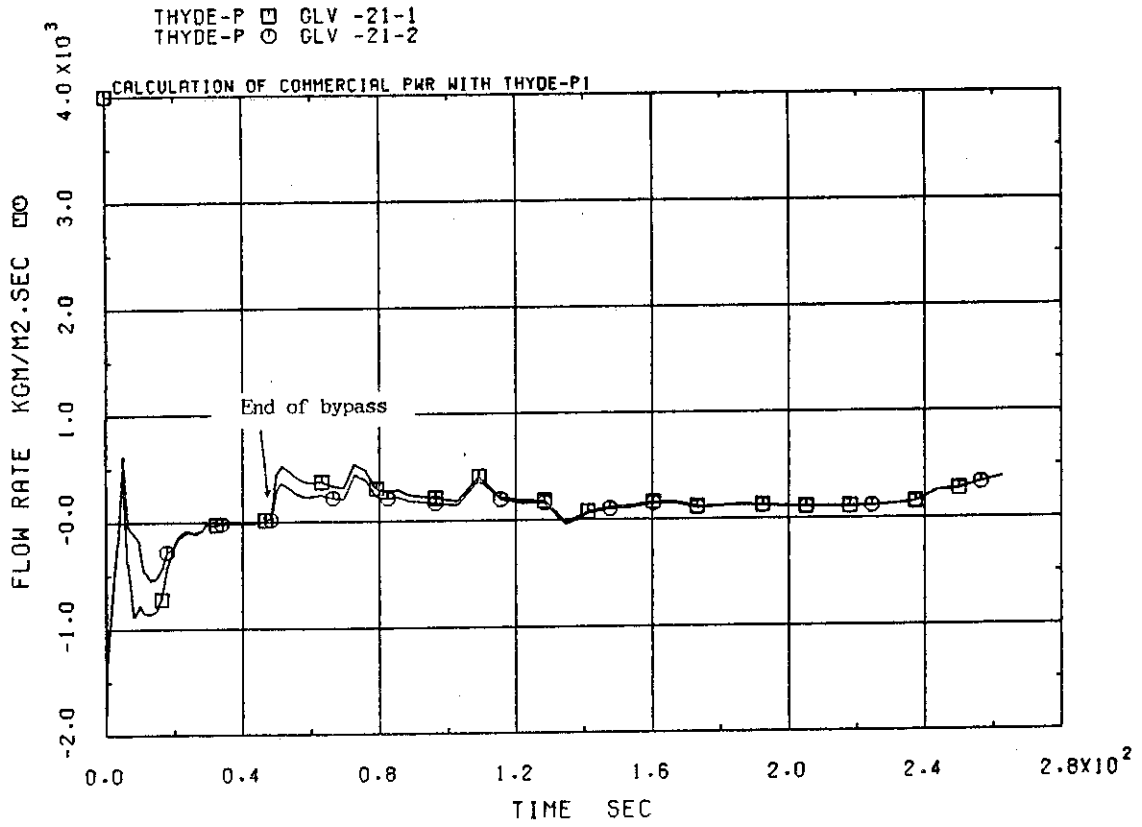


Fig.3-3-1 Mass fluxes at inlet and outlet of downcomer

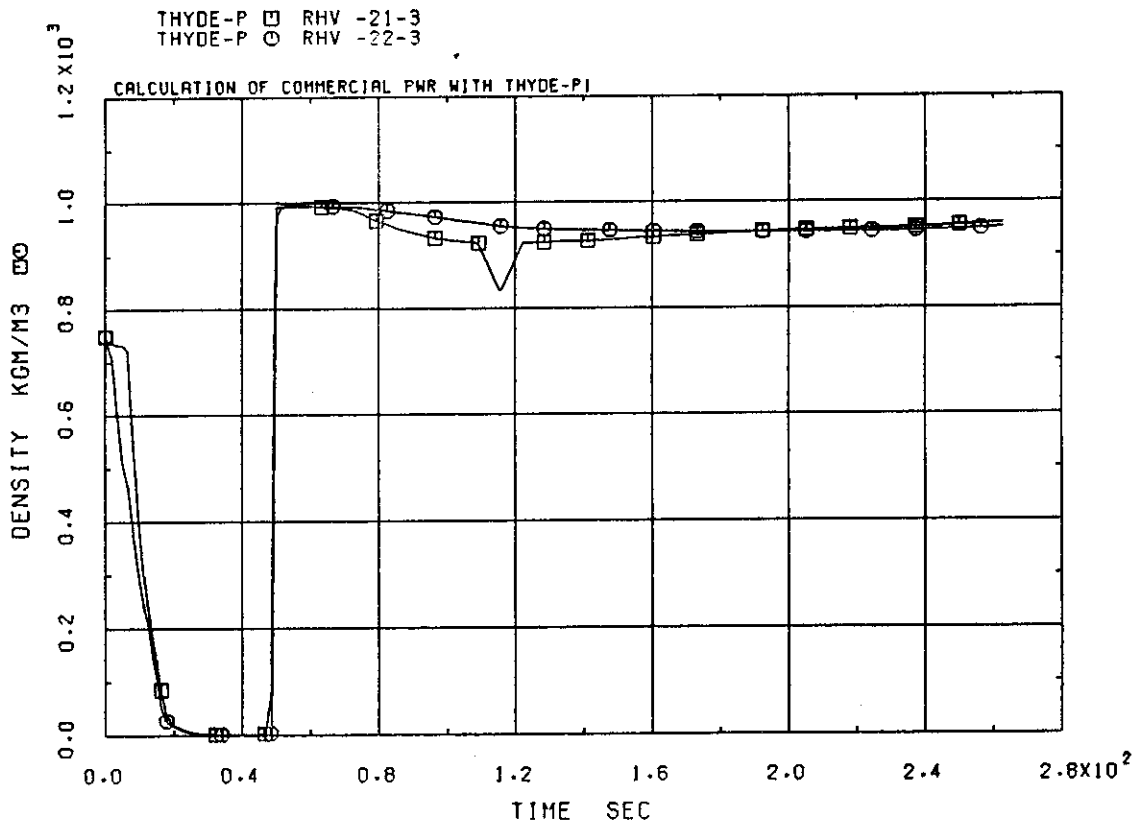


Fig.3-3-2 Equilibrium node average densities at downcomer and

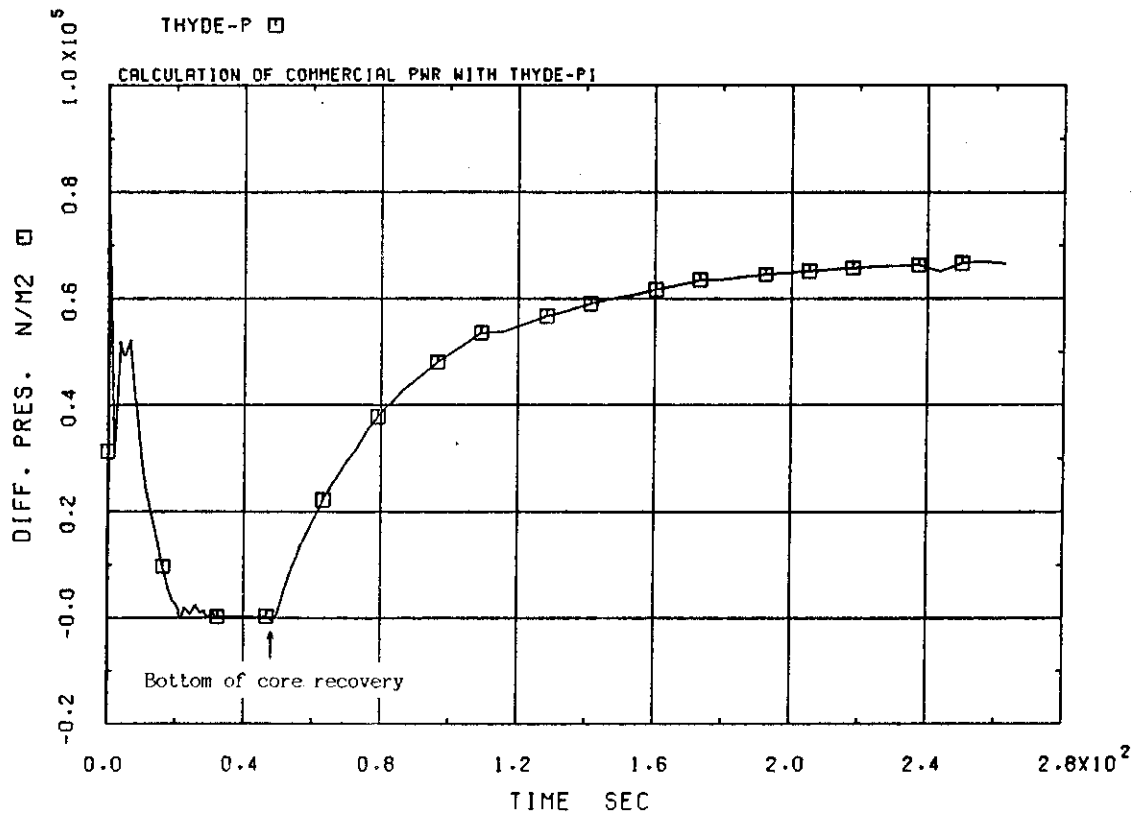


Fig.3-3-3 Differential pressure through downcomer

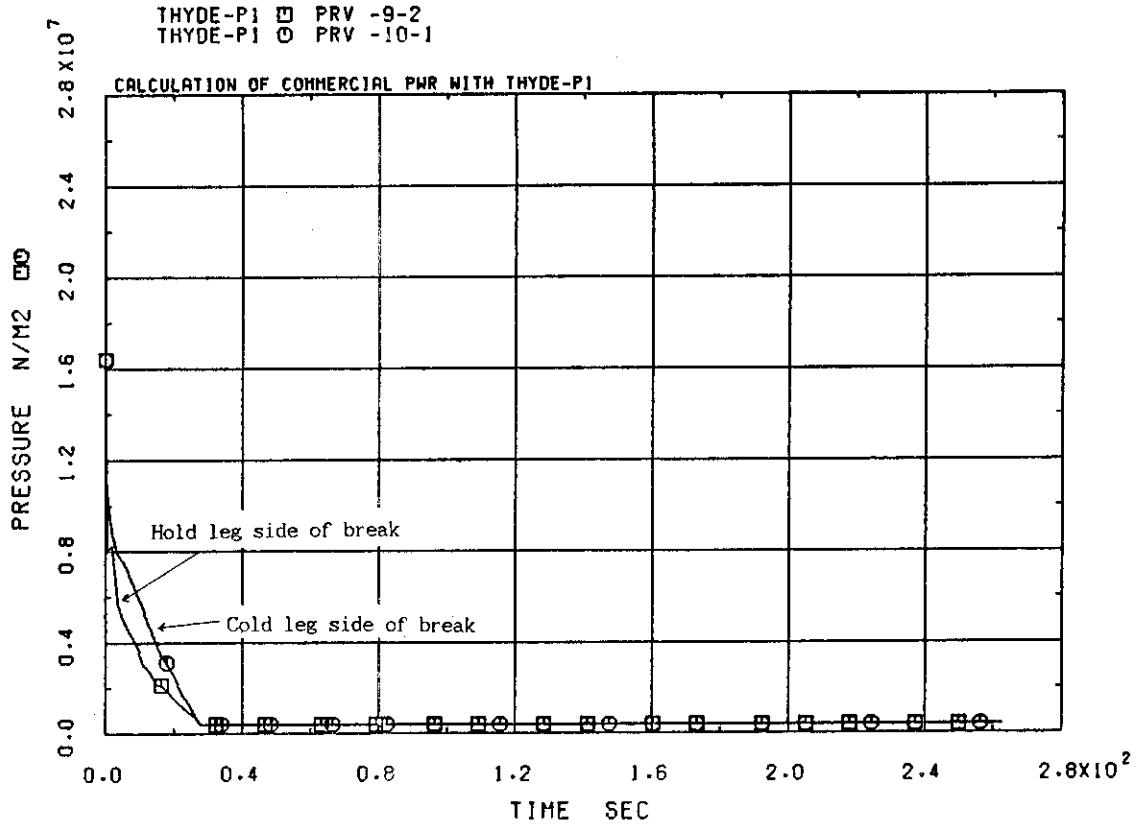


Fig.3-4-1 Pressures at break point

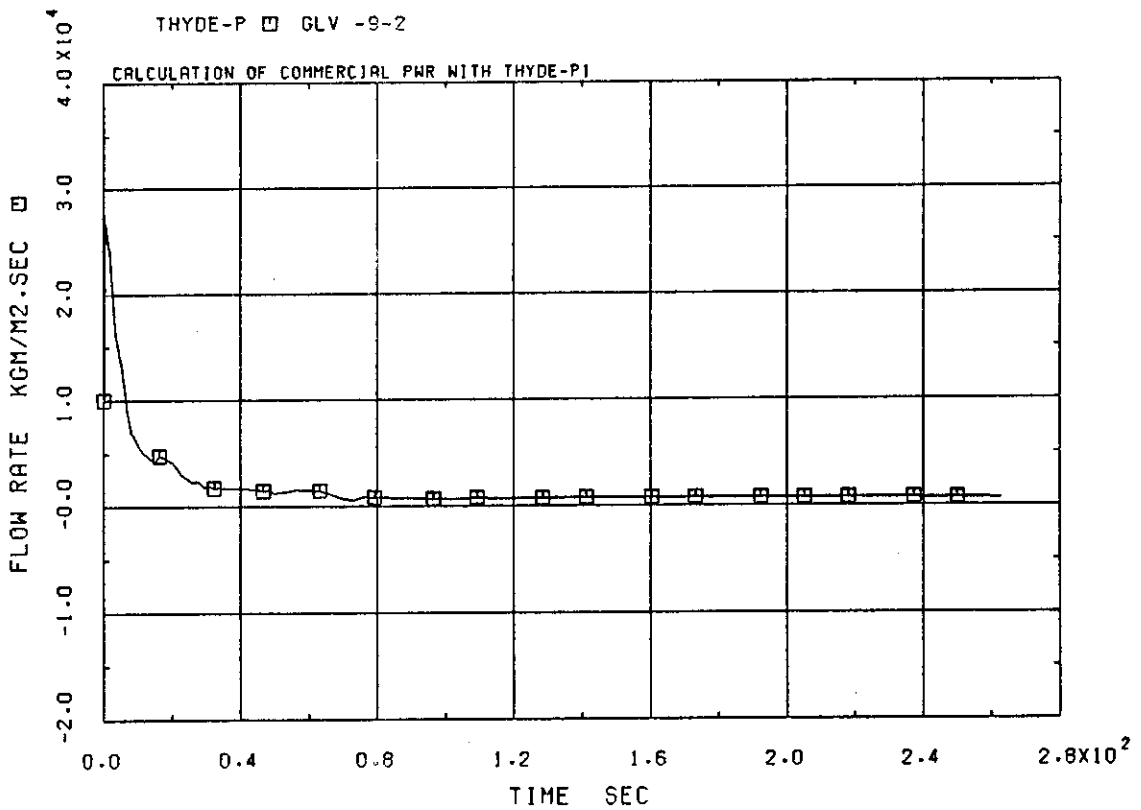


Fig.3-4-2 Hot leg side of break flow

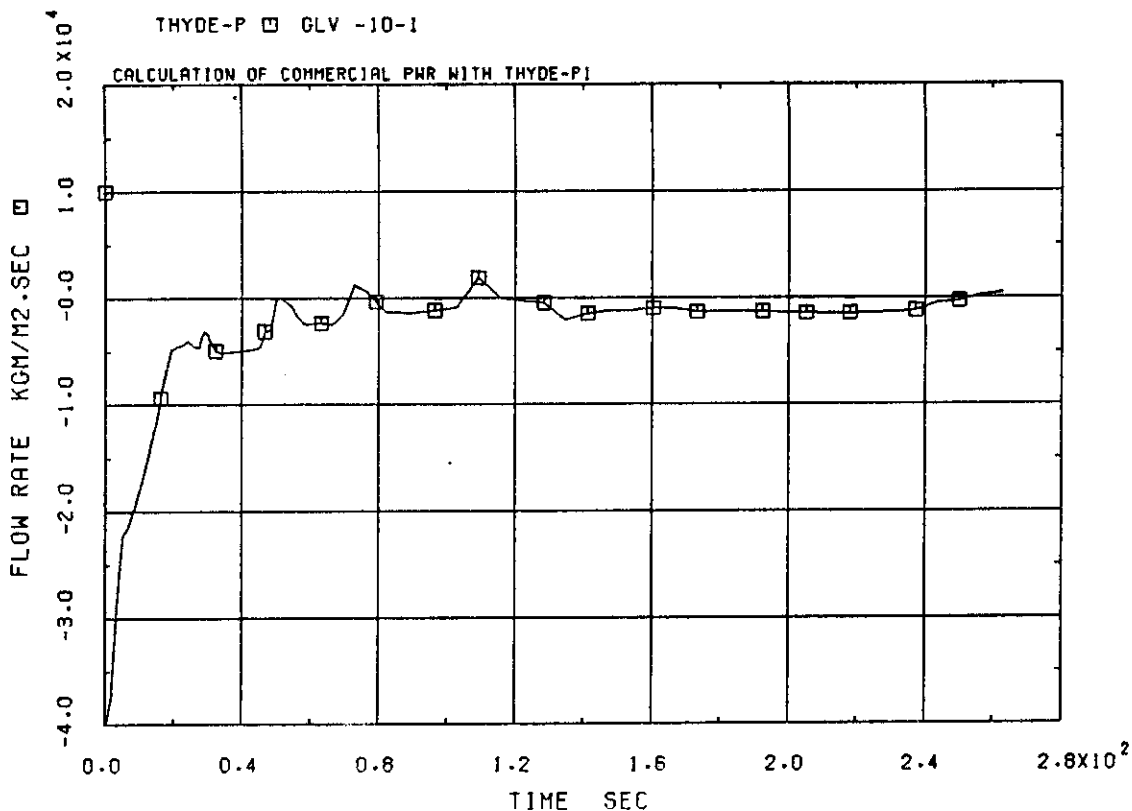


Fig.3-4-3 Cold leg side of break flow

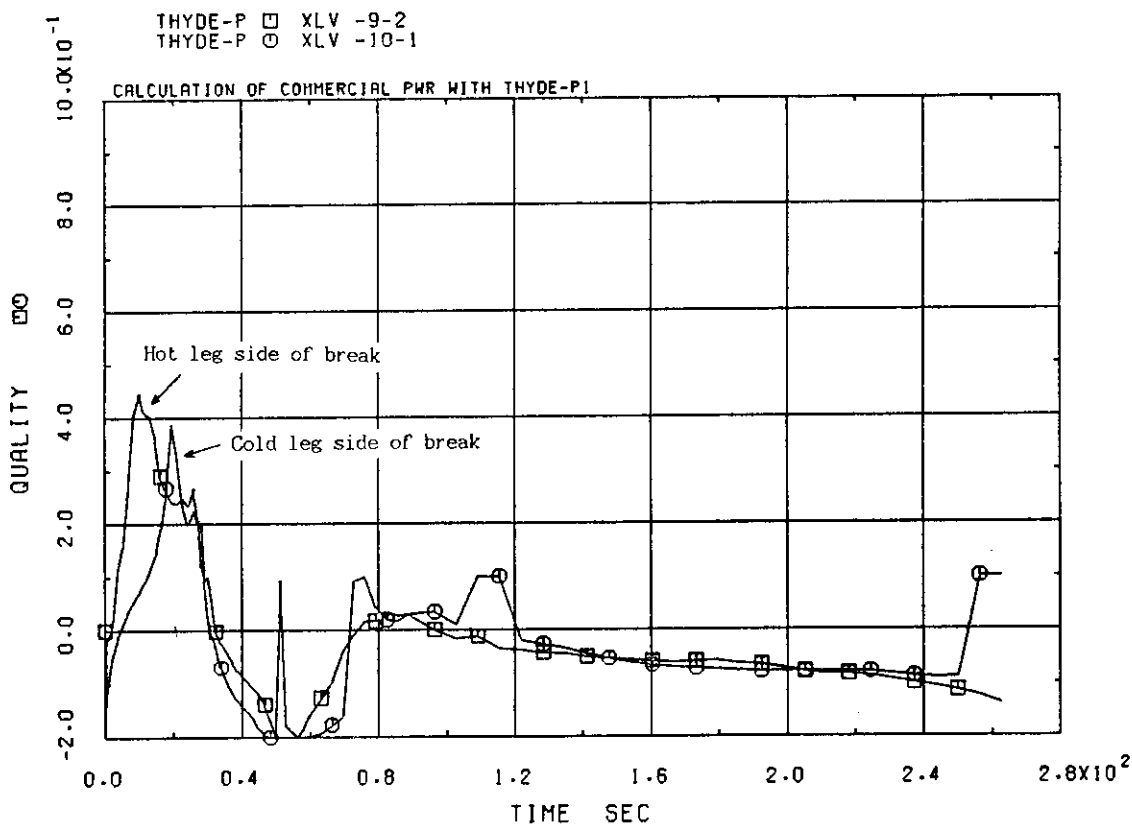


Fig.3-4-4 Equilibrium coolant qualities at break points

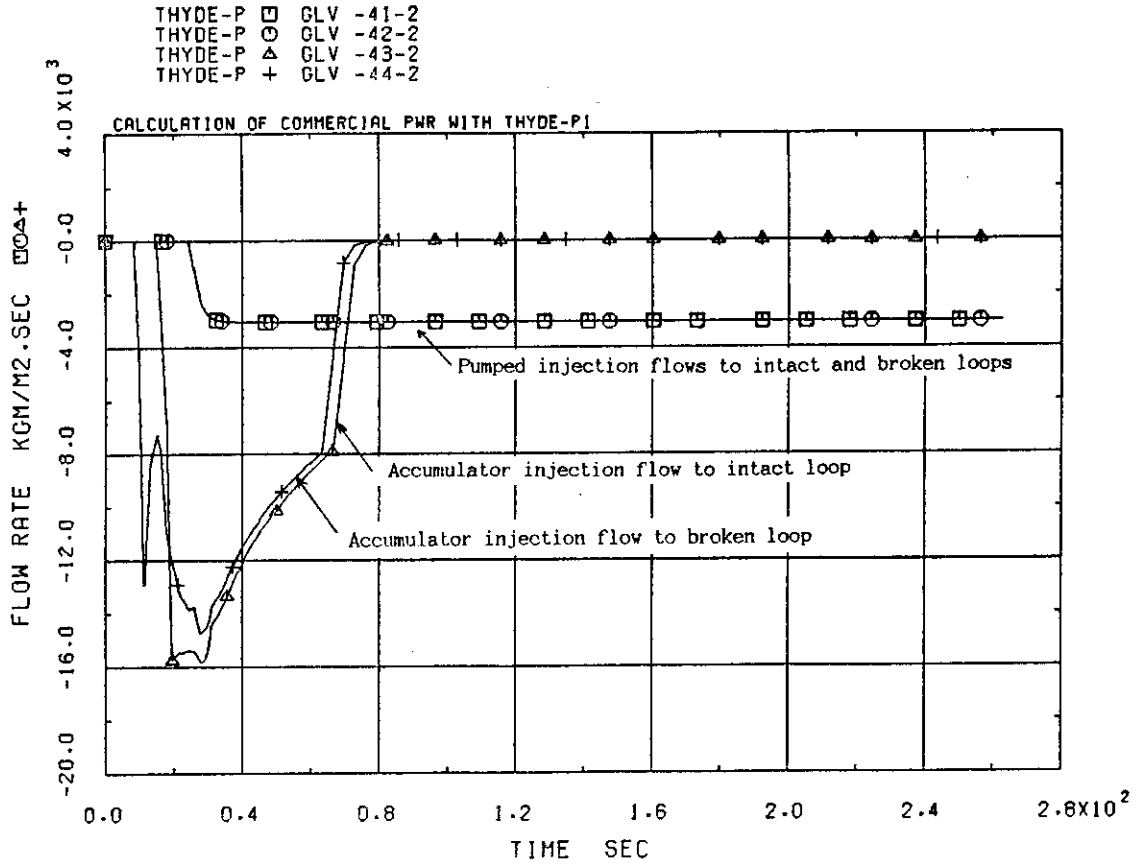


Fig.3-5-1 ECC injection mass fluxes

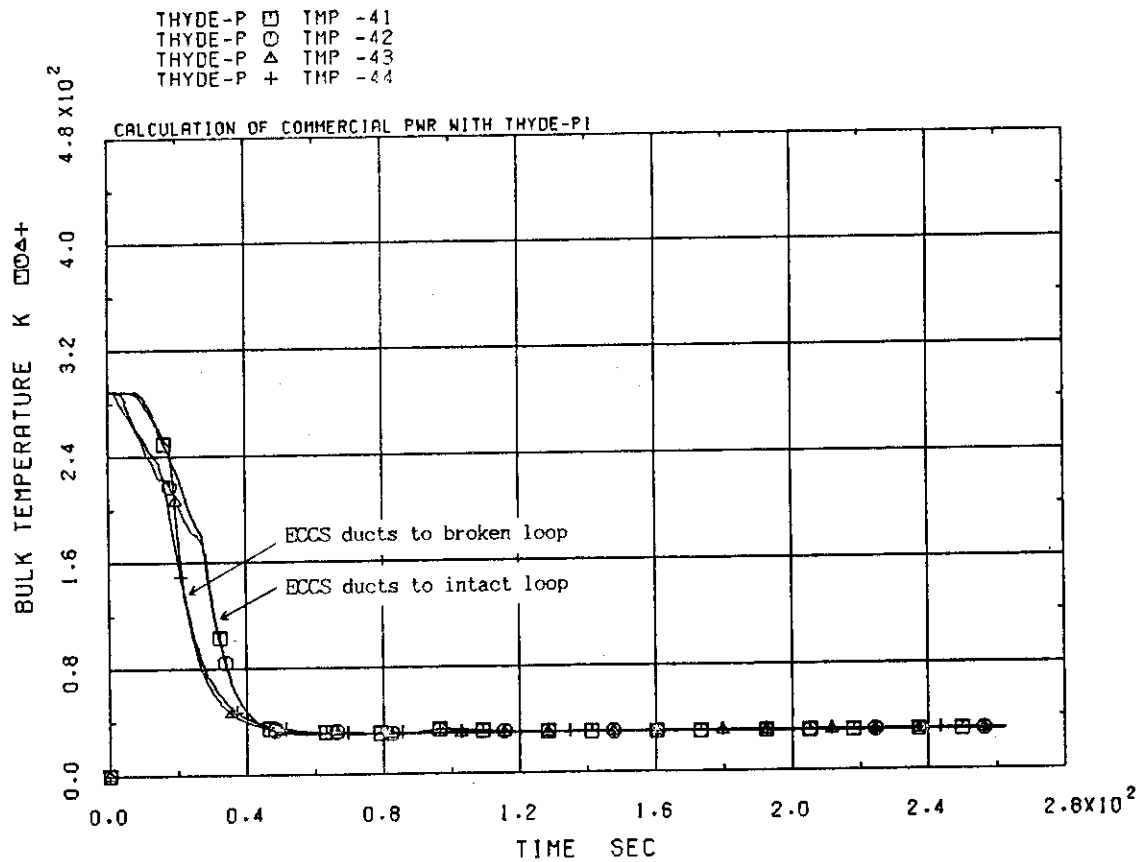


Fig.3-5-2 Coolant temperatures at ECC injection ducts

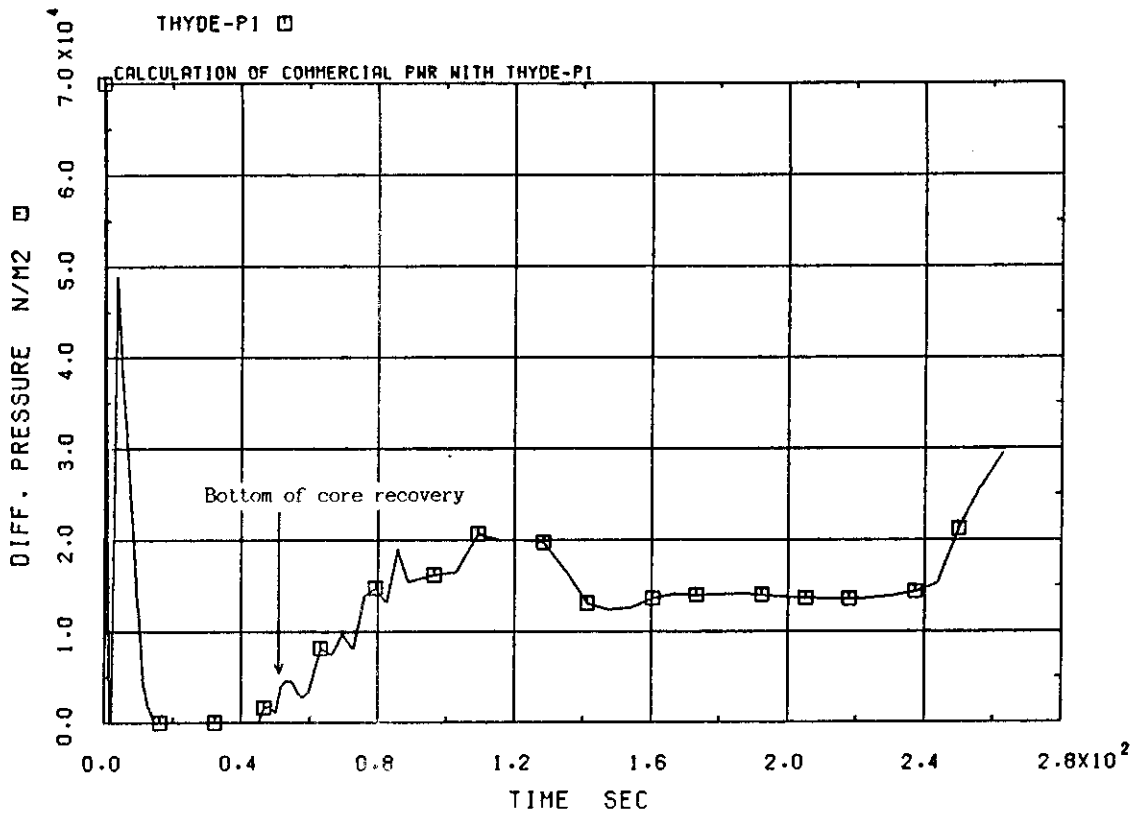


Fig.3-6-1 Differential pressure through core

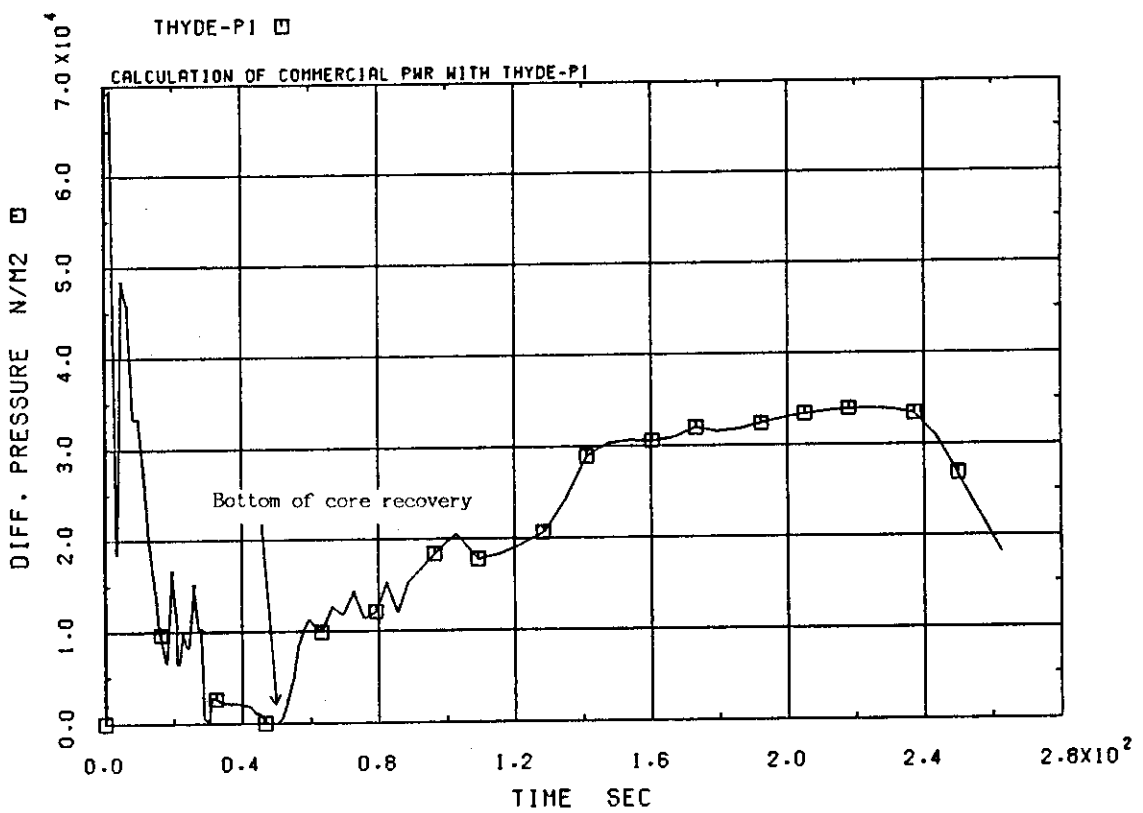


Fig.3-6-2 Differential pressure through intact loop

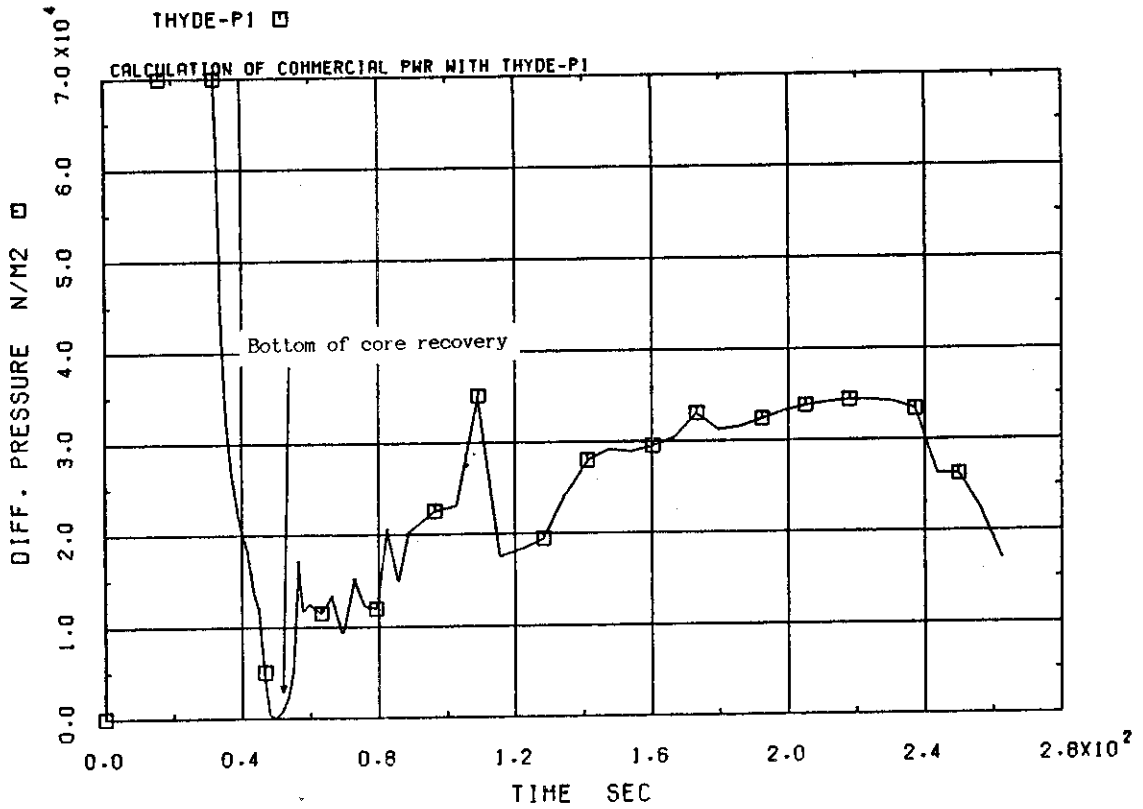


Fig.3-6-3 Differential pressure through broken loop

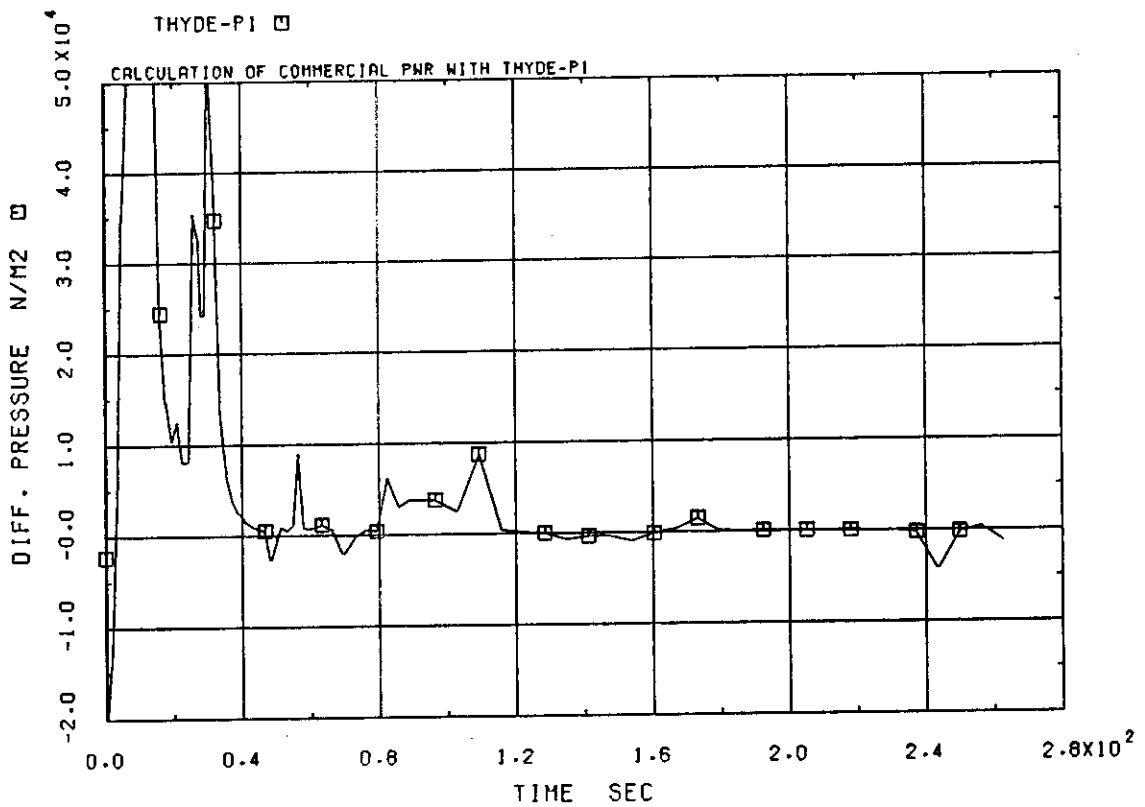


Fig.3-6-4 Differential pressure through broken loop cold leg

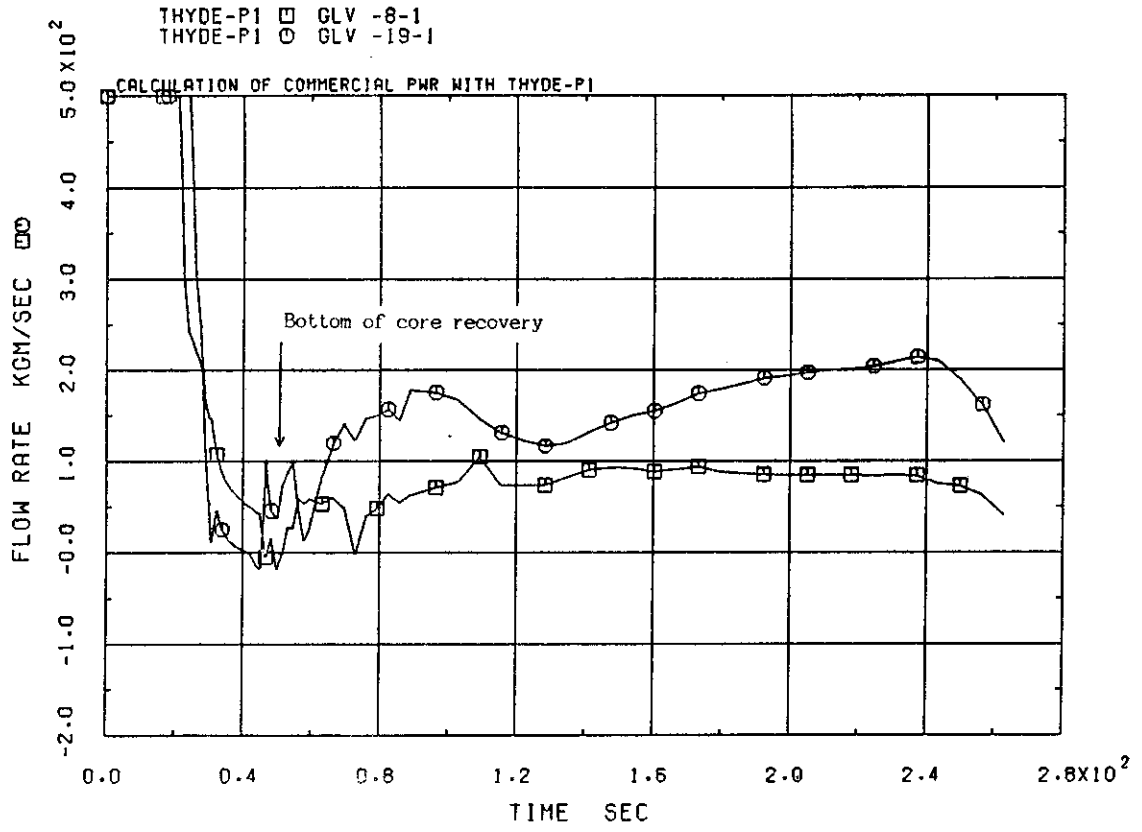


Fig.3-6-5 Mass flow rates through hot legs of intact and broken loops

4. Sensitivity Calculations

In this section, the results from three kinds of sensitivity calculations are presented: the pump operational conditions, CHF correlations and a minimum stable film boiling temperature (MSFBT) correlation. The first two sensitivity studies have been performed with the published version of THYDE-P1 without modification. In the last sensitivity study, however, a model has been developed and tentatively implemented into the code.

4.1. Pump On and Off

Two additional calculations with different pump conditions from Run 21 have been performed as an example of sensitivity calculations utilizing the base input data. Pump coastdown just after scram is assumed to occur in Run 21. In the additional calculations, however, pump running with a constant speed and pump rotor locking just after scram are assumed.

Fig. 4-1-1 shows the experimental cladding surface temperatures at the middle of the core in the pump on and off cases of the LOFT experiments, L2-3(11) and L2-5(12,13). Experiment L2-3 simulated a large break LOCA of a commercial PWR and the primary coolant pumps were running throughout the experiment. Experiment L2-5 was conducted under almost the same conditions as those in Experiment L2-3 except the pump condition, where an atypically fast pump coastdown was simulated. As shown in Fig 4-1-1, early rewetting was observed in Experiment L2-3 but was not observed in L2-5 due to the effects of the primary coolant pump condition. Although quantitative comparisons between the results from the LOFT experiments and those from the present sensitivity calculations have less meaning, qualitative ones may be useful to verify the system responses of THYDE-P1 to the pump conditions.

Figures. 4-1-2, 4-1-3, 4-1-4 and 4-1-5 show the normalized pump speeds, the pump heads, the normalized pump hydraulic torques, and the normalized pump volumetric flows, respectively. In the pump locking case, the pump speed is made to rapidly decrease to be zero just after scram with a time constant 0.05 sec. Fig. 4-1-6 shows the calculated cladding surface temperatures at the middle of the core. Early core-wide rewetting is

calculated to occur in the pump running case but is not in the other two pump conditions. These results are qualitatively consistent with the LOFT experimental results. Fig. 4-1-7 shows the core inlet flows. The core inlet flow until 15 sec is highest in the pump running case and the lowest in the pump locking case. It is clearly shown in this figure that the positive core flow recovery in the pump running case brings about the early rewetting.

Figs. 4-1-8 and 4-1-9 shows the hot leg side and cold leg side of the break flows. The effects of the pump condition to the hot leg side of the break flow seem to be small but those to the cold leg side of the break flow are considerable. In the case of pump rotor locking, the cold leg side of the break flow is considerably smaller than that in the other two cases.

Fig. 4-1-10 shows the calculated pressure transients. The pressures in the pump running case and the coastdown case are similar to each other. Because of the early rewetting, the pressure is calculated to be higher in the pump running case or the coastdown case than in the pump locking case until 15 sec. These results are also consistent with the LOFT experimental results⁽¹³⁾. The reason why the the pressure after 15 sec is calculated to be higher in the pump locking case than in the other cases is due to the effects of the break flow.

4.2. CHF Correlations

In THYDE-P1, there are three and two options for the CHF calculation under a forced convection condition and a pool flow condition, respectively, as follows:

For the forced convection condition,

- (1) The Biasi correlation⁽²⁰⁾,
- (2) The GE correlation⁽²¹⁾ and
- (3) RELAP4 type correlation⁽¹⁹⁾ (interpolation of the CHF values calculated using the B&W2⁽²²⁾, Barnett⁽²³⁾ and modified Barnett⁽²⁴⁾ correlations), and

For the pool flow condition,

- (1) Interpolation by a mass flux G between the CHF values evaluated at $G = G_{\min}$ ($= 273 \text{ kg/m}^2/\text{sec}$) and $67.9 \text{ kcal/m}^2/\text{sec}$, and

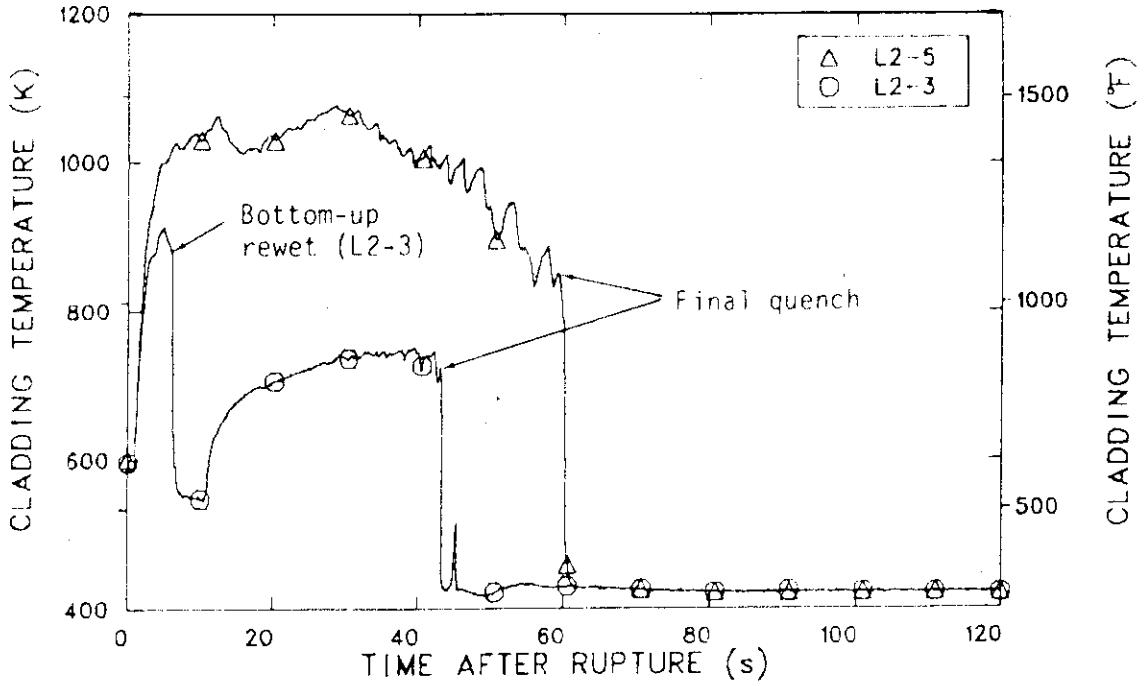


Fig.4-1-1 Experimental cladding surface temperatures in LOFT Large Break Experiments L2-3 and L2-5

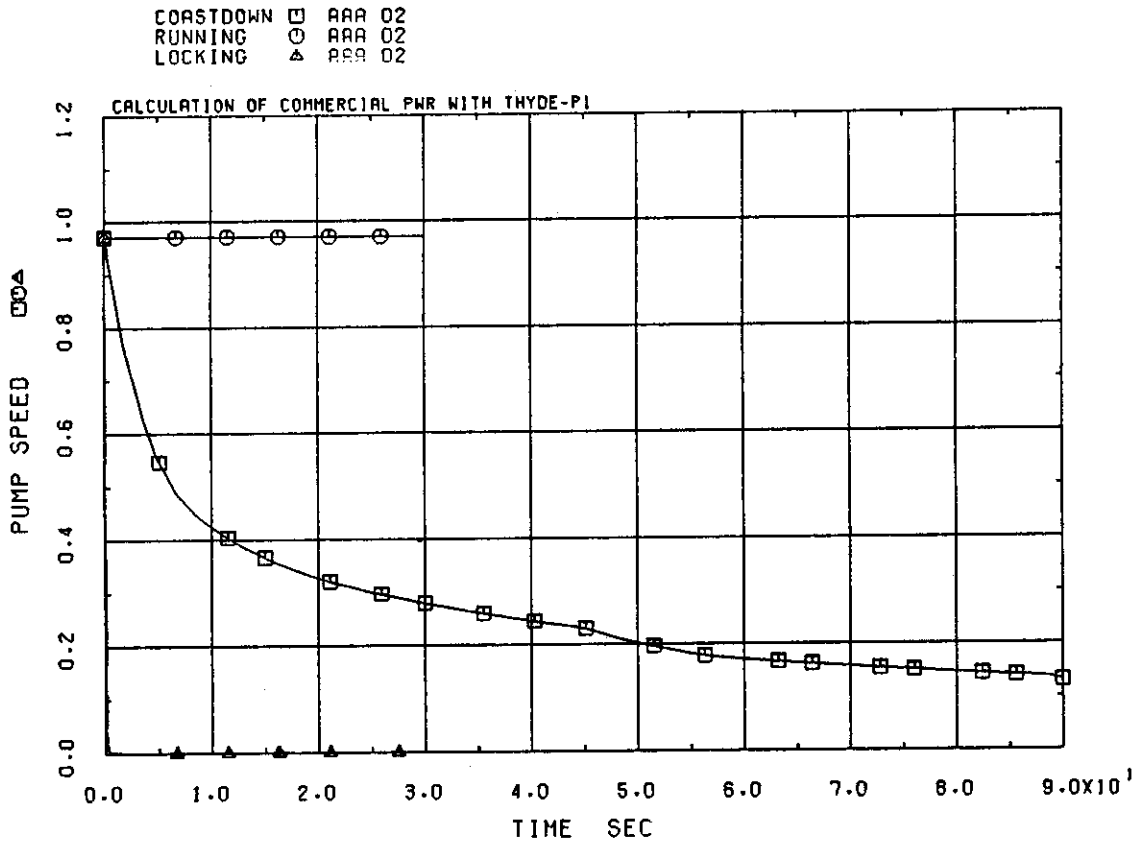


Fig.4-1-2 Normalized pump speeds

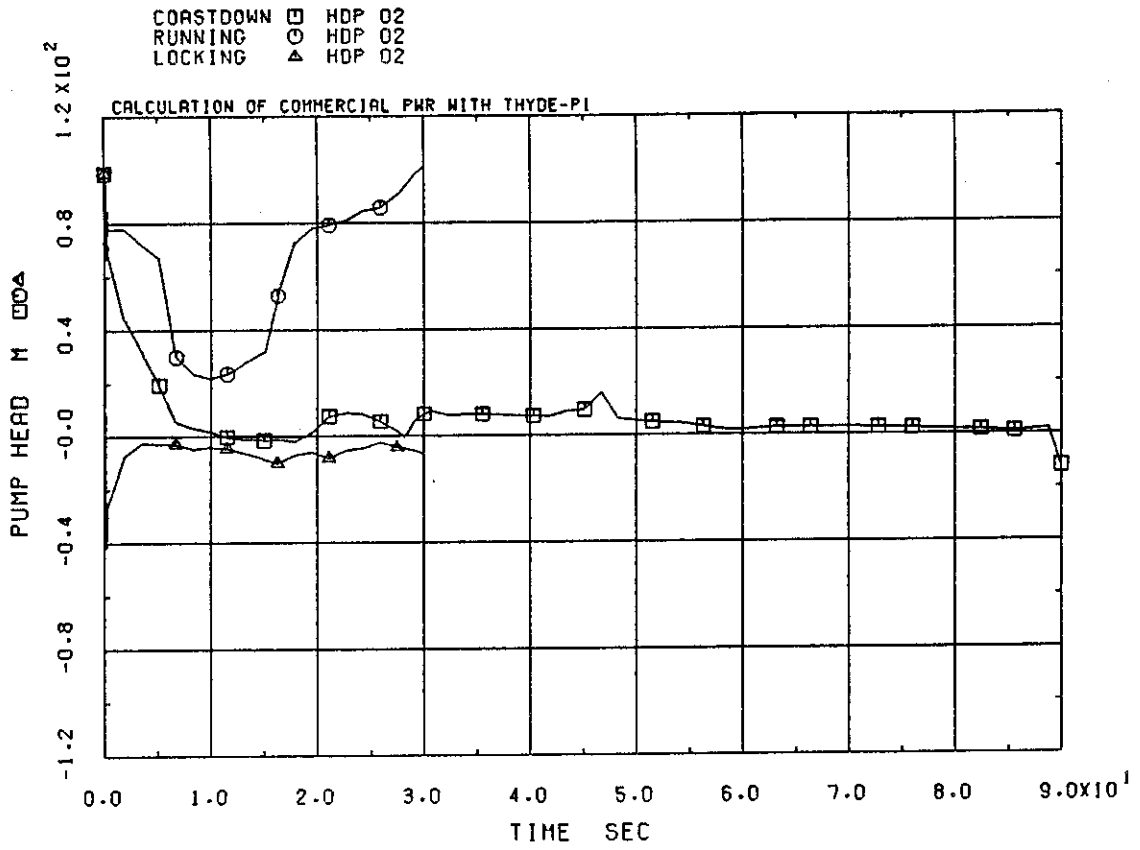


Fig.4-1-3 Pump heads

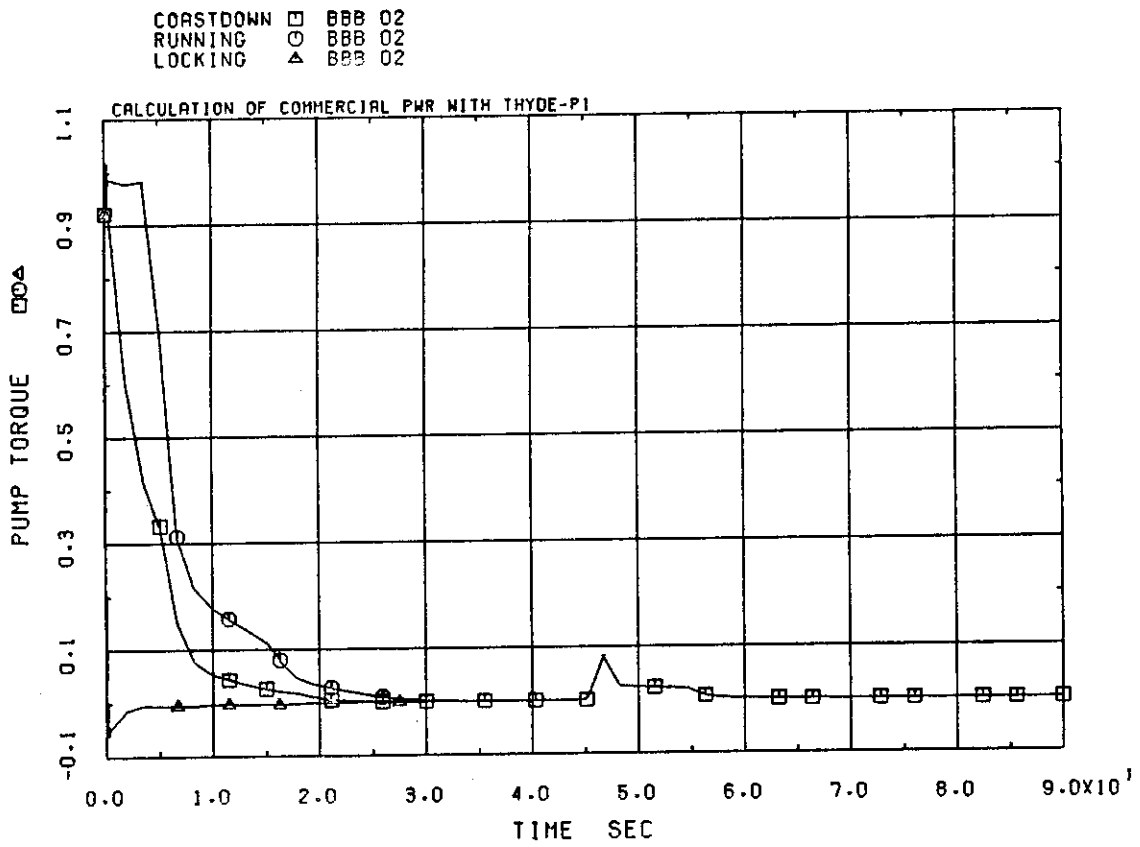


Fig.4-1-4 Normalized pump hydraulic torques

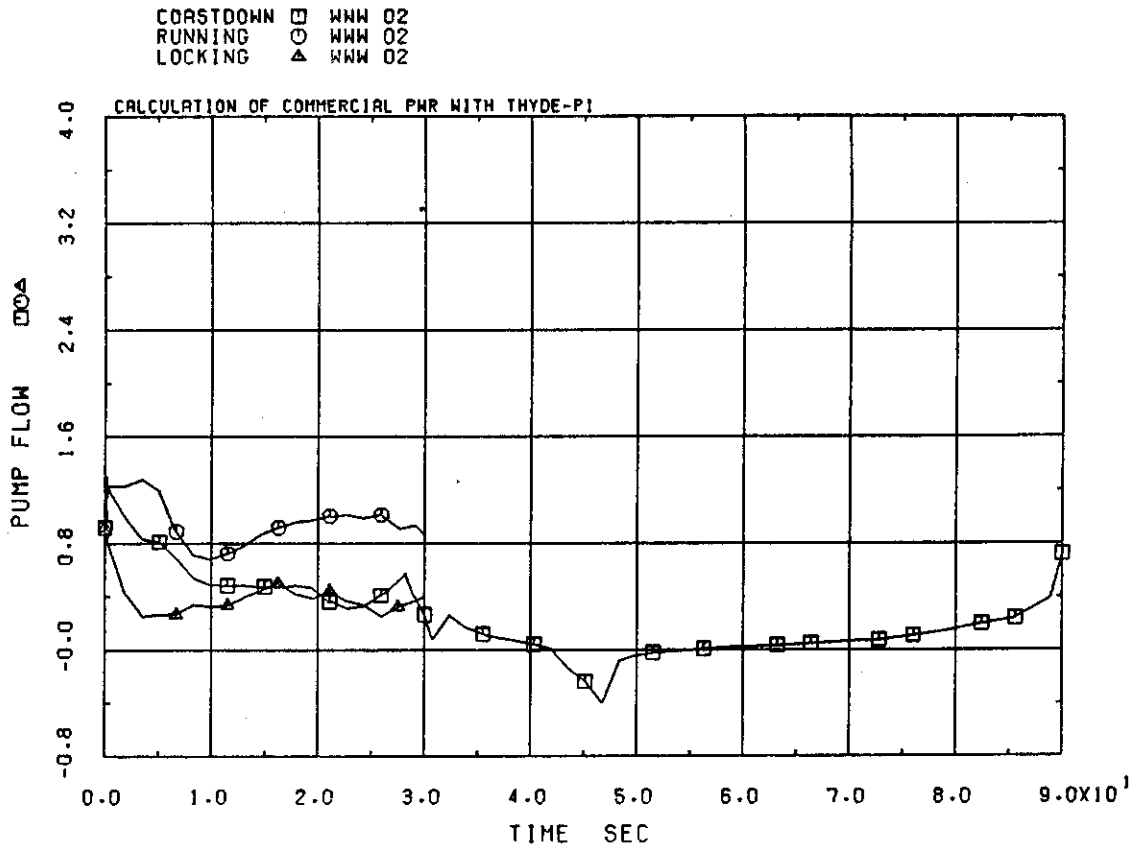


Fig.4-1-5 Normalized pump flows

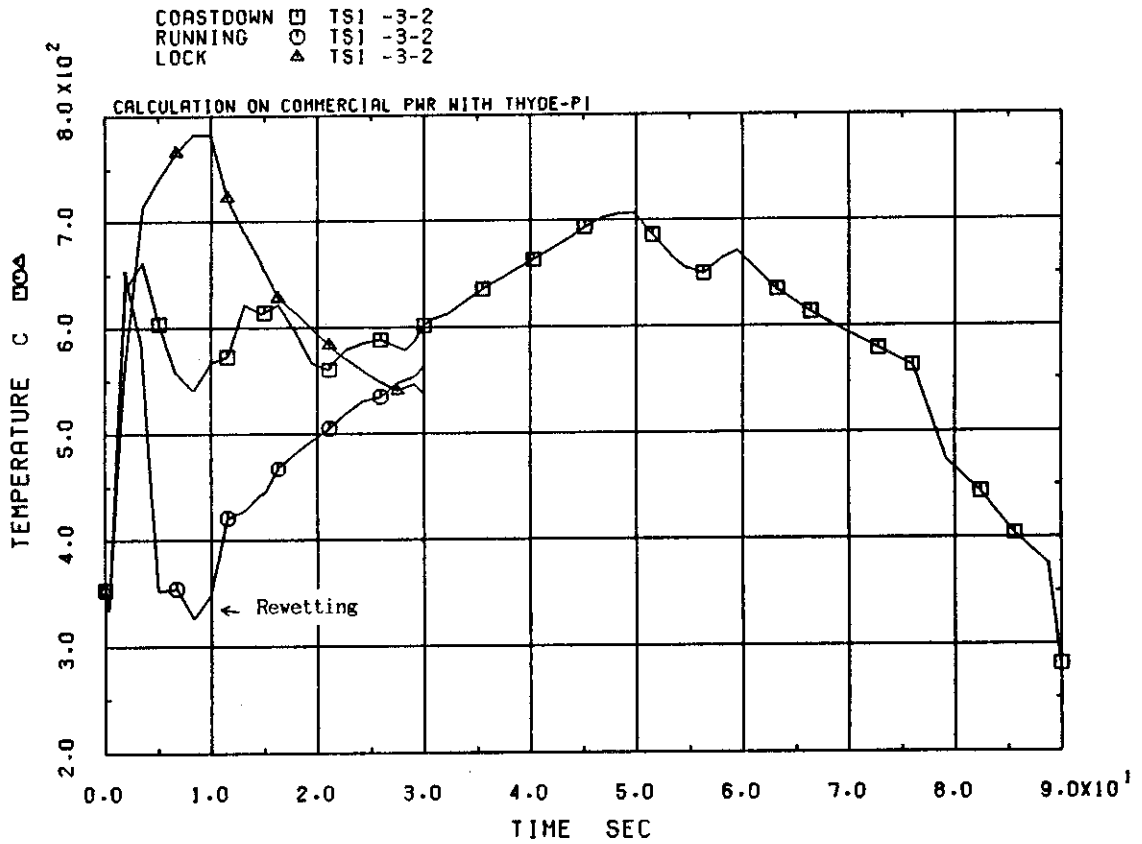


Fig.4-1-6 Cladding surface temperatures at middle of hot channel

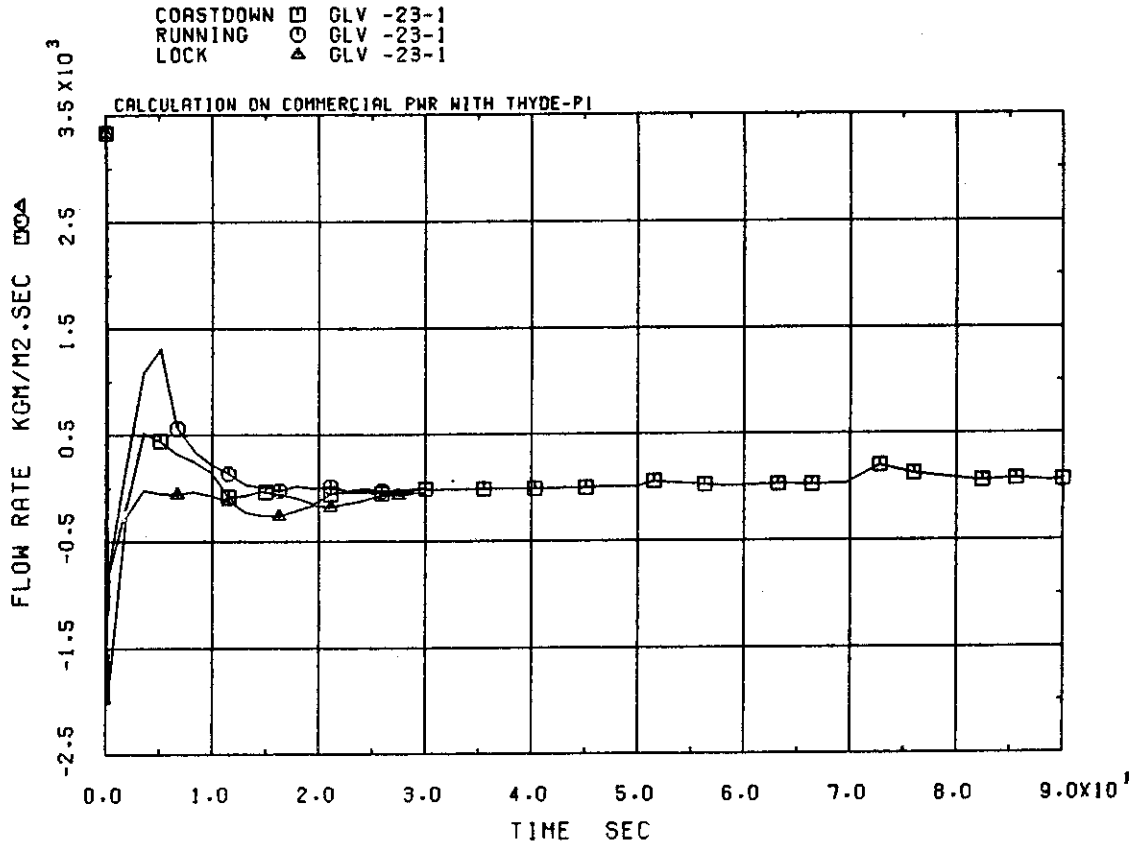


Fig.4-1-7 Core inlet mass fluxes

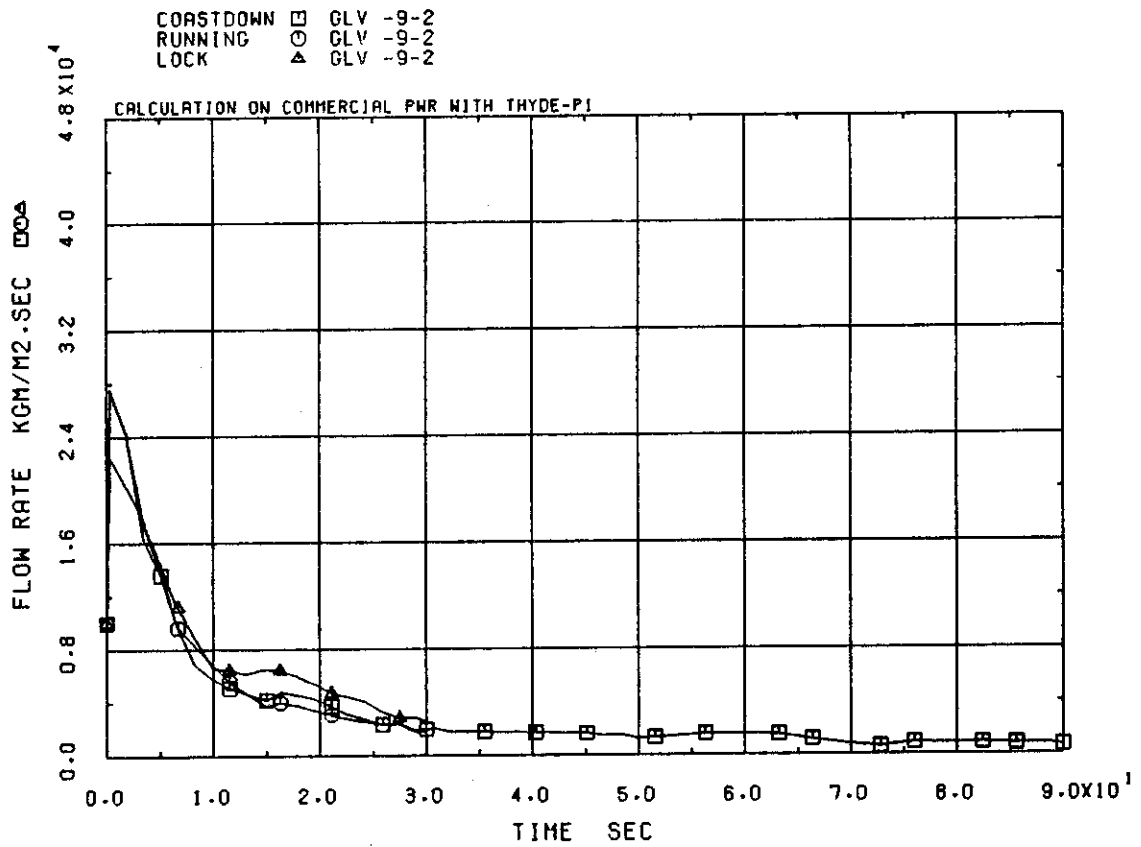


Fig.4-1-8 Hot leg side of break flows

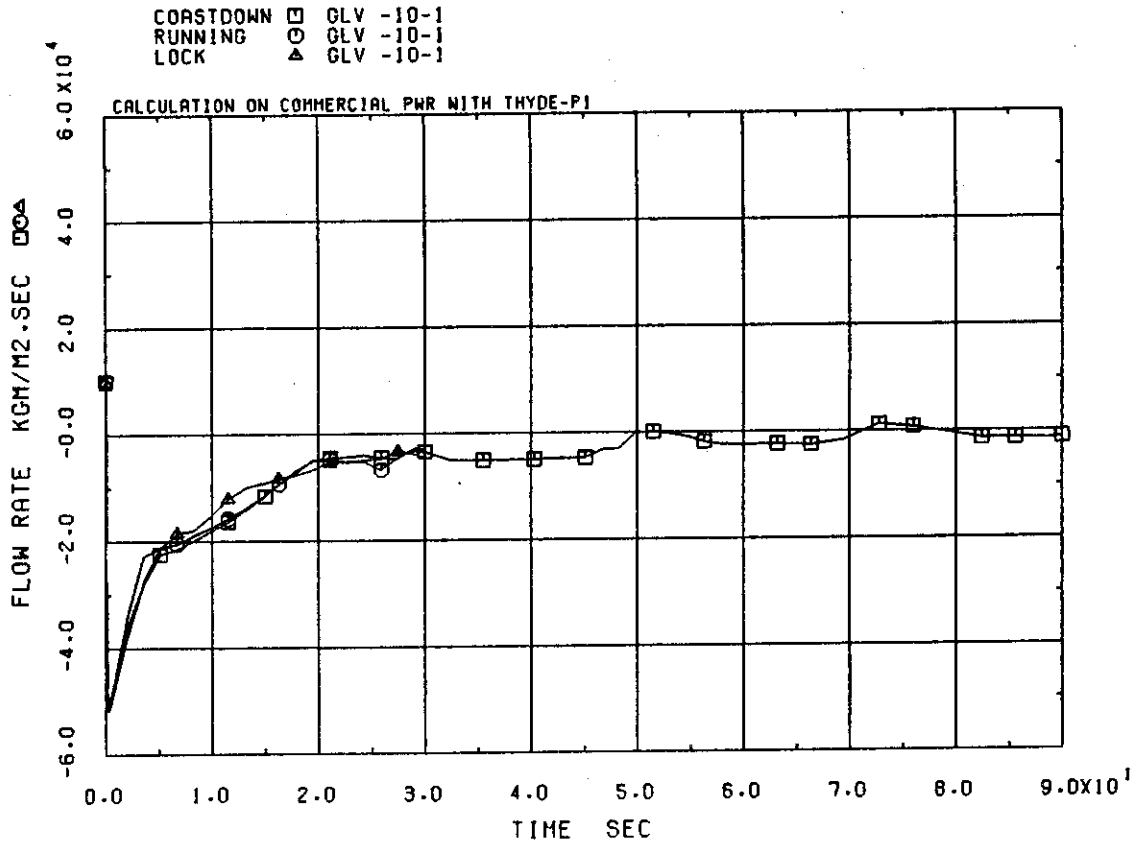


Fig.4-1-9 Cold leg side of break flows

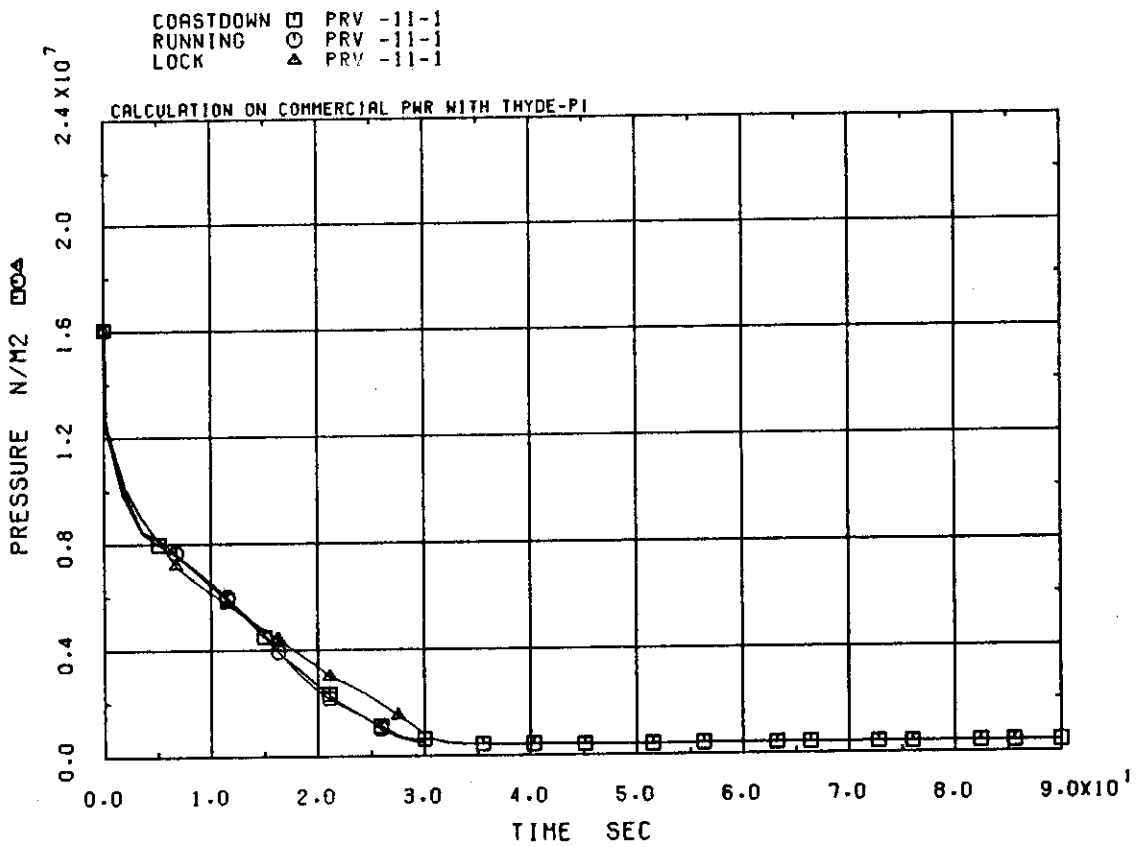


Fig.4-1-10 Intact loop hot leg pressures

(2) Modified Zuber⁽²⁵⁾ correlation.

In the base case calculation, Run 21, the options (3) and (1) are selected for the forced convection condition and the pool flow condition, respectively. In the additional calculation, however, the options (1) and (2) are selected.

The comparisons of the cladding surface temperatures, the fuel centre temperatures and the heat transfer coefficients between the base case calculation and the additional calculation are shown in Figs. 4-2-1, 4-2-2 and 4-2-3, respectively. The differences in the two calculations do not seem considerable.

4.3 Minimum Stable Film Boiling Temperature Model

In the published version of THYDE-P1, an empirical correlation for minimum stable film boiling temperature (MSFBT) is not implemented. Since in THYDE-P1, quenching is caused only when the quality of a core node under consideration decreases below 0.1, the quenching time at the higher elevation is considerably delayed. In order to improve this point, a model has been tentatively implemented and studied. In the present MSFBT model, the quenching is also assumed to occur when the cladding surface temperature decreases below MSFB temperature T_{MSFB} . Therefore this model is expected to improve the histories of the cladding surface temperatures at the higher elevation and of the quench front.

In the present model, in order to apply the MSFBT, two types of boiling curves are assumed to exist for DNB and quenching separately as shown later. It should be noted that the model may be regarded as temporary and opportune.

T_{MSFB} is defined to be the wall temperature which is required to maintain film boiling. In this analysis, T_{MSFB} was obtained based on the same formula as TRAC-P1A⁽¹⁴⁾. For low pressures, the classic film boiling instability analysis has been successfully used by Berenson⁽¹⁵⁾ to predict this temperature. Henry⁽¹⁶⁾ modified that analysis to account for surface effects:

$$T_{MINHB} = T_{MINB} + 0.42(T_{MINB} - T_l) \left[\frac{h_{lg} ((k\rho c_p)_l)^{1/2}}{(c_p)_w D T_{MINB} ((k\rho c_p)_w)^{1/2}} \right]^{0.6} \quad (4-3-1)$$

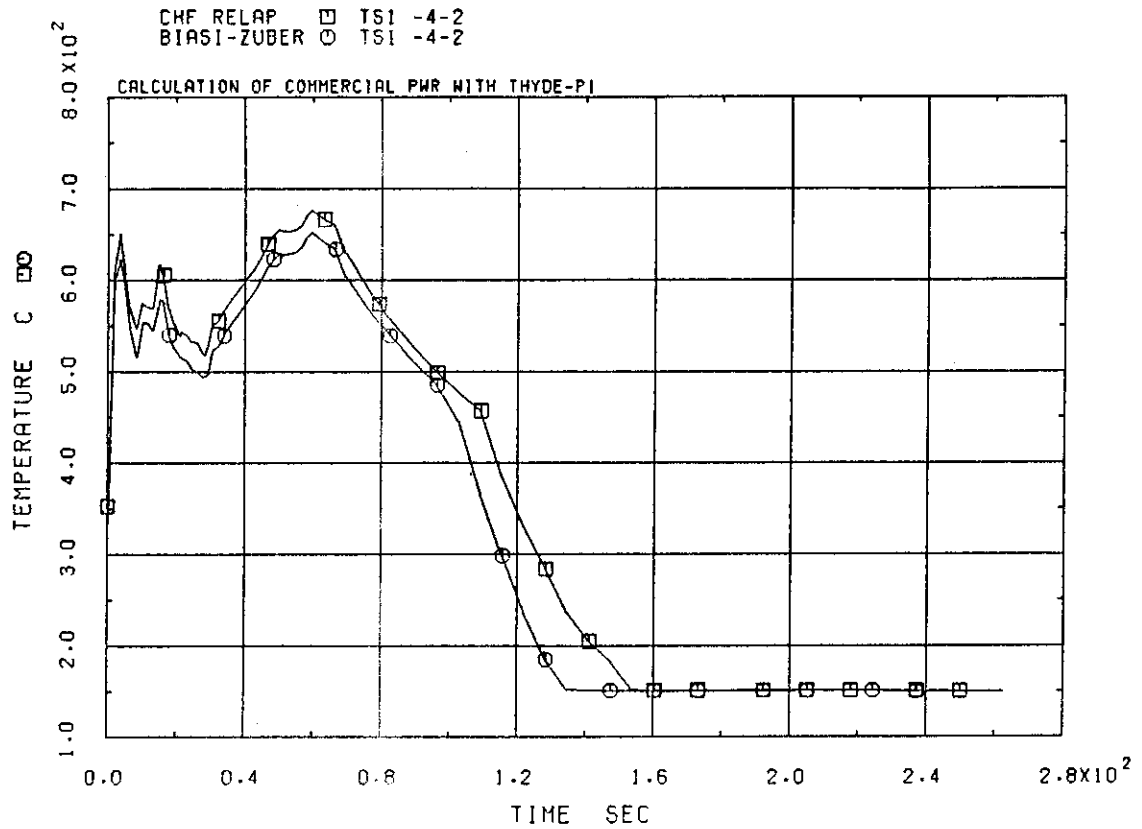


Fig.4-2-1 Cladding surface temperatures at middle of hot channel

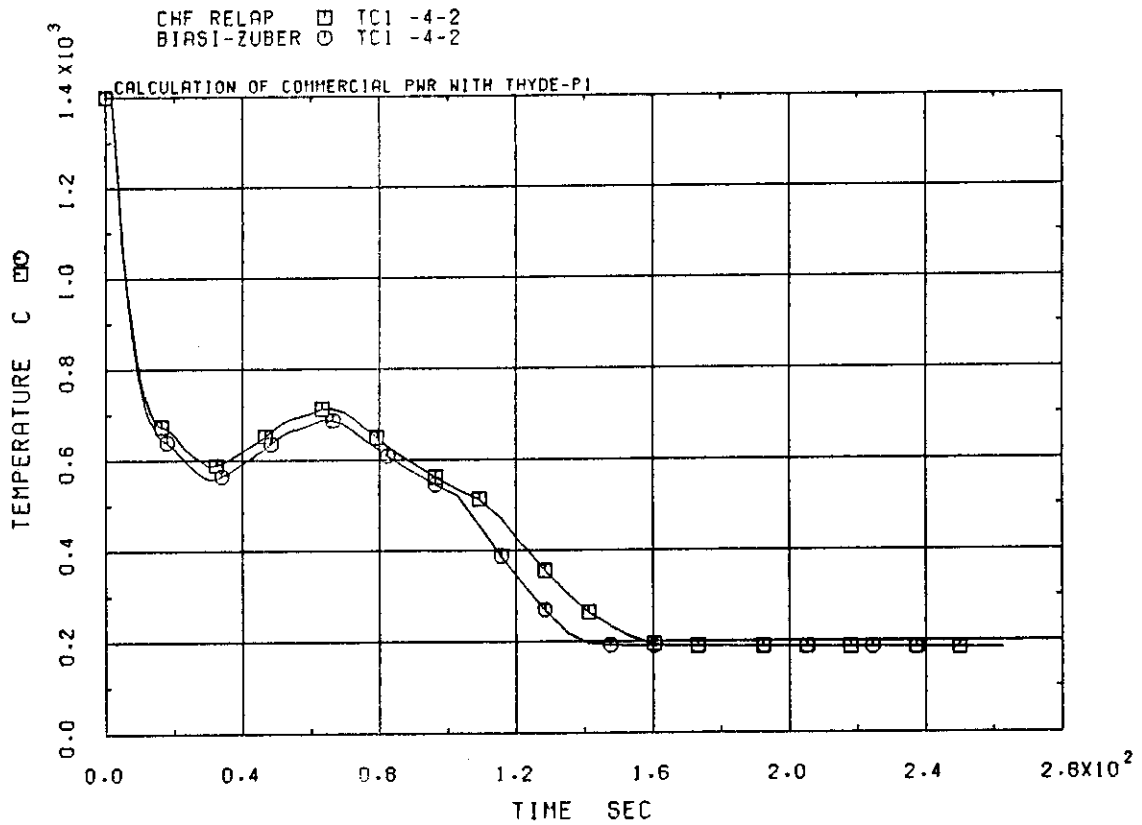


Fig.4-2-2 Fuel centre temperatures at middle of hot channel

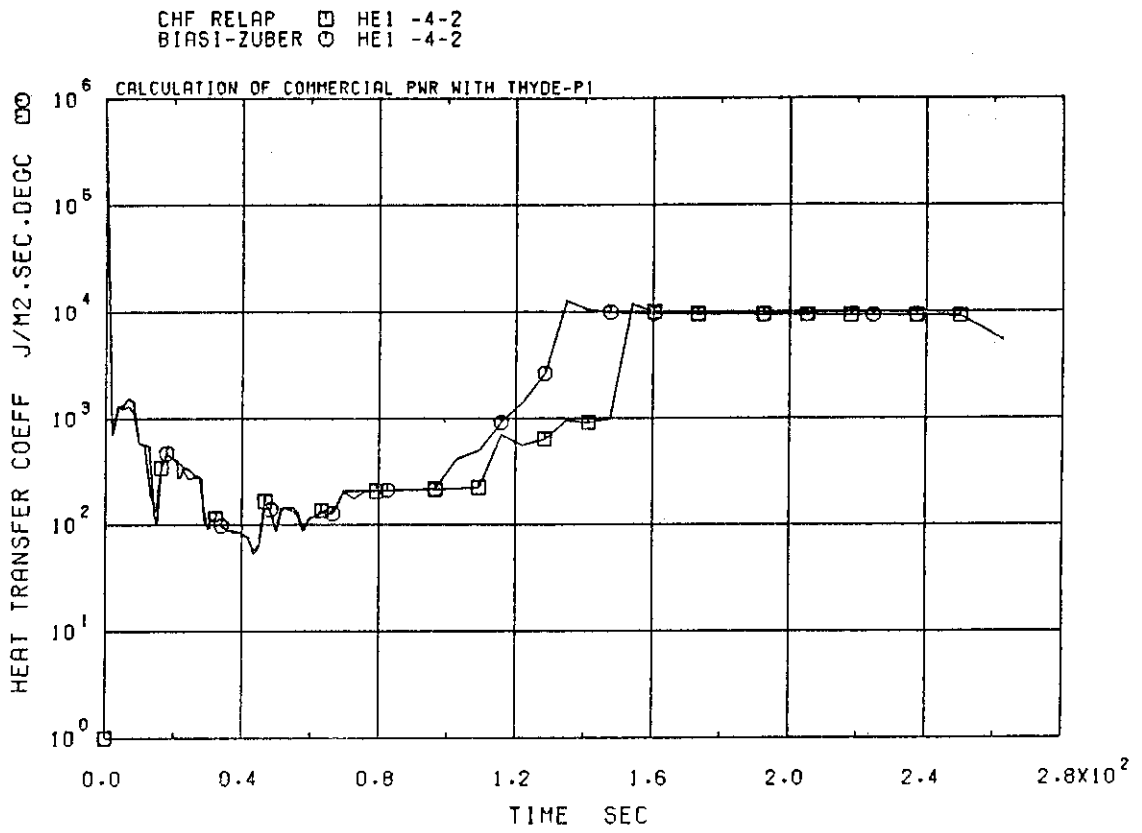


Fig.4-2-3 Heat transfer coefficients at middle of hot channel

and

$$T_{MINB} = T_s + 0.127 \frac{\rho_l h_{lg}}{k_g} \left[\frac{g(\rho_l - \rho_g)}{\rho_l + \rho_g} \right]^{2/3} \left[\frac{\sigma}{g(\rho_l - \rho_g)} \right]^{1/2} \left[\frac{\mu_g}{g(\rho_l - \rho_g)} \right]^{1/3} \quad (4-3-2)$$

where

- T_l ; liquid temperature
- T_s ; saturation temperature
- ρ ; density
- C_p ; specific heat at constant pressure
- k ; thermal conductivity
- h_{lg} ; latent heat of vaporization
- g ; acceleration due to gravity
- σ ; surface tension
- μ ; viscosity.

At higher pressures, the homogeneous nucleation mechanism⁽¹⁷⁾ seems to dominate. Bjornard and Griffith⁽¹⁸⁾ recommended Henry's modification to the Berenson formula also for the homogeneous nucleation phenomena:

$$T_{MINHN} = T_{HN} + (T_{HN} - T_l) \left[\frac{(k\rho c_p)_{liquid}}{(k\rho c_p)_{wall}} \right]^{1/2} \quad (4-3-3)$$

where T_{HN} is the homogeneous nucleation temperature. It is a weak function of pressure and varies from 307 C at atmospheric pressure to the critical temperature (374 C) at the critical pressure for water. The larger value is used in Eq.(4-3-3). The minimum of Eqs.(4-3-1) and (4-3-3) was chosen as T_{MSFB} in this analysis.

A boiling curve can be divided into three major regions according to the wall superheat. These are the pre-CHF (wet wall), transition boiling (alternating wet and dry walls) and film boiling (dry wall) regions. As shown in Fig. 4-3-1, it is assumed in the present analysis that there are two curves in the transition region. The curve (1) is applied to the transition from the nucleate boiling to the post-CHF (DNB). The curve (2) is used for the transition from the post-CHF to the nucleate

boiling (quenching)⁽²⁶⁾. When the curve of type (2) is also applied to DNB, DNB may not be calculated to occur. We now introduce an index I whose values correspond to the type of the above curves: when the index $I = 1$ (or 2), the curve (1) (or (2)) is adopted. The index I is determined as follows. At first I is set to be 0 for the steady state. When the wall temperature becomes larger than T_{MSFB} , or when the heat transfer mode of a core node under consideration becomes the superheated vapor mode, I is altered from 0 to 1. Then I is set to be 0 again if the heat transfer mode goes back to the nucleate boiling mode.

The results from the calculation with MSFBT model are compared in Figs. 4-3-2 to 4-3-4 with those from the base case calculation where the MSFBT model is not applied. As has been expected, the effects of the MSFBT model are remarkable for the histories of the cladding surface temperatures at the higher nodes (see Fig. 4-3-4). When this model is taken into account, the quenching occurs during the early stage of the reflooding at the upper core nodes. On the other hand, this model has rather small effects on the bottom flooding (see Figs. 4-3-2 and 4-3-3).

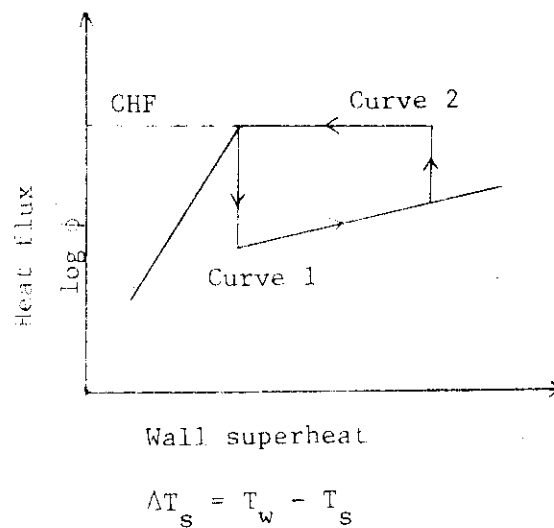


Fig. 4-3-1 Boiling curve in present MSFBT model

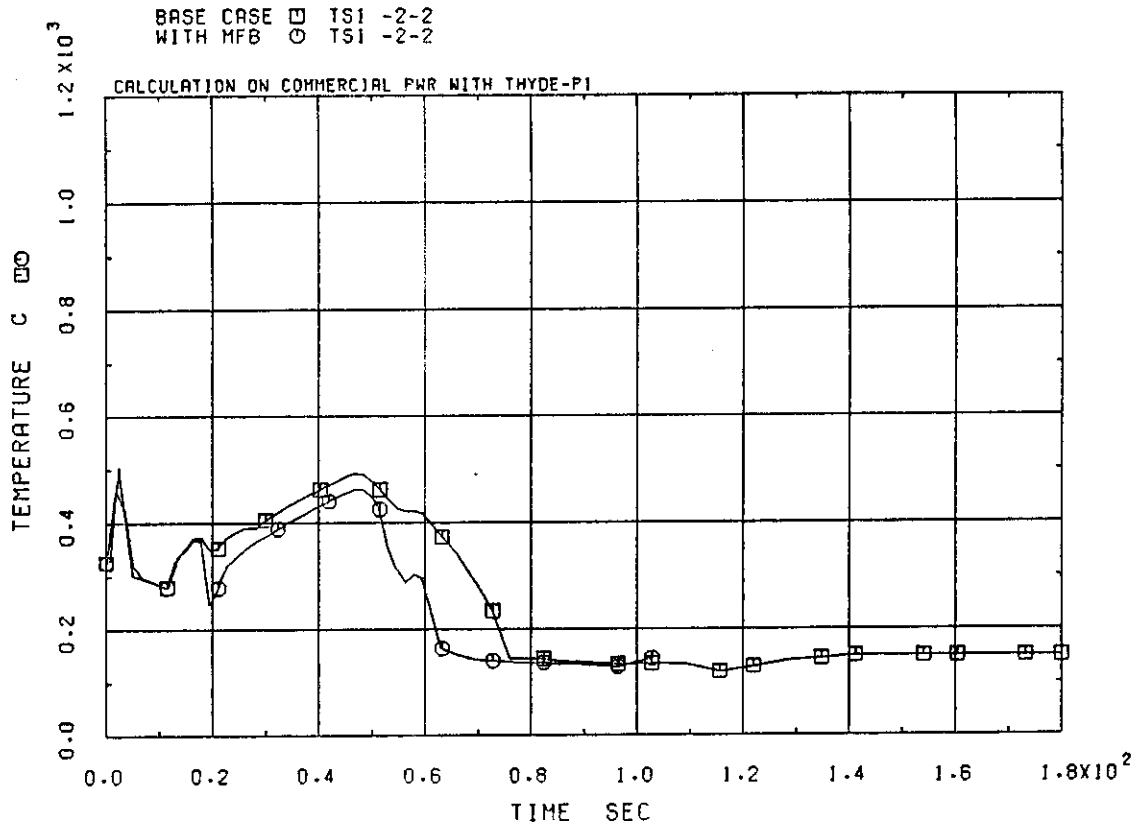


Fig.4-3-2 Cladding surface temperatures at bottom of hot channel

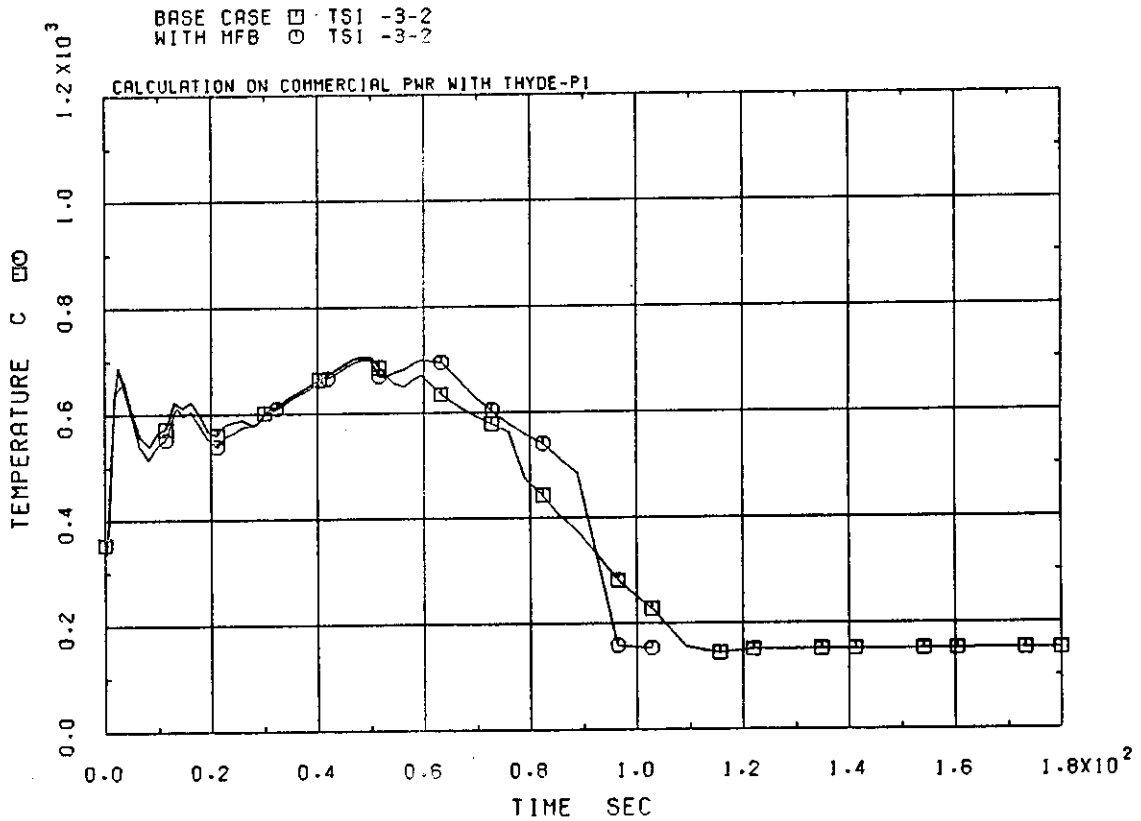


Fig.4-3-3 Cladding surface temperatures at middle of hot channel

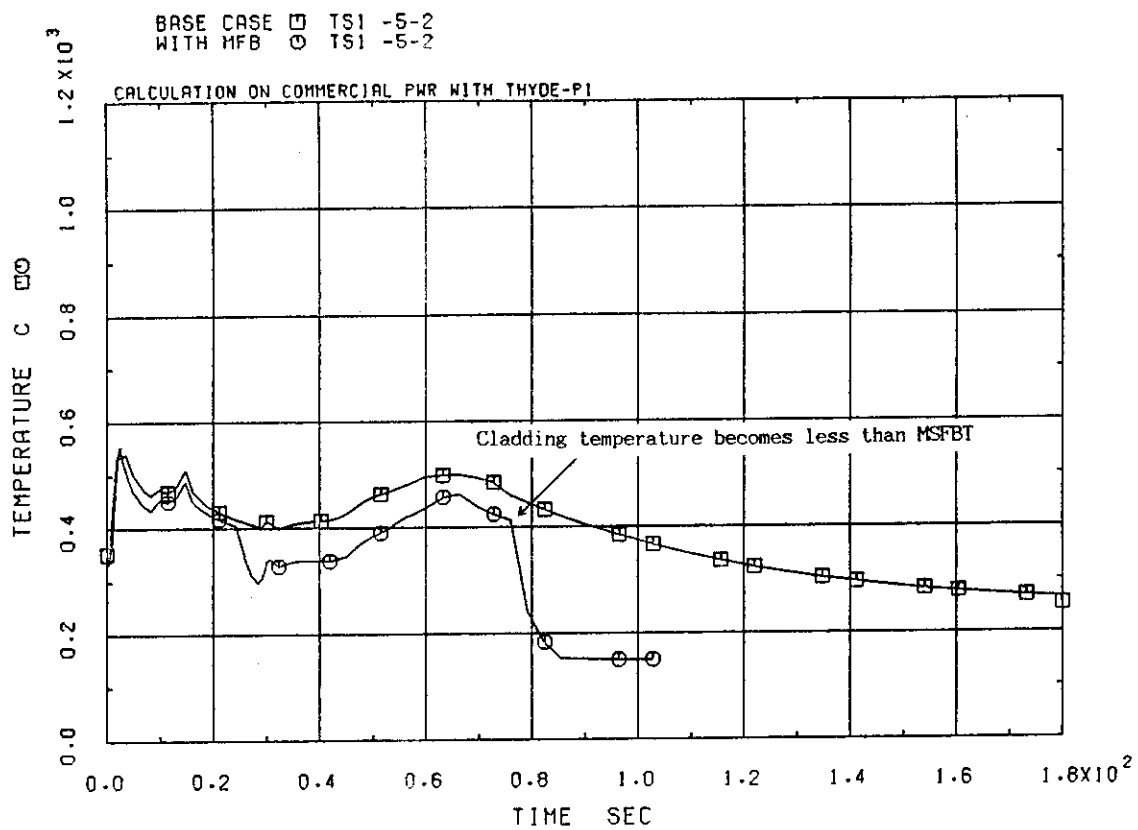


Fig.4-3-4 Cladding surface temperatures at top of hot channel

5. Conclusion

In this report, the base input for a postulated large break LOCA of a commercial PWR to be used with the published version of THYDE-P1 (SV02L03), and its calculated results have been presented. The present work has been done in order to provide users sample input data sets which can be used for a through calculation without any code modification. In the present calculation using the base input, the cladding surface temperature reached a peak of about 700°C at 50 sec after rupture, during the early portion of the reflooding. The core was reflooded at about 230 sec after rupture.

This base input has also been used as a bench mark for the sensitivity calculations (pump on and off, and selection of the CHF correlations) and a model development (a minimum stable film boiling temperature (MSFBT) model). In the sensitivity calculations for the pump operational conditions, the results were shown to be qualitatively consistent with those observed in the LOFT large break experiments. As a result from applying the present MSFBT model, quenching characteristics at high elevation were shown to be markedly improved. Such a usage of the base input has been found to be very useful and expected to be widely done.

Acknowledgement

The authors would like to express their sincere thanks to the members of Nuclear Safety Code Development Laboratory, especially to Mr. M. Akimoto, for his valuable discussions to carry out the present work.

In the present work, the SPLPLOT-1 program, which has been developed by Mr. K. Muramatsu in the laboratory, was used to plot the calculated results. The authors are also grateful to him for his appropriate suggestions.

5. Conclusion

In this report, the base input for a postulated large break LOCA of a commercial PWR to be used with the published version of THYDE-P1 (SV02L03), and its calculated results have been presented. The present work has been done in order to provide users sample input data sets which can be used for a through calculation without any code modification. In the present calculation using the base input, the cladding surface temperature reached a peak of about 700°C at 50 sec after rupture, during the early portion of the reflooding. The core was reflooded at about 230 sec after rupture.

This base input has also been used as a bench mark for the sensitivity calculations (pump on and off, and selection of the CHF correlations) and a model development (a minimum stable film boiling temperature (MSFBT) model). In the sensitivity calculations for the pump operational conditions, the results were shown to be qualitatively consistent with those observed in the LOFT large break experiments. As a result from applying the present MSFBT model, quenching characteristics at high elevation were shown to be markedly improved. Such a usage of the base input has been found to be very useful and expected to be widely done.

Acknowledgement

The authors would like to express their sincere thanks to the members of Nuclear Safety Code Development Laboratory, especially to Mr. M. Akimoto, for his valuable discussions to carry out the present work.

In the present work, the SPLPLOT-1 program, which has been developed by Mr. K. Muramatsu in the laboratory, was used to plot the calculated results. The authors are also grateful to him for his appropriate suggestions.

References

- (1) Asahi, Y., "Description of THYDE-P Code (Preliminary Report of Methods and Models)", JAERI-M 7751, 1978.
- (2) Asahi, Y., "User's Manual for THYDE-P1", JAERI-M 82-38, 1982.
- (3) Asahi, Y. and Hirano, M., "Verification Study of LOCA Analysis Code THYDE-P (Sample Calculation Run 10)", JAERI-M 8560, 1979.
- (4) Shimizu, T. and Asahi, Y., "A Through Calculation of 1,100 MWe PWR Large Break LOCA by THYDE-P code 1 (Sample Calculation Run 20)", JAERI-M 9319, 1981.
- (5) Hirano, M. and Asahi, Y., "Through Analysis of LOFT L2-2 by THYDE-P Code (1) (Sample Calculation Run 30)", JAERI-M 9535, 1981.
- (6) Hirano, M., "Through Analysis of LOFT L2-3 by THYDE-P Code (Sample Calculation Run 40)", JAERI-M 9765, 1981.
- (7) Hirano, M. and et al., "Analysis of LOFT Small Break Experiment L3-1 with THYDE-P Code (CSNI International Standard Problem No. 9 and THYDE-P Sample Calculation Run 50)", JAERI-M 82-008, 1982.
- (8) Hirano, M., "Analysis of LOFT L3-6/L8-1 with THYDE-P (CSNI International Standard Problem No. 11 and THYDE-P Sample Calculation Run 60)", JAERI-M 82-028, 1982.
- (9) Kosugi, S. and Asahi, Y., "Analysis of PKL K9 by THYDE-P Code (CSNI ISP No. 10 and THYDE-P Sample Calculation Run 70)", JAERI-M 82-115, 1982.
- (10) Chalton, et al., "RELAP4/MOD5 User's Manual Volume 3 (Checkout Applications)", ANCR-NUREG-1335(Vol. 3), 1976.

- (11) Prassions, P. G., "Experimental Data Report for LOFT Power Ascension Test L2-3", NUREG/CR-0792 TREE-1326, July 1979.
- (12) Bayless, P. D., et al., "Experimental Data Report for Large Break Loss-of-Coolant Experiment L2-5", NUREG/CR-2826 EGG-2210, August 1982.
- (13) Adams, P. J., "Quick-Look Report of LOFT Nuclear Experiment L2-5", EGG-LOFT-5921, June 1982.
- (14) Thermal Reactor Safety Group, TRAC-P1 : An Advanced Best-Estimate Computer Program for PWR LOCA Analysis, Los Alamos Scientific Laboratory (undated).
- (15) Berenson, P. J., "Film-Boiling Heat Transfer from a horizontal surface", ASME paper 60-WA-147, 1960.
- (16) Henry, R. E., "A Correlation for a Minimum Film Boiling Temperature", AIChE Symposium Series 138, 81-90, 1974.
- (17) Fauske, H. K., "Some Aspects of Liquid-Liquid Heat Transfer and Explosive Boiling", Proceedings of Fast Reactor Safety Meeting, Vol. 2, pp. 992-1005, Beverly Hills, CA, 1974.
- (18) Bjornard, T. A. and Griffith, P., "PWR Blowdown Heat Transfer", in Thermal and Hydraulic Aspects of Nuclear Reactor Safety, Vol. 1, pp. 17-41, American Society of Mechanical Engineers, New York, 1977.
- (19) Moore, K. V., "RELAP4 A Computer Program for Transient Thermal-Hydraulic Analysis", ANCR-1127, December 1973.
- (20) Biasi, L. et al., "Studies on Burnout : Part 3", Energia Nucleare, pp 550-536, 1967.
- (21) Slifer, B. S. and Hench, J. E., "Loss-of-Coolant and Emergency Core Cooling Models for General Electric Boiling Water Reactors", NEDO-10329, General Electric Company, April 1971.

- (22) Gellerstedt, J. S. et al., "Correlation of Critical Heat Flux in a Bundle Cooled by Pressurized Water", pp 63-71 of Two-Phase Flow and Heat Transfer in Rod Bundles, Symposium presented at the Winter Annual Meeting of the American Society of Mechanical Engineers, Loss Angeles, California, November 1969.
- (23) Barnett, P. G., "A Correlation of Burnout Data for Uniformly Heated Annuli and Its Use for Predicting Burnout in Uniformly Heated Rod Bundles", AEEW-R 463, 1966.
- (24) Hughes, E. D., "A Correlation of Rod Bundle Critical Heat Flux for Water in the pressure Range 150 to 725 psia", IN-1421, July 1970.
- (25) Zuber, N. et al., "The Hydrodynamic Crisis in Pool Boiling of Saturated and Subcooled Liquids", International Developments in Heat Transfer, Part II, pp 230-236, 1961.
- (26) Murao, Y., "An Analytical Study of the Thermal-Hydrodynamic Behavior of the Reflood-Phase During a LOCA", KFK-2545, 1977.

Appendix A Input data list

```

LARGE BREAK OF 1,100 MWE PWR (2 CHANNELS) * DATA 1 * 82.07.09
/
/ **** DIMENSION DATA ****
BB01
0 0 9 4 16 49 40 9 2 2 2 2 3 6 5 3 0 2
/
/ **** MINOR EDIT DATA ****
BB02
PRE-08 PRA-12 GLA-23 GLA-29 GLE-35 GLE-36 GLA-37 GLA-38 PRA-26
/
/ **** TIME STEP CONTROL DATA ****
BB03
SB0301
0.2 0.2 100.
SB0302
20 3 50 0 1.0E-3 1.0E-6 0.3 0.1
SB0303
200 3 50 0 8.0E-3 1.0E-6 60.0 0.1
SB0304
200 3 50 0 16.0E-3 1.0E-6 90.0 0.1
SB0305
200 3 50 0 32.0E-3 1.0E-6 2000.0 0.1
/
/ **** TRIP CONTROL DATA ****
BB04
SB0480
1 0 1 0 1000.0 0.0
SB0481
5 46 1 0 0.4 0.0
SB0482
5 47 1 0 0.4 0.0
SB0483
2 8 1 0 0.01 0.0
SB0484
2 19 1 0 0.01 0.0
SB0485
3 0 1 0 0.01 0.0
SB0486
4 1 1 0 25.01 0.0
SB0487
-4 1 1 0 1000.0 0.
SB0488
4 2 1 0 25.01 0.0
SB0489
-4 2 1 0 1000.0 0.
SB0492
6 1 -3 1 240.0 0.005
SB0493
6 2 -3 1 250.0 0.0
SB0494

```

```

00000100
00000200
00000300
00000400
00000500
00000600
00000700
00000800
00000900
00001000
00001100
00001200
00001300
00001400
00001500
00001600
00001700
00001800
00001900
00002000
00002100
00002200
00002300
00002400
00002500
00002600
00002700
00002800
00002900
00003000
00003100
00003200
00003300
00003400
00003500
00003600
00003700
00003800
00003900
00004000
00004100
00004200
00004300
00004400
00004500
00004600
00004700
00004800
00004900
00005000

```

```

-----*-----1-----*-----2-----*-----3-----*-----4-----*-----5-----*-----6-----*-----7-R-----*-----8
  6 3 -3 1 360.0 0.0 00005100
SB0495 00005200
 -6 1 3 1 350.0 0.0 00005300
SB0496 00005400
 -6 2 3 1 305.0 0.0 00005500
SB0497 00005600
 -6 3 3 1 380.0 0.00 00005700
 / 00005800
 / **** FLOW AJUST DATA **** 00005900
BB05 00006000
 1 9000.0 360.0 00006100
 / 00006200
 / **** NODE DATA **** 00006300
BB06 00006400
SB0601 00006500
 1 1 26 1 0 1 158.4538 0.737 0. 5.24 0.0 00006600
 0.043 0.084 0.0 0.0 00006700
SB0602 00006800
 2 1 1 2 0 1 158.9708 1.92 0. 1.665 1.665 00006900
 3.73 1.97 0.0 0.0 00007000
SB0603 00007100
 3 7 2 3 1 3265 158.7624 0.0197 0. 5.0 5.0 00007200
 0.033 0.048 0.0 0.0 00007300
SB0604 00007400
 4 7 3 4 1 3265 158.1581 0.0197 0. 5.46 5.46 00007500
 0.0 0.0 0.0 0.0 00007600
SB0605 00007700
 5 7 4 5 1 3265 157.4898 0.0197 0. 10.46 -10.46 00007800
 0.0 0.0 0.033 0.048 00007900
SB0606 00008000
 6 1 5 6 0 1 157.7862 1.92 0. 1.665 -1.665 00008100
 0.0 0.0 3.73 1.97 00008200
SB0607 00008300
 7 1 6 7 0 1 157.4466 0.787 0. 7.34 -3.54 00008400
 0.042 0.077 -1. -1. 00008500
SB0608 00008600
 8 8 7 34 0 1 157.5243 0.737 0. 5.57635 3.54 00008700
 -1. -1. 0.2029 0.2027 00008800
SB0609 00008900
 9 1 34 8 0 1 162.0607 0.699 0. 2.825 0.0 00009000
 0.0 0.0 0.0 0.0 00009100
SB0610 00009200
10 1 8 29 0 1 162.0332 0.699 0. 3.13 0.0 00009300
 0.0 0.0 0.0 0.0 00009400
SB0611 00009500
11 1 26 27 0 3 158.4538 0.737 0. 2.0 0. 00009600
 0.043 0.083 0.0 0.0 00009700
SB0612 00009800
12 1 27 9 0 3 158.4334 0.737 0. 3.24 0. 00009900
 0.0 0.0 0.0 0.0 0010000
SB0613 0010100
13 1 9 10 0 3 158.9528 1.92 0. 1.665 1.665 0010100
 3.73 1.97 0.0 0.0 0010200
SB0614 0010300
14 7 10 11 1 9795 158.7445 0.0197 0. 5.0 5.0 0010400
 0.033 0.048 0.0 0.0 0010500
SB0615 0010600
15 7 11 12 1 9795 158.1387 0.0197 0. 5.46 5.46 0010700
 0.0 0.0 0.0 0.0 0010800
 0010900

```

	1	2	3	4	5	6	7-R	8
SB0616	16	7 12 13	1 9795	157.4691	0.0197	0. 10.46	-10.46	00011000
				0.0	0.0	0.033	0.048	00011100
								00011200
								00011300
SB0617	17	1 13 14	0 3	157.7645	1.92	0. 1.665	-1.665	00011400
				0.0	0.0	3.73	1.97	00011500
								00011600
SB0618	18	1 14 15	0 3	157.4249	0.787	0. 7.34	-3.54	00011700
				0.042	0.077	-1.	-1.	00011800
								00011900
SB0619	19	8 15 28	0 3	157.5027	0.737	0. 5.57635	3.54	00012000
				-1.	-1.	0.2029	0.2027	00012100
								00012200
SB0620	20	1 28 29	0 3	162.0373	0.699	0. 5.955	0.	00012300
				0.0	0.0	0.0	0.0	00012400
								00012500
SB0621	21	4 29 16	0 1	162.4638	1.869	0. 7.248	-7.248	00012600
				0.0	0.0	0.0	0.0	00012700
								00012800
SB0622	22	5 16 30	0 1	162.9140	2.487	0. 6.075	1.948	00012900
				0.0	0.0	0.0	0.0	00013000
								00013100
SB0623	23	2 30 17	0 39170	162.6047	1.0	0. 0.23	0.23	00013200
				0.74	0.74	0.0	0.0	00013300
								00013400
SB0624	24	2 17 18	1 39170	162.1173	1.0	0. 0.80	0.80	00013500
				0.0	0.0	0.0	0.0	00013600
								00013700
SB0625	25	2 18 31	1 39170	161.5410	1.0	0. 0.80	0.80	00013800
				0.0	0.0	0.0	0.0	00013900
								00014000
SB0626	26	2 31 19	1 39170	160.9517	1.0	0. 0.80	0.80	00014100
				0.0	0.0	0.0	0.0	00014200
								00014300
SB0627	27	2 19 20	1 39170	160.3296	1.0	0. 0.80	0.80	00014400
				0.0	0.0	0.0	0.0	00014500
								00014600
SB0628	28	2 20 33	0 39170	159.7062	1.0	0. 0.23	0.23	00014700
				0.0	0.0	0.0	0.0	00014800
								00014900
SB0629	29	2 30 21	0 200	162.6047	1.0	0. 0.23	0.23	00015000
				1.284	2.482	0.0	0.0	00015100
								00015200
SB0630	30	2 21 22	1 200	162.1173	1.0	0. 0.80	0.80	00015300
				0.0	0.0	0.0	0.0	00015400
								00015500
SB0631	31	2 22 32	1 200	161.5410	1.0	0. 0.80	0.80	00015600
				0.0	0.0	0.0	0.0	00015700
								00015800
SB0632	32	2 32 23	1 200	160.946155	1.0	0. 0.80	0.80	00015900
				0.0	0.0	0.0	0.0	00016000
								00016100
SB0633	33	2 23 24	1 200	160.3296	1.0	0. 0.80	0.80	00016200
				0.0	0.0	0.0	0.0	00016300
								00016400
SB0634	34	2 24 33	0 200	159.7062	1.0	0. 0.23	0.23	00016500
				0.76	0.34	0.0	0.0	00016600
								00016700
SB0635	35	3 30 33	0 1	162.6047	0.555	0. 3.66	3.66	00016800

	1	2	3	4	5	6	7-R	8
		0.77	0.83	0.87	0.78			00016900
SB0636								00017000
36	1 32 31	0 200	161.029550	0.034	0. 0.1	0.		00017100
			0.0	0.0	0.0	0.0		00017200
SB0637								00017300
37	1 33 26	0 1	159.17209	3.44	0. 4.341	1.64		00017400
			0.0	0.0	0.0	0.0		00017500
SB0638								00017600
38	13 26 40	0 1	5.0	2.216	0. 3.658	2.073		00017700
			1.491E4	1.491E4	0.0	0.0		00017800
SB0639								00017900
39	13 27 25	0 1	5.0	0.29	0. 15.0	1.7		00018000
			0.41	0.87	0.0	0.0		00018100
SB0640								00018200
40	13 25 35	0 1	5.0	0.29	0. 14.3	1.6		00018300
			0.0	0.0	0.0	0.0		00018400
SB0641								00018500
41	13 28 37	0 3	10.0	0.305	0. 12.0	0.0		00018600
			0.0	0.0	0.0	0.0		00018700
SB0642								00018800
42	13 34 38	0 1	10.0	0.305	0. 12.0	0.0		00018900
			0.0	0.0	0.0	0.0		00019000
SB0643								00019100
43	13 28 36	0 3	10.0	0.222	0. 120.0	0.0		00019200
			0.109	0.049	0.0	0.0		00019300
SB0644								00019400
44	13 34 39	0 1	10.0	0.222	0. 120.0	0.0		00019500
			0.109	0.049	0.0	0.0		00019600
/								00019700
/	**** JUNCTION DATA ****							00019800
BB07								00019900
	1	1	0.0					00020000
	2	1	0.0					00020100
	3	1	0.0					00020200
	4	1	0.0					00020300
	5	1	0.0					00020400
	6	1	0.0					00020500
	7	1	0.0					00020600
	8	1	0.0					00020700
	9	1	0.0					00020800
	10	1	0.0					00020900
	11	1	0.					00021000
	12	1	0.0					00021100
	13	1	0.0					00021200
	14	1	0.0					00021300
	15	1	0.0					00021400
	16	1	0.0					00021500
	17	1	0.0					00021600
	18	1	0.0					00021700
	19	1	0.0					00021800
	20	1	0.0					00021900
	21	1	0.					00022000
	22	1	0.					00022100
	23	1	0.					00022200
	24	1	0.					00022300
	25	1	0.					00022400
	26	2	1.027					00022500
	27	4	0.049					00022600
	28	4	0.351					00022700

```

-----*-----1-----*-----2-----*-----3-----*-----4-----*-----5-----*-----6-----*-----7-R-----*-----8
29 3 0.531 00022800
30 4 0.1 00022900
31 4 0.01 00023000
32 4 0.01 00023100
33 4 0.05 00023200
34 4 0.117 00023300
35 6 0. 00023400
36 5 0. 00023500
37 7 0. 00023600
38 7 0. 00023700
39 5 0. 00023800
40 8 0. 00023900
/ 00024000
/ **** MIXING JUNCTION DATA ****
BB08 00024100
SB0801 00024200
26 3 1 11 38 0 0.25 0.75 0. 0. 00024300
SB0802 00024400
27 2 12 39 0 0 1.0 0.0 0. 0. 00024500
SB0803 00024600
28 3 20 41 43 0 1.0 0.0 0.0 0.0 00024700
SB0804 00024800
29 1 21 0 0 0 1.0 0.0 0.0 0.0 00024900
SB0805 00025000
30 3 23 29 35 0 0.945 0.005 0.05 0.0 00025100
SB0806 00025200
31 1 26 0 0 0 1.0 0.0 0. 0. 00025300
SB0807 00025400
32 2 32 36 0 0 0.99 0.01 0. 0. 00025500
SB0808 00025600
33 1 37 0 0 0 1.0 0.0 0.0 0.0 00025700
SB0809 00025800
34 3 9 42 44 0 1.0 0.0 0.0 0.0 00025900
/ 00026000
/ **** PUMPED INJECTION DATA ****
BB09 00026100
SB0901 00026200
1 37 30.0 00026300
2 1 00026400
0.0 666.0 1000.0 666.0 00026500
SB0902 00026600
2 38 30.0 00026700
2 1 00026800
0.0 222.0 1000.0 222.0 00026900
/ 00027000
/ **** PUMP DATA ****
BB10 00027100
SB1001 00027200
8 1 1 1185.0 5.58 4.33E4 105.0 749.0 1150.0 3460.0 0.5 0.0 00027300
0.05 00027400
SB1002 00027500
19 1 1 1185.0 5.58 4.33E4 105.0 749.0 1150.0 3460.0 0.5 0.0 00027600
0.05 00027700
/ 00027800
/ **** PUMP DATA TABLE ****
BB11 00027900
SB1101 00028000
1 00028100
14 00028200
00028300
00028400
00028500
00028600

```

	1	2	3	4	5	6	7	8	
	-1.0	1.56	-0.85	1.33	-0.80	1.28	-0.72	1.30	00028700
	-0.62	1.35	-0.50	1.36	-0.34	1.34	-0.21	1.29	00028800
	-0.11	1.23	0.0	1.22	0.25	1.16	0.50	1.13	00028900
	0.75	1.07	1.0	0.98					00029000
14									00029100
	-1.0	0.18	-0.85	0.34	-0.80	0.40	-0.72	0.48	00029200
	-0.62	0.556	-0.50	0.67	-0.34	0.77	-0.21	0.84	00029300
	-0.11	0.89	0.0	0.95	0.25	1.16	0.50	1.35	00029400
	0.75	1.62	1.0	1.94					00029500
11									00029600
	-1.0	0.18	-0.75	-0.13	-0.50	-0.32	-0.32	-0.40	00029700
	-0.16	-0.42	0.0	-0.39	0.16	-0.28	0.32	0.16	00029800
	0.50	0.01	0.75	0.40	1.0	0.98			00029900
11									00030000
	-1.0	1.56	-0.75	1.12	-0.50	0.90	-0.32	0.82	00030100
	-0.16	0.76	0.0	0.71	0.16	0.71	0.32	0.76	00030200
	0.50	0.90	0.75	1.33	1.0	1.94			00030300
14									00030400
	-1.0	0.70	-0.90	0.70	-0.80	0.68	-0.70	0.63	00030500
	-0.60	0.53	-0.50	0.47	-0.40	0.46	-0.30	0.45	00030600
	-0.20	0.45	0.0	0.48	0.25	0.55	0.50	0.66	00030700
	0.75	0.83	1.0	1.02					00030800
14									00030900
	-1.0	-1.42	-0.90	-1.32	-0.80	-1.23	-0.70	-1.14	00031000
	-0.60	-1.07	-0.50	-0.99	-0.40	-0.91	-0.30	-0.84	00031100
	-0.20	-0.77	0.0	-0.64	0.25	-0.49	0.50	-0.34	00031200
	0.75	-0.20	1.0	-1.10					00031300
13									00031400
	-1.0	-1.42	-0.8	-1.12	-0.6	-0.82	-0.5	-0.68	00031500
	-0.4	-0.55	-0.2	-0.28	0.0	-0.08	0.11	0.0	00031600
	0.25	0.12	0.50	0.33	0.75	0.61	0.92	0.82	00031700
	1.0	1.02							00031800
13									00031900
	-1.0	0.70	-0.8	0.5	-0.6	0.4	-0.5	0.39	00032000
	-0.4	0.38	-0.2	0.33	0.0	0.28	0.11	0.25	00032100
	0.25	0.22	0.50	0.14	0.75	0.03	0.92	0.01	00032200
	1.0	-0.10							00032300
/ 2									00032400
/ 0.0 1.0 1000.0 0.5									00032500
/ 2									00032600
/ -1.0 -50.0 1.0 50.0									00032700
12									00032800
	-1.0	-1.15	-0.9	-1.24	-0.6	-2.8	-0.5	-2.9	00032900
	-0.4	-2.7	0.0	0.0	0.12	0.85	0.2	1.1	00033000
	0.5	1.02	0.7	1.0	0.9	0.95	1.0	1.0	00033100
4									00033200
	-1.0	0.0	0.0	0.0	0.5	-0.8	1.0	-1.46	00033300
7									00033400
	-1.0	0.0	0.0	0.0	0.1	-0.02	0.2	0.0	00033500
	0.3	0.1	0.9	0.78	1.0	1.0			00033600
12									00033700
	-1.0	-1.15	-0.8	-0.5	-0.6	-0.2	-0.4	0.03	00033800
	-0.2	0.04	0.0	0.1	0.2	0.15	0.4	0.12	00033900
	0.6	0.05	0.8	-0.5	0.9	-0.9	1.0	-1.46	00034000
0									00034100
0									00034200
0									00034300
0									00034400
13									00034500

	1	2	3	4	5	6	7	R	8		
0.0	0.0	0.05	0.0	0.1	0.025	0.15	0.075	0.2	0.18	00034600	
0.3	0.475	0.4	0.625	0.5	0.74	0.6	0.82			00034700	
0.7	0.87	0.8	0.84	0.9	0.72	1.0	0.08			00034800	
11										00034900	
0.0	0.0	0.1	0.0	0.20	0.13	0.3	0.24			00035000	
0.4	0.31	0.5	0.33	0.6	0.3	0.7	0.23			00035100	
0.8	0.16	0.9	0.08	1.0	0.0					00035200	
6	6									00035300	
0.0	0.2	0.4	0.6	0.8	1.0					00035400	
0.0	0.0	0.0	0.0	0.0	0.0					00035500	
0.2	0.0	3.065E-5	7.7239E-5	1.3263E-4	1.946E-4	2.6207E-4				00035600	
0.4	0.0	4.866E-5	1.2261E-4	2.1053E-4	3.0996E-4	4.1602E-4				00035700	
0.6	0.0	6.376E-5	1.6066E-4	2.7587E-4	4.0485E-4	5.4514E-4				00035800	
0.8	0.0	7.7239E-5	1.9463E-4	3.3419E-4	4.9044E-4	6.6037E-4				00035900	
1.0	0.0	8.9628E-5	2.2585E-4	3.878E-4	5.691E-4	7.6631E-4				00036000	
/										00036100	
/	**** ACCUMLATOR DATA ****									00036200	
BB12										00036300	
SB1201										00036400	
48	36	70.	30.	30.0	44.					00036500	
0.9	3.0									00036600	
SB1202										00036700	
49	39	23.3	10.	30.0	44.					00036800	
0.9	1.0									00036900	
/										00037000	
/	**** BREAK POINT DATA ****									00037100	
BB13										00037200	
8	0.01	0.4	0.8	0.6	0.6	0.8	0.6	0.6		00037300	
6										00037400	
0.0	1.0	7.5	2.7	15.	4.0	30.	4.0	60.	4.0	1000. 4.0	
/										00037600	
/	**** PRESSURIZER DATA ****									00037700	
BB14										00037800	
45	35	11	3.58	15.56	9.0	0.99	0.1			00037900	
	1.7	385.0								00038000	
50.0	1.0	0.1	0.0	0.0						00038100	
0.915	0.915	0.915	1.525	3.05	4.58					00038200	
0.564	0.67	0.619								00038300	
2										00038400	
0.1	1.0	1.0	1.0	1000.	1.0	1.0	1.0			00038500	
/										00038600	
/	**** STEAM GENERATOR DATA ****									00038700	
BB15										00038800	
SB1501										00038900	
46	3265	3	5	3	1					00039000	
5.5	18.9	0.7	0.5	3.0E-2	1.0E-2	10.4	4.0	222.1	474.5	00039100	
0.1	0.95	62.0								00039200	
	2.0	11.0								00039300	
-40.	-30.	-25.								00039400	
	0.001	80.	0.5	0.5	0.5					00039500	
3										00039600	
0.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1000.0	1.0	1.0	0.0
SB1502										00039700	
47	9795	14	16	3	1					00039800	
16.5	18.9	2.1	0.5	3.0E-2	1.0E-2	10.4	4.0	222.1	1423.5	00039900	
0.1	0.95	62.0								00040000	
	2.0	11.0								00040100	
-40.0	-30.0	-25.0								00040200	
	0.003	80.	0.5	0.5	0.5					00040300	
										00040400	


```

-----1-----2-----3-----4-----5-----6-----7-R-----8
3
0.0 1.0 1.0 1.0 1.0 1.0 1.0 1.0 1000.0 1.0 1.0 0.0
/
/ **** CORE DATA ****
BB16
/ --- AVERAGE CHANNEL ----
SB1601
1
39170 23 28 0 3 1 2 2
9000.0 5.3658E-3 0.6187E-3 4.6573E-3 1.42E-2 0.6 1.0E-4
0.0124 0.0212E-02 0.0305 0.1402E-02
0.111 0.1254E-02 0.301 0.2529E-02
1.13 0.0736E-02 3.00 0.0269E-02
5.0 0.6 4.91E-04 3.41E-06 1.2 1.54E03
0. 156. 234. 234. 156. 0.
1.6122E-07 6.42E-07 7.56E-07 7.56E-07 6.42E-07 1.622E-07
1.6122E-07 6.42E-07 7.56E-07 7.56E-07 6.42E-07 1.622E-07
1.6122E-07 6.42E-07 7.56E-07 7.56E-07 6.42E-07 1.622E-07
1.6122E-07 6.42E-07 7.56E-07 7.56E-07 6.42E-07 1.622E-07
/ --- HOT CHANNEL ---
SB1602
2
200 29 34 0 3 1 2 2
9000.0 5.3665E-3 0.6187E-3 4.6682E-3 1.42E-2 0.6 1.0E-4
0. 203.0 304.0 304.0 203.0 0.
1.6122E-07 6.42E-07 7.56E-07 7.56E-07 6.42E-07 1.622E-07
1.6122E-07 6.42E-07 7.56E-07 7.56E-07 6.42E-07 1.622E-07
1.6122E-07 6.42E-07 7.56E-07 7.56E-07 6.42E-07 1.622E-07
1.6122E-07 6.42E-07 7.56E-07 7.56E-07 6.42E-07 1.622E-07
/
/ **** REACTIVITY DATA ****
BB17
3
0. 0. 0.5 -5. 1. -25.
5
18. 3.56E-3 538. 0. 1093. -3.08E-3 1649. -2.7E-3 2760. -2.44E-3
5
0.01 0.0 1.0 -0.1 1.5 -0.2 2.0 -3.0 1000. -8.0
/
/ ****METAL WATER REACTION DATA ****
BB18
1.54E03 0.775E-04 2.29E04
/
/ **** FUEL GAP DATA ****
BB19
0.0301 0.0 1.235E-5 0.0 0.0 0.0 0.0 0.6 0.6 0.0
0.9495 0.0157 0.0028 0.0 0.032 0.0 0.0
/
/ **** BURST DATA ****
BB21
2 2 5.0E7 6.96E-08 2.87E4 2.86E-03 1.15E0 1.528E0
1.49E-07 2.0E-08 1.25E-16 1.85E-01 8.0E09 3.3E-03
0.1
/
/ **** OTHER DATA ****
BB22
0. 1.4 1.4 0.
BEND
10
0 0 0 0 0 15.
0. 1.0-7 0. -1.0E+10 0.01 0.01
0
0 0.0
0 0.0

```

```

LARGE BREAK OF 1,100 MWE PWR (2 CHANNELS) * DATA 2 * 82.07.09      00000100
/
/ **** DIMENSION DATA ****      00000200
BB01      00000300
  0  2  9  4  16  49  40  9  2  2  2  2  3  6  5  3  0  2      00000400
/      00000500
/ **** MINOR EDIT DATA ****      00000600
BB02      00000700
PRE-08  PRA-12  GLA-23  GLA-29  GLE-35  GLE-36  GLA-37  GLA-38  PRA-26      00000800
/      00000900
/ **** TIME STEP CONTROL DATA ****      00001000
BB03      00001100
SB0301      00001200
  0.2  0.2  100.      00001300
SB0302      00001400
  20  3  50  0  1.0E-3  1.0E-6  0.3  0.1      00001500
SB0303      00001600
  200 3  50  0  8.0E-3  1.0E-6  60.0  0.1      00001700
SB0304      00001800
  200 3  50  0 16.0E-3  1.0E-6  90.0  0.1      00001900
SB0305      00002000
  200 3  50  0 32.0E-3  1.0E-6 2000.0  0.1      00002100
/      00002200
/ **** TRIP CONTROLL DATA ****      00002300
BB04      00002400
SB0480      00002500
  1  0  1  0 1000.0  0.0      00002600
SB0481      00002700
  5 46  1  0  0.4  0.0      00002800
SB0482      00002900
  5 47  1  0  0.4  0.0      00003000
SB0483      00003100
  2  8  1  0  0.01  0.0      00003200
SB0484      00003300
  2 19  1  0  0.01  0.0      00003400
SB0485      00003500
  3  0  1  0  0.01  0.0      00003600
SB0486      00003700
  4  1  1  0 25.01  0.0      00003800
SB0487      00003900
 -4  1  1  0 1000.0  0.      00004000
SB0488      00004100
  4  2  1  0 25.01  0.0      00004200
SB0489      00004300
 -4  2  1  0 1000.0  0.      00004400
SB0492      00004500
  6  1 -3  1 240.0  0.005      00004600
SB0493      00004700
  6  2 -3  1 250.0  0.0      00004800
SB0494      00004900
      00005000

```

	1	2	3	4	5	6	7-R	8
6 3 -3 1	360.0	0.0						00005100
SB0495								00005200
-6 1 3 1	350.0	0.0						00005300
SB0496								00005400
-6 2 3 1	305.0	0.0						00005500
SB0497								00005600
-6 3 3 1	380.0	0.00						00005700
BEND								00005800
10								00005900
0 0 0 0 0 30.0								00006000
0. 1.0-7 0. -1.0E+10	0.01	0.01						00006100
0								00006200
11 0.								00006300
7 8 9 10 18 19 20 41 42 43								00006400
4. 4. 4. 4. 4. 4. 4. 4. 4. 4.								00006500
44								00006600
4.								00006700
0 4.								00006800

```

LARGE BREAK OF 1,100 MWE PWR (2 CHANNELS) * DATA 3 * 82.07.09      00000100
/      00000200
/ **** DIMENSION DATA ****      00000300
BB01      00000400
0 2 9 4 16 49 40 9 2 2 2 2 3 6 5 3 0 2      00000500
/      00000600
/ **** MINOR EDIT DATA ****      00000700
BB02      00000800
PRE-08 PRA-12 GLA-23 GLA-29 GLE-35 GLE-36 GLA-37 GLA-38 PRA-26      00000900
/      00001000
/ **** TIME STEP CONTROL DATA ****      00001100
BB03      00001200
SB0301      00001300
0.2 0.2 100.      00001400
SB0302      00001500
20 3 50 0 1.0E-3 1.0E-6 0.3 0.1      00001600
SB0303      00001700
200 3 50 0 8.0E-3 1.0E-6 60.0 0.1      00001800
SB0304      00001900
200 3 50 0 16.0E-3 1.0E-6 90.0 0.1      00002000
SB0305      00002100
200 3 50 0 32.0E-3 1.0E-6 2000.0 0.1      00002200
/      00002300
/ **** TRIP CONTROLL DATA ****      00002400
BB04      00002500
SB0480      00002600
1 0 1 0 1000.0 0.0      00002700
SB0481      00002800
5 46 1 0 0.4 0.0      00002900
SB0482      00003000
5 47 1 0 0.4 0.0      00003100
SB0483      00003200
2 8 1 0 0.01 0.0      00003300
SB0484      00003400
2 19 1 0 0.01 0.0      00003500
SB0485      00003600
3 0 1 0 0.01 0.0      00003700
SB0486      00003800
4 1 1 0 25.01 0.0      00003900
SB0487      00004000
-4 1 1 0 1000.0 0.      00004100
SB0488      00004200
4 2 1 0 25.01 0.0      00004300
SB0489      00004400
-4 2 1 0 1000.0 0.      00004500
SB0492      00004600
6 1 -3 1 240.0 0.005      00004700
SB0493      00004800
6 2 -3 1 250.0 0.0      00004900
SB0494      00005000

```

	1	2	3	4	5	6	7	R	8
6 3 -3 1	360.0	0.0							00005100
SB0495									00005200
-6 1 3 1	350.0	0.0							00005300
SB0496									00005400
-6 2 3 1	305.0	0.0							00005500
SB0497									00005600
-6 3 3 1	380.0	0.00							00005700
BEND									00005800
12									00005900
0 0 0 0 0 250.									00006000
0. 1.0-7 0. -1.0E+10	0.01	0.01							00006100
0									00006200
18 10.									00006300
21 22 23 24 25 26 27 28 29 30									00006400
40. 40. 4. 4. 4. 4. 4. 4. 4. 4.									00006500
31 32 33 34 35 36 37 8									00006600
4. 4. 4. 4. 4. 4. 40. 40.									00006700
0 10.									00006800

Appendix B Figures showing results from base calculation

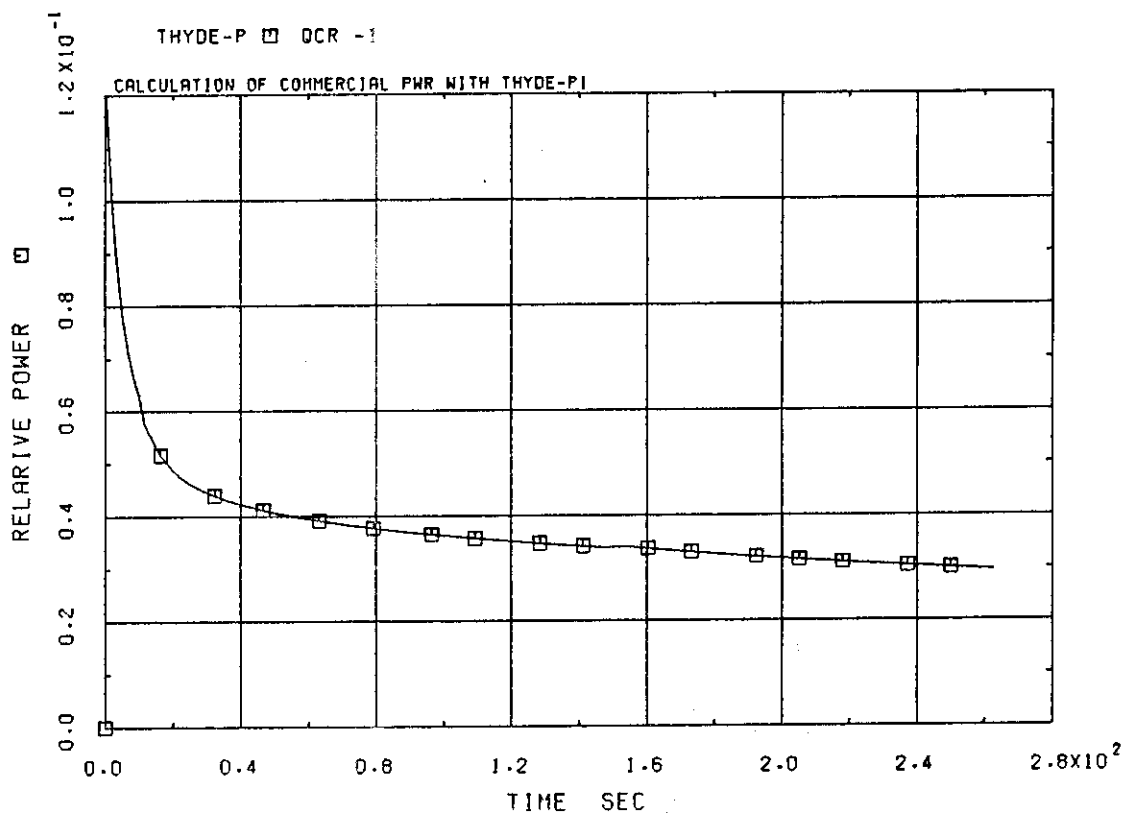


Fig.B-1 Normalized power

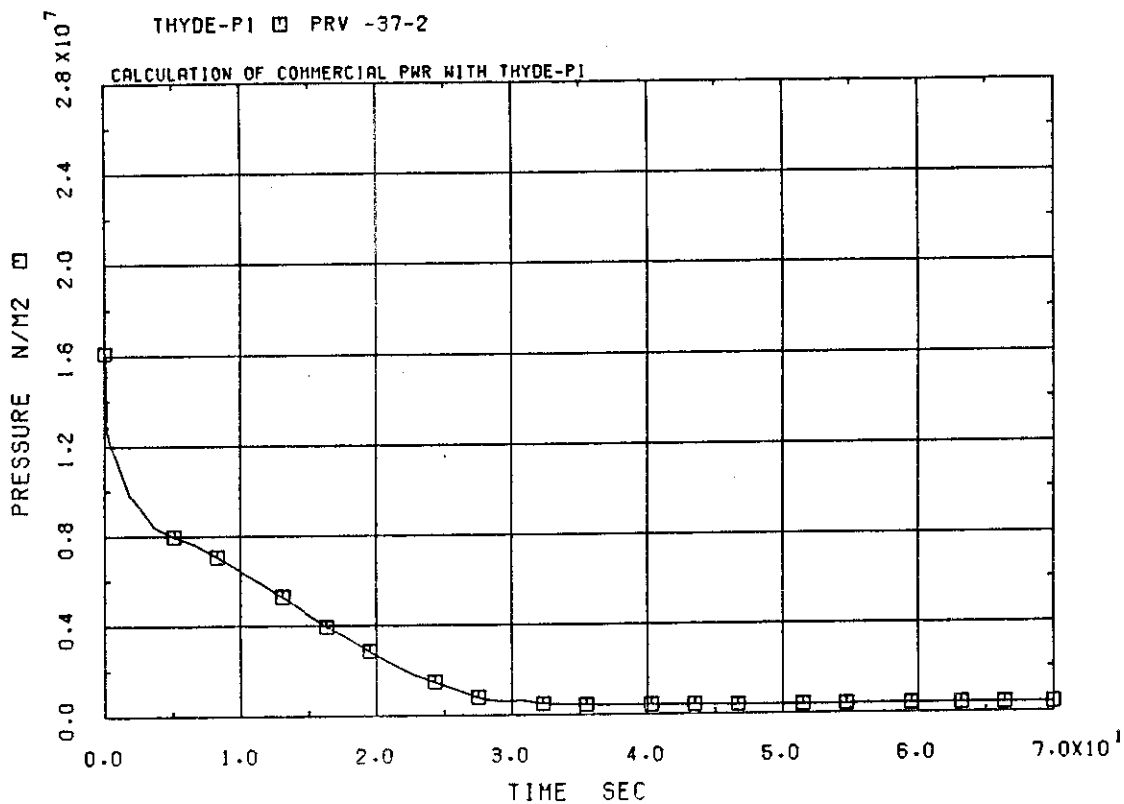


Fig.B-2-1 Upper plenum pressure (short range)

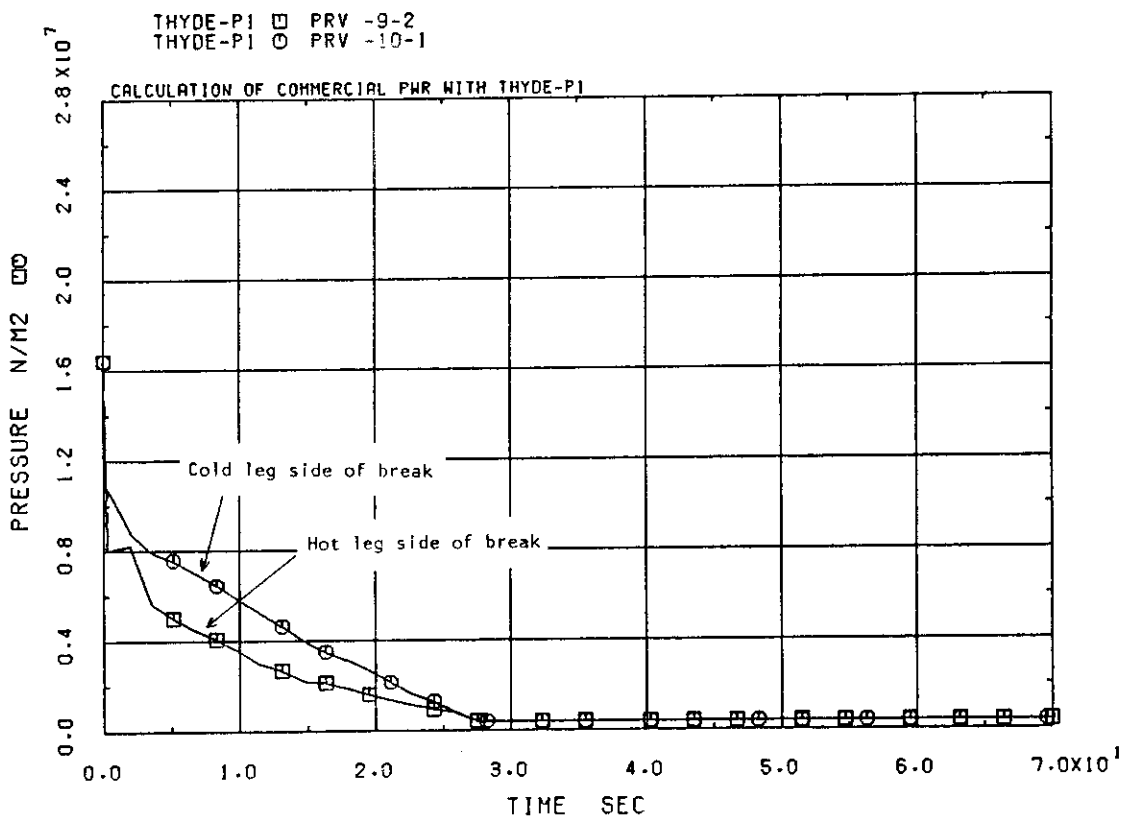


Fig.B-2-2 Break pressures (short range)

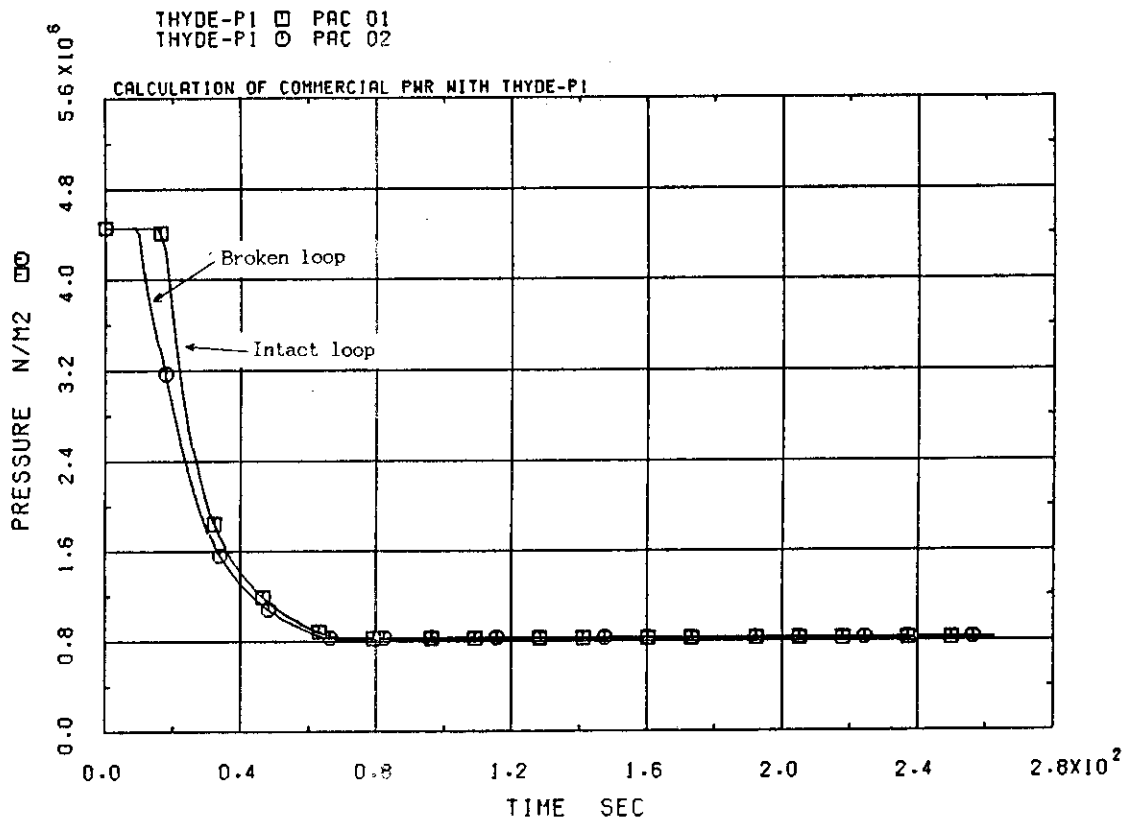


Fig.B-2-3 Accumulator pressures (short range)

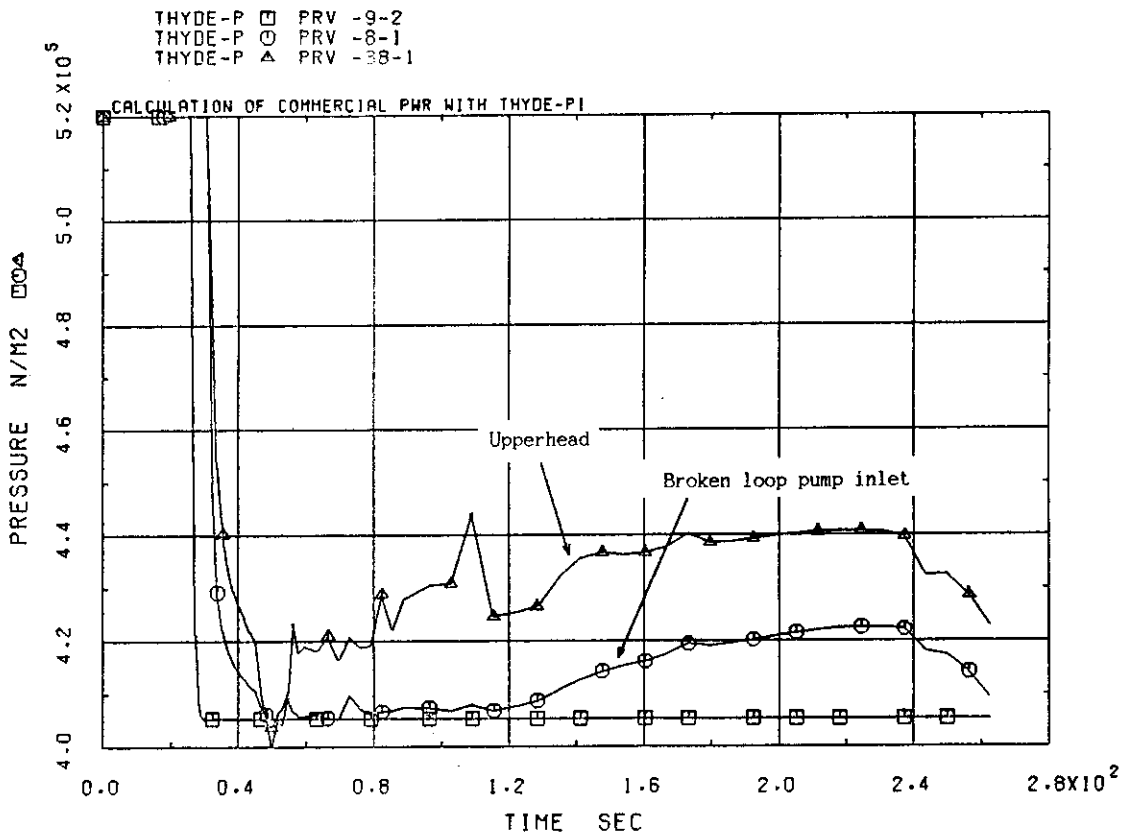


Fig.B-2-4 Pressures during reflooding (broken loop)

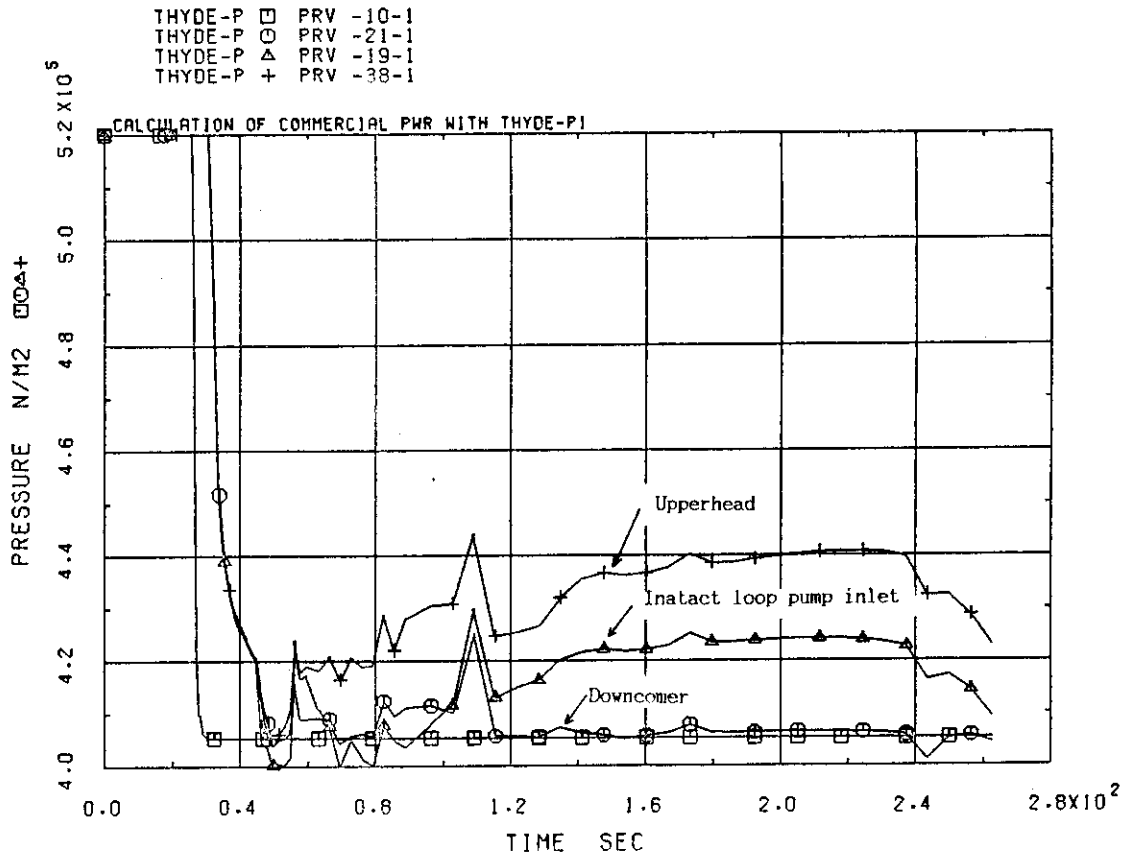


Fig.B-2-5 Pressures during reflooding (intact loop)

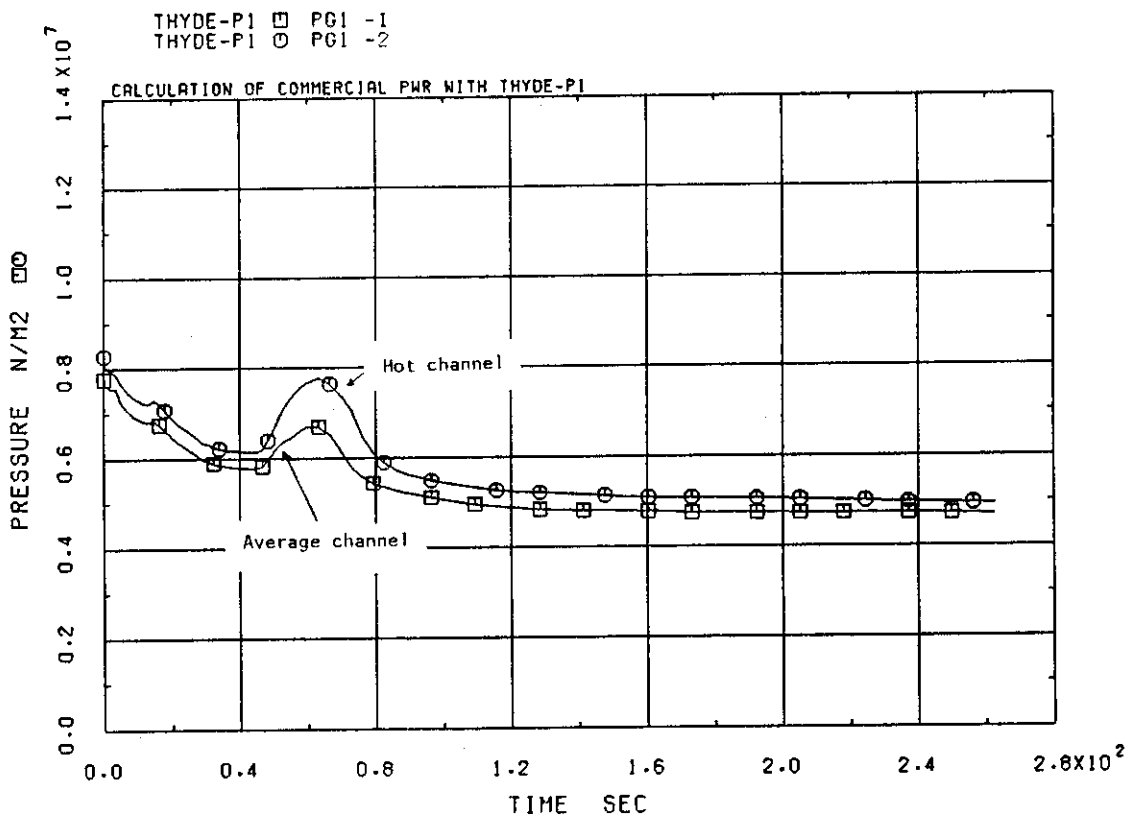


Fig.B-2-6 Gap pressures

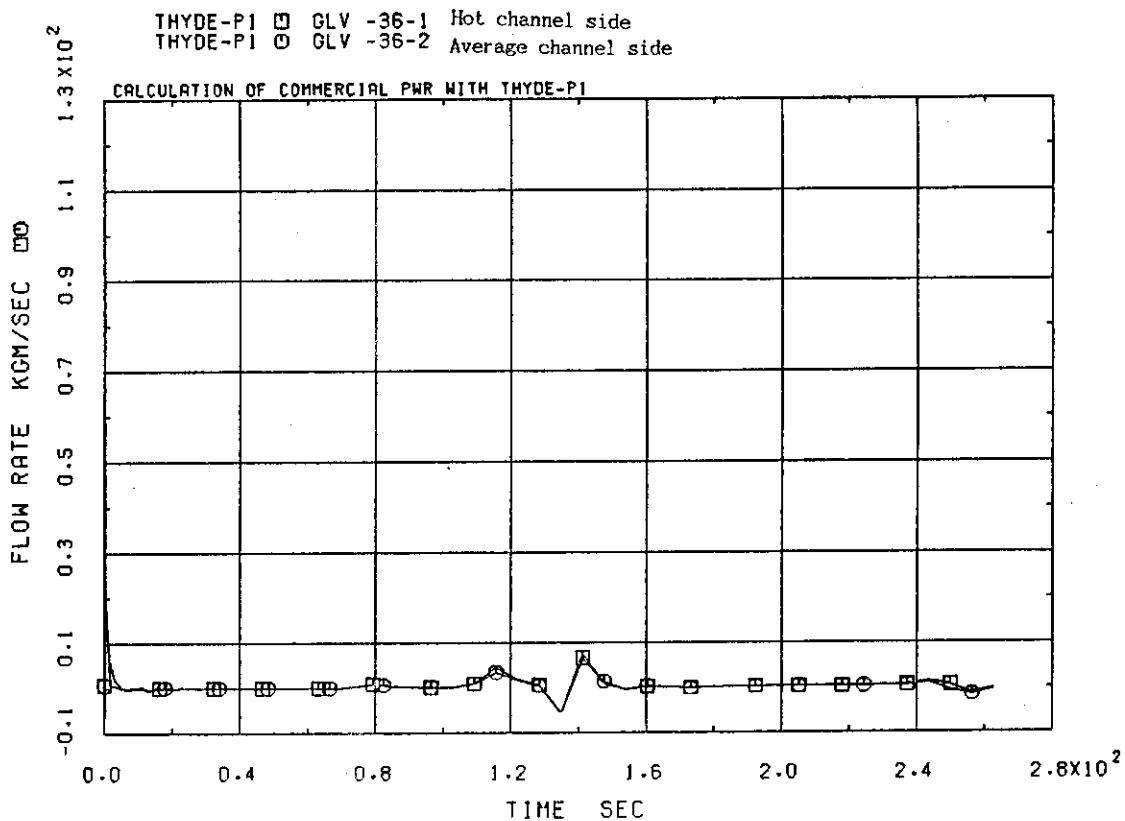


Fig.B-3-1 Mass flow rates at cross flow area

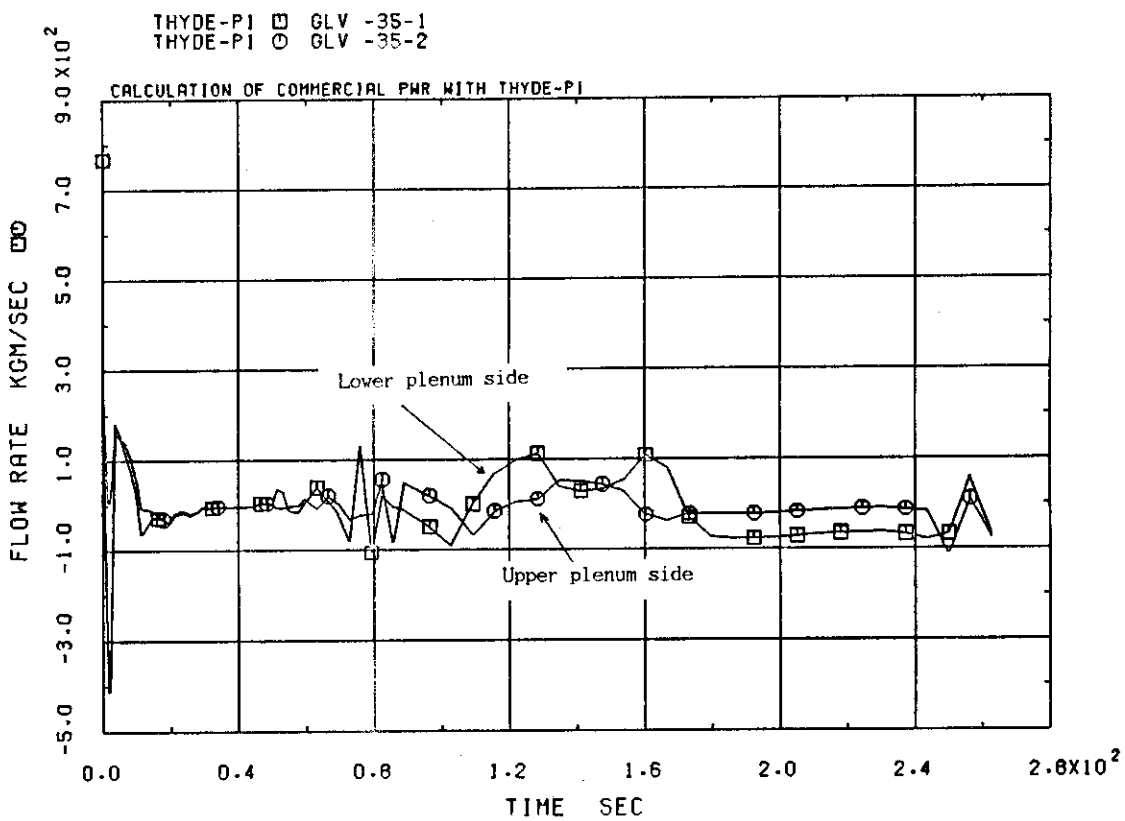


Fig.B-3-2 Mass flow rates at core bypass

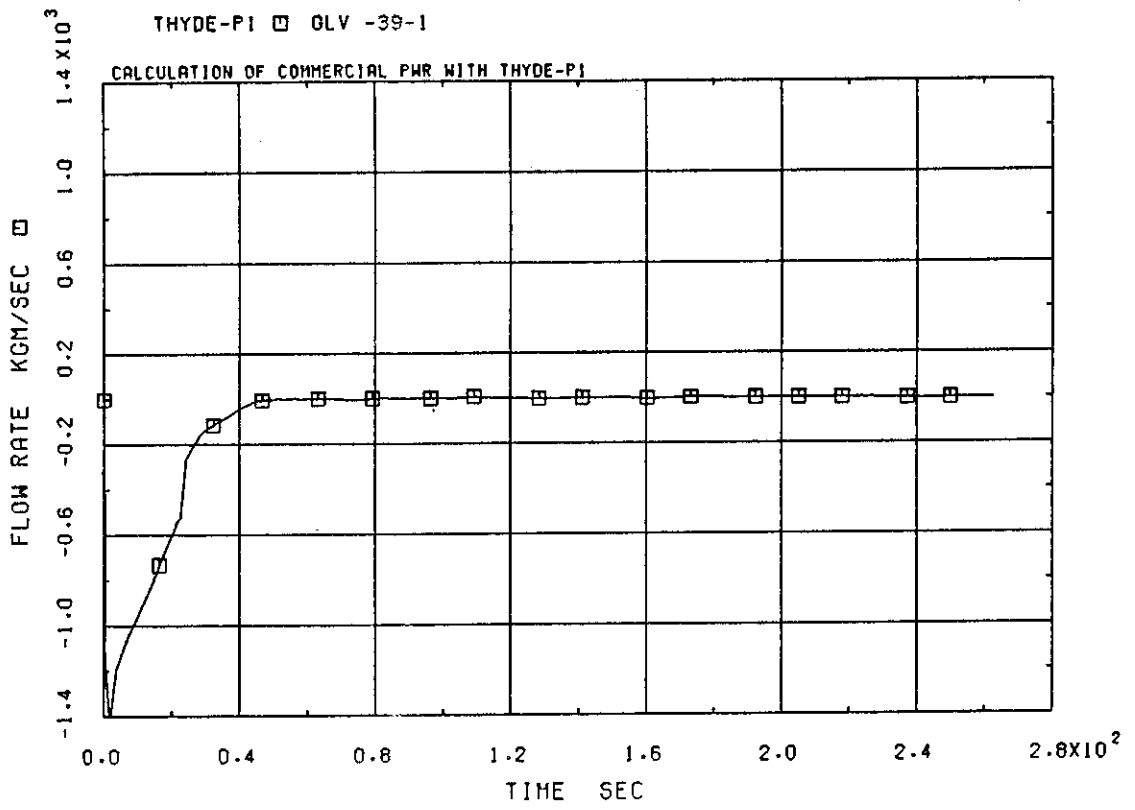


Fig.B-3-3 Mass flow rate at pressurizer surge line

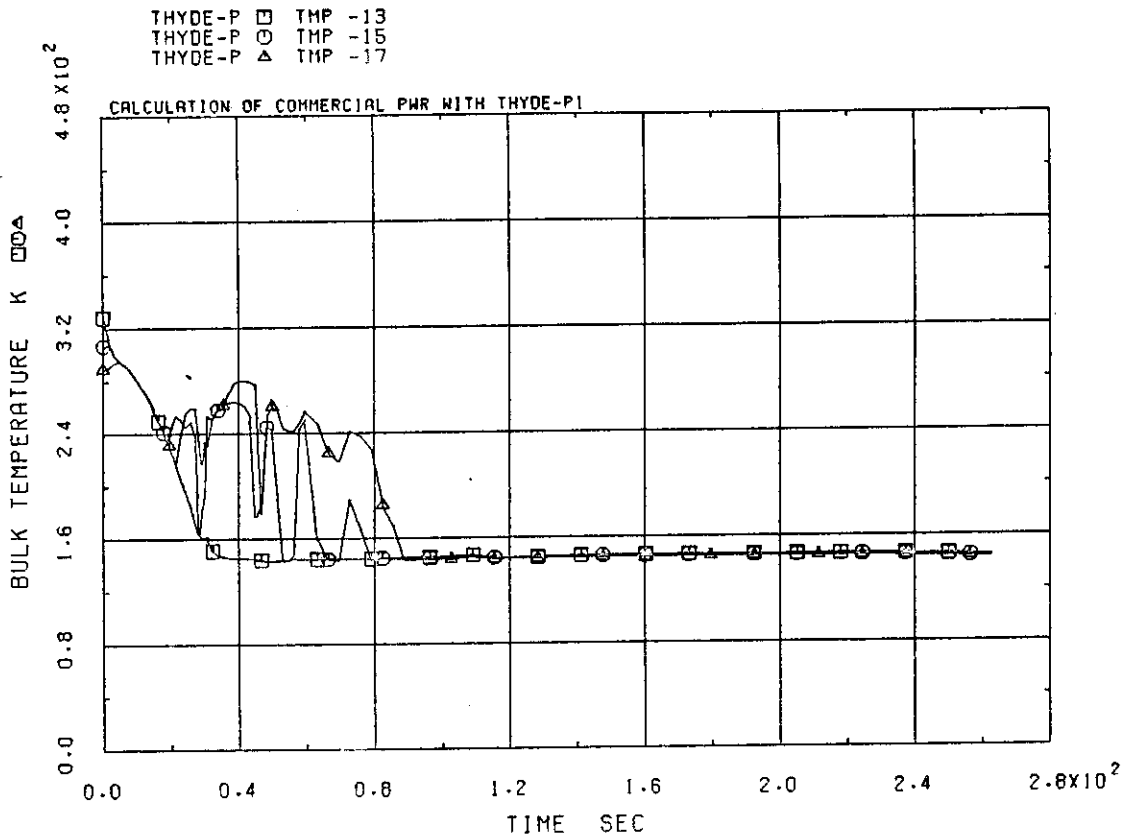


Fig.B-4-1 Coolant temperatures at SG primary system of intact loop

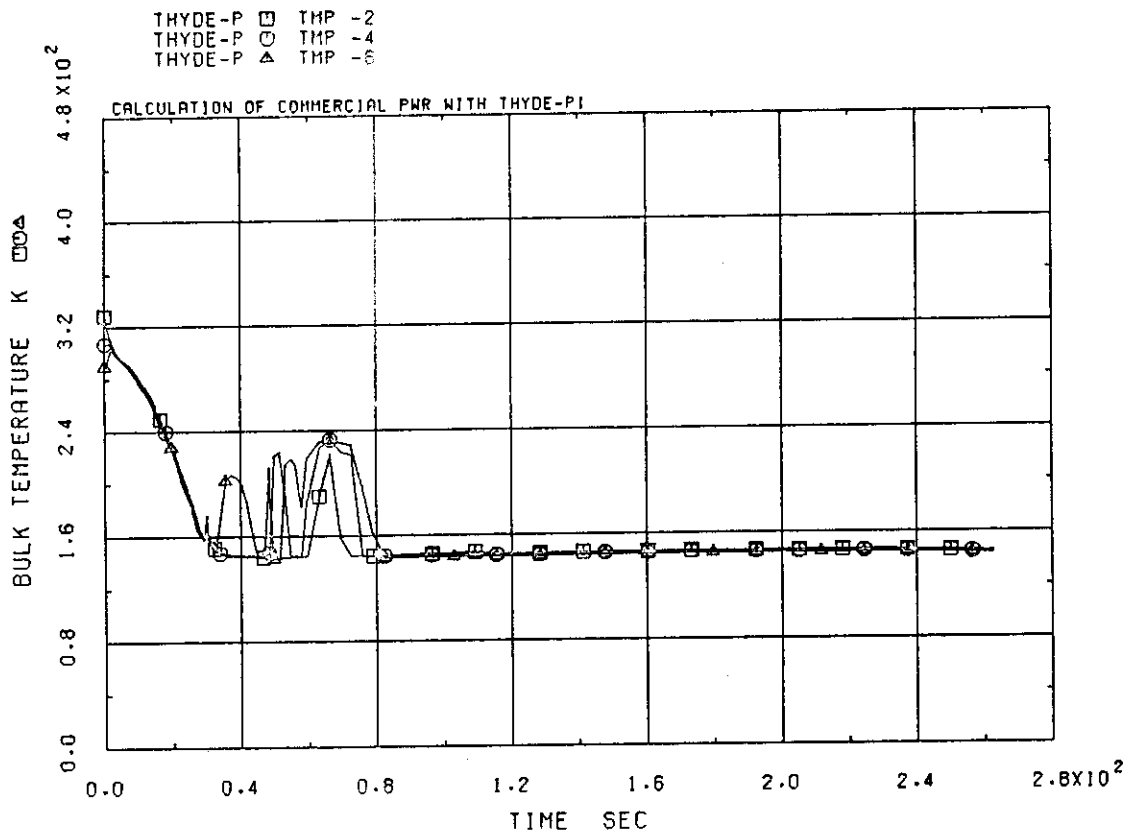


Fig.B-4-2 Coolant temperatures at SG primary system of broken loop

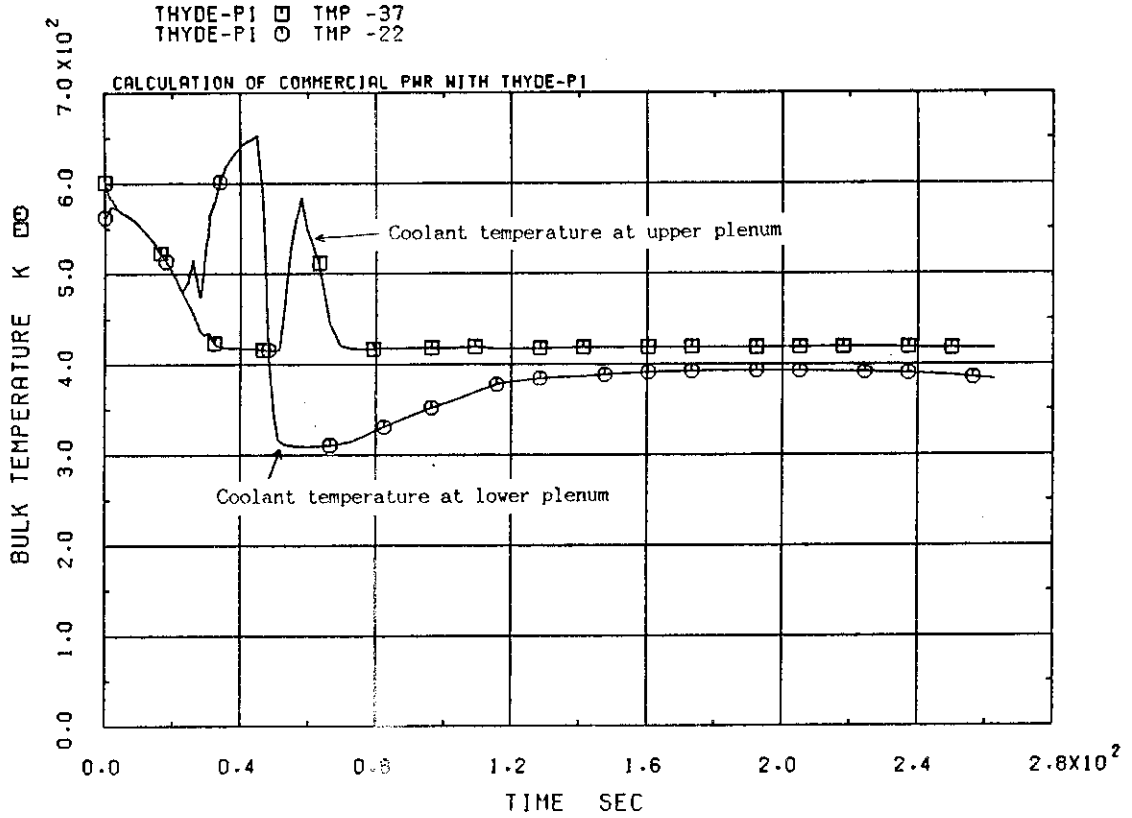


Fig.B-4-3 Coolant temperatures at upper plenum and lower plenum

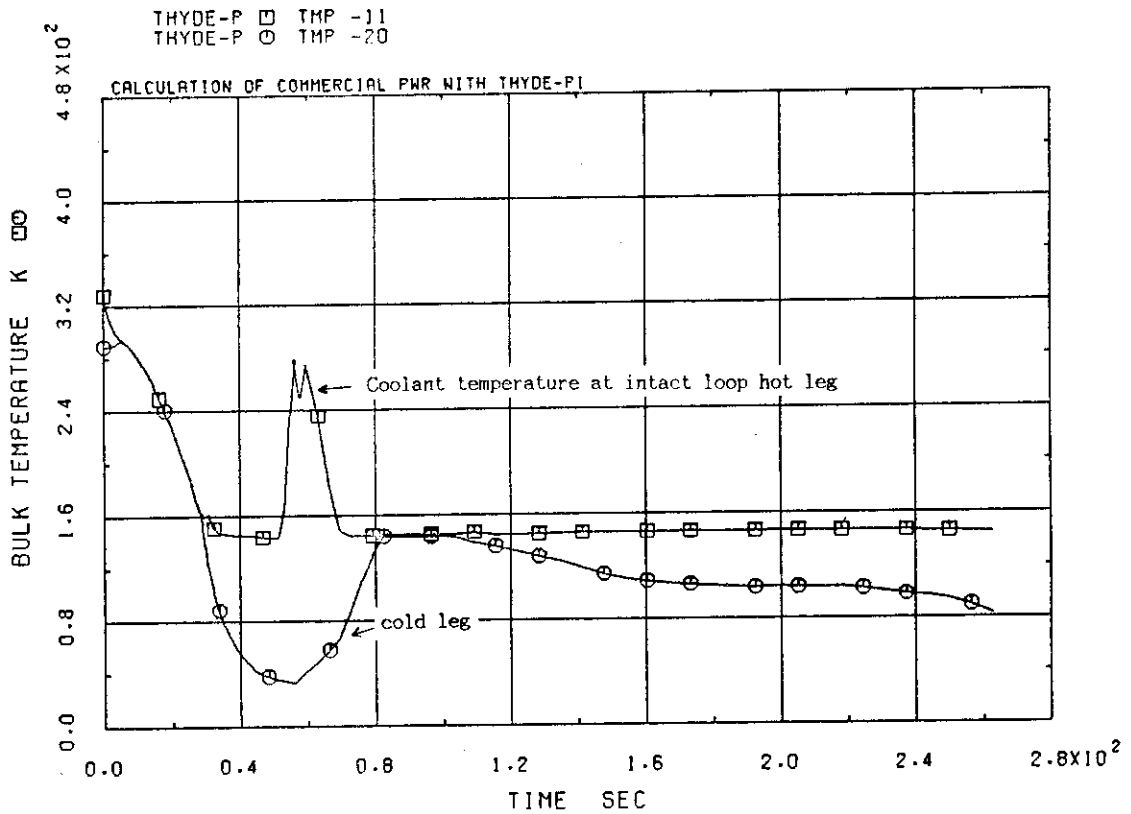


Fig.B-4-4 Coolant temperatures at intact loop hot leg and downcomer

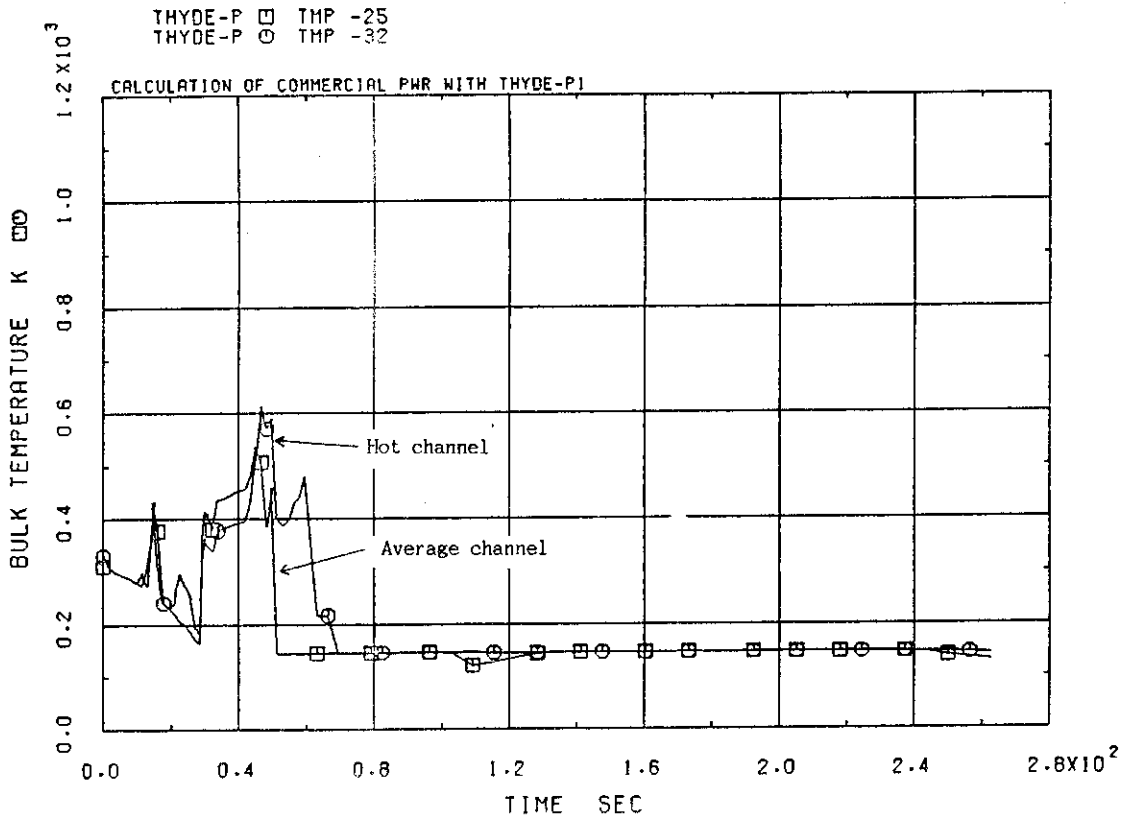


Fig.B-4-5 Coolant temperatures at middle of core

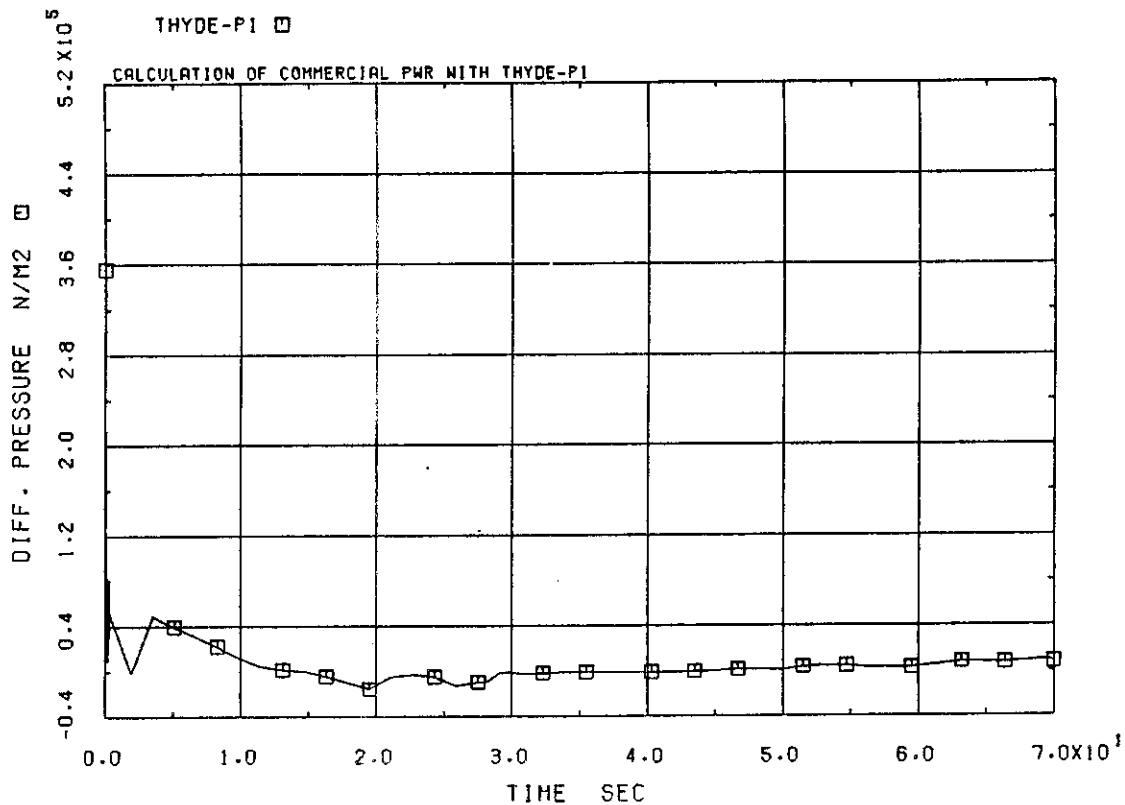


Fig.B-5-1 Differential pressure through core (short range)

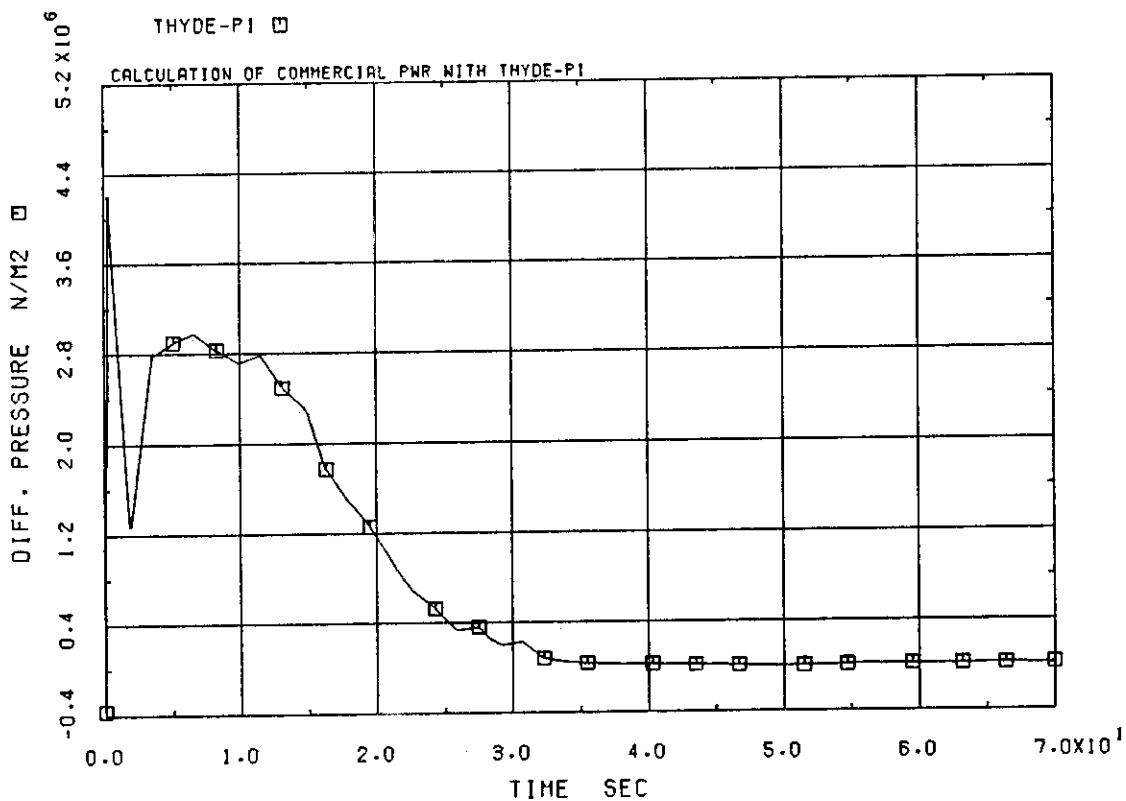


Fig.B-5-2 Differential pressure through broken loop (short range)

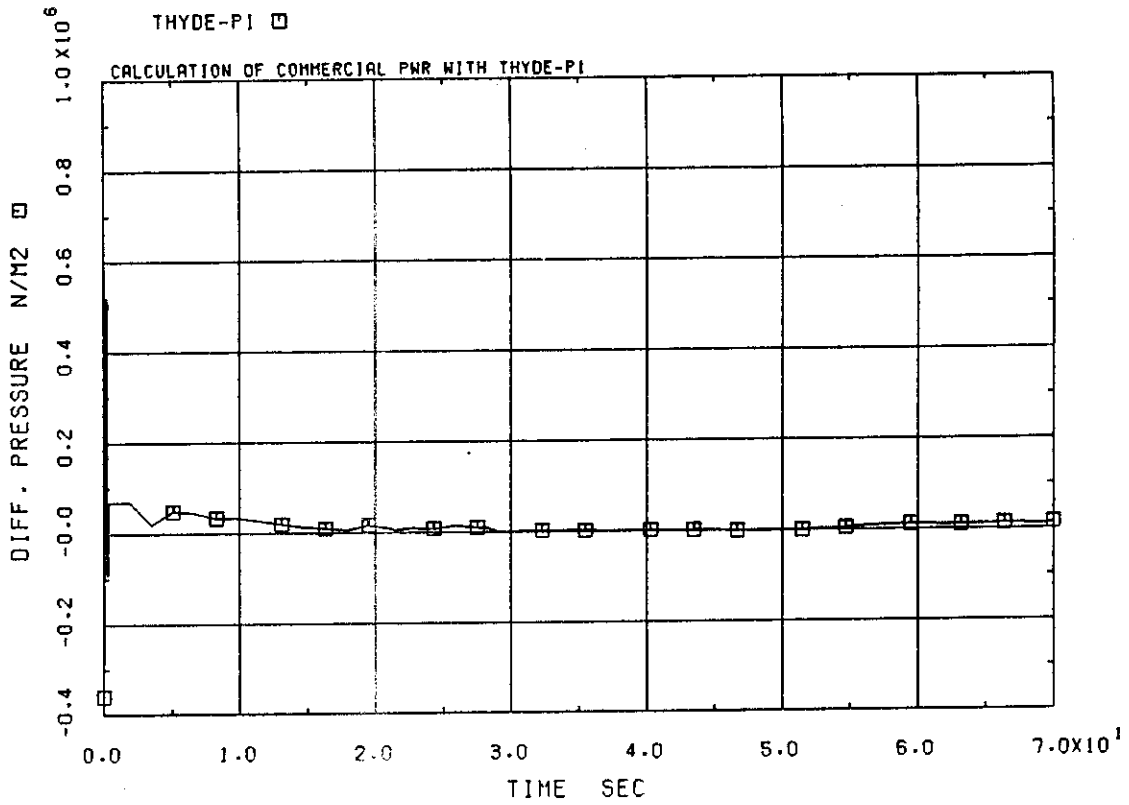


Fig.B-5-3 Differential pressure through intact loop (short range)

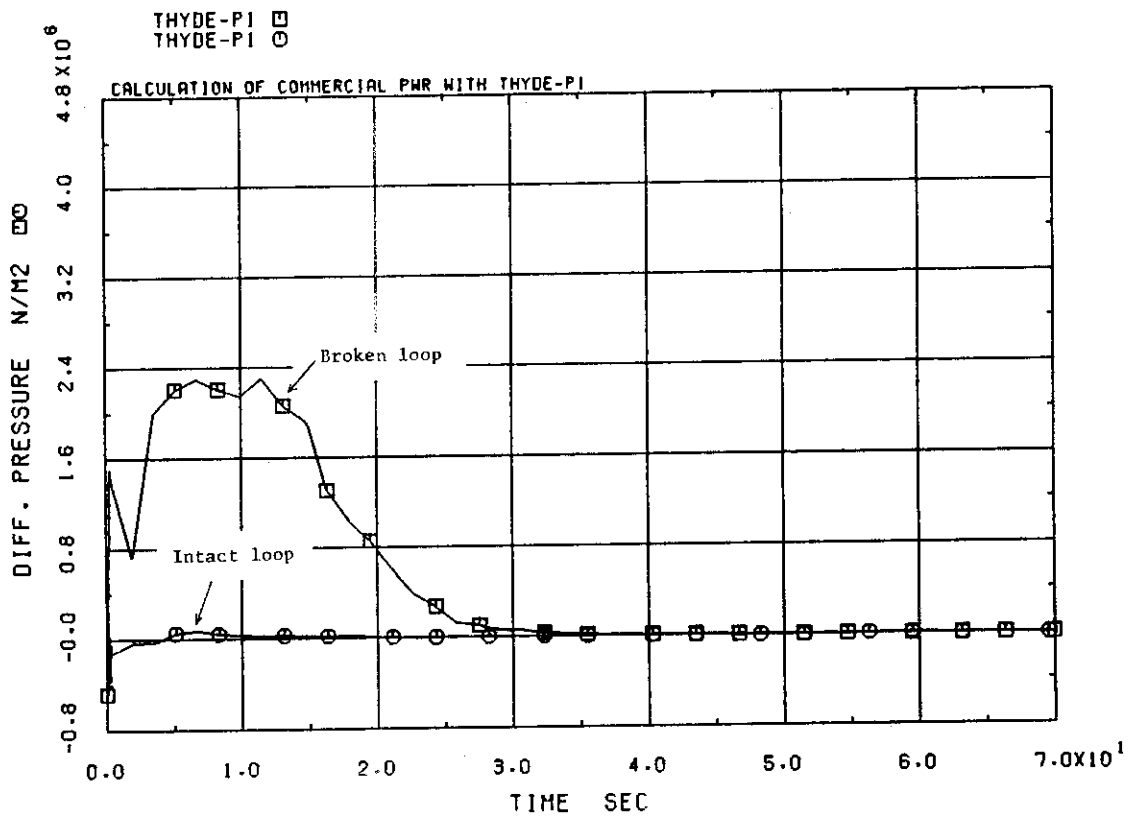


Fig.B-5-4 Differential pressures through pumps (short range)

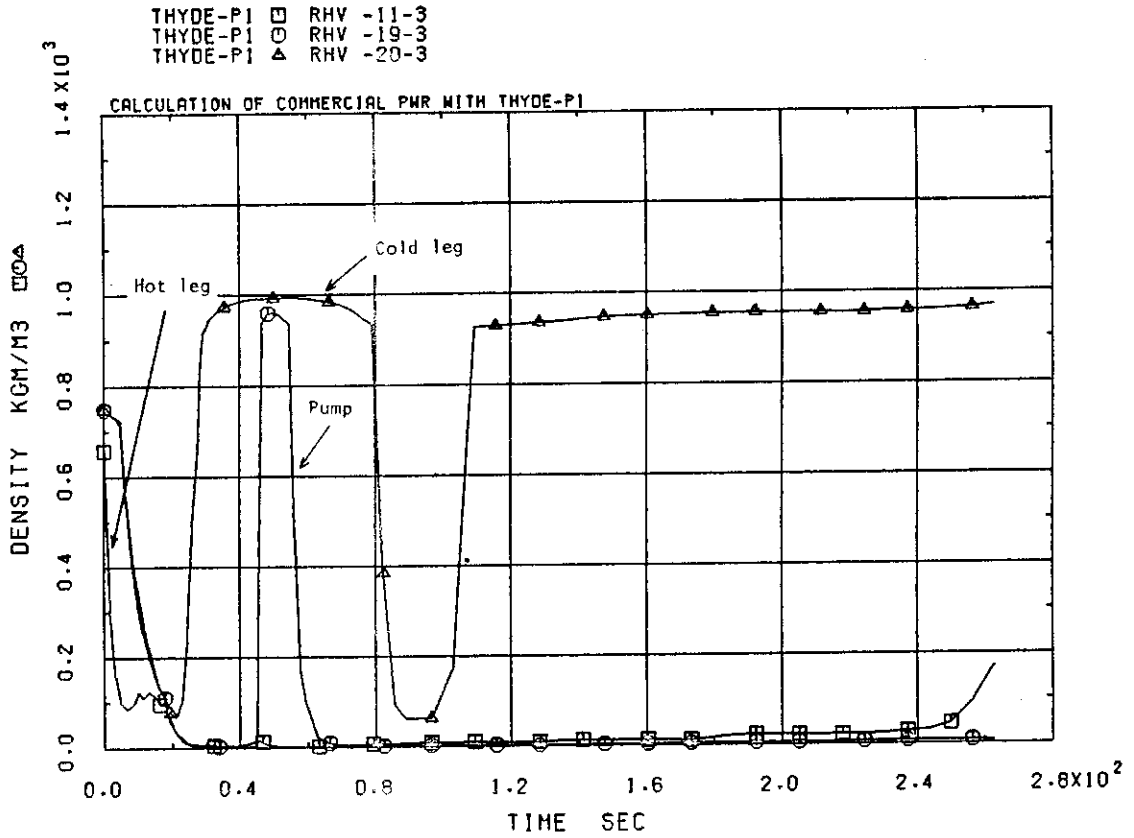


Fig.B-6-1 Equilibrium densities at intact loop

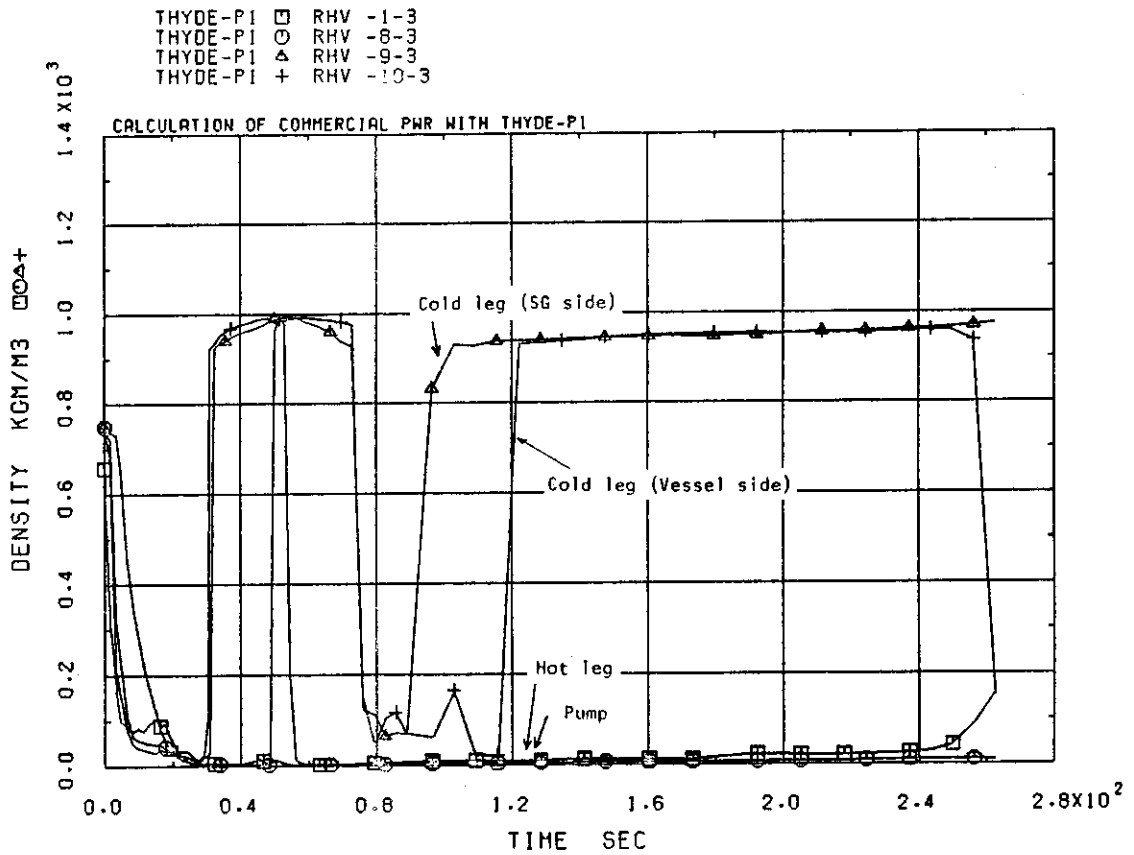


Fig.B-6-2 Equilibrium densities at broken loop

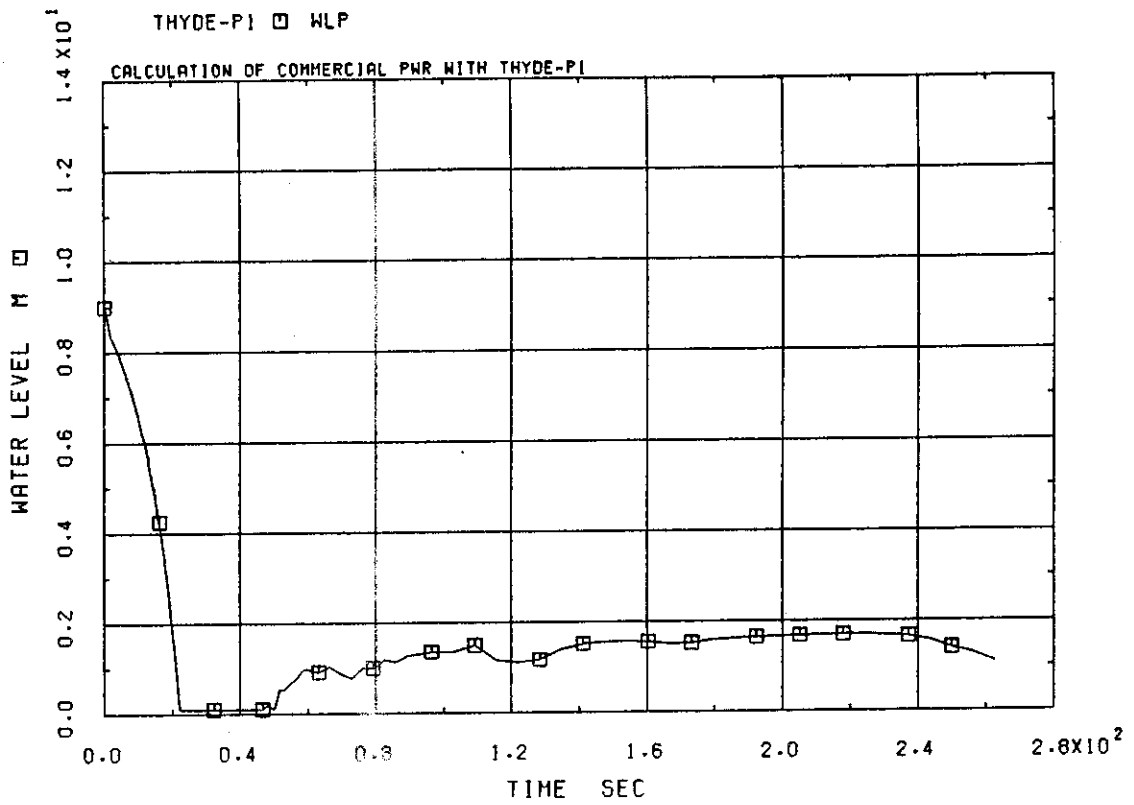


Fig.B-7-1 Pressurizer water level

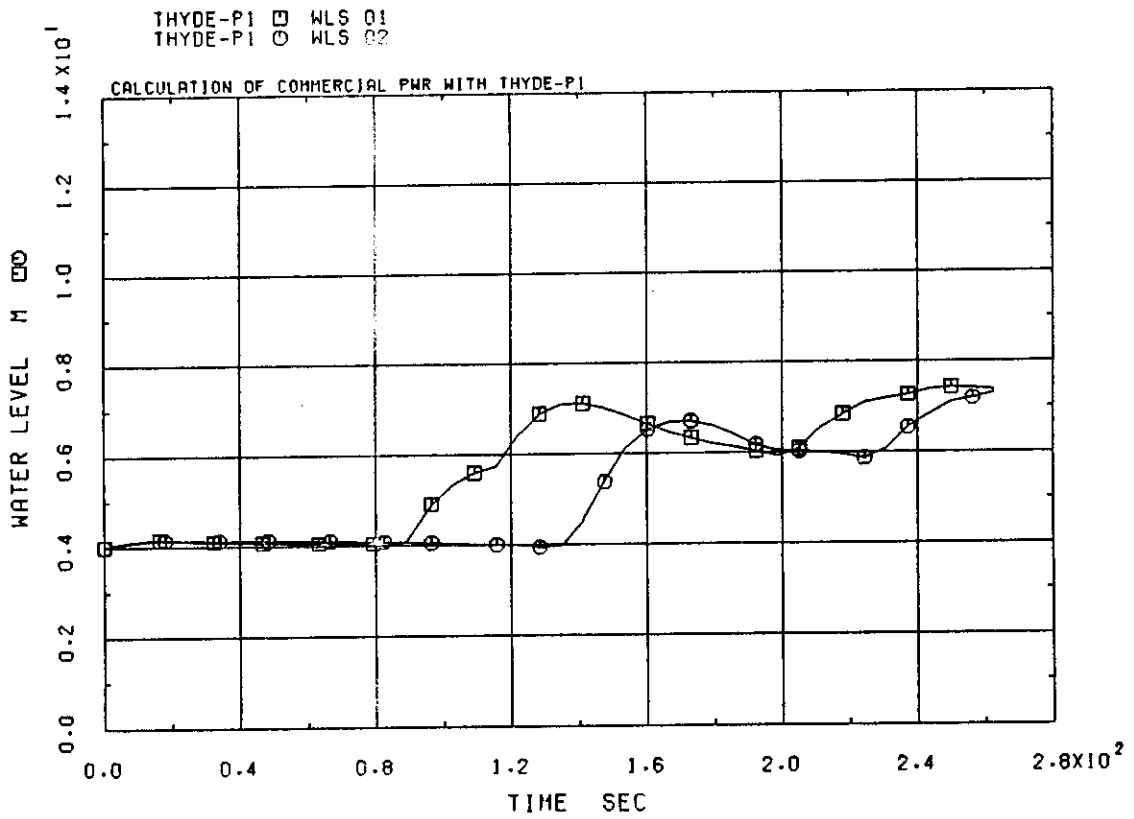


Fig.B-7-2 Water levels at SG secondary systems

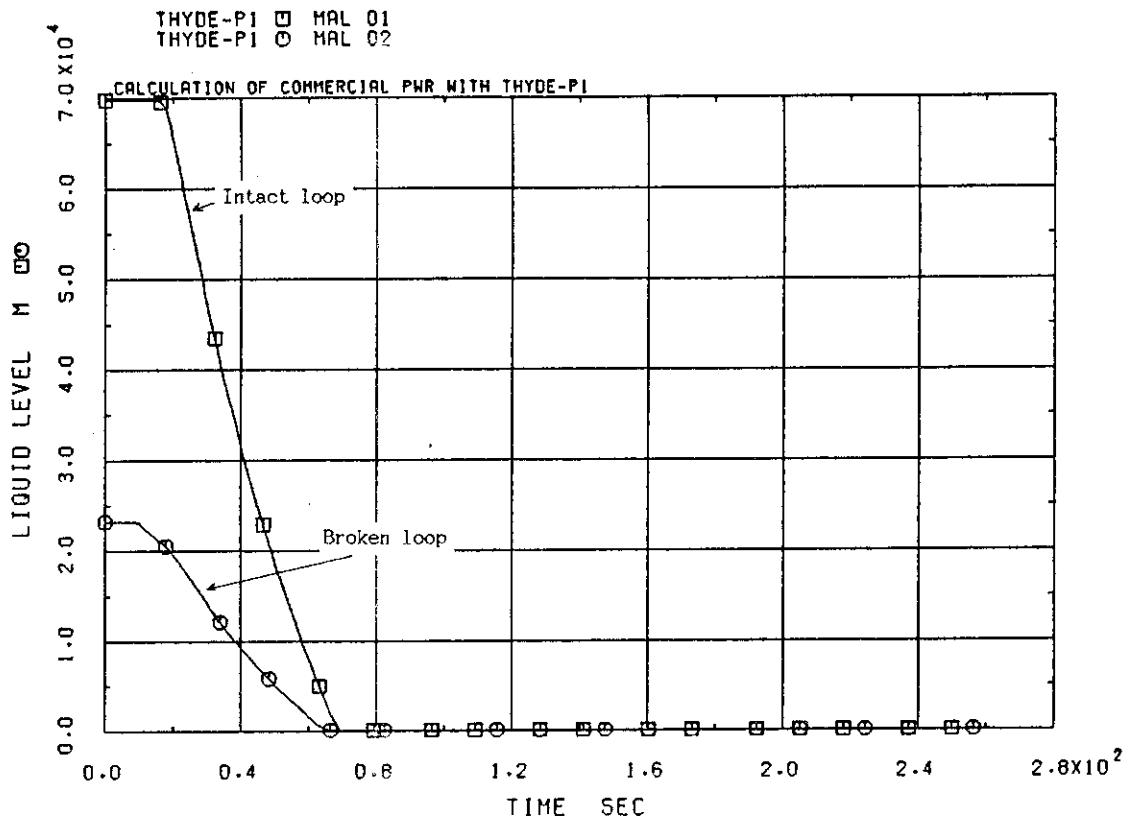


Fig.B-7-3 Accumulator water levels

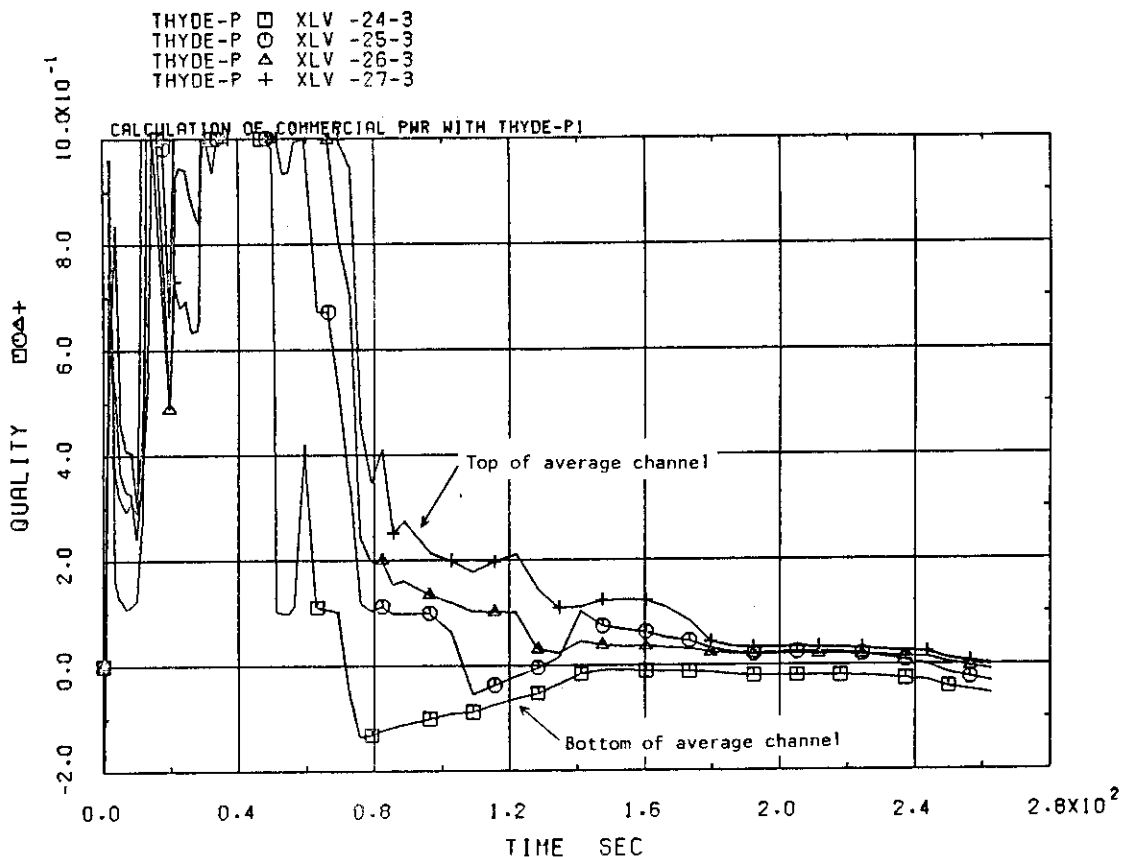


Fig.B-8-1 Equilibrium coolant qualities at average channel

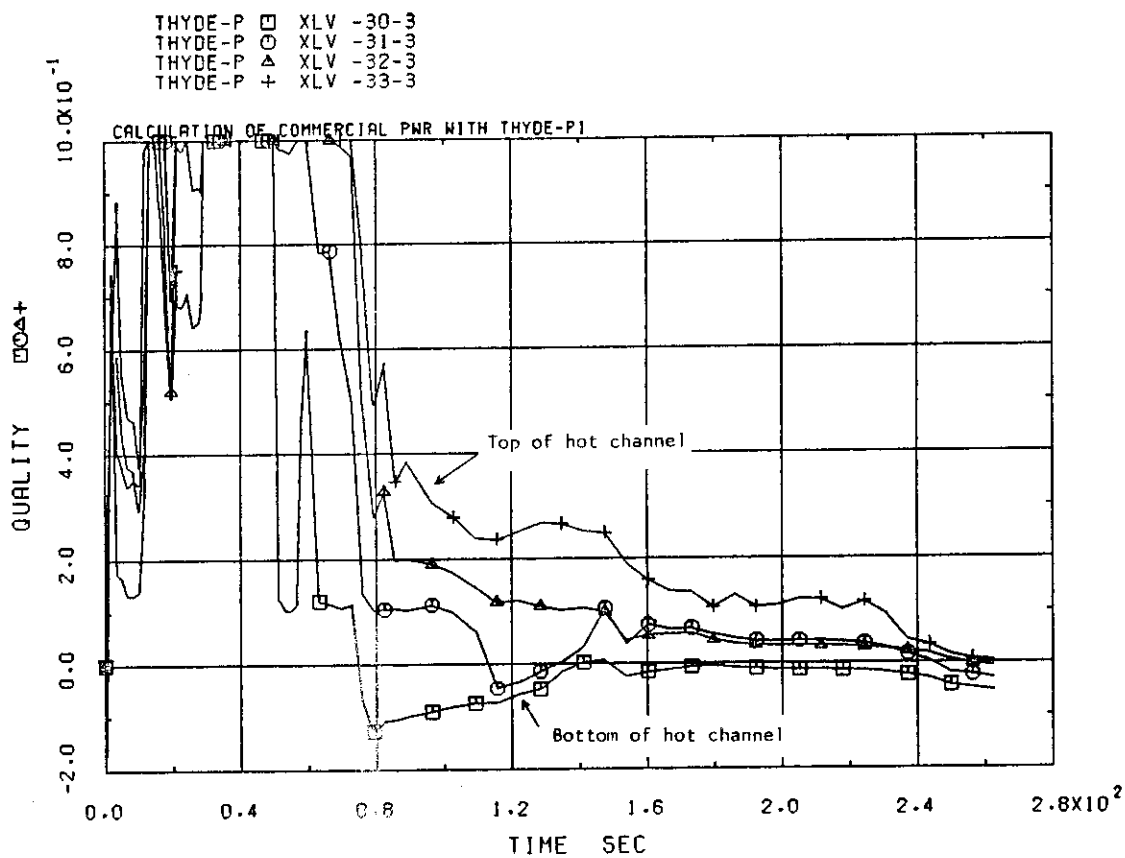


Fig.B-8-2 Equilibrium coolant qualities at hot channel

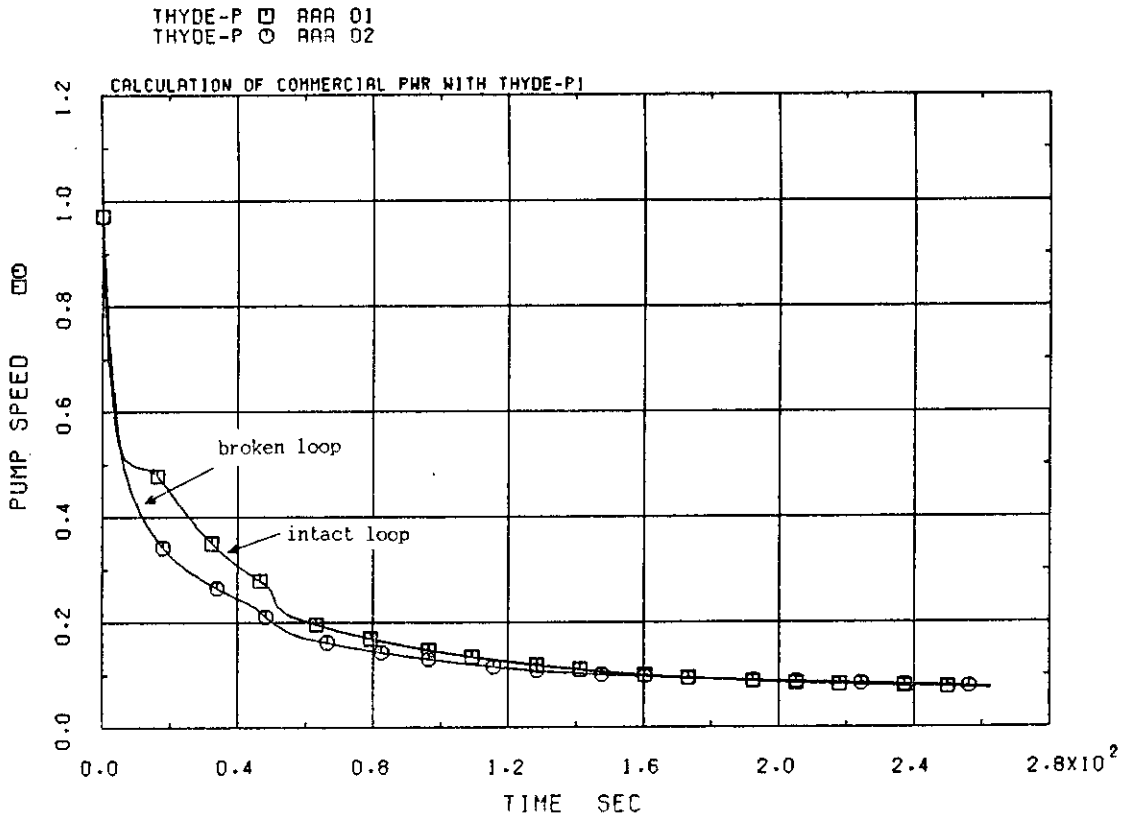


Fig.B-9-1 Normalized pump speeds

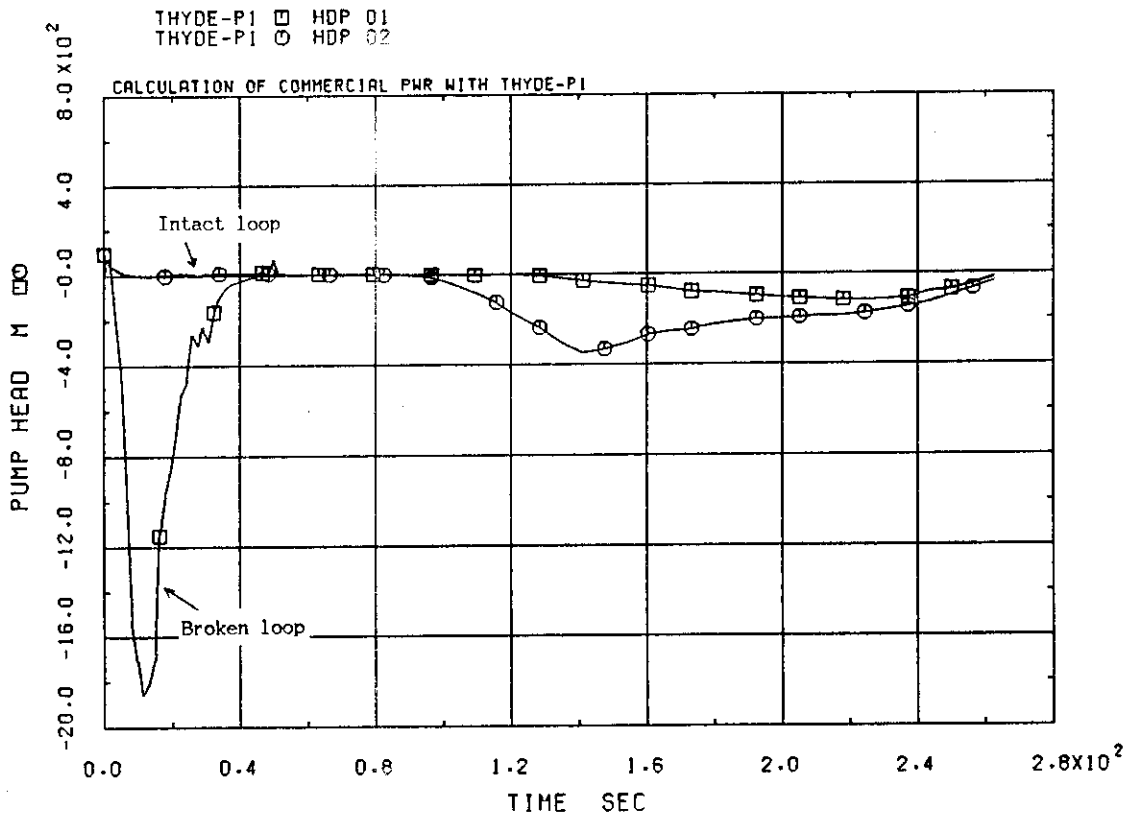


Fig.B-9-2 Pump heads

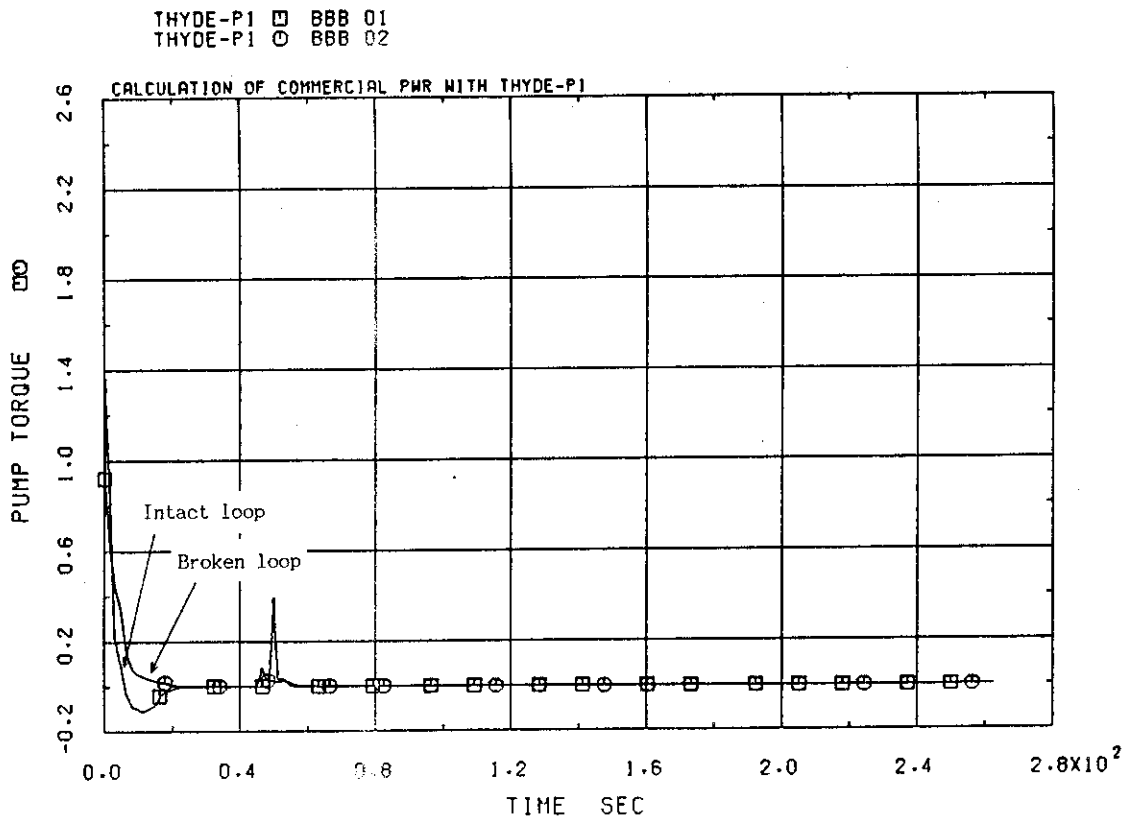


Fig.B-9-3 Normalized pump hydraulic torques

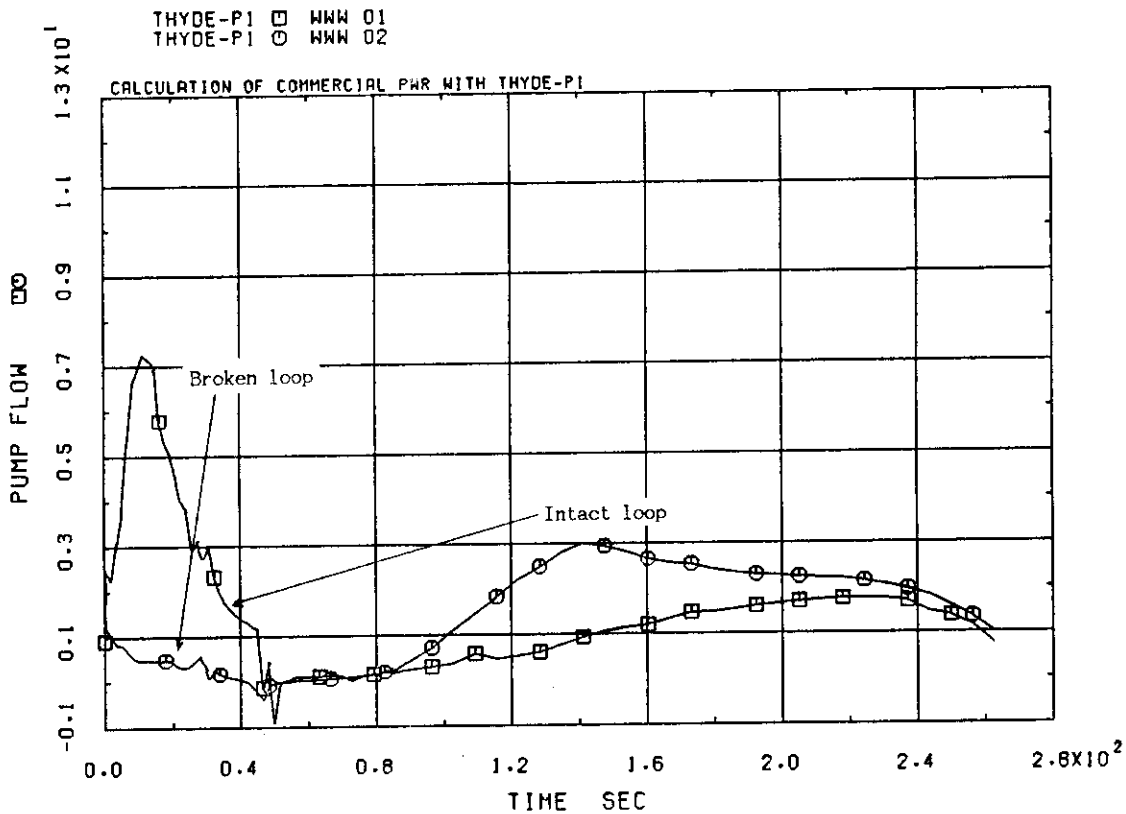


Fig.B-9-4 Normalized pump volumetric flows

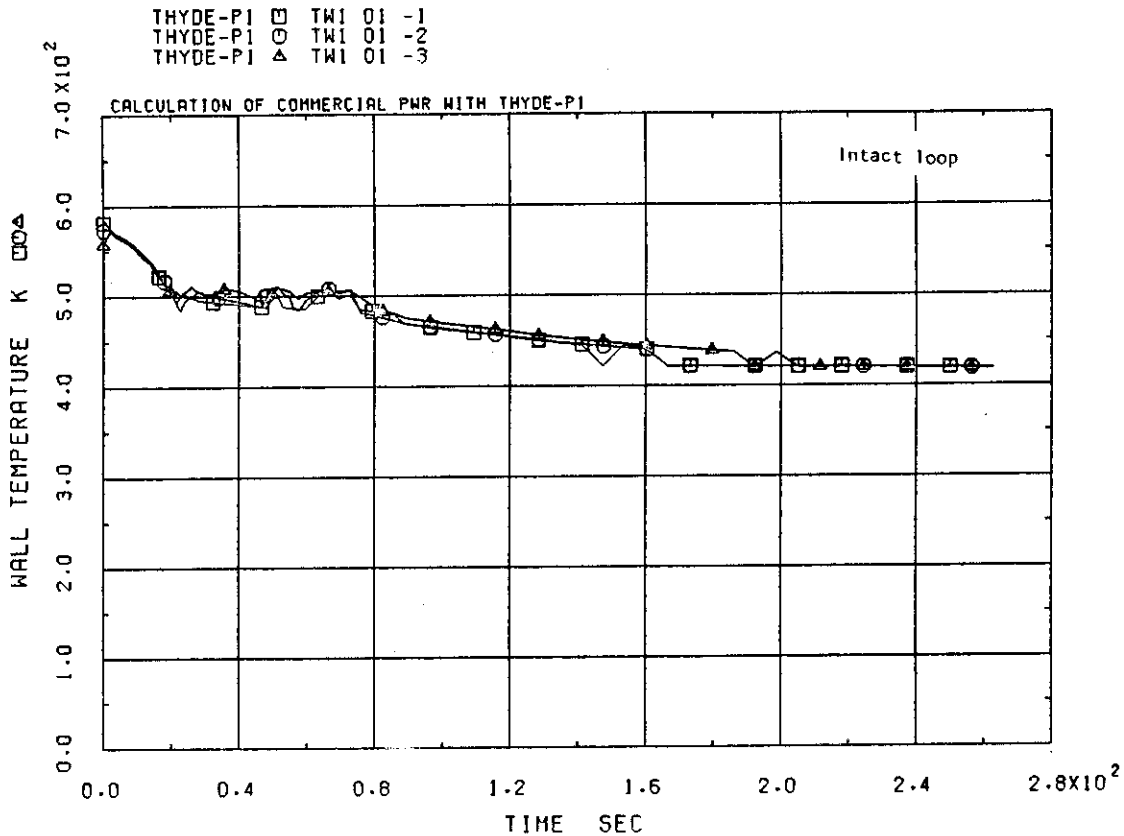


Fig.B-10-1 Wall temperatures at SG primary system of intact loop

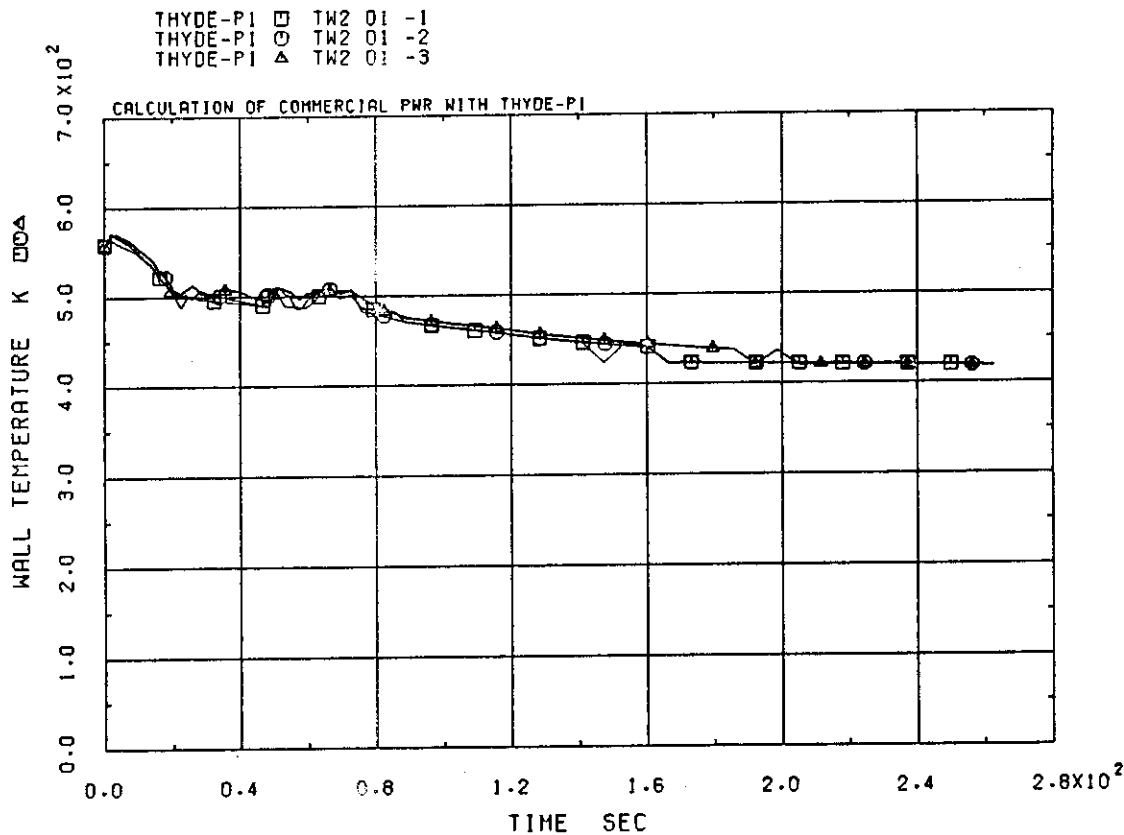


Fig.B-10-2 Wall temperatures at SG secondary system of intact loop

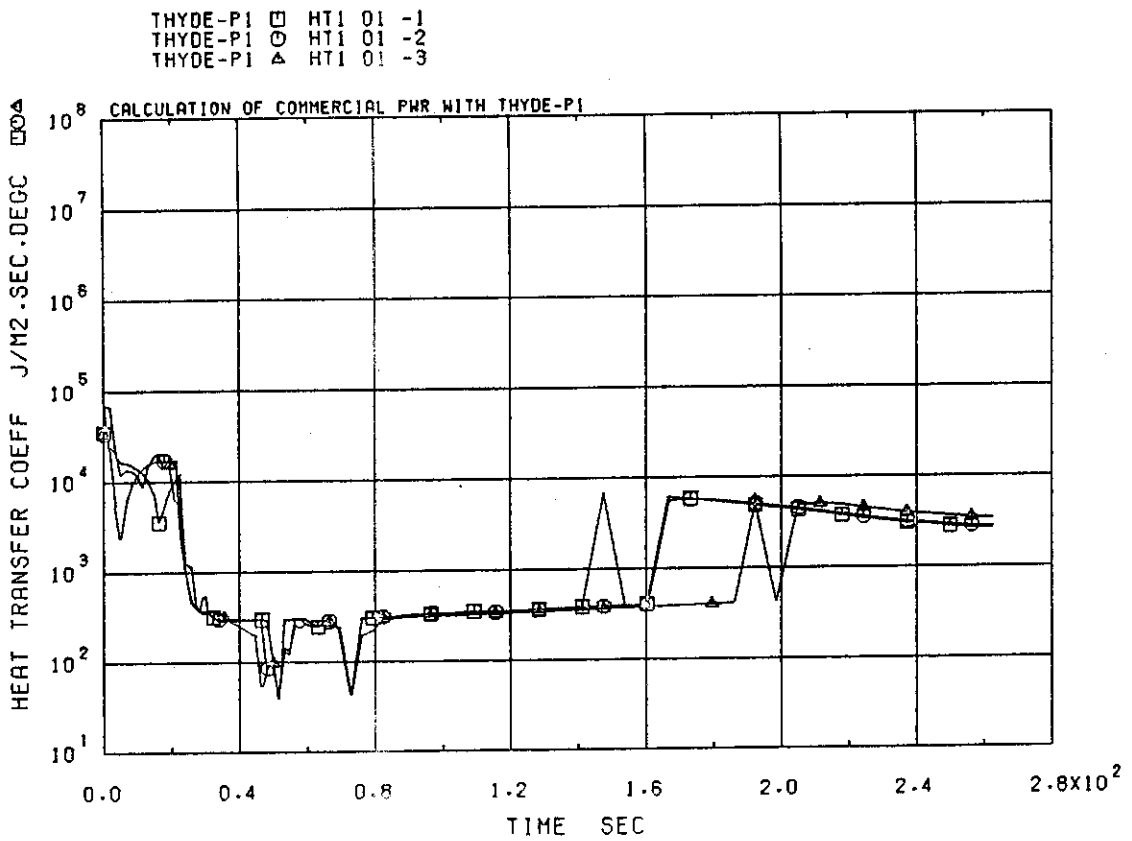


Fig.B-10-3 Heat transfer coefficients at SG primary system of intact loop

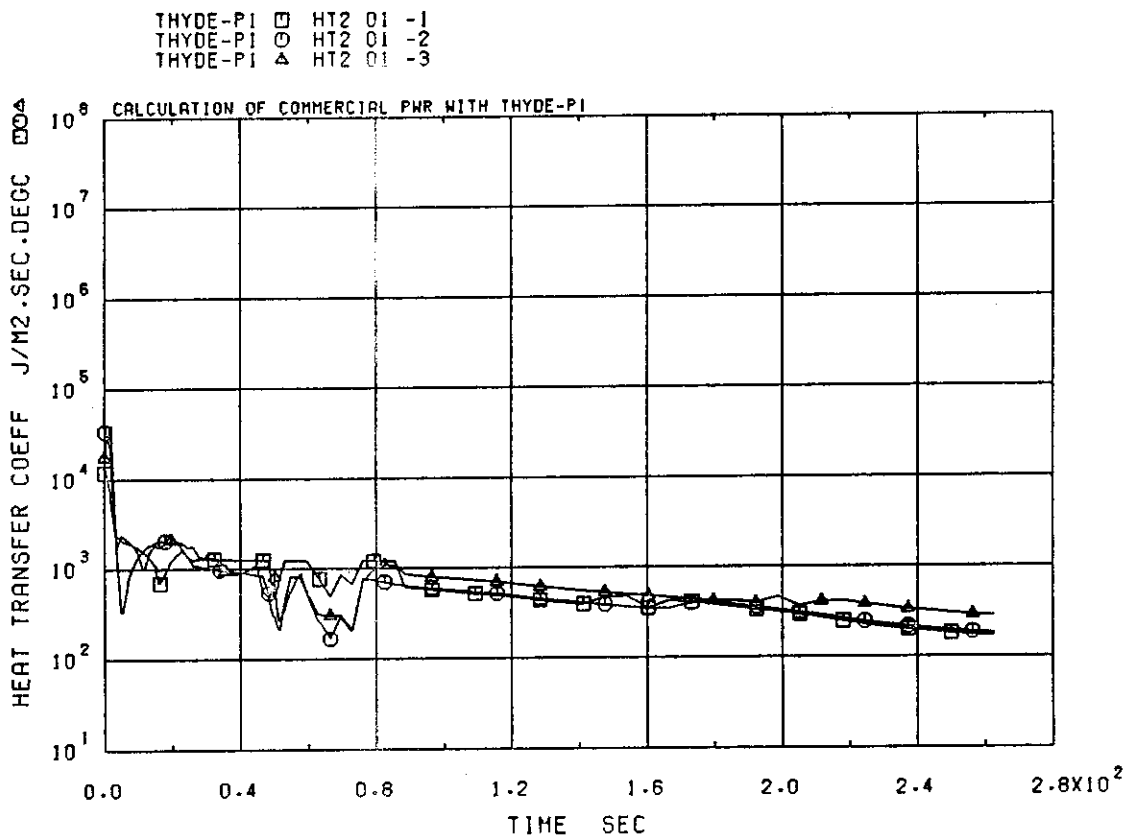


Fig.B-10-4 Heat transfer coefficients at SG secondary system of intact loop

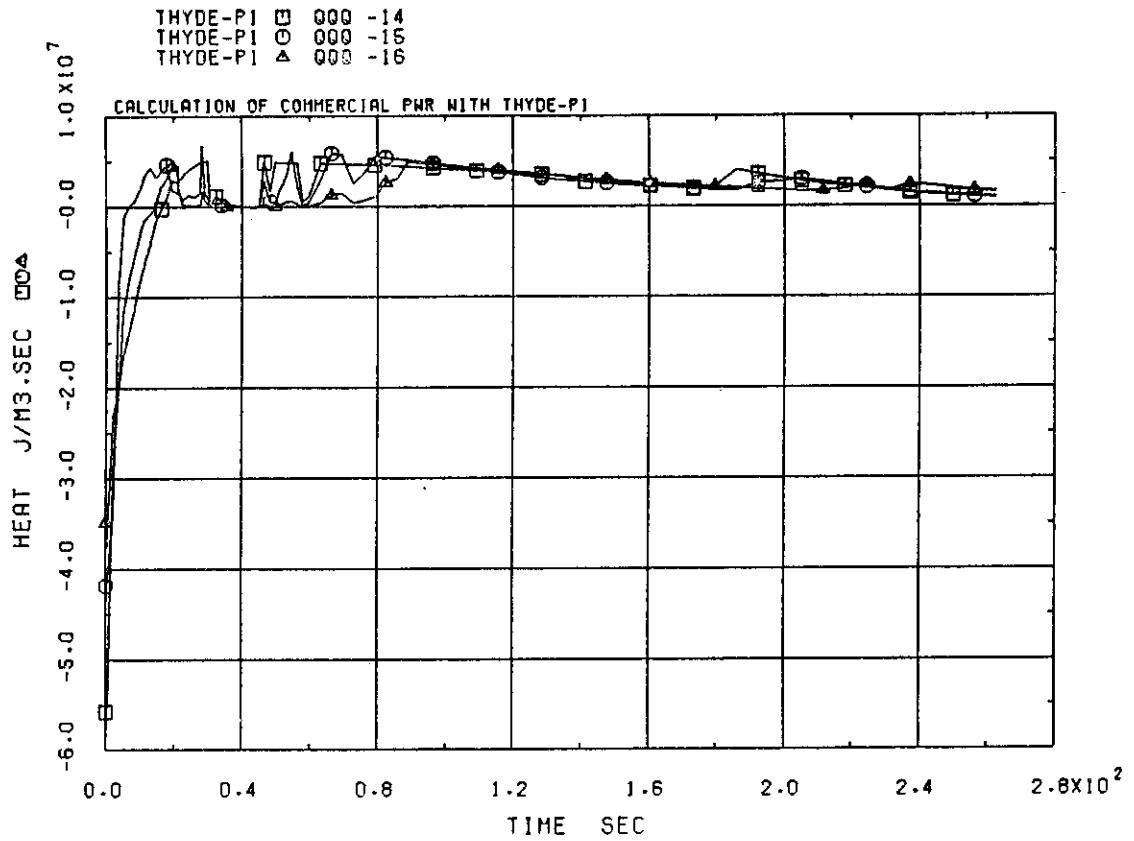


Fig.B-10-5 Heat inputs to coolant per unit volume at SG of intact loop

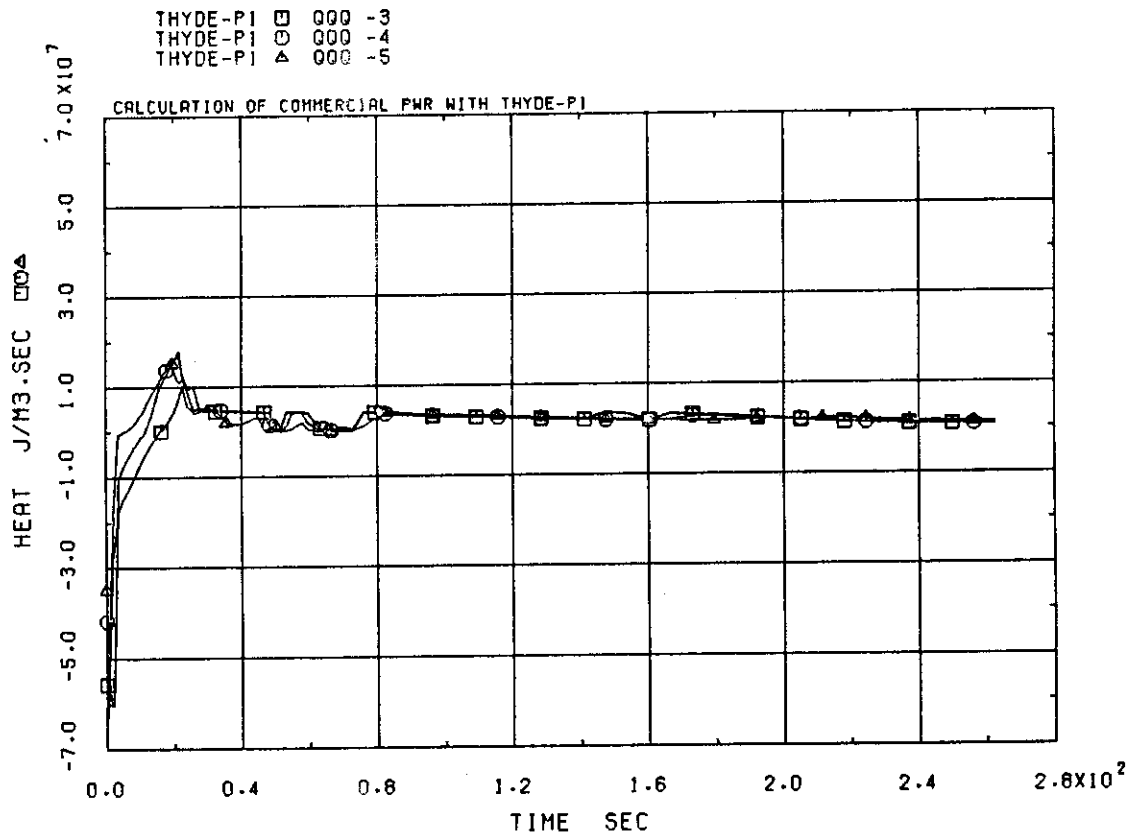


Fig.B-10-6 Heat inputs to coolant per unit volume at SG of broken loop