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ASSESSMENT OF THE THYDE-BI /MOD O  
CODE WITH DATA FROM ROSA-III  
LOSS-OF-COOLANT EXPERIMENTS

October 1984

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Assessment of the THYDE-B1/Mod 0 Code with  
Data from ROSA-III Loss-of-Coolant Experiments

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The calculational capability of the THYDE-B1 (Mod 0) computer code, a fast-running best-estimate code for prediction of thermal-hydraulic response of a boiling water reactor during a loss-of-coolant accident, was assessed against test data from ten runs of ROSA-III recirculation-line break tests, where break area was changed parametrically from 0 to 200%. The overall system response during these tests was well reproduced by the code, however, the detailed response was not reproduced correctly because of various simplified assumptions in the code, e.g., neglecting the core-spray cooling effects. Discrepancy between the calculated and measured responses was observed particularly for:

- (1) the time of initiation of steam discharge through the automatic depressurization system for small breaks (<5%),
- (2) in-vessel steam generation due to flashing of coolant and vaporization of emergency core cooling water for intermediate and large breaks ( $\geq 5\%$ ), and
- (3) rod surface heat transfer regimes for large breaks (>50%).

The calculation reproduced PCTs for the small breaks, but underpredicted PCTs for the intermediate breaks. The calculated rod temperature behaviors for the large breaks were qualitatively different from the data.

Keywords: BWR, LOCA, ECCS, ROSA-III, THYDE-B1, PCT, Break Size,  
Code Assessment

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\* On leave from Computer Service Co. (CSK)

ROSA-Ⅲ 冷却材喪失実験による THYDE-B1/Mod O コードの評価

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(1984年9月20日受理)

本報は、日本原子力研究所で開発された、沸騰水型原子炉の冷却材喪失事故時熱水力挙動の解析のための計算コード THYDE - B1 の性能評価に関するものである。ROSA - Ⅲ 実験装置による10ランの再循環ポンプ入口側配管破断実験(破断面積 = 0 ~ 200%)を THYDE - B1 コードで解析し、その結果を実験結果と比較することによりコードの性能評価を行った。

計算結果は、実験中の基本的な熱水力挙動を定性的に再現した。しかし、解析モデルが単純化されているため、以下の点について計算結果と実験結果の相違がみられた。(1) 小破断実験 (< 5%) における自動減圧系の動作時刻、(2) 中・大破断実験 ( $\geq 5\%$ ) における圧力容器内の減圧沸騰および ECC 水の沸騰による蒸気発生、および (3) 大破断実験 (> 50%) における被覆管表面伝熱様式。

被覆管最高温度 (PCT) は、小破断実験では良好に再現されたが、中破断実験では一般に過小評価された。大破断実験における被覆管表面温度の計算結果は、実験結果と定性的に異なる挙動を示した。

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## 1. Introduction

The Japan Atomic Energy Research Institute (JAERI) conducted the Rig of Safety Assessment (ROSA)-III program from April 1978 to March 1984 to investigate thermal-hydraulic response of a boiling water reactor (BWR) during a postulated loss-of-coolant accident (LOCA). A broad spectrum of accidental conditions were tested. These tests provided a significant data base for code assessment and development.

The ROSA-III facility was designed to simulate the BWR thermal-hydraulic response on real-time basis, however, several scaling compromises involved in the facility design may have limited the similarity between the ROSA-III and BWR thermal-hydraulic responses and hence limited applicability of the ROSA-III test results to an actual BWR. Such Scaling compromises included a half-length core, smaller-than-scaled initial core power, larger-than-scaled structure heat transfer area, and distorted downcomer/jet pump geometry.

The similarity between ROSA-III and the reference BWR has been investigated using computer codes. The approach taken has been either to compare analytical results obtained for BWR and ROSA-III, or to compare analytical results for BWR with ROSA-III test data.

The similarity for large (200%) and relatively small (5%) breaks has been investigated using the RELAP 4/Mod 6/U4/J3 code.<sup>(1)(2)</sup> This study concluded that ROSA-III well represented major BWR thermal-hydraulic responses.

The THYDE-B1 code<sup>(3)</sup> also has been used for the similarity study. The THYDE-B1 code is a fast-running code developed by JAERI for best-estimate calculation of BWR small- and intermediate-break LOCAs. The calculational capability of THYDE-B1 (Mod 0) has been assessed against ROSA-III test data obtained from a 5% break test (Run 804).<sup>(4)</sup>

This report documents an extensive assessment of the THYDE-B1 (Mod 0) code. Data obtained from ten ROSA-III tests where break area was changed parametrically from 0 to 200% are used. The assessment described herein provides a basis for, and defines limitation of, the ROSA-III/BWR similarity study to be made using the THYDE-B1 code.

In the following Sections, first the ROSA-III tests analyzed are outlined in Section 2. The computer code (THYDE-B1), models, and the analytical conditions are described in Section 3. Comparisons between the analytical results and ROSA-III test data are presented in Section 4. The conclusions are given in Section 5.

## 2. Test Description

### 2.1 ROSA-III Test Facility

The ROSA-III facility<sup>(5)</sup> was a volumetrically scaled (1/424) model of a General Electric BWR/6-251 (1100 MWe) system.<sup>(6)</sup> The outline of the facility is shown in Fig. 2.1. The major design characteristics of the ROSA-III facility and the reference BWR are compared in Table 2.1.

The test facility design objective was to represent, on a real-time basis, thermal-hydraulic performance of a BWR system during a postulated LOCA. Major BWR components which would influence LOCA/emergency core cooling (ECC) phenomena were represented. The represented components included a pressure vessel, vessel internals, two recirculation lines each with a simulated recirculation pump, a feedwater system, a main steam system and emergency core cooling systems (ECCS). The simulated pressure vessel (Fig. 2.2) modeled the lower plenum, the core bundles and bypass region, the upper plenum, the steam separator, the downcomer, and the steam dome. The volumes of these regions were scaled as correctly as practicable.

The ROSA-III core consisted of four half-length bundles. This core design enabled investigating the thermal-hydraulic interactions among the bundles, and was the basis for scaling of the test facility.

Each of the four core bundles comprised 62 electrically heated rods and two water rods spaced in a 8×8 square array as shown in Figs. 2.3 and 2.4. The prototypical rod diameter and array geometry were preserved. The axial power distribution along a heated rod was chopped-cosine with an axial peaking factor of 1.4 (Fig. 2.5). The power input to the simulated peak-power bundle (Bundle A) was 1.4 times as large as that to each of other bundles (Bundles B, C and D) which simulated average-power bundles. The radial power distribution within each bundle corresponded to a local peaking factor of 1.1.

Because of the half-length core, the steam generation rate per rod was one half of that in the reference BWR. Consequently, the upper tieplate flow area was reduced to one-half of the scaled area to approximately preserve the core exit counter-current flow limiting (CCFL) conditions.

The capacity of the core electric power supply was 4.24 MW, which was 47% of the volume-scaled (1/424) reference BWR rated core power.<sup>(6)</sup>

The jet pumps were located outside the pressure vessel, whereas the BWR jet pumps are located in the vessel downcomer. This was necessary to conserve the volume scaling and relative elevations of the jet pumps and downcomer.

The ECCS in the ROSA-III facility simulated the high pressure core spray system (HPCS), the low pressure core spray system (LPCS), the low pressure coolant injection system (LPCI) and the automatic depressurization system (ADS). The simulated ECC systems were designed to provide scaled ECC flow rates as functions of system pressure. The ADS, a backup system of HPCS, was simulated by a valve and a flow-limiting orifice in the simulated main steam line. The ECCS trip logics were identical to those of the reference BWR.<sup>(6)</sup>

The simulated main steam line had three branches as shown in Fig. 2.6. Only the first and second branches were used in the tests analyzed herein. The first branch had a control valve (CV-130) which was used to maintain the initial steady-state system pressure and also to simulate the operation of the pressure control system, the safety relief valves (SRVs) and the main steam isolation valves (MSIVs).

## 2.2 Test Conditions and Experimental Procedure

The test conditions of the ten tests analyzed in this report are summarized in Table 2.2. The tests<sup>(7)</sup> were conducted changing the break area parametrically; the tested break areas were 0, 1, 2, 5, 15, 25, 50, 75, 100, and 200% of the scaled (1/424) piping crosssectional area at the recirculation pump inlet line of the reference BWR. The 1% through 100% break tests simulated a split break at the recirculation pump inlet line. The 200% break test simulated a double-ended break at the same location. The 0% break test simulated a non-LOCA transient initiated by reactor scram without piping rupture.

The test initial conditions were almost identical for all the tests. The steam dome pressure was 7.35 MPa, corresponding to a saturation temperature of 562 K. The steady state core power was  $\sim 4$  MW, corresponding to a maximum linear heat rate (MLHR) of  $\sim 16.7$  kW/m.

The downcomer liquid level signals were used to trip closure of the MSIV and to actuate ECCS as is the case in the reference BWR. The downcomer initial liquid level was  $\sim 5.0$  m above the vessel bottom. With

this liquid level, the fluid volume in the downcomer was correctly scaled to the volume below the scram level (L3 level) in the reference BWR.<sup>(6)</sup> Similarly, the L2 and L1 levels in the ROSA-III downcomer were 4.76 and 4.25 m, respectively. The closure of MSIV was tripped by an L2-level signal with a time delay of 3 s. The LPCS, LPCI and ADS were actuated by an L1-level signal with delays of 40, 40 and 120 s, respectively. These time delays are those assumed in plant safety analyses.<sup>(6)</sup> The LPCS and LPCI injection pressures were 2.2 and 1.6 MPa, respectively.<sup>(6)</sup> The HPCS was assumed to be inactive. The failure of HPCS represents the severest single failure of ECCS.<sup>(8)</sup>

Reactor scram was assumed to occur at the time of break. However, as shown in Fig. 2.7, the initial core power ( $\sim 44\%$  of the scaled BWR rated power) was maintained for approximately 9 s after the break, when the core power per unit fluid volume matched with that of the reference BWR.<sup>(6)</sup>

Recirculation pumps were tripped off at the time of break.

The feedwater line valve was throttled from 2 s after the break until it was closed completely at 4 s.

The control valve CV-130 in the main steam line was manually opened full at the time of break. This increased steam discharge flow rate to  $\sim 15\%$  above the initial value. Then CV-130 was automatically throttled to simulate the operation of the pressure control system which is designed to maintain the system pressure above 6.7 MPa. The valve CV-130 was automatically closed from 3 s after the generation of an L2-level signal to simulate the MSIV closure. Thereafter, CV-130 also simulated SRVs by maintaining the system pressure below 8.1 MPa. The simulated ADS valve, AV-169, was opened at 120 s after the generation of an L1-level signal.

## 2.3 Test Results

The system pressure transients, measured in the steam dome, are shown in Fig. 2.8 for all the ten tests with break areas ranging from 0 to 200%. The system initially depressurized due to discharge through the break and main steam line. The initial depressurization was arrested at 6.7 MPa for the breaks  $\leq 5\%$  by the operation of the simulated pressure control system. The system repressurized after the simulated MSIV closure, which was tripped by an L2-level signal with a time delay of

3 s. For the breaks  $\geq 15\%$ , MSIV closed before the system pressure decreased to the pressure control system's setpoint of 6.7 MPa. The simulated SRV opened for breaks  $\leq 5\%$  as system pressure exceeded the setpoint of 8.1 MPa.

For the small breaks ( $< 5\%$ ), system depressurization started again when ADS was actuated by an L1-level signal. For the large and intermediate breaks ( $\geq 5\%$ ), system depressurization started again when the inlet of the broken recirculation line open to the downcomer was uncovered and steam began to leak from the break.

The in-vessel two-phase mixture levels measured by conductivity probes are shown in Figs. 2.9 and 2.10 for the 1% and 100% breaks, respectively. The system pressure and cladding temperatures along a peak-power rod are also shown for comparison. For the 100% break test, the downcome mixture level began to drop immediately after the break, and the level inside the shroud followed this. However, for the 1% break the downcomer mixture level stayed above the highest probe elevation (3.325 m) throughout the test.

The lower plenum fluid initiated to flash to steam when the system pressure decreased to 6.4 MPa, approximately the saturation pressure at the lower plenum fluid initial temperature. The lower plenum flashing (LPF) temporarily raised core mixture level and thus terminated the early dryout in the upper core region (see Fig. 2.10(c)).

The core mixture level decreased and the whole core was exposed eventually to steam environment as the surge of LPF weakened. The rod surface dryout and resultant temperature excursion propagated from the top to bottom of the core, as the core mixture level receded (see Figs. 2.9(c) and 2.10(c)).

The low pressure core spray system (LPCS) and the low pressure coolant injection system (LPCI) operated at system pressures below 2.2 and 1.6 MPa, respectively. The LPCS sprayed water on the top of the core. The LPCI injected water into the core bypass region.

For the breaks  $\leq 1\%$ , the whole core was reflooded by LPCS alone, before the initiation of the LPCI flow. For larger breaks ( $\geq 2\%$ ), reflooding of the whole core occurred only after the initiation of the LPCI flow. The difference between the core mixture levels in the average-power and peak-power channels was generally small.

After the LPCS flow initiated at a system pressure of  $\sim 2.2$  MPa, the system depressurization became slower because the injection of LPCS

water onto the top of the core augmented in-vessel steam generation.

Approximately at the LPCS injection pressure of 2.2 MPa, fluid in the feedwater line began to flash. This was known from two-phase inflow detected by a flowmeter in the feedwater line. The feedwater line flashing (FLF), together with the in-vessel steam generation due to the vaporization of LPCS water, slowed the system depressurization, and therefore delayed the initiation of the LPCI flow. It is interesting to note that the core emptying was temporarily accelerated when the system depressurization rate decreased after the initiation of the LPCS flow and FLF, probably because of decrease in the steam generation rate in the mixture region.

The heater rod surface temperature was measured at seven elevations (Positions 1 through 7) indicated in Fig. 2.5. The rod surface temperatures showed clear correspondence with the core mixture level behavior as shown in Figs. 2.9(c) and 2.10(c). Namely, temperature excursion occurred as the rod surface was dried out, and was terminated as the rod surface was reflooded. The exceptions were temperatures at upper core elevations where, particularly for the smaller breaks, temperature turnaround occurred due to the spray (LPCS) flow on the top of the core, before reflooding.

Figure 2.11 shows rod surface temperatures for all the ten tests. Temperatures at thermocouple locations where PCT occurred in each test are shown. The temperature behavior after the dryout is of particular interest. The effect of LPCS was pronounced for the breaks  $\leq 25\%$ , for which the rod surface heatup rate decreased shortly after the initiation of the LPCS flow.

Figure 2.12 summarizes the timings of major events in all the ten tests. The times of dryout (uncovering), reflooding and quenching at the location where PCT occurred in each test are shown. From this figure, the following observations are derived.

- (1) For the 0 and 1% breaks, PCT occurred immediately after the initiation of the LPCS flow. The PCT occurred at position 3 (353 mm above the core midplane) on a peak-power rod. The rod surface at position 3 was quenched under the effect of the top spray (LPCS) alone, before the mixture level reached that elevation.
- (2) For the 2 and 5% breaks, PCT occurred shortly before, or at the same time as, the initiation of the LPCI flow. The temperature turnaround occurred under the effect of LPCS alone, as the core power



decayed. The PCT occurred at position 4 (the core midplane). Quenching at that elevation occurred after the arrival of mixture level (reflooding) after the initiation of the LPCI flow.

- (3) For the larger breaks (15, 25, 50, 75, 100 and 200%), the temperature turn-around occurred after the initiation of the LPCI flow, due to reflooding. The effect of the top spray (LPCS) cooling became less and less pronounced as the break size was increased.

The measured PCTs, the times when the PCT occurred and the locations where the PCTs occurred are listed in Table 2.3. The PCTs occurred in all the test on peak-power rods (having a local peaking factor of 1.1) in the peak-power bundle.

Table 2.1 Primary characteristics of BWR/6 and ROSA-III

	BWR*	ROSA-III	BWR/ROSA-III
Number of Recirc. Lines	2	2	1
Number of Jet Pumps	24	4	6
Number of Separators	251	1	251
Number of Fuel Assemblies	848	4	212
Active Fuel Length (m)	3.76	1.88	2
Total Volume (m <sup>3</sup> )	621	1.42	437
Power (MW)	3,800	4.40	864
Pressure (MPa)	7.23	7.23	1
Core Flow (kg/s)	1.54x10 <sup>4</sup>	36.4**	424
Recirculation Flow (l/s)	2,970	7.01**	424
Feedwater Flow (kg/s)	2,060	4.86**	424
Feedwater Temp. (K)	489	489	1

\* BWR/6-251

\*\* Maximum Rated

Table 2.2 Test Conditions

Break Area (%)	Tect ID.	Initial Conditions					Simulation of Pressure Control System	Date of Performance
		Core Power (MW)	Lower Plenum Subcooling (K)	Core Exit Quality (%)	Core Inlet Flow (kg/s)	Downcomer Collapsed Level (m)		
0	923	3.962	10.3	15.8	16.4	5.00	YES	81. 9.25
1	921	3.976	10.4	15.8	16.4	5.09	YES	81. 9.11
2	920	3.962	10.3	15.7	16.5	5.00	YES	81. 9. 4
5	922	3.962	10.5	15.8	16.4	5.00	YES	81. 9.18
15	913	3.964	11.1	14.7	16.4	5.00	NO	81. 5.28
25	930	3.960	10.1	16.3	16.1	5.04	YES	82. 2.18
50	916	3.963	10.8	14.3	16.5	5.05	NO	81. 6.18
75	929	3.966	10.3	16.0	16.2	5.05	YES	82. 2.12
100	914	3.972	11.3	14.5	16.2	5.03	NO	81. 6. 3
200	926	3.967	10.0	16.1	16.3	5.05	YES	81.10.29

Table 2.3 List of peak cladding temperatures

Break Area (%)	PCT (K)	Time (s)	Position	Rod
0	637	696	P3 <sup>a</sup>	A11
1	754	546	P3	A87
2	804	531	P4 <sup>b</sup>	A68
5	835	410	P4	A17
15	846	336	P4	A82
25	872	274	P4	A71
50	925	189	P4	A82
75	885	154	P4	A71
100	832	133	P4	A11
200	785	119	P4	A71

<sup>a</sup> 353 mm above the core midplane.

<sup>b</sup> core midplane.

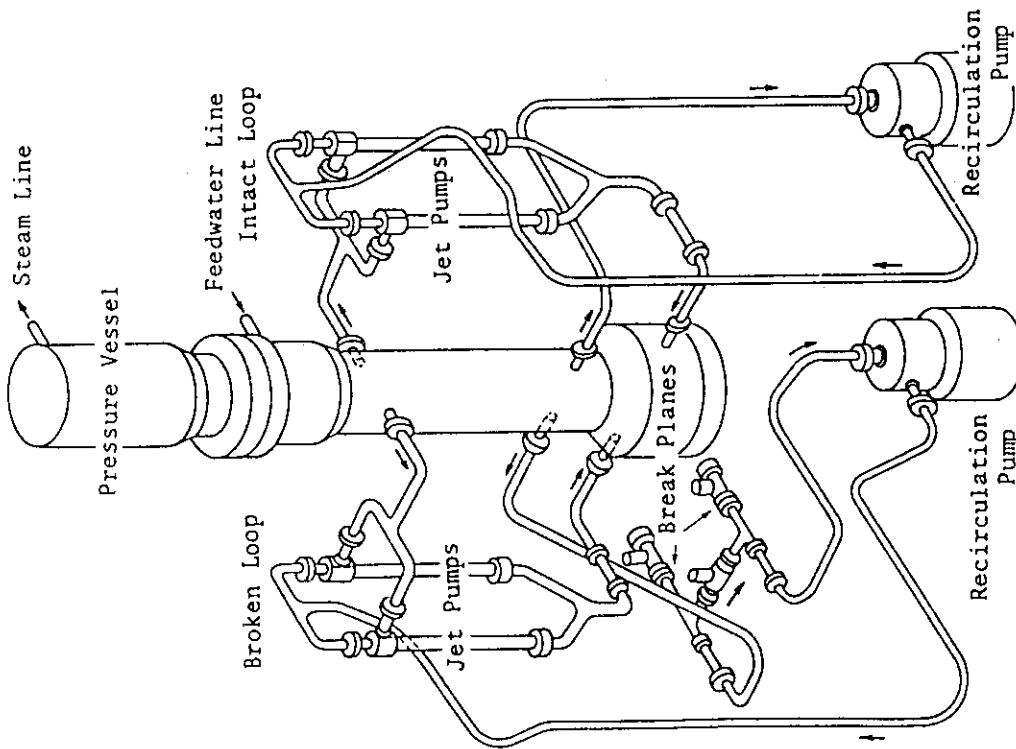
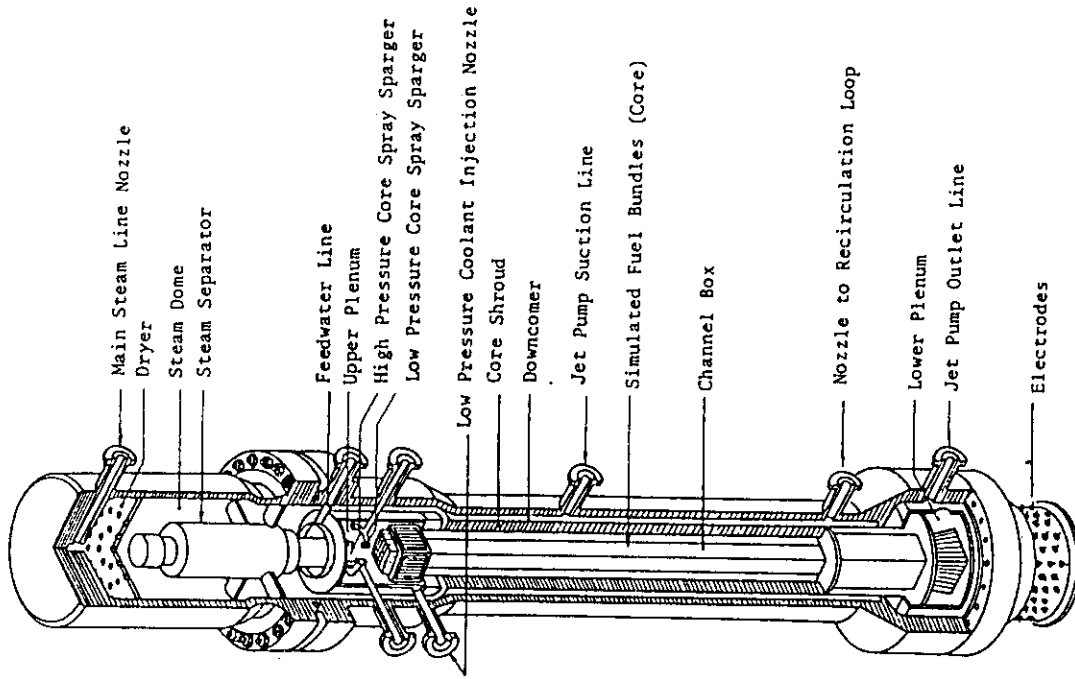


Fig. 2.1 Schematic Diagram of ROSA-III Test Facility

Fig. 2.2 Internal Structure of Pressure Vessel

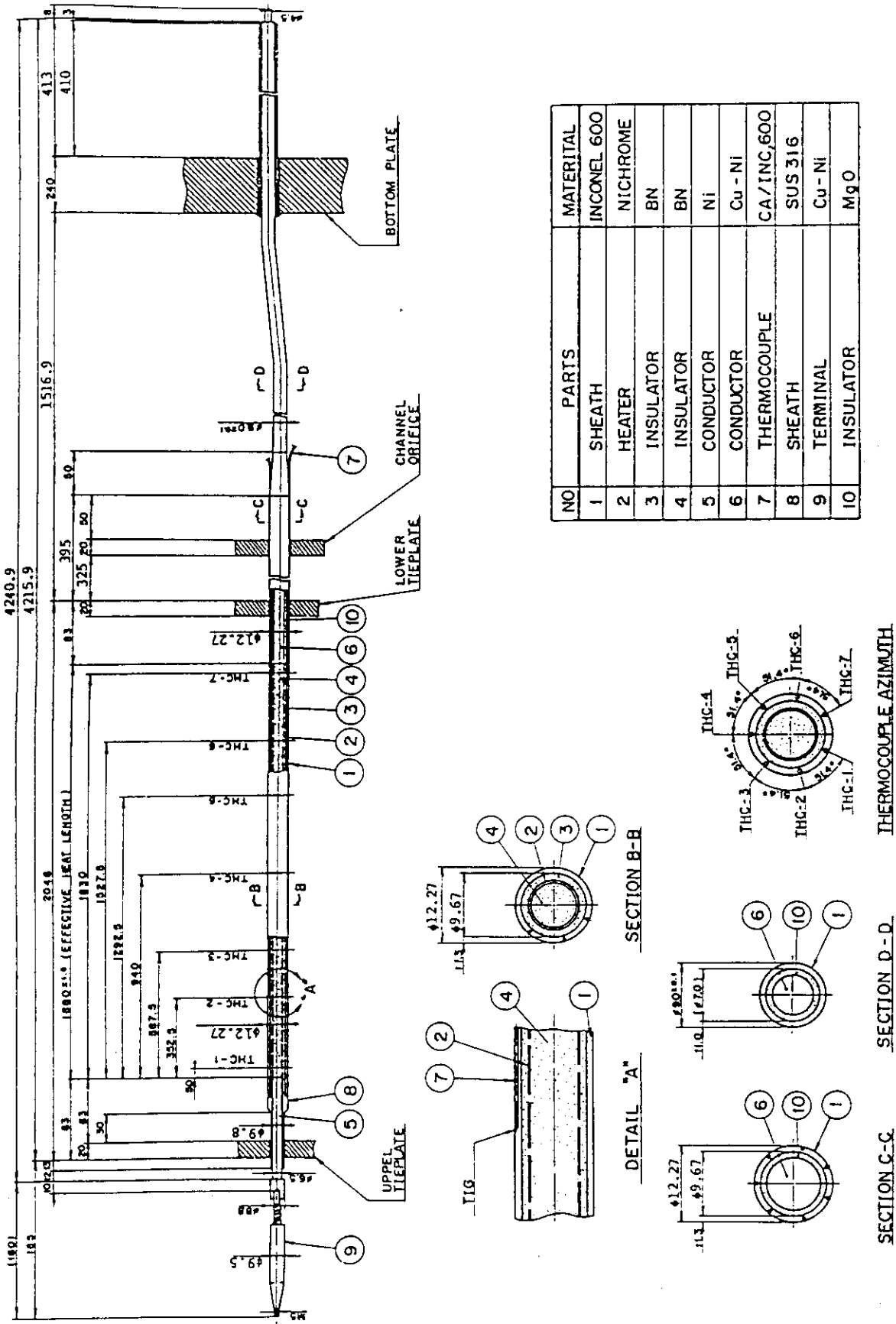
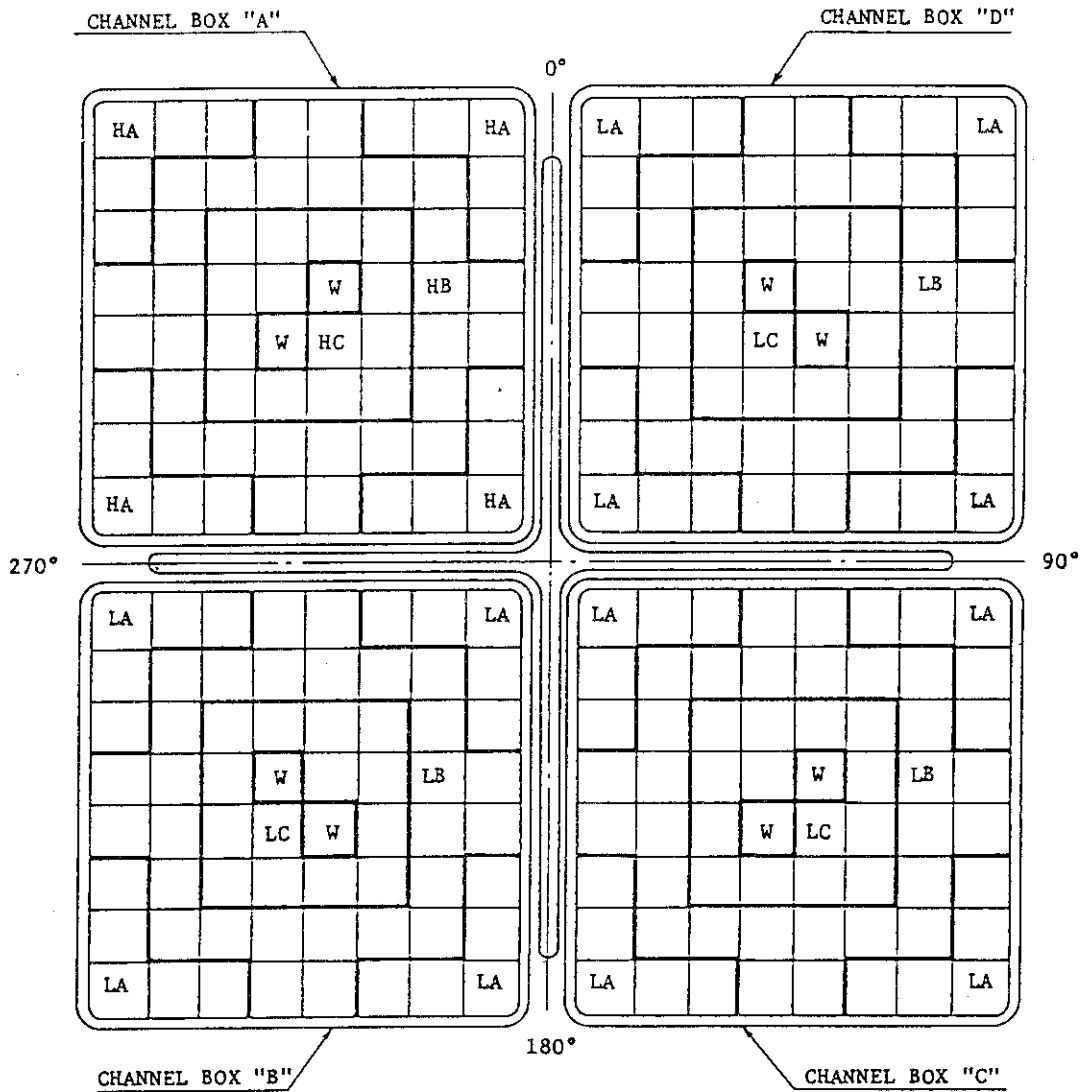


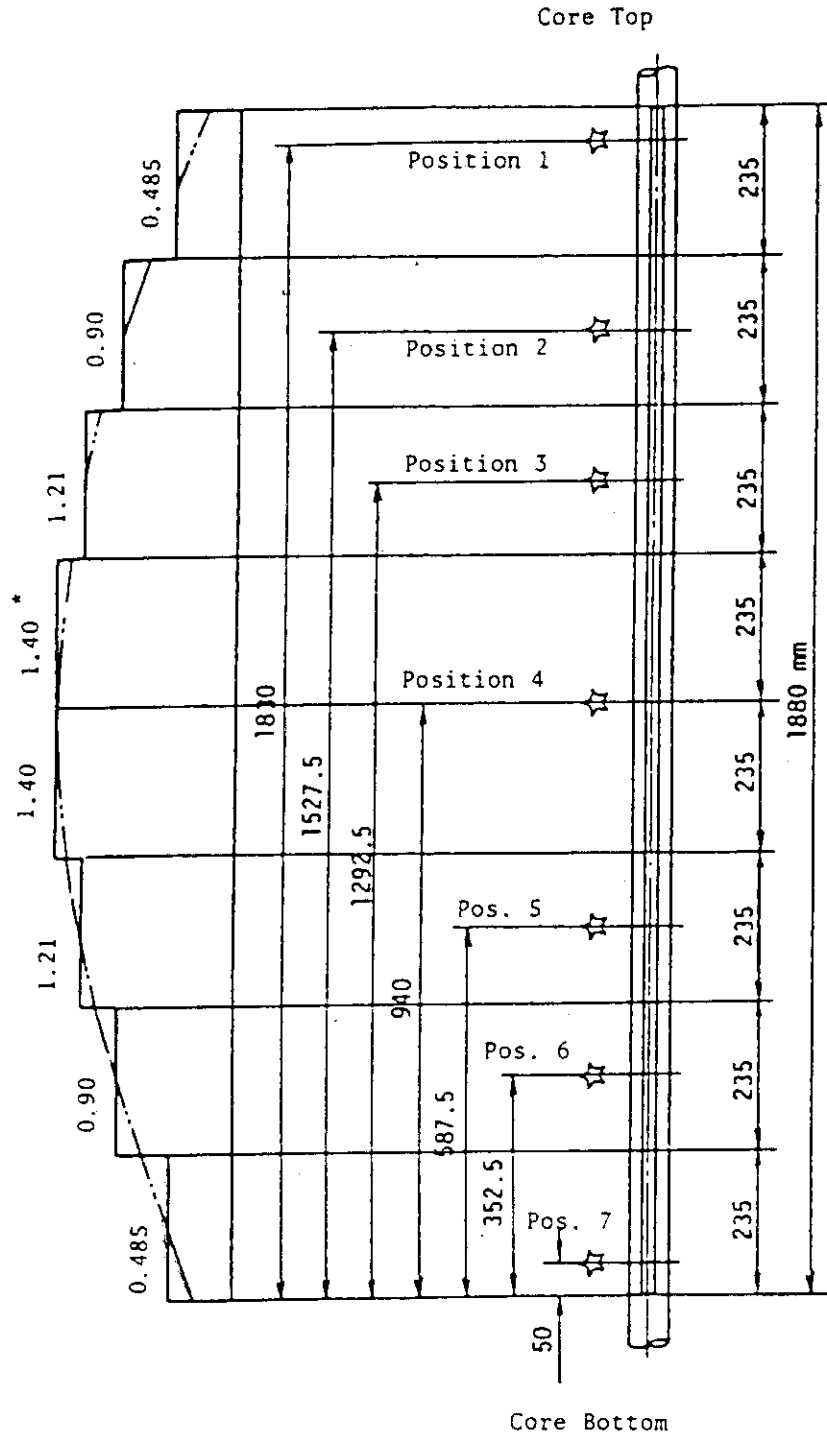
Fig. 2.3 Simulated fuel rod



Region	HA	HB	HC	LA	LB	LC	W
Linear Heat Rate (kW/m)	18.5	16.81	14.41	13.21	12.01	10.29	0.0
Local peaking factor	1.1	1.0	0.875	1.1	1.0	0.875	0.0
No. of Rods	20	28	14	60	84	42	8

\* note : Radial peaking factor is 1.4

Fig. 2.4 Radial core power distribution



☆ Indicates position of thermocouple. \* Axial Peaking Factor

Fig. 2.5 Axial power distribution along heater rod

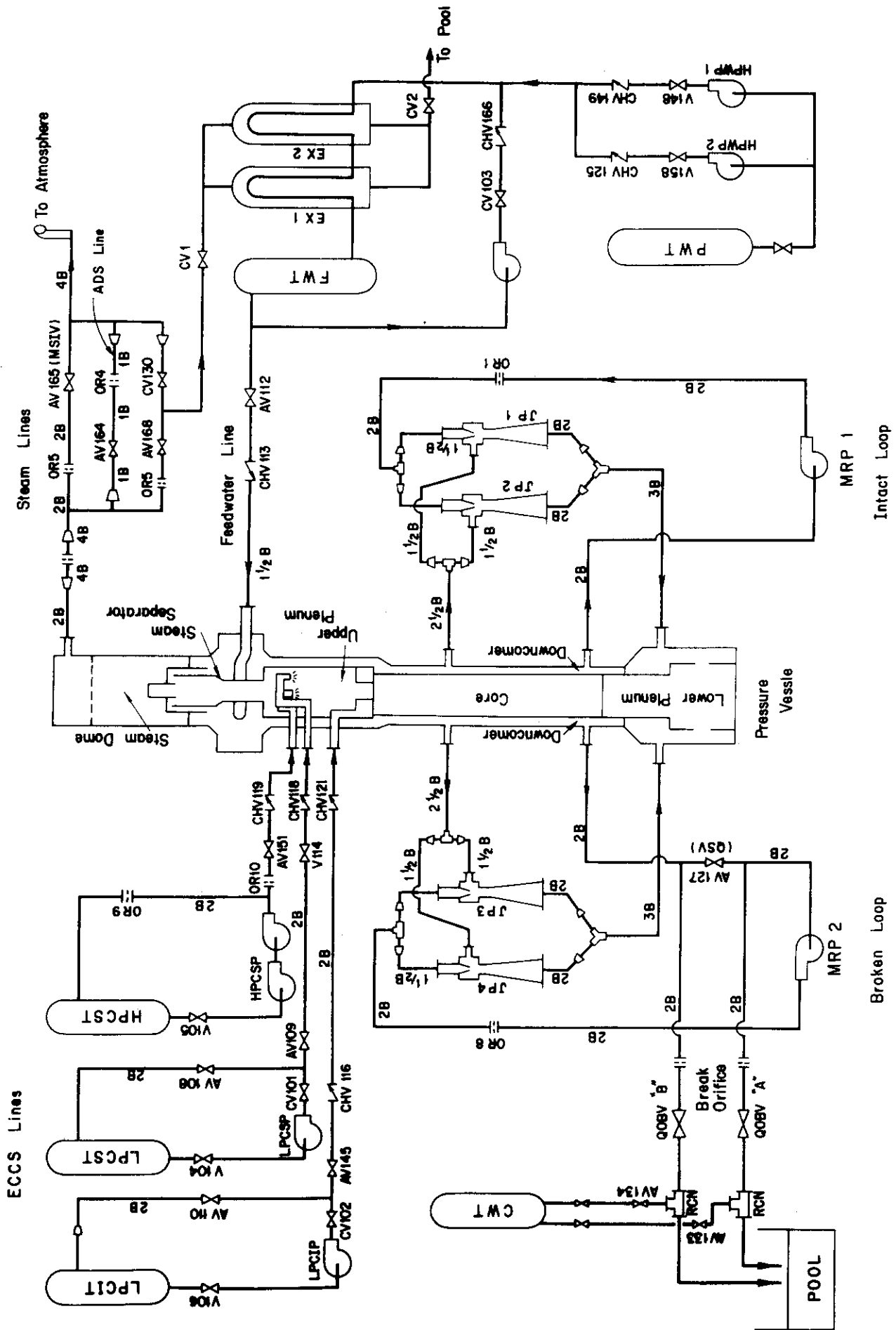


Fig. 2.6 Test facility flow diagram



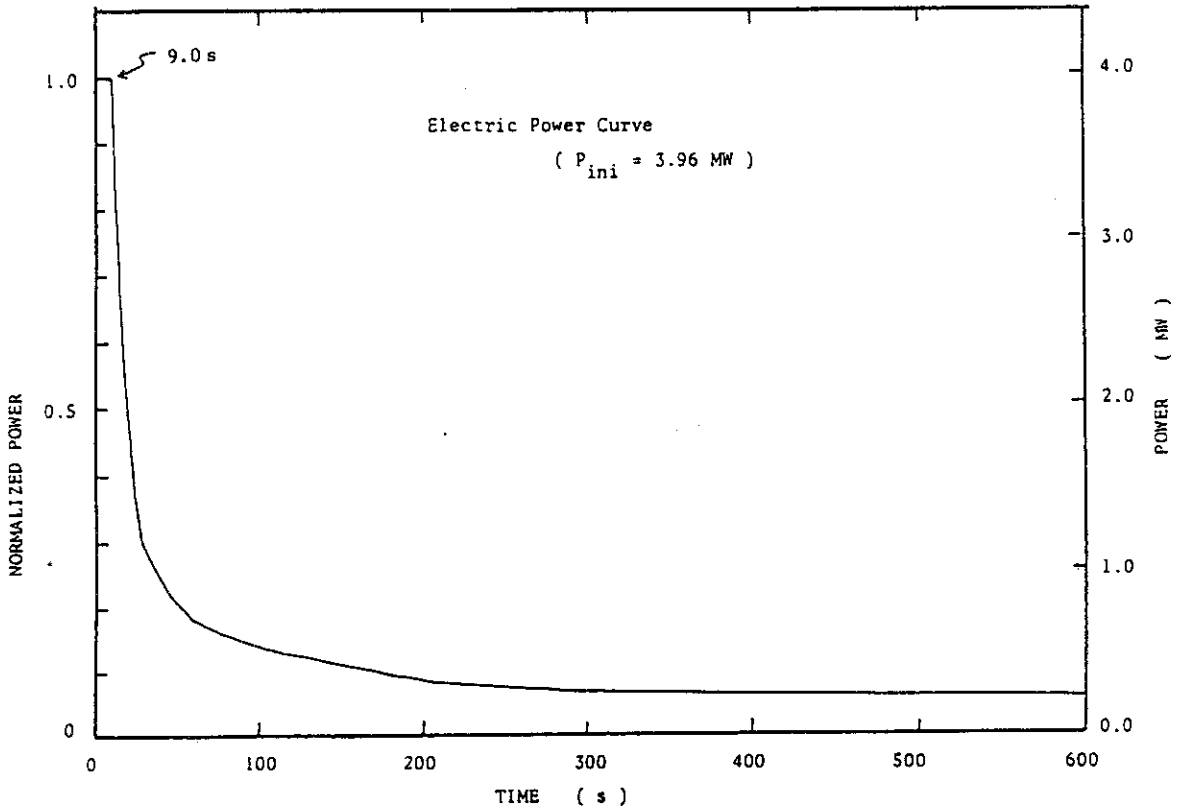


Fig. 2.7 Normalized core power transient

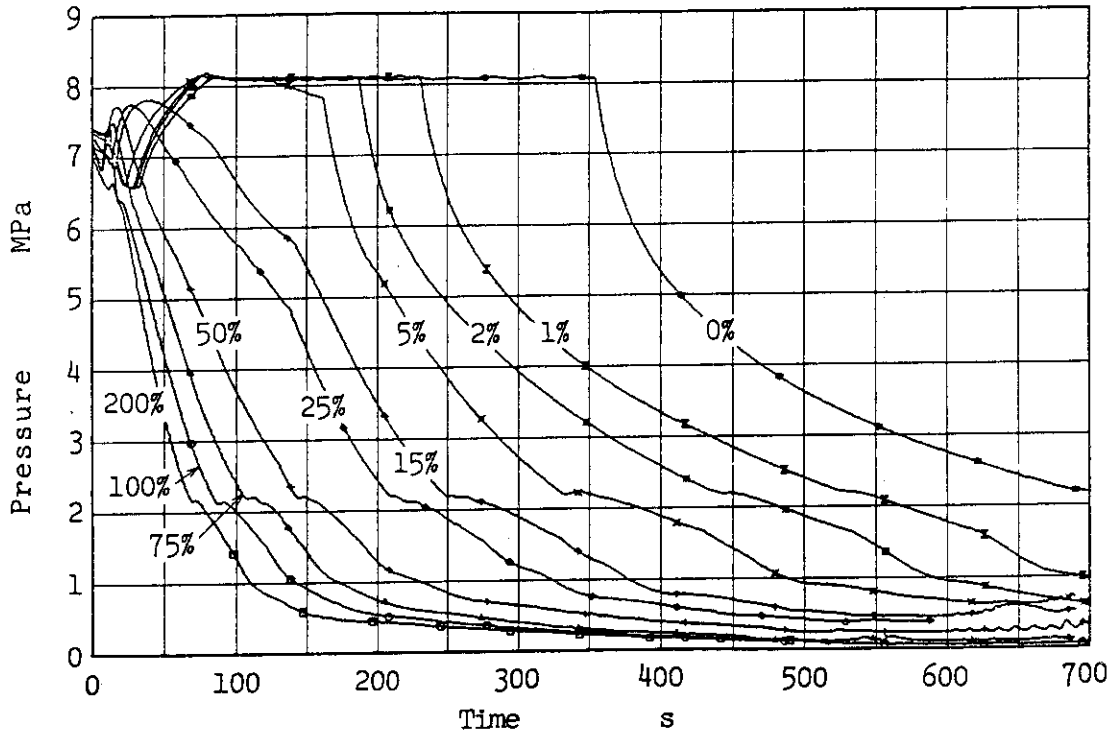


Fig. 2.8 Measured system pressures for all tests

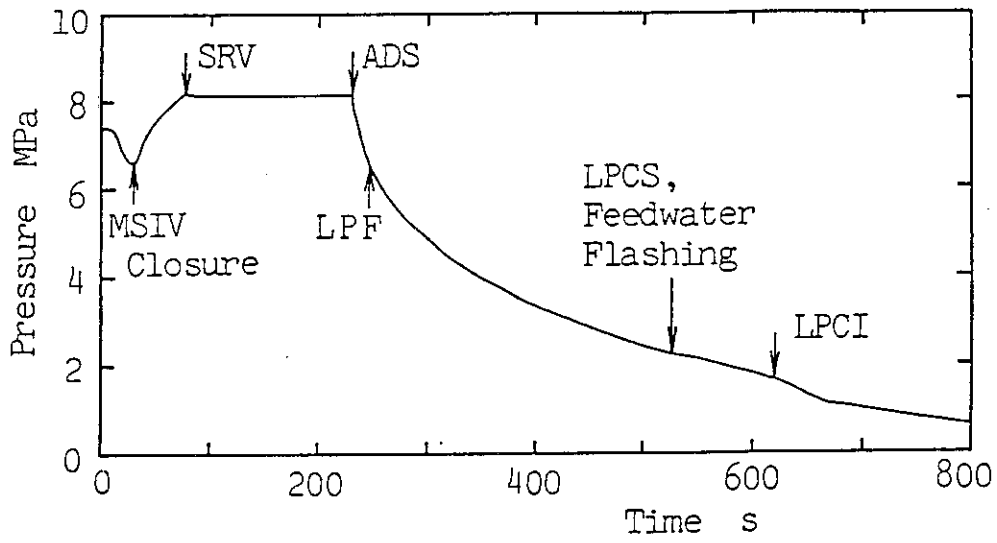


Fig. 2.9(a) Measured system pressure - 1 % break test

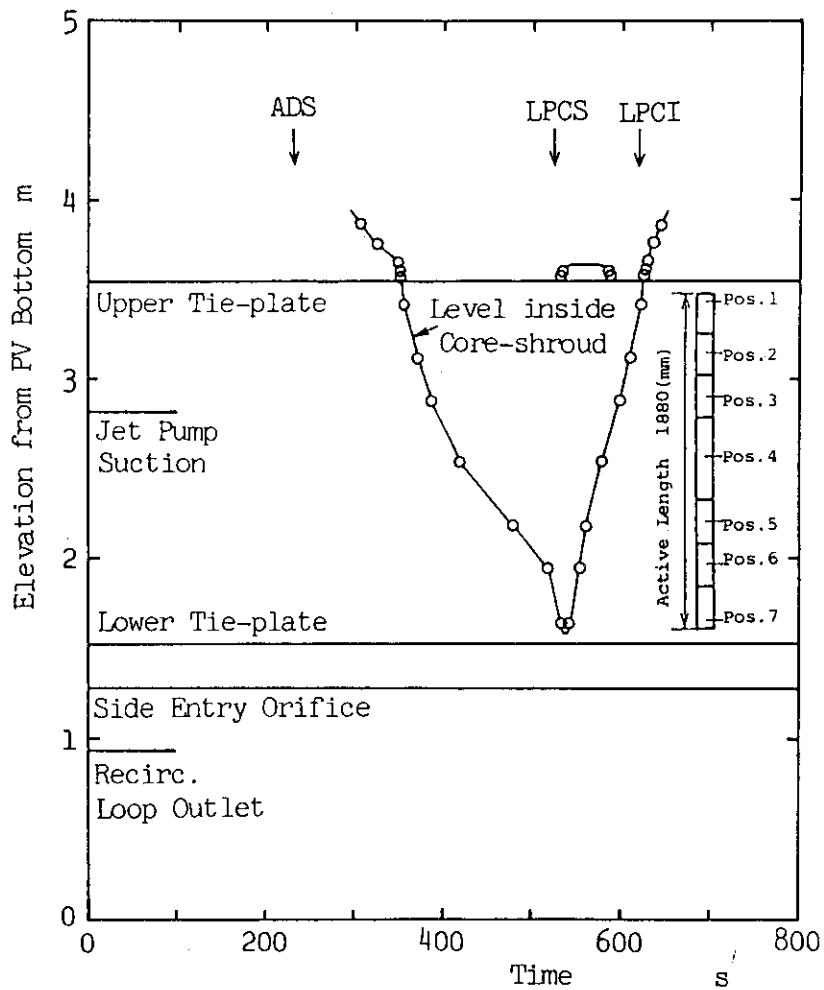


Fig. 2.9(b) Measured core mixture level - 1 % break test

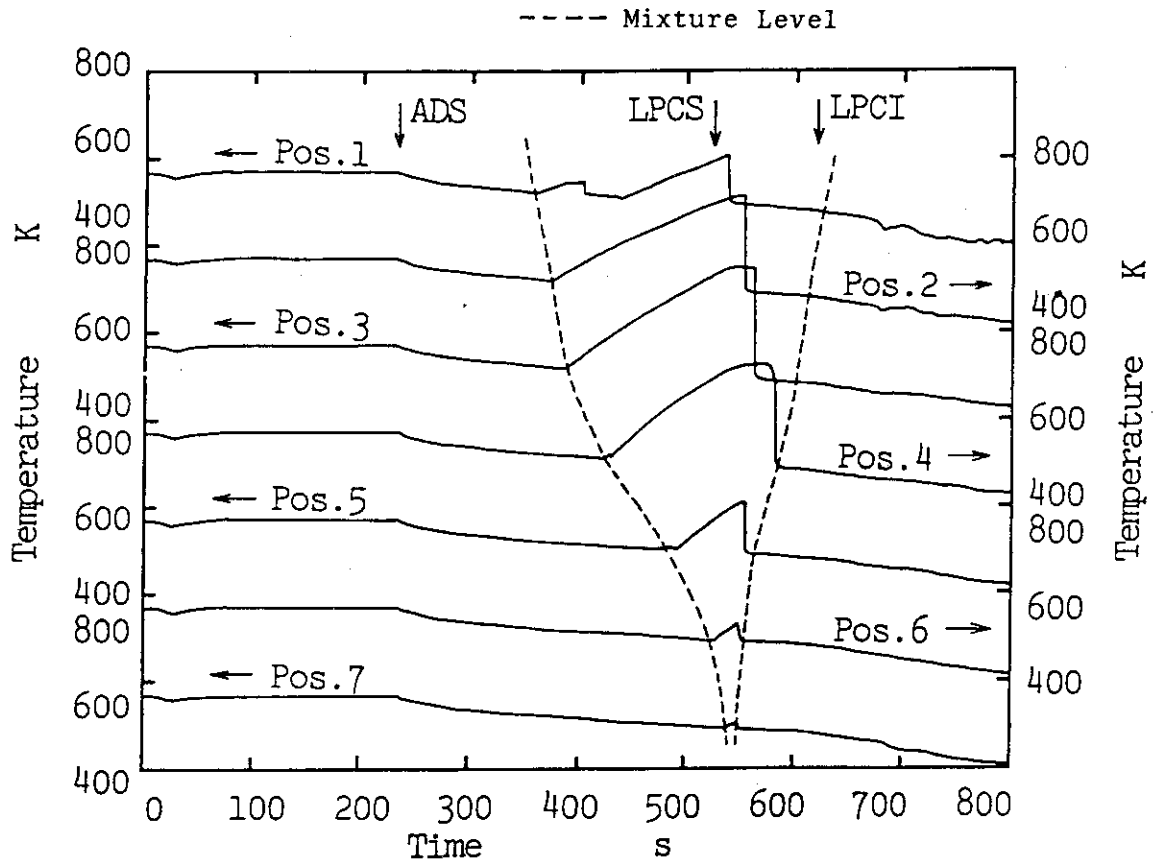


Fig. 2.9(c) Measured peak-power rod temperatures - 1 % break test

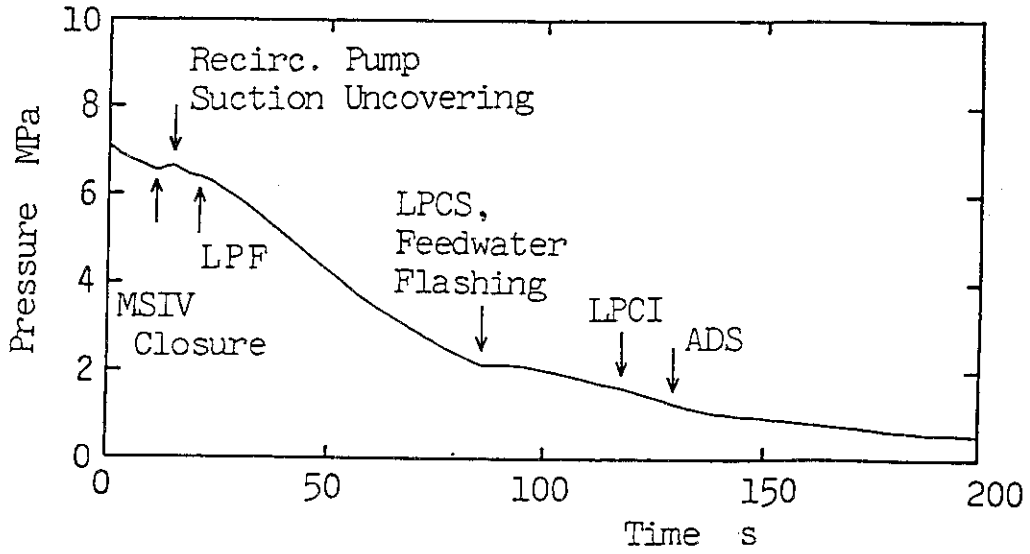


Fig. 2.10(a) Measured system pressure - 100 % break test

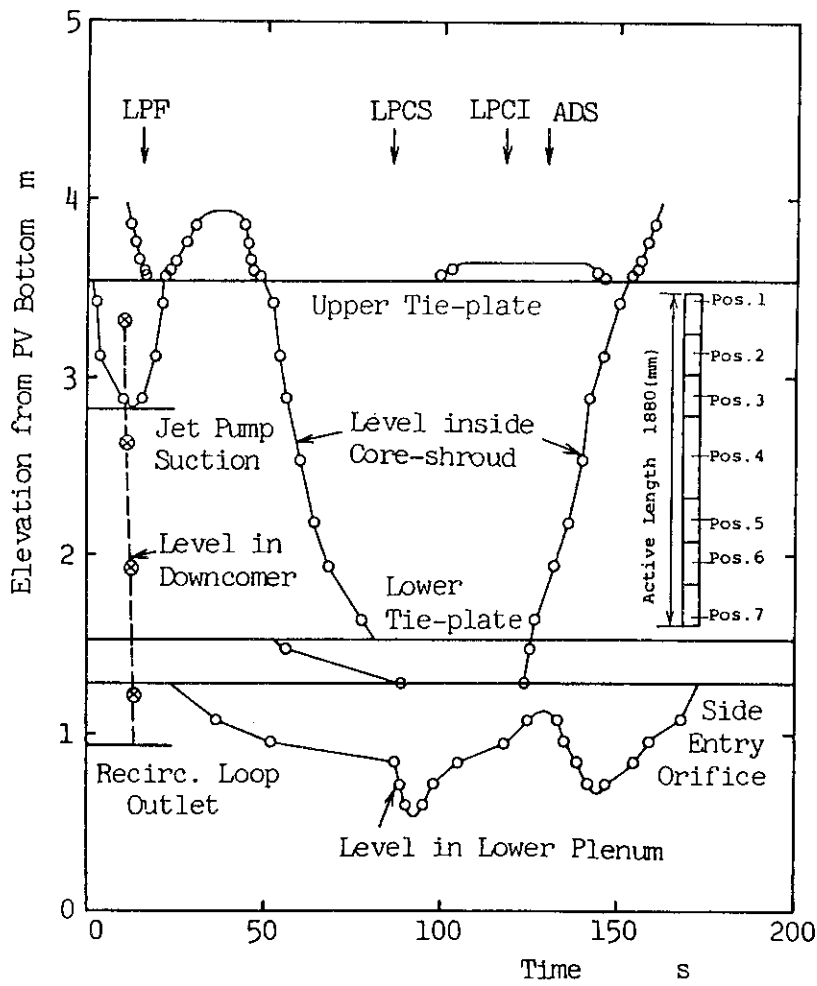


Fig. 2.10(b) Measured core mixture level - 100 % break test

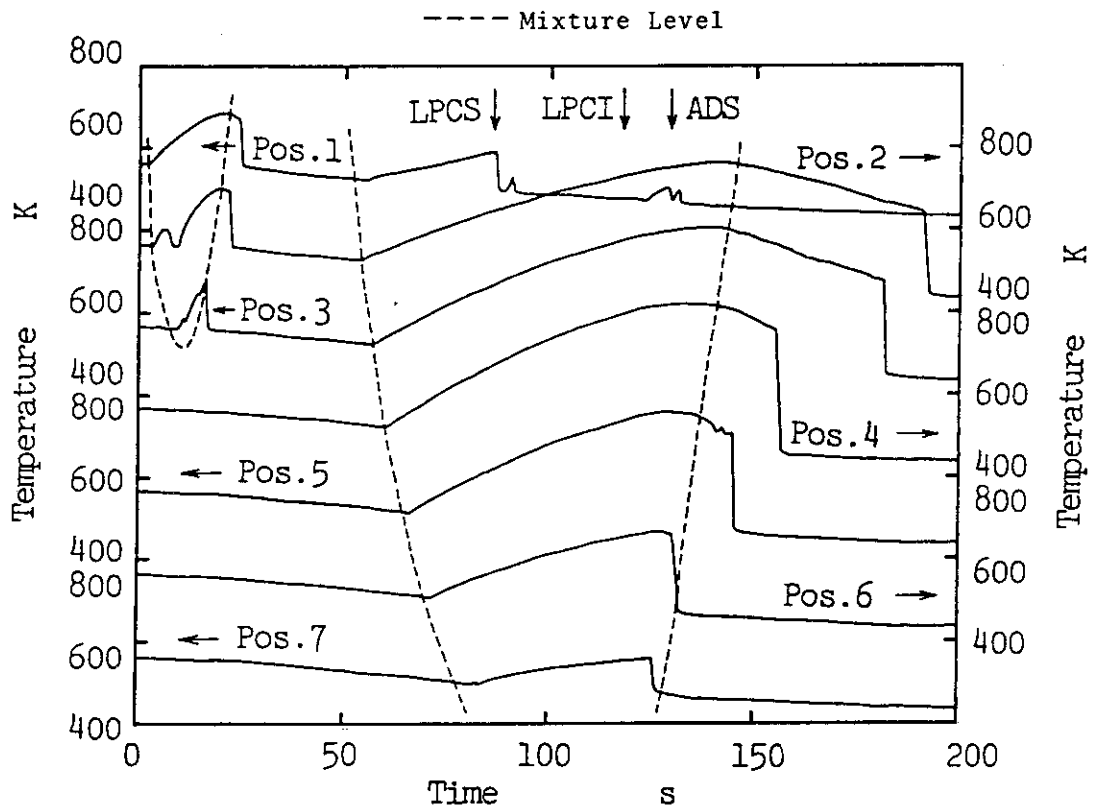


Fig. 2.10(c) Measured peak-power rod temperatures - 100 % break test

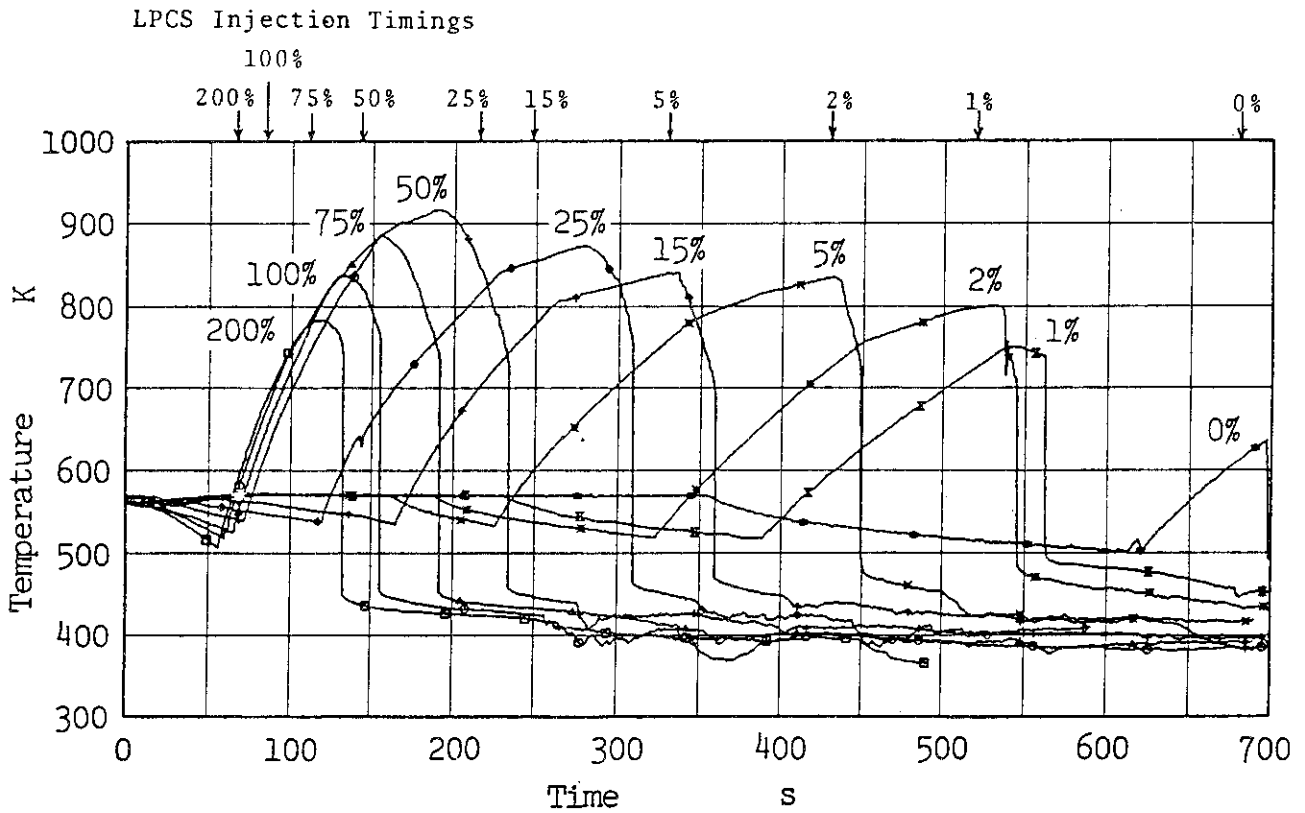


Fig. 2.11 Measured cladding temperatures at locations where PCT occurred

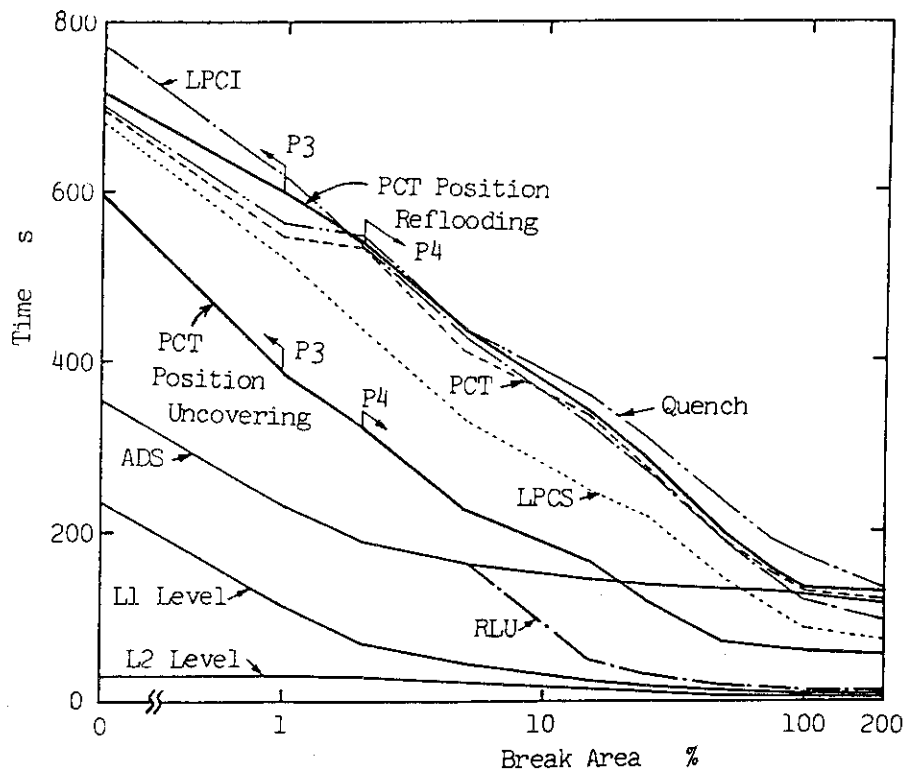


Fig. 2.12 Measured timings of events vs. break area

### 3. Computer code and Analytical Models

#### 3.1 Description of THYDE-B1 Code

The THYDE-B1 code is a fast-running best-estimate computer code developed by JAERI for analyzing thermal-hydraulic response of a BWR during a LOCA. With its unique features described below, the THYDE-B1 code is particularly suitable for predicting the system pressure and core fluid behaviors during a small- or intermediate-break LOCA.

The THYDE-B1 code is a lumped parameter code. The reactor core and coolant system are represented by multiple fluid nodes. For each node the conservation laws of mass and energy apply. Fluid flow rate between nodes is determined from momentum balance along the flow path (junction). Heat transfer to fluid from the fuel or other metal structure is calculated using a one-dimensional heat slab model. The RELAP 4 heat transfer correlation package is used.

##### 3.1.1 Node Models

Two node model options are provided in THYDE-B1: a homogeneous node model and a three-region node model.

The homogeneous node model assumes that fluids in the node are homogeneously mixed and in thermodynamic equilibrium.

The three-region node model, unique to THYDE-B1, can consider up to three subnodes which represent a vapor region, a saturated two-phase mixture region and a subcooled liquid region, respectively. The three regions are partitioned by horizontal moving boundaries. The elevations of the boundaries are determined from mass and energy balance in each region. The three-region node model includes the following assumptions:

- a) The node's pressure is represented by a pressure at a certain height in the node. The physical properties in the three subnodes are defined at that pressure. The differences in the physical properties caused by the pressure differential within a node are ignored.
- b) The vapor region is assumed to be saturated. Therefore, heat added to the vapor region does not superheat the vapor region but is added to the saturated mixture region to cause phase change from liquid water to vapor.

c) The temperature distribution in the subcooled liquid region and the void distribution in the saturated mixture region are assumed to be uniform in the vertical and horizontal directions.

Mass and energy transport among the regions occurs as steam is separated from the mixture region, or as subcooled and saturated fluids are mixed. THYDE-B1 provides several options to consider such mass and energy transport among the regions.

The option used in the present calculations assume that the steam separation rate  $W_B$  is a simple function of the total steam mass in the mixture region  $M_B$ , a representative travelling distance of a steam bubble during its life time  $X_B$ , and a representative bubble rise velocity  $V_B$ . Thus,

$$W_B = \frac{M_B \cdot V_B}{X_B} \quad (3-1)$$

This equation implies that the total steam mass is replaced in a representative life time of a steam bubble  $X_B/V_B$ . The bubble travelling distance  $X_B$ , referred to as "bubble sweep-out length" in the code, is assumed to be the smaller of an input-specified length or the thickness of the mixture region. The bubble rise velocity  $V_B$  is calculated with the Wilson's correlation as a function of void fraction, hydraulic diameter, and fluid properties. The representative void fraction for the mixture region is defined as

$$\alpha = \frac{M_B}{X_B \cdot A} \quad (3-2)$$

where A is the flow area at the top of the mixture region.

## (2) ECCS Mixing Model

The ECC water is injected into either the upper plenum (LPCS) or the core bypass region (LPCI). Options are provided to account for the time and distance required for complete mixing of the ECC water with saturated fluid. In the present calculations the LPCS water was assumed to be mixed either with the vapor or two-phase mixture which is present at the injection location. The LPCI water was assumed to be mixed only with two-phase mixture. Almost instantaneous mixing was assumed for either cases.

Using the three-region model enables simple nodalization without losing the accuracy of calculation. However, because of the simplicity



of the model, detailed core thermal-hydraulic responses, such as the counter-current flow limiting (CCFL) phenomenon at the core inlet and outlet, cannot be considered. Thus, the code is suitable for prediction of rather slow transients associated with small- or intermediate-break LOCAs.

### 3.1.2 Junction Models

THYDE-B1 has junction model options to represent various BWR hydraulic components. These options include:

(1) Homogeneous Junction

The flow rate between two adjacent nodes is given by solving a momentum equation neglecting the momentum flux terms and the effect of relative velocity between the vapor and liquid phases.

(2) Steam Separator Junction (Slip Junction)

Slip between the vapor and liquid phases is allowed to account for phase separation in the separator. The separator efficiency is to be specified as a function of the downcomer mixture level.

(3) Jet Pump Model

A jet pump is represented by a set of three special junctions where convection and mixing of momentum flux are taken into account.

(4) Leak Junction

Flow rate through breaks or relief valves can be calculated using either a flow-rate vs. time (or pressure) table or using a choked flow model.

(5) Fill Junction

Flow rate from an injection system should be specified as a function of time, or of pressure in the connected node.

### 3.1.3 Pump Model

The head of the recirculation pump can be included in the momentum balance of either a normal junction or the jet pump drive flow junctions. The pump head is calculated using a head vs. flow table as a function of the pump suction quality. This model is used only when the flow direction is normal; the recirculation pump is treated as a flow resist-

ance when flow direction is reversed.

### 3.1.4 Heat Structure Model

The fuel rods and other structures are modelled as one-dimensional heat slabs in cylindrical or rectangular geometry. The RELAP4<sup>(9)</sup> heat transfer package is used. Steam cooling after rod surface dryout is calculated using the Dittus-Boelter correlation.

## 3.2 Analytical Models

### 3.2.1 Nodalization

Two nodalization schemes were used to represent the ROSA-III test facility. One nodalization scheme, shown in Fig. 3.1, was used for the 200% break test, and the other shown in Fig. 3.2 for other tests. The 200% break test model includes 8 nodes, 20 junctions and 21 heat slabs. The other model includes 6 nodes, 19 junctions and 21 heat slabs. The difference between the two models was in the number of nodes and break junctions. The 200% break test was a double-ended break test, and thus the model included two break junctions. THYDE-B1 input deck for the 15% break test is presented in Appendix A.

As shown in Table 3.1, a large portion of the pressure vessel was represented by a single three-region node model, node 1. It included the lower plenum, the guide tubes, the core and core bypass, the upper plenum and the jet pump discharge lines. This was intended to make the best use of the THYDE-B1 three-region node model. Similarly, the downcomer, including the jet pump suction lines, and the steam dome are represented by another three-region node, node 2. The recirculation pump suction lines and discharge lines are represented by homogeneous nodes: nodes 3 and 5 for the broken loop, and nodes 4 and 6 for the intact loop, respectively.

The THYDE-B1 heat slab models were used to represent the core electric heater rods and facility structures. Each of the ROSA-III heater bundles contained 62 heated rods, out of which 20 had a local peaking factor (P.F.) of 1.1, 28 a P.F. of 1.0, and 14 a P.F. of 0.875.

The power per bundle for the peak-power bundle (Bundle A) was 1.4 times as large as that for each of the average power bundles (Bundles B, C and D). Thus, there were six groups of heater rods broken down by power level. As listed in Table 3.2, the heater rods were represented by two groups of heat slabs, Slabs 1 through 7 and Slabs 11 through 17. The two groups represented heater rods having average local P.F. (1.006) in average- and peak-power bundles, respectively. The total volumes, heat capacities, heat transfer areas, heat generation rates in the average- and peak-power bundles were correctly represented.

The junctions are listed in Table 3.3.

### 3.2.2 Break flow model

The break mass flow rates were calculated as follows:

For  $x \leq 0$ , use single-phase orifice flow model, i.e.,

$$W = C_1 A \sqrt{2 \rho_j g_c (P_o - P_b)}, \quad (3-3)$$

for  $x > x_{\text{tran}}$ , use the Moody's critical flow model, i.e.,

$$W = C_0 A G_M(P_o, h_o), \quad (3-4)$$

and for  $0 < x < x_{\text{tran}}$ ,

use linear interpolation of Equations (3-3) and (3-4),

where,

$C_0$  = discharge coefficient (user input),

$C_1$  = contraction coefficient (user input),

$A$  = junction flow area

$G_M(P_o, h_o)$  = critical mass flux determined by the Moody's slip flow model,

$P_b$  = back pressure

$\rho_j$  = fluid density at  $(P_o, h_o)$ ,

$x$  = fluid quality at  $(P_o, h_o)$ .

The values of  $C_0$ ,  $C_1$  and  $x_{\text{tran}}$  used in the present calculations were 0.61, 0.6 and 0.02, respectively. These values were recommended by previous analyses. (4)(10)

### 3.2.3 Main Steam Line Model

The Moody critical flow model [Equation (3-4)] was used also for calculation of the steam flow rates through the main steam line and the automatic depressurization system (ADS).

### 3.2.4 ECCS Model

The HPCS, LPCI and LPCS were represented by fill junctions. The mass flow rate for each was given by a pressure vs. mass flow rate table.

### 3.2.5 Feedwater Line Model

The feedwater line was represented by a fill junction. The mass flow rate was given by a time vs. mass flow rate table. The volume in the feedwater line was not modelled. Thus, the feedwater line flashing (FLF) phenomenon was not calculated.

### 3.2.6 Steam Separation Model

The steam separation model (3.1.1 (1)) was used for node 1 and 2. The initial value of the bubble sweep-out length for node 1 was determined to be 2.4 m, as calculation with this value reproduced the steam flow rate and core mixture level measured during the steady state prior to the initiation of the tests. Thus, when the thickness of the mixture region became  $< 2.4$  m, the sweep-out length was equated to the mixture region thickness. The sweep-out length for node 2 was assumed to be the thickness of the mixture from the initiation of a calculation.

### 3.2.7 Recirculation Pump Model

The pump head was calculated using an input-specified head vs. flow table as a function of quality.

### 3.2.8 Trip Conditions

The trip conditions used in the tests were modeled exactly.

Table 3.1 Description of nodes

Node No.	component	model option
1	space inside core shroud	three-region node
2	space outside core shroud	three-region node
3	broken recirculation line from vessel to MRP	homogeneous node
(3)	broken recirculation line from break to MRP	homogeneous node
4	break side recirculation line from MRP to JP	homogeneous node
5	intact recirculation line from vessel to MRP	homogeneous node
6	intact recirculation line from MRP to vessel	homogeneous node
(7)	broken recirculation line from vessel to break	homogeneous node

Table 3.2 Description of heat slabs

Slab No.	Description
1 to 7	low power rod
8	lead rods
9	pressure vessel wall
10	pressure vessel wall
11 to 17	high power rod
18	lead rods
19	channel box
20	filler block
21	lower plenum structures
22	control rod

Table 3.3 Description of junctions

Junction No.	Component	Junction model option
1	steam separator	steam separator junction
2	recirculation line	normal junction
3	recirculation line	normal junction with pump
4	J.P. drive line	} jet pump junctions
5	J.P. discharge line	
6	J.P. suction line	
7	recirculation line	normal junction
8	recirculation line	normal junction with pump
9	J.P. drive line	} jet pump junctions
10	J.P. discharge line	
11	J.P. suction line	
12	high pressure core spray	fill junction
13	low pressure core spray	fill junction
14	low pressure coolant injection	fill junction
15	automatic depressurization system	leak junction
16	break 1	leak junction
17	safety relief valve	leak junction
18	feed water line	fill junction
19	main steam line	leak junction
(20)	break 2	leak junction

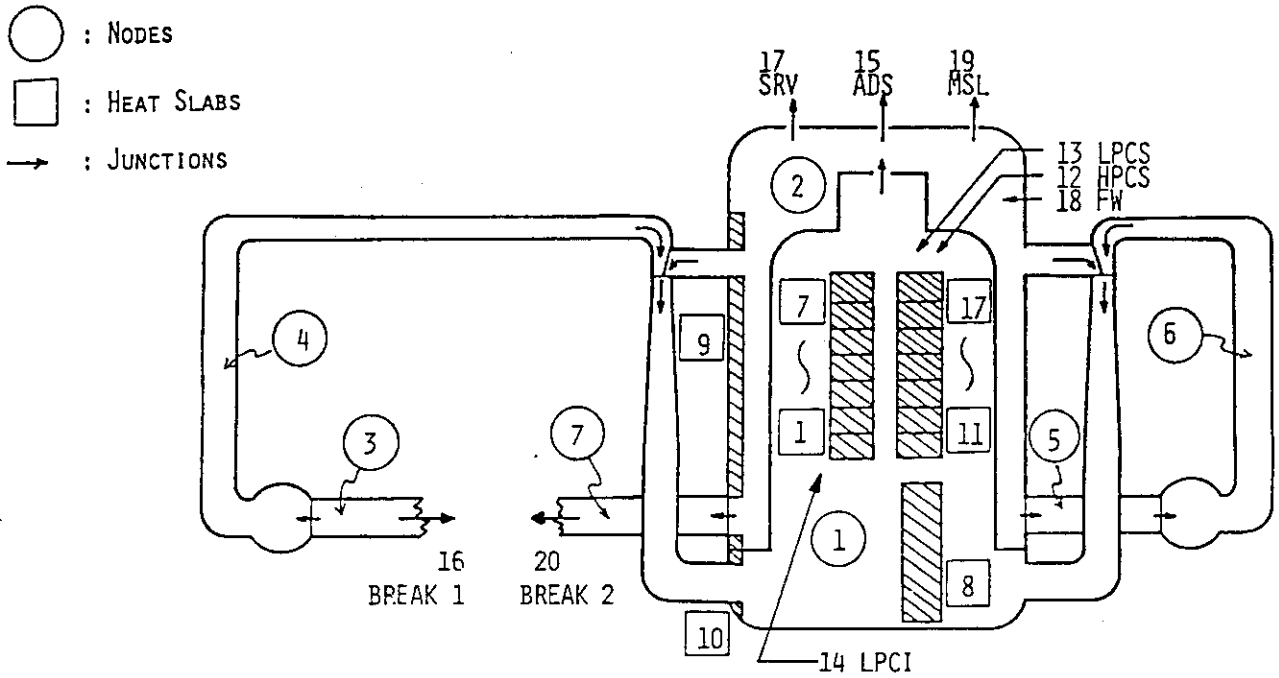


Fig. 3.1 Nodalization diagram - 200 % break test

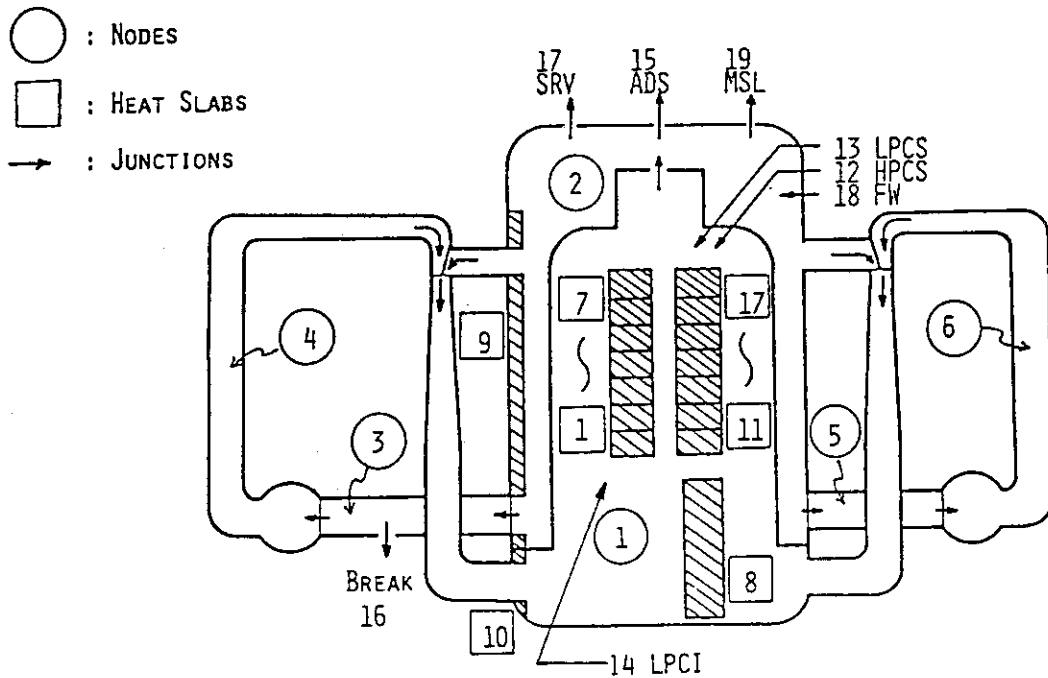


Fig. 3.2 Nodalization diagram - 0 through 100 % break tests

## 4. Analytical Results and Discussion

In this Section, the capability of the THYDE-B1 (Mod 0) code to reproduce the ROSA-III test results is investigated by comparing the experimental and analytical results. The ten ROSA-III tests analyzed herein are broken down by size of break into three groups, i.e., small, intermediate and large breaks. Comparison plots between the experimental and analytical results are shown for one typical test selected from each group. Comparison plots for other tests are presented in Appendix B.

### 4.1 Small Break Tests (Break Areas <5%)

Three tests were conducted for this range of break area. The tested break areas were 0,1 and 2%. Figures 4.1 through 4.5 compare the major transient parameters obtained from the 1% break test and calculation.

For this range of break area, the initial system depressurization was arrested at  $\sim 6.7$  MPa, as typically shown in Fig. 4.1, as the simulated pressure control system throttled the main steam line. After the subsequent closure of MSIV, the system repressurized to the setpoint pressure of SRVs of 8.1 MPa. Then the system started to depressurize again as ADS operated. Thereafter, the steam discharge through ADS dictated the system overall behavior.

The purpose of ADS is to depressurize the system to prompt ECC water delivery. This effect was emphasized in the ROSA-III small-break tests analyzed in this report. Since failure of HPCS was assumed in these tests, ECC water became first available when ADS depressurized the system to the shutoff head of LPCS of 2.16 MPa.

Thus, the time of initiation of the ADS's operation as well as the ADS flow rates were important for calculation of the system behavior during the small break tests.

The ADS was tripped on (with a time delay of 120 s) when the downcomer collapsed level decreased to the L1 level. The calculated time of the ADS initiation delayed relative to the measurement for the small breaks, as the calculated downcomer liquid level decreased more slowly than the test data.

For the 1% break test, the calculated time of the ADS initiation



delayed 15 s relative to the measurement. However, the calculated and measured behaviors of the downcomer level agreed qualitatively as shown in Fig. 4.2. It should be noted that in Fig. 4.2 the calculated two-phase mixture level is compared with test data of collapsed liquid level, because the code does not explicitly calculate the collapsed liquid level whereas mixture level was not measured at upper downcomer elevations. Thus, the comparison is meaningful until  $\sim 250$  s, when the downcomer fluid began to flash. The downcomer collapsed liquid level was measured with two transducers which measured differential pressures in the upper downcomer (between 2.814 m and 5.910 m above the vessel bottom) and the lower downcomer (between 0.938 m and 3.90 m above the bottom).

The ADS steam discharge flow rates were calculated using the Moody critical flow model with a discharge coefficient of 0.6. The calculated flow rates agreed with the test data fairly well, but were found to be slightly ( $\sim 10\%$ ) smaller than the data as shown in Fig. 4.3.

Figure 4.4 compares the calculated and measured mixture level inside the core shroud. Core uncover occurred both in the test and in the calculation as coolant was lost through ADS and break. The core was refilled as LPCS water accumulated in the core. Since the calculated initiation of the ADS flow delayed relative to the measurement, and hence the initiation of the LPCS flow delayed, the calculated core mixture level behavior delayed relative to the measurement. Both core uncover and reflooding delayed, however, the delay was greater for reflooding than for uncover. Thus, the calculated duration of core uncover was longer than the measurement.

Figure 4.5 compares the calculated and measured peak-power rod cladding temperatures. The calculated initiation of cladding temperature excursion delayed relative to the measurement, as the calculated core uncover delayed. The heatup rate after the dryout was calculated fairly well. Temperature turn-around and quenching propagated in the test from the top to the bottom of the core, under the effect of the LPCS injection on the top of the core. However, in the calculation the quench front moved upward, from the bottom to top of the core, as the core mixture level recovered due to accumulation of the LPCS water. This disagreement occurred because the code does not model the contact between the heater rods and the falling LPCS water. This caused dryout at the higher core elevations (positions 1 through 3) to continue longer than the test.

The calculated PCT occurred at position 3 of the peak power rod (as was the case in the test) at 634.5 s upon reflooding at the elevation (vs. 546 s, ~45 s before reflooding in the test) before the initiation of LPCI flow (as was the case in the test). The calculated PCT was 758 K and agreed closely with the measured PCT of 754 K.

#### 4.2 Intermediate Break Tests ( $5\% \leq \text{Break Areas} \leq 50\%$ )

Four tests were conducted for this range of break area. The tested break areas were 5, 15, 25 and 50%. Figures 4.6 through 4.10 compare the major transient parameters obtained from the 15%-break test and calculation.

The system thermal-hydraulic behavior for this range of break area was different from that for the small (<5%) breaks, in that gross system depressurization was caused by uncovering of the recirculation pump suction line inlet as typically shown in Fig. 4.6, rather than by the operation of ADS. In addition to this, the in-vessel steam generation, due to both flashing in the pressure vessel (including the feedwater line) and vaporization of ECC water, had more significant influence on the system behavior than for the small breaks.

Thus, the downcomer mixture level behavior and break mass and energy flow rates are important for the system behavior for this range of break area.

Figure 4.7 compares calculated and measured break mass flow rates for the 15% break test. The calculation and measurement agreed within the measurement uncertainty. The calculated and measured times of recirculation line uncovering (RLU) compared favorably as well, as shown in Fig. 4.8.

However, the effect of RLU on the system pressure behavior was not correctly represented in the calculation. As typically shown in Fig. 4.6, RLU led an immediate system depressurization in the tests, however, this did not occur in the calculation. The calculated initiation of depressurization delayed relative to the test data. (The delay was greater for the smaller intermediate breaks. Also, the depressurization rate after RLU was underestimated for the smaller intermediate breaks).

These discrepancies between the measured and calculated system pressures appear to have resulted from underprediction of the break flow

rate (Fig. 4.7) and break flow quality.

The downcomer mixture level has significant influence on the break flow quality. As shown in Fig. 4.8, the downcomer mixture level was overpredicted after the initial RLU up to  $\sim 80$  s. The THYDE-B1 steam separation model (3.1.1 (1)) and the jet pump model are probably responsible for such discrepancy between the measured and calculated downcomer level behavior.

Although the calculated system depressurization delayed relative to the data, the difference between the measured and calculated pressure decreased with time, and the calculated pressure eventually became lower than the data after the LPCS injection began. This overprediction of the system depressurization rate appears to have resulted from underprediction of the in-vessel steam generation, as will be discussed in the following paragraphs.

The calculated and measured system pressures behaved differently after the initiation of LPCS flow. The system depressurization was decelerated after the initiation of LPCS flow in the tests, however this did not occur in the calculations as typically shown in Fig. 4.6. The experimentally observed decrease in the depressurization rate appears to have resulted from vaporization of LPCS water. Vaporization may have occurred as the falling LPCS water contacted with either solid surfaces heated above the saturation temperature (heater rods and vessel structures exposed to steam) or with superheated steam.

These vaporization modes for the LPCS water were not modeled in the present calculations. Direct contact between the falling ECCS water and solid surfaces was not accounted for, since the THYDE-B1 three-region node model, used to represent the core region, does not account for the presence of liquid phase above the mixture level. Vaporization due to contact with superheated steam cannot be accounted for either, because the code assumes that vapor is always saturated. As a result, the initiation of LPCS injection resulted in accelerating the system depressurization in the calculation, rather than decelerating, as saturated vapor condensed on the injected LPCS water.

In addition to the vaporization of LPCS water, there occurred in the tests flashing in the feedwater line at the system pressure of  $\sim 2.2$  MPa, which was approximately equal to the LPCS injection pressure. The steam generated by the feedwater line flashing (FLF) also contributed to the decrease in the system depressurization rate. However, the effect

of FLF was not accounted for in the present calculations where the volume in the feedwater line was not modeled.

Since steam generation due to these mechanisms was underestimated or neglected, the calculated system depressurization was faster than the measurement during the later phase of the intermediate-break tests. The faster depressurization led to earlier initiation of the LPCI flow than in the tests.

Figure 4.9 compares the calculated and measured core mixture level for the 15% break test. The comparison is generally favorable during the core uncovering process, although the initial core uncovering was predicted to occur slightly ( $\sim 16$ s) later than the test. The temporary recovery of the core mixture level at  $\sim 115$ s, due to concurrent initiation of the ADS flow and lower plenum flashing (LPF), was well calculated. However, the experimentally observed formation of mixture level above the upper tieplate (from 194 to 231s, and from 252 to 264s), or above and below the channel side entry orifice (from 130 to 203s) was not calculated, because such mixture level resulted from the counter current flow limiting (CCFL) phenomenon, which was not accounted for by the code.

Despite that the core uncovering process was calculated fairly well, the reflooding was calculated to occur considerably earlier than that in the tests. This resulted from that the calculated system depressurization was faster than the measurement after the initiation of LPCS flow. The faster depressurization prompted the initiation of LPCI flow and caused greater LPCS and LPCI flow rates than in the tests. These together prompted core reflooding.

Figure 4.10 compares the calculated and measured cladding temperatures along a peak-power rod. Since the calculation well represented the core uncovering process, except for that at the upper core region, the calculated times of rod surface dryout at Positions 3 through 7 agreed well with the test data. The calculation also succeeded to reproduce the initial cladding heatup behavior after the dryout. However, since the code assumes that steam is always saturated, whereas steam actually becomes superheated as it flows along heater rods, the calculation overestimated heat transfer from the heater rod to steam environment. Thus, the calculated heatup rate became smaller than the measurement as cladding temperature increased.

It is interesting to note that such overprediction of the steam cooling effect was much less pronounced for the small breaks, because

the calculated heat transfer coefficients were smaller than those calculated for the larger breaks. The heat transfer coefficient for steam cooling was calculated using the Dittus-Boelter correlation. Thus, the calculated heat transfer coefficient depended on the steam mass flux through the core, which was induced by system discharge through the break and ADS. For the small breaks the core steam flow was induced primarily by the ADS flow, since core uncover occurred before RLU. Since the ADS flow was relatively small because the core uncover occurred after the system had depressurized considerably, the core steam mass flux was small and hence the calculated heat transfer coefficient was relatively small for the small breaks.

Quenching of the rod surface occurred only in the bottom-up fashion in the calculation, because of the code's limitations already mentioned. Accordingly, the top-down quench experimentally observed at the upper core region (Positions 1 through 3), was not represented. Because of this, the calculated quenching for these locations delayed relative to the measurements. However, for other locations where quenching occurred in the bottom-up fashion in the test, the calculation predicted earlier quenching than the measurements as reflooding was calculated to occur earlier than the tests.

The calculated PCT for the 15% break test occurred at position 4 of the peak power rod (as was the case in the test) at 294 s upon reflooding at that elevation (vs. 336 s in the test, also upon reflooding), after the initiation of the LPCI flow (as was the case in the test). The calculated PCT was 740 K vs. the measured PCT of 864 K.

#### 4.3 Large Break Tests (Break Areas >50%)

Three tests were conducted for this range of break area. The tested break areas were 75, 100 and 200%. Figures 4.11 through 4.13 compare the major transient parameters obtained from the 100%-break test and calculation.

For this range of break area, the overall system behavior was similar to that for the intermediate ( $\leq 50\%$ ) breaks. However, the effects of break flow and in-vessel steam generation on the system behavior were more significant. The effect of ADS was small, because ADS operated only after the system had depressurized so that all other ECCS (LPCS

and LPCI) had begun to operate.

Although the system response was primarily governed by the break flow, the system pressure was initially affected by discharge through the main steam line until MSIV closed, since this was the only path for steam discharge until the recirculation line uncover (RLU). Thus, the difference between the calculated and measured timings of the MSIV closure caused the difference between the initial system pressure behavior shown in Fig. 4.11. The difference between the times of the MSIV closure (tripped by an L2-signal) resulted from difference between the calculated and measured downcomer liquid level behaviors. The calculated time of the MSIV closure was generally earlier than the measurement for the large breaks, whereas it showed good agreement with the measurement for the small and intermediate breaks.

The RLU led gross system depressurization both in the experiment and calculation. The calculated RLU was more straightforward than that for the intermediate breaks in the sense that the calculated downcomer mixture level never recovered, after the initial RLU, to the elevation of the recirculation pump suction line inlet.

The effect of LPF on the system pressure behavior was to decelerate the system depressurization. This was less pronounced in the calculations than in the tests, since in the calculations LPF caused smaller increase in the core mixture level and hence smaller amount of steam generation. However, the calculated system pressure behavior agreed well with the test data until initiation of LPCS flow.

The calculated and measured system pressures after the initiation of LPCS flow behaved differently as was the case for the intermediate breaks. The LPCS injection, together with the feedwater line flashing (FLF), decelerated the system depressurization in the tests, but this did not occur in the calculations. Since the calculated depressurization after the initiation of LPCS flow was faster than the measurement, injection from LPCI was calculated to occur earlier than the tests. Major in-vessel steam generation in the calculations occurred only after the initiation of reflooding.

Figure 4.12 compares the calculated and measured core mixture levels for the 100% break test. The swelling of core mixture level due to LPF was much smaller in the calculation than in the test. Thus gross core uncover was calculated to occur earlier than in the test. The core emptying in the calculation progressed more quickly than in the test

also because the effect of CCFL on liquid drainage at the channel side entry orifice was not accounted for by the code. Since the injection from LPCS and LPCI was calculated to begin earlier than the test, the calculated core mixture level began to recover earlier than the test.

Figure 4.13 compares the measured and calculated cladding temperatures along a peak-power rod. The measured and calculated temperature behaviors were qualitatively different. The calculation predicted early temperature excursion for positions 3 through 5, starting well before these locations were uncovered. However, such temperature excursion due to departure from nucleate boiling (DNB) did not occur in the test, and nucleate boiling continued until the rod surface was uncovered. The calculated temperature excursion continued until the rod surface was finally quenched after reflooding; although the rod surface heat transfer was improved temporarily after LPF, the rod surface at positions 3 through 5 remained dry, and temperature excursion continued as these locations were uncovered above the mixture level.

The PCT was calculated to occur at the peak-power rod position 4 (as was the case in the test) at 111 s when reflooding occurred at that location (vs. 134 s in the test, upon reflooding). The calculated PCT was 846 K vs. the measured PCT was 832 K.

The prediction of unrealistic early DNB by the code was found to have resulted from inadequate calculation of the core flow. The DNB was calculated to occur for break areas  $\geq 50\%$  at positions 3 through 5 on the peak-power rod. The DNB occurred concurrently with the closure of MSIV, when a vapor region began to exist in node 1 (see Fig. 3.2) as the mixture level dropped from the top of the node. It was found that the code calculated the mass flux in the saturated mixture region to be zero when there existed three regions (vapor, mixture and subcooled) in a three-region node, because the order of definition of variables was inadequate. Thus, DNB was calculated to occur as soon as MSIV closed, if the rod surface heat flux exceeded the assumed critical heat flux ( $90000 \text{ BTU/ft}^2 \cdot \text{hr}$ ) for pool boiling. The DNB was calculated to occur only for the larger breaks ( $\geq 50\%$ ), where the above condition was satisfied.

#### 4.4 Peak Cladding Temperature vs. Break Area

Figure 4.14 compares the measured and calculated PCTs for all the tests analyzed. Comparison of the measured and calculated PCTs, the times of PCT and the locations where the PCTs occurred are also given in Table 4.1.

The calculated PCTs were in fair agreement with the test data for the small (<5%) and large (>50%) break areas, however, for the intermediate-breaks the PCTs were underpredicted as much as 124 K.

The PCT depends much on the timing of dryout and the duration of dryout before temperature turnaround. Figure 4.19 compares the measured and calculated timings of events. The timings of dryout and reflooding are shown for the positions where PCT occurred in the calculations and tests, respectively.

For the small (0, 1 and 2%) breaks, the calculated times of both dryout and PCT were later than the measurements. The temperature turnaround was caused by the core spray (LPCS) in the tests, and by reflooding in the calculations. However, the calculated and measured PCTs agreed fairly well, because the duration of dryout was well calculated. The duration of dryout is more important for the small breaks than the timings, because dryout occurs only after the variation of core power with time has become very slow.

For the intermediate breaks (between 5 and 50%), the timing of dryout was predicted well. However, the temperature turnaround was calculated to occur earlier than the tests. Thus, the calculated duration of dryout was shorter than the measurements, and hence the calculated PCTs were lower than the measurements. The underprediction of PCT resulted also from overprediction of steam cooling after dryout, as discussed in Subsection 4.2.

For the large breaks, the calculated timings of both dryout and PCT were earlier than the measurements. However, it is difficult to discuss how such disagreement between the calculated and measured timings affected the PCT, because the calculations indicated unrealistic early DNB which may have had a considerable influence on the PCTs calculated for these tests. The calculated PCTs occurred earlier than the tests, because reflooding was calculated to occur earlier than the tests. The overprediction of steam cooling also should have affected the calculated PCTs.



#### 4.5 Parametric Calculations

As has been discussed in the previous Subsections, the major factors which caused the underprediction of PCT appear to include the overprediction of the ECC flow rates, resulting from underprediction of the system pressure after the initiation of LPCS flow. Thus, additional parametric calculations were conducted to investigate the impact of ECC flow on the system behavior. In these calculations the ECC flow rates measured in the tests (as a function of time) were used instead of using the flow vs. pressure tables. Figure 4.16 compares calculated (baseline) and measured ECC flow rate (LPCS plus LPCI) vs. time for the 15% break test. Both in the calculation and test PCT occurred shortly after the initiation of the LPCI flow. The LPCI flow was about four times larger than the LPCS flow, and led immediately to core reflooding. The core mixture levels calculated for the 1, 15 and 100% break tests are shown in Figs. 4.17 through 4.19, respectively. The parametric calculations show much better agreement with the experimental data than the baseline calculations, for the 15 and 100% breaks (Results for other tests are shown in Appendix B). Thus, it is evident that the disagreement observed between the baseline calculations and experimental data of the core mixture level primarily resulted from the underprediction of the system pressure. Correct prediction of the system pressure is important particularly when the LPCI setpoint pressure is approached, because LPCI lead to immediate reflooding, up to the core midplane or higher, for the intermediate breaks.

Table 4.1 Measured and calculated peak cladding temperatures.

Break Area (%)	Position (No.)		Time (s)		PCT (K)		PCT occurred before LPCI injection	
	Exp.	Cal.	Exp.	Cal.	Exp.	Cal.	Exp.	Cal.
0	3	3	696	850	637	684	×	×
1	3	3	546	634.5	754	758	×	×
2	4	3	531	556.5	804	776	×	×
5	4	4	410	381	835	753	×	
15	4	4	336	294	846	740		
25	4	4	274	253.5	872	748		
50	4	4	189	177	925	821		
75	4	4	154	137	885	843		
100	4	4	133	111	832	846		
200	4	4	119	85	785	886		

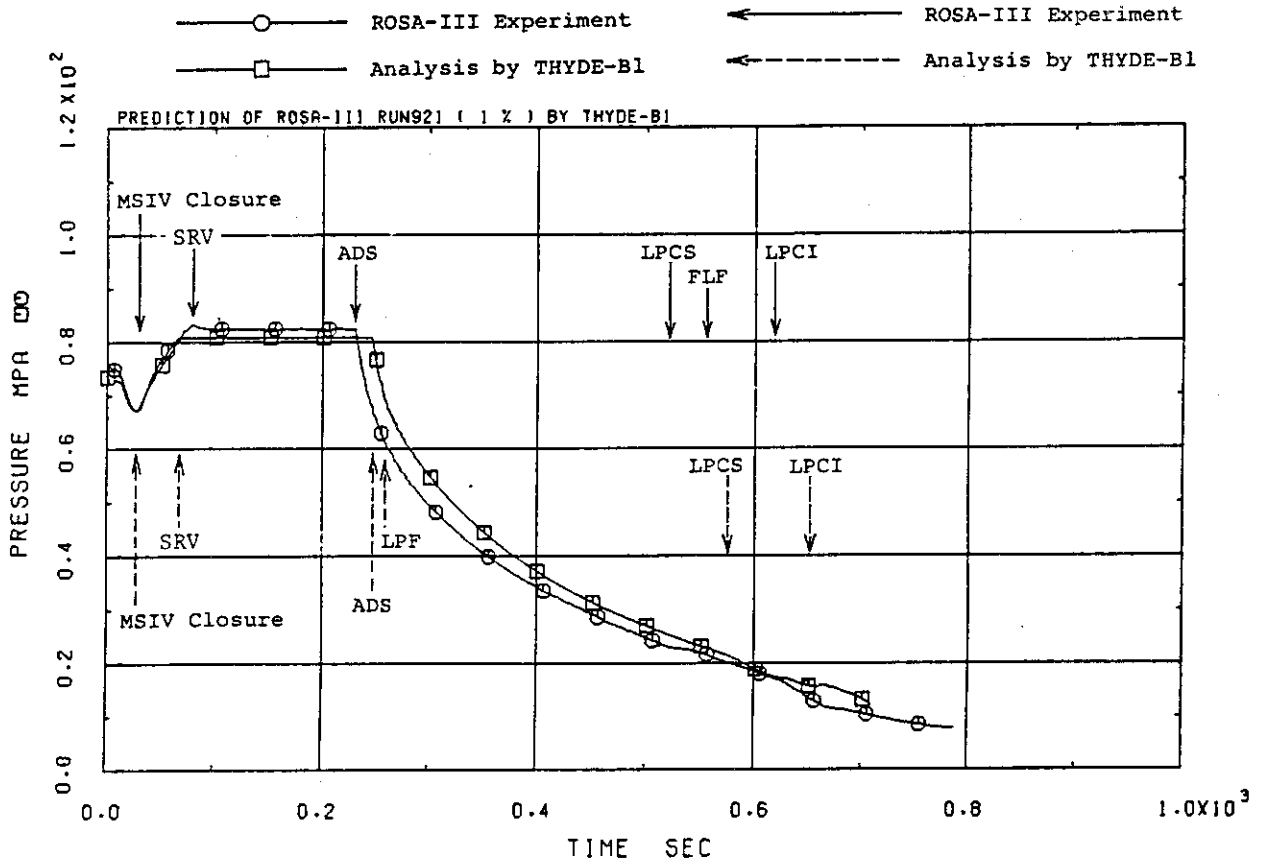


Fig. 4.1 Measured vs. calculated system pressures - 1 % break test

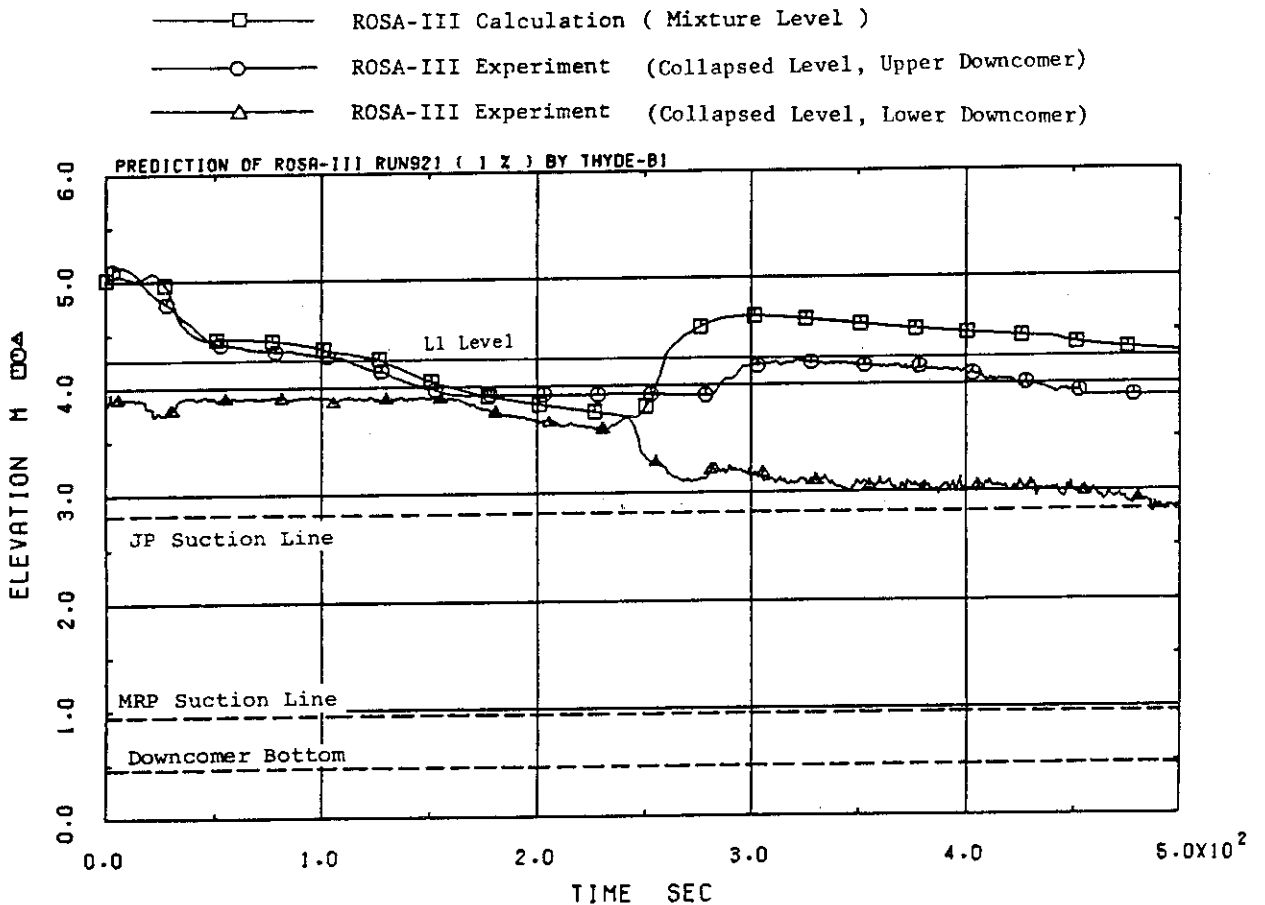


Fig. 4.2 Measured vs. calculated downcomer mixture levels - 1 % break test

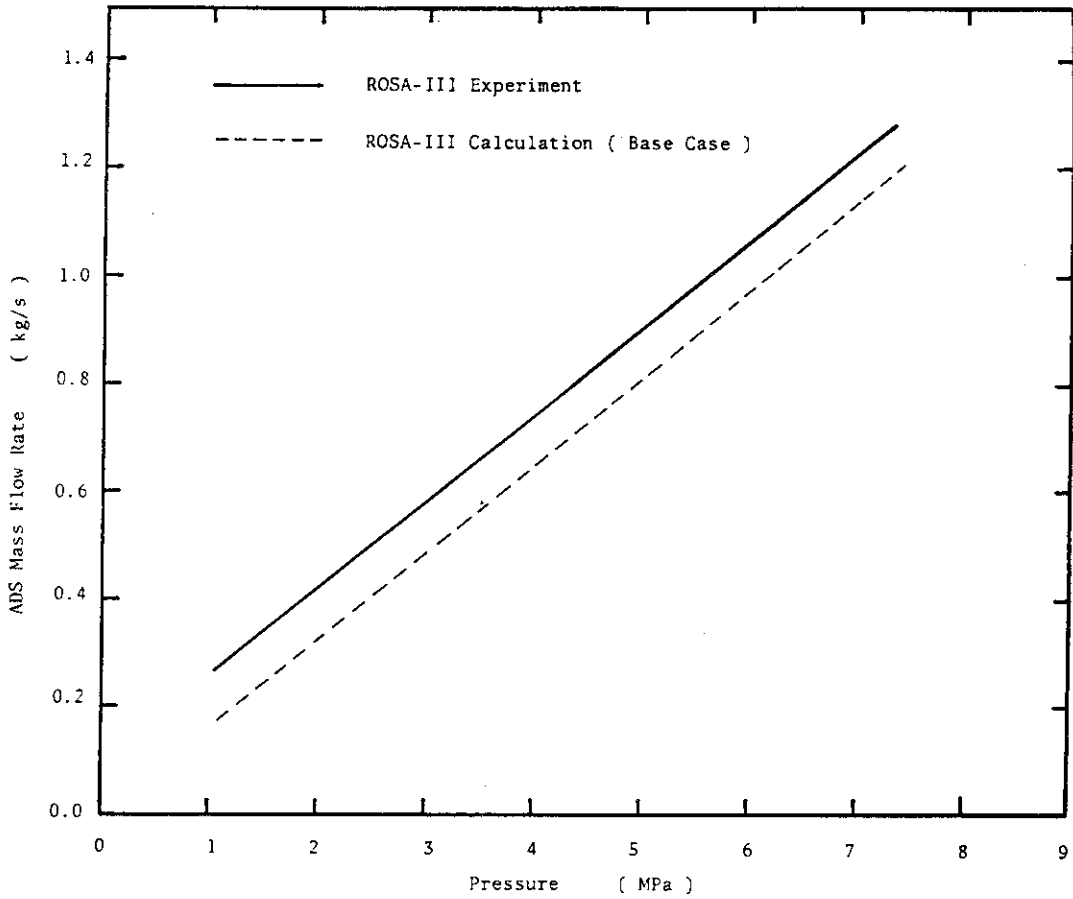


Fig. 4.3 Measured vs. calculated ADS flow rates

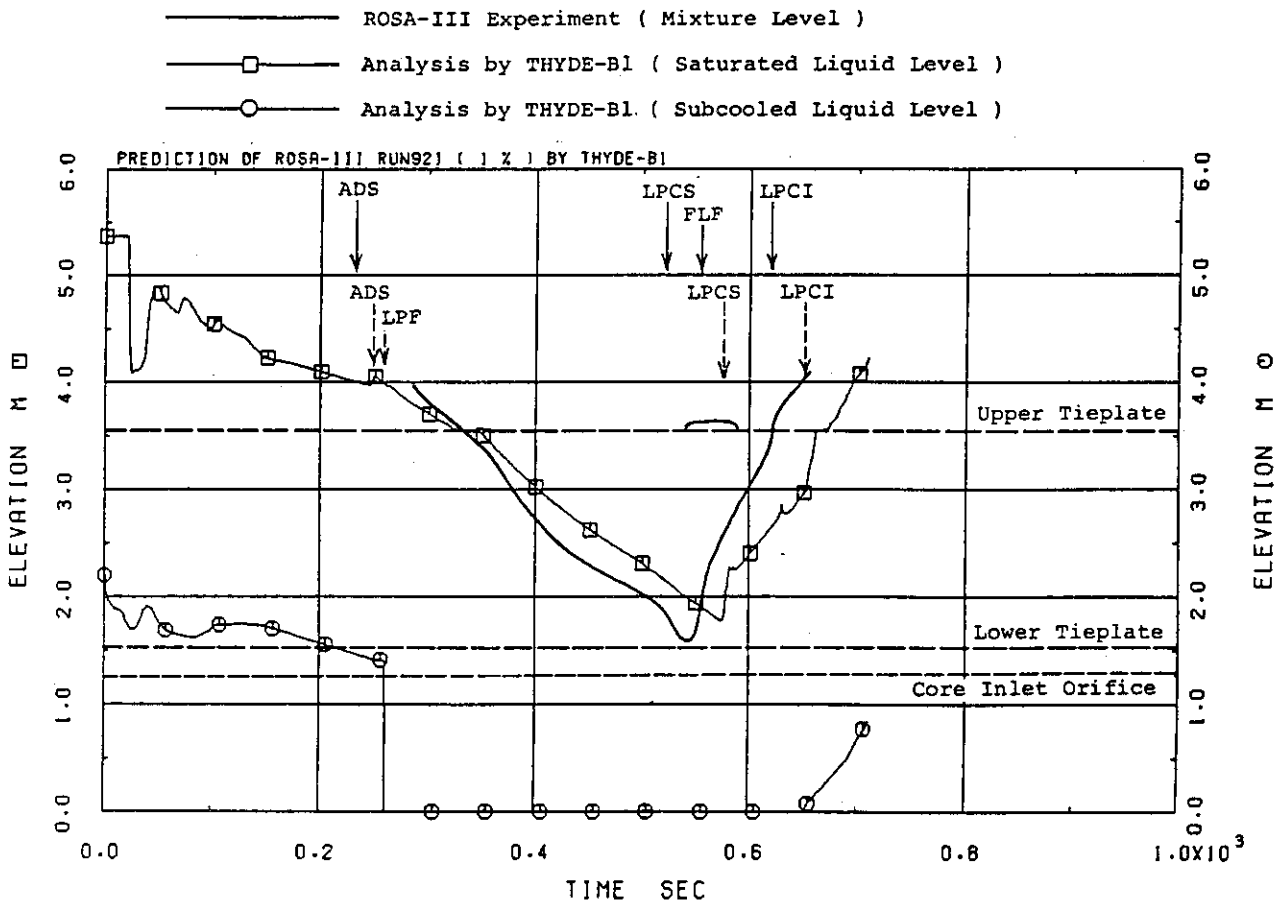


Fig. 4.4 Measured vs. calculated core mixture levels - 1 % break test

× ◇ ▲ ✕      ROSA-III Experiment  
 □ ○ △ +      Analysis by THYDE-B1

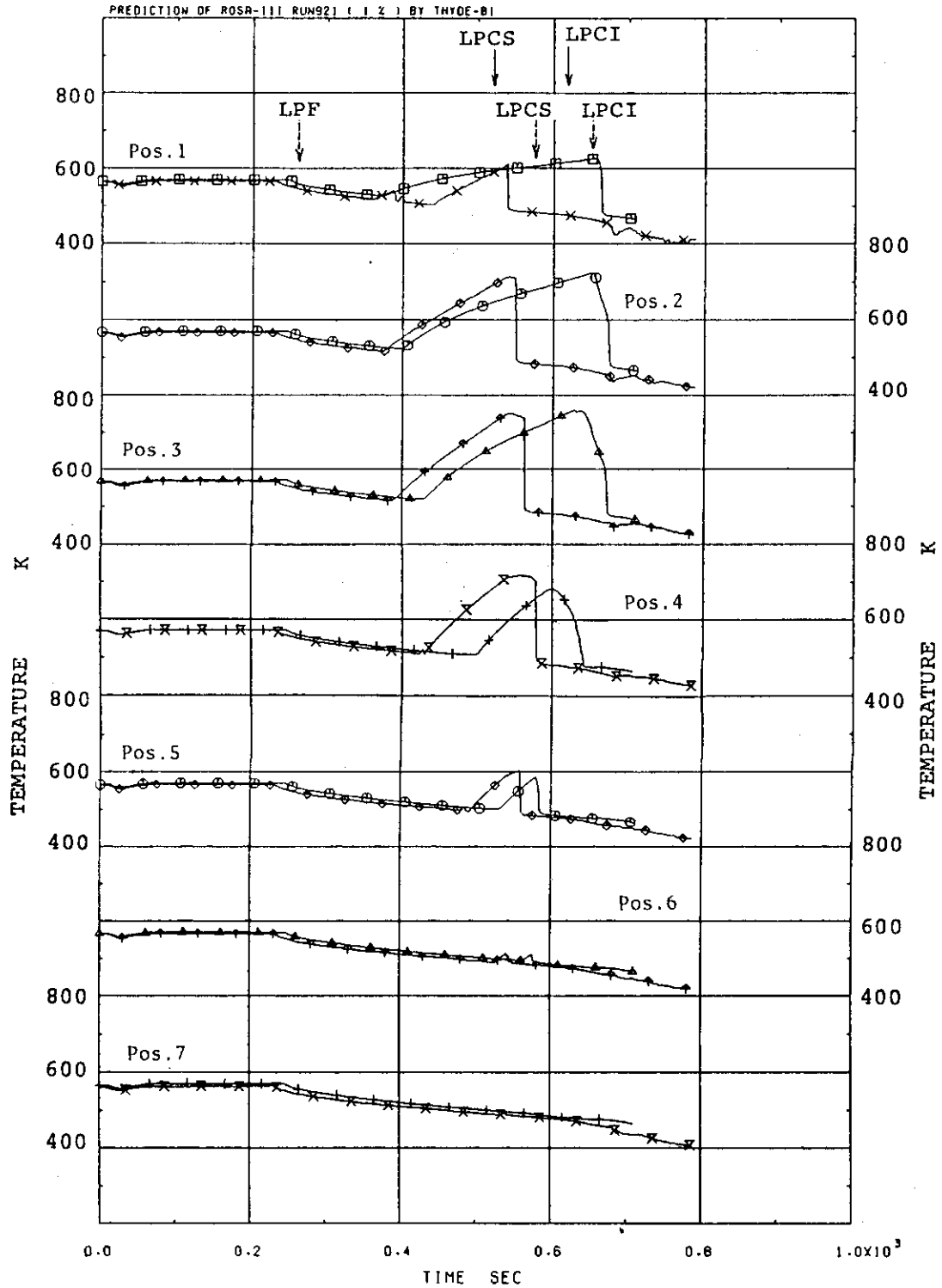


Fig. 4.5 Measured vs. calculated peak-power rod temperature - 1 % break test

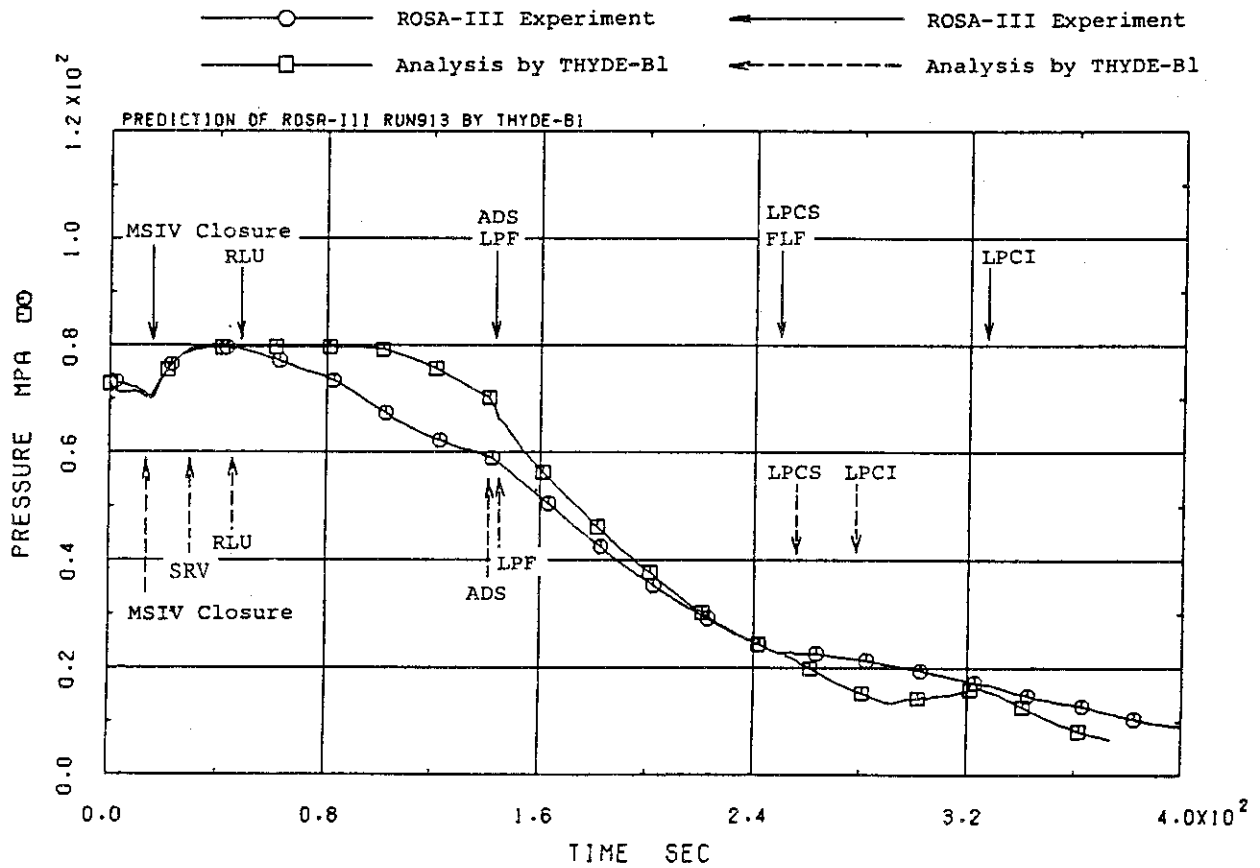


Fig. 4.6 Measured vs. calculated system pressures - 15 % break test

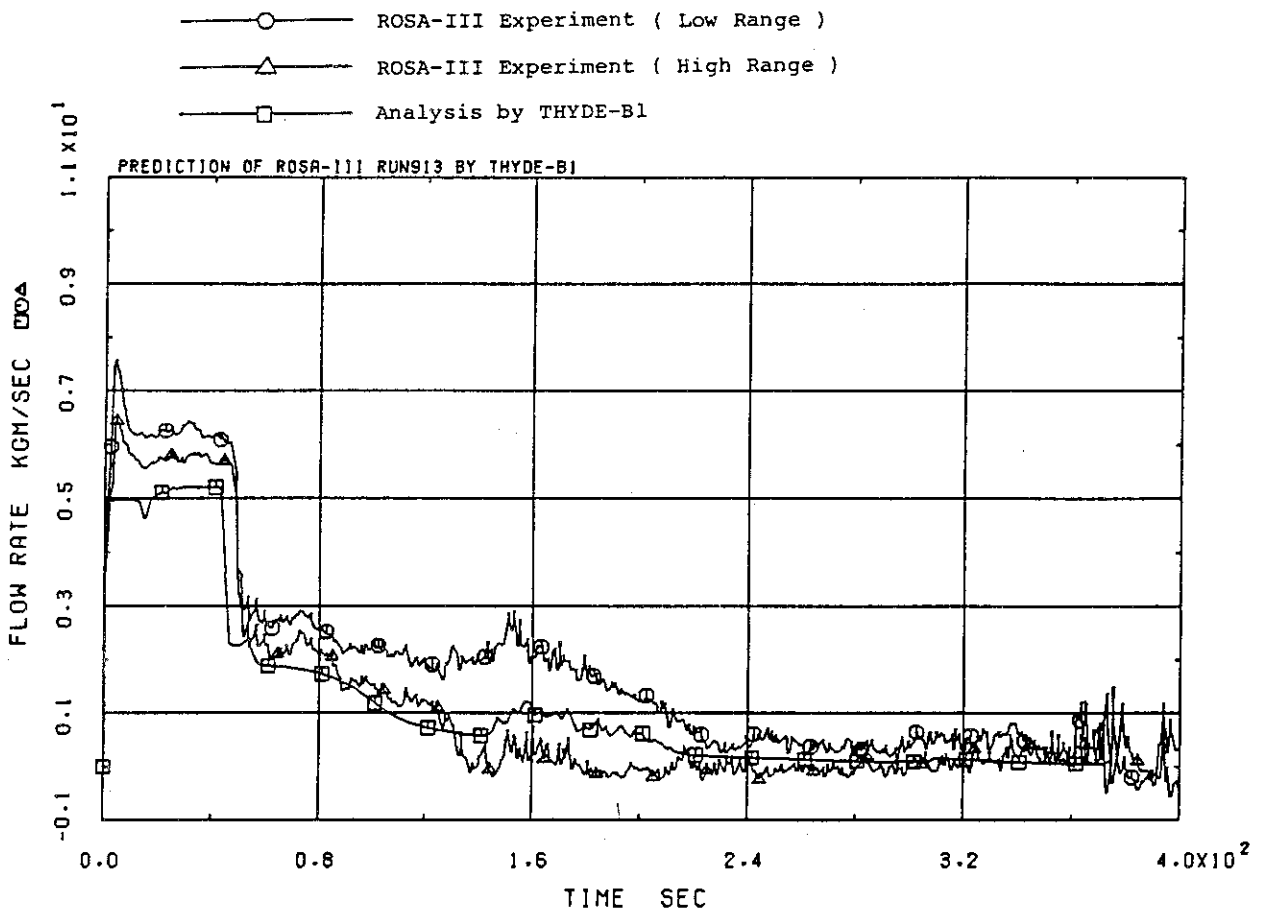


Fig. 4.7 Measured vs. calculated break flow rates - 15 % break test

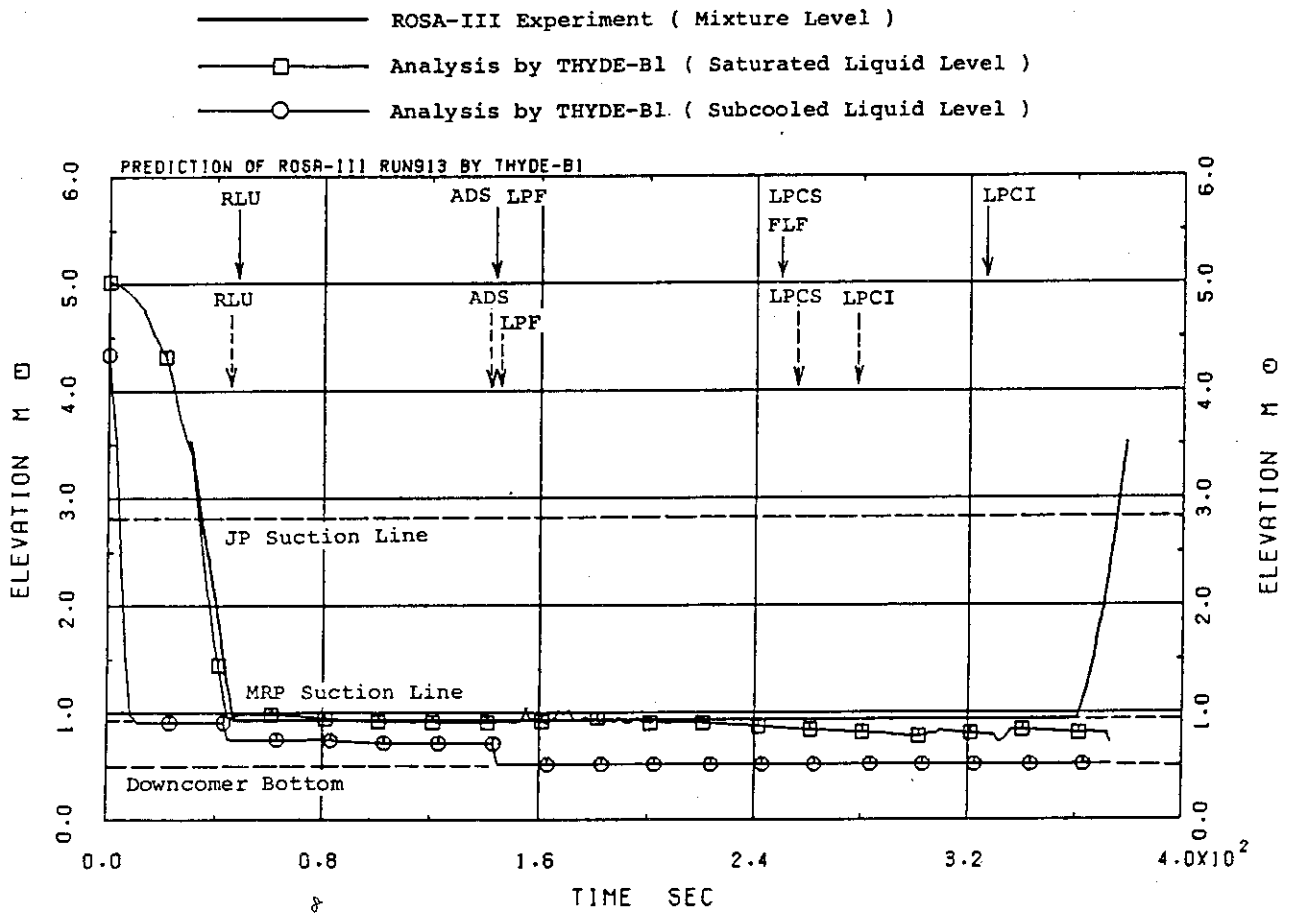


Fig. 4.8 Measured vs. calculated downcomer mixture levels - 15 % break test

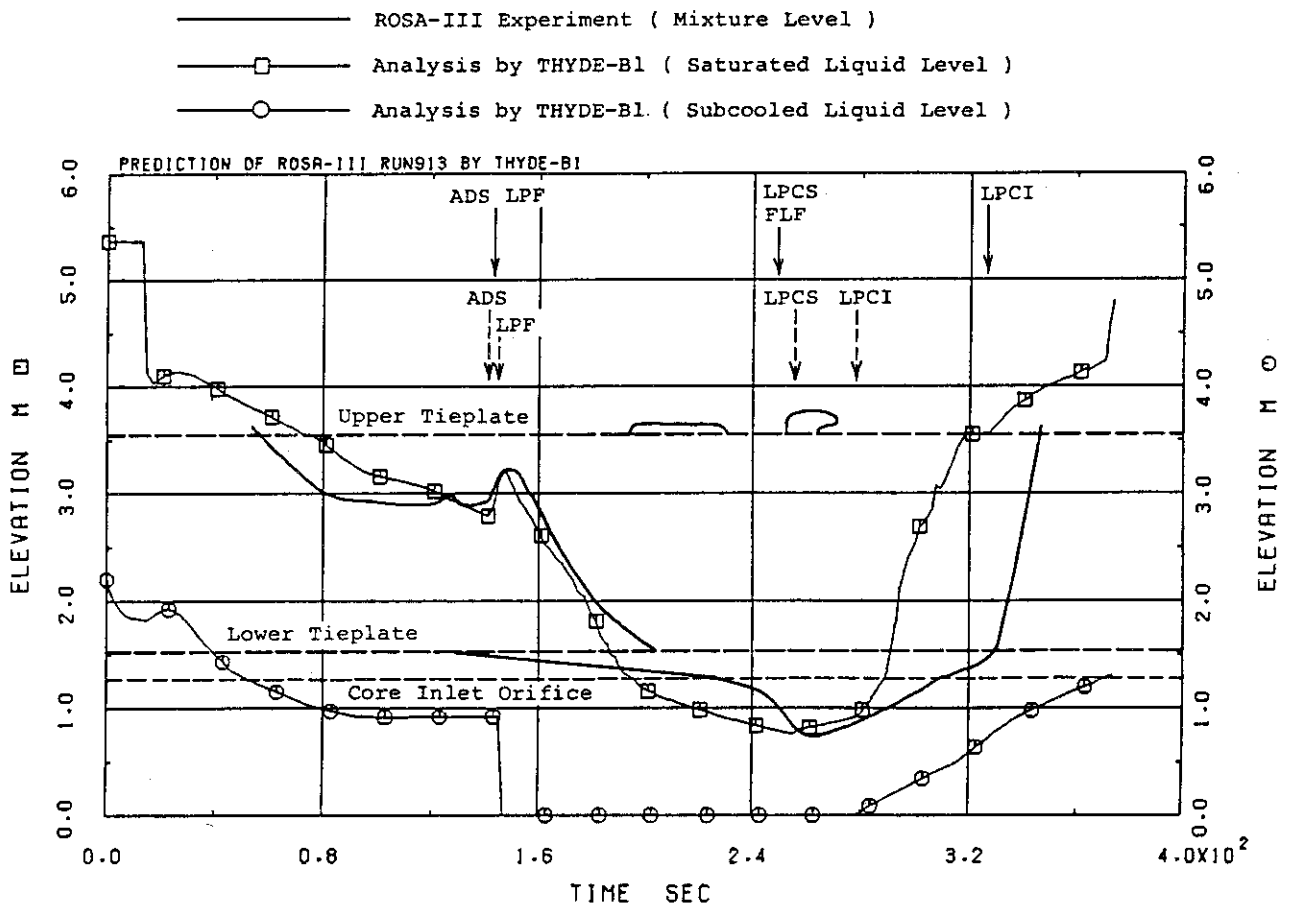


Fig. 4.9 Measured vs. calculated core mixture levels - 15 % break test

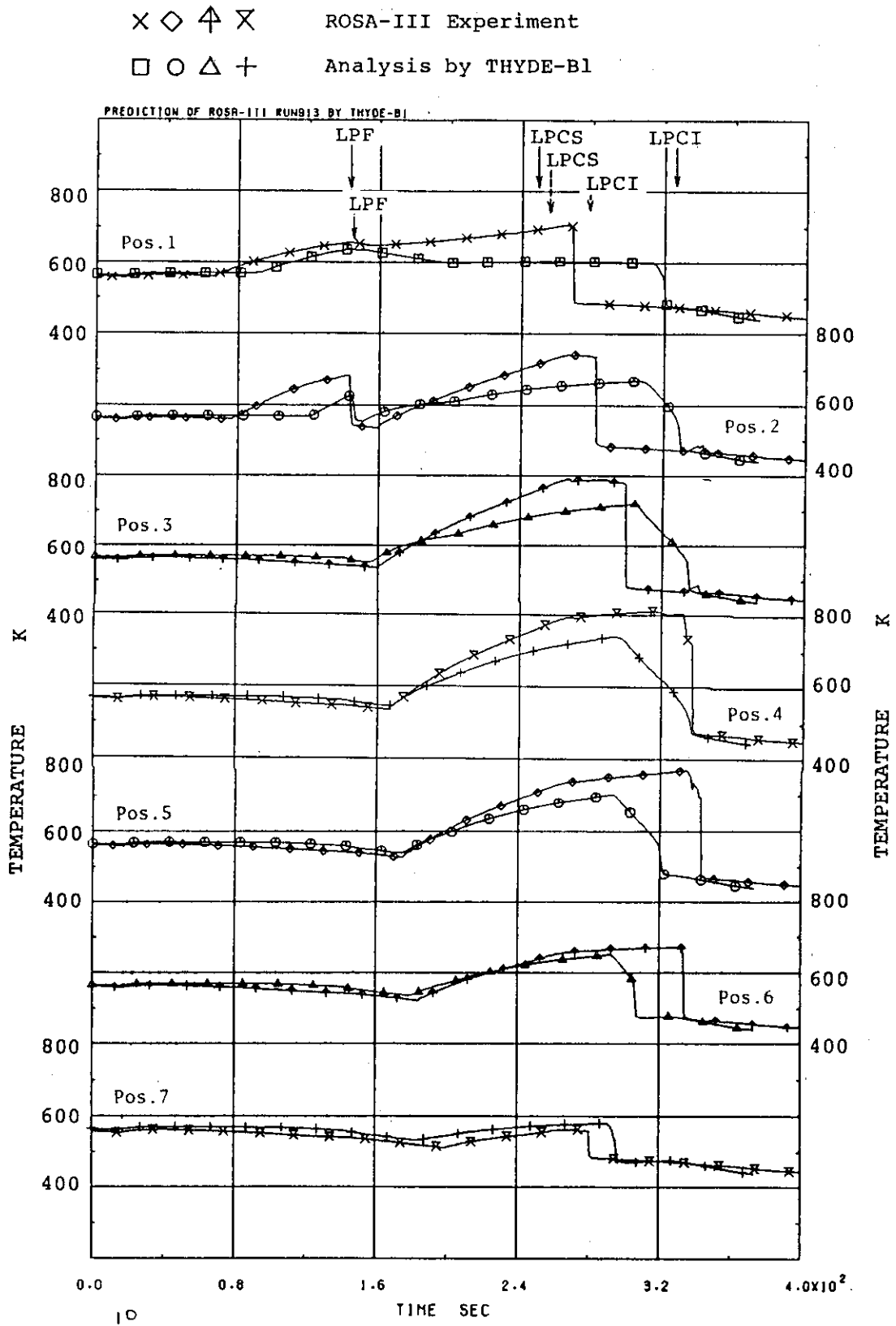


Fig. 4.10 Measured vs. calculated peak-power rod temperatures - 15 % break test



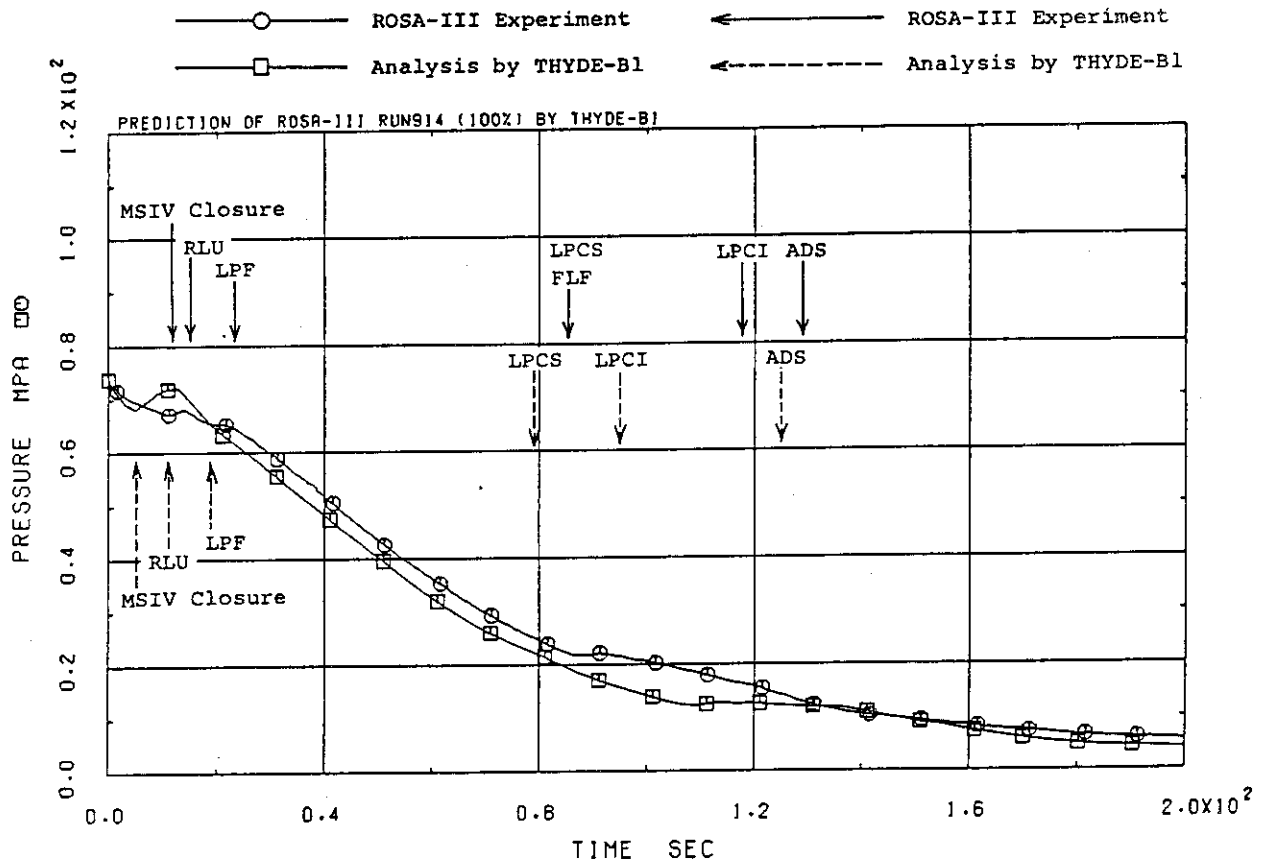


Fig. 4.11 Measured vs. calculated system pressures - 100 % break test

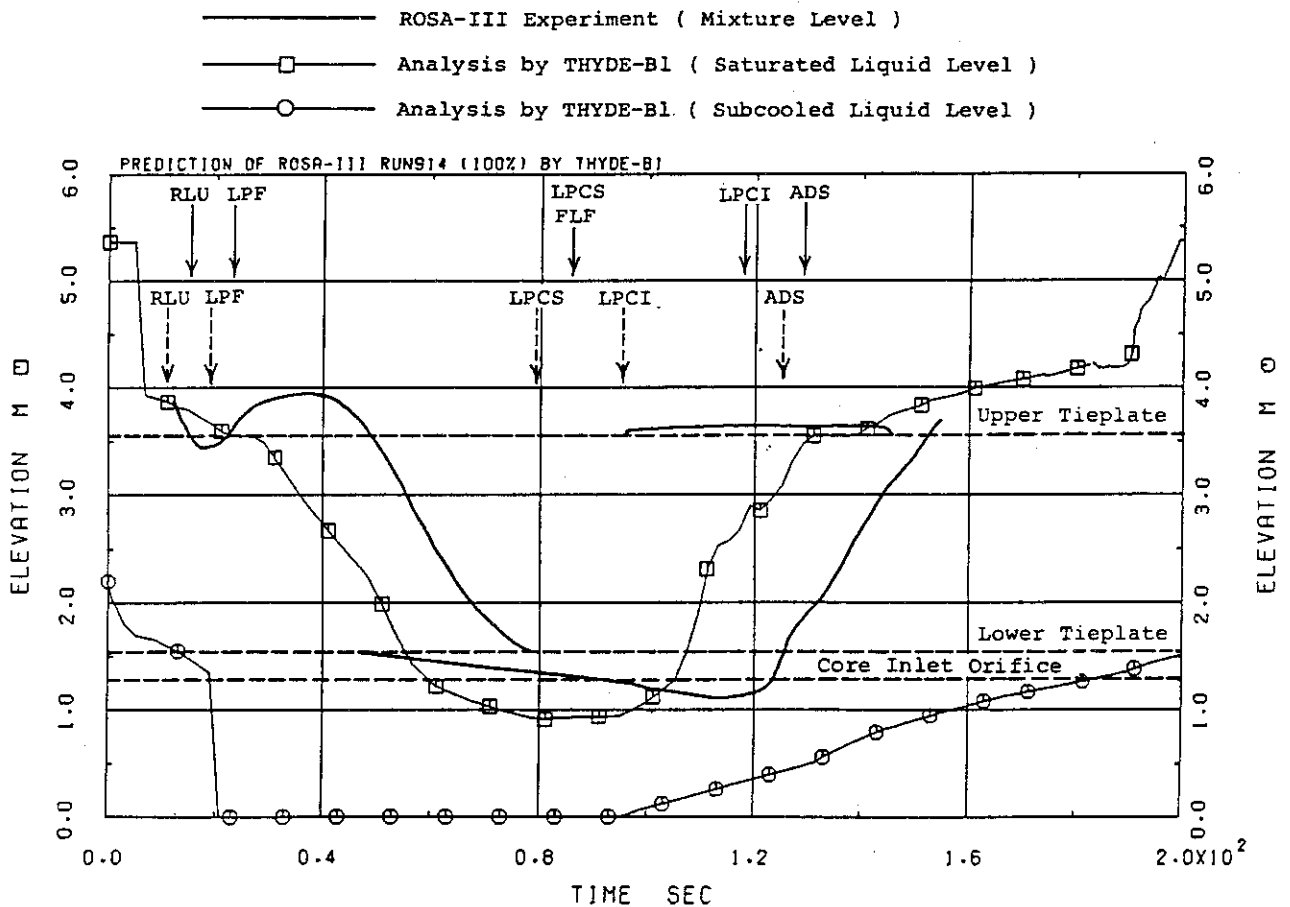


Fig. 4.12 Measured vs. calculated core mixture levels - 100 % break test

× ◇ ↑ × ROSA-III Experiment  
 □ ○ △ + Analysis by THYDE-B1

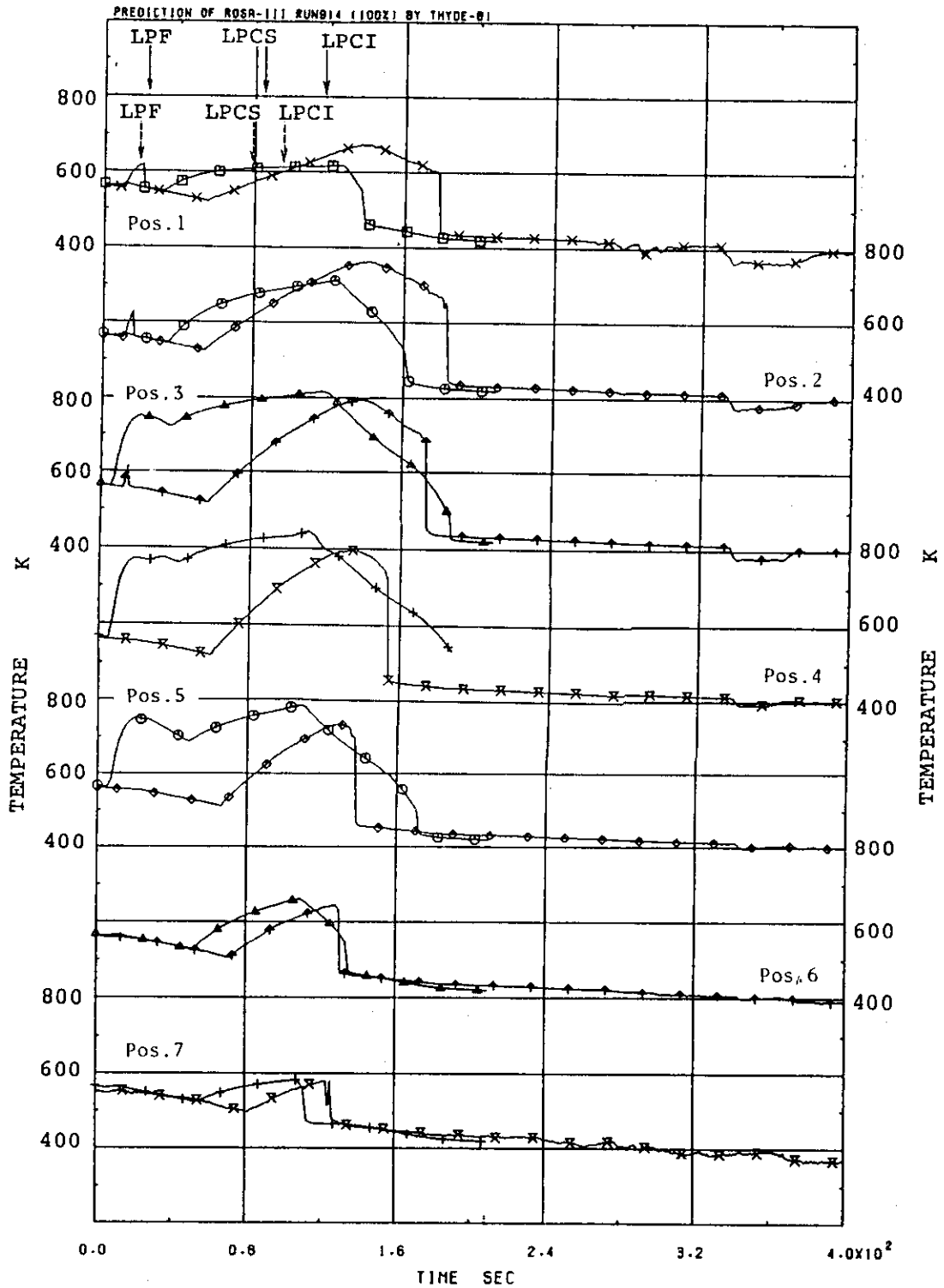


Fig. 4.13 Measured vs. calculated peak-power rod temperatures - 100 % break test

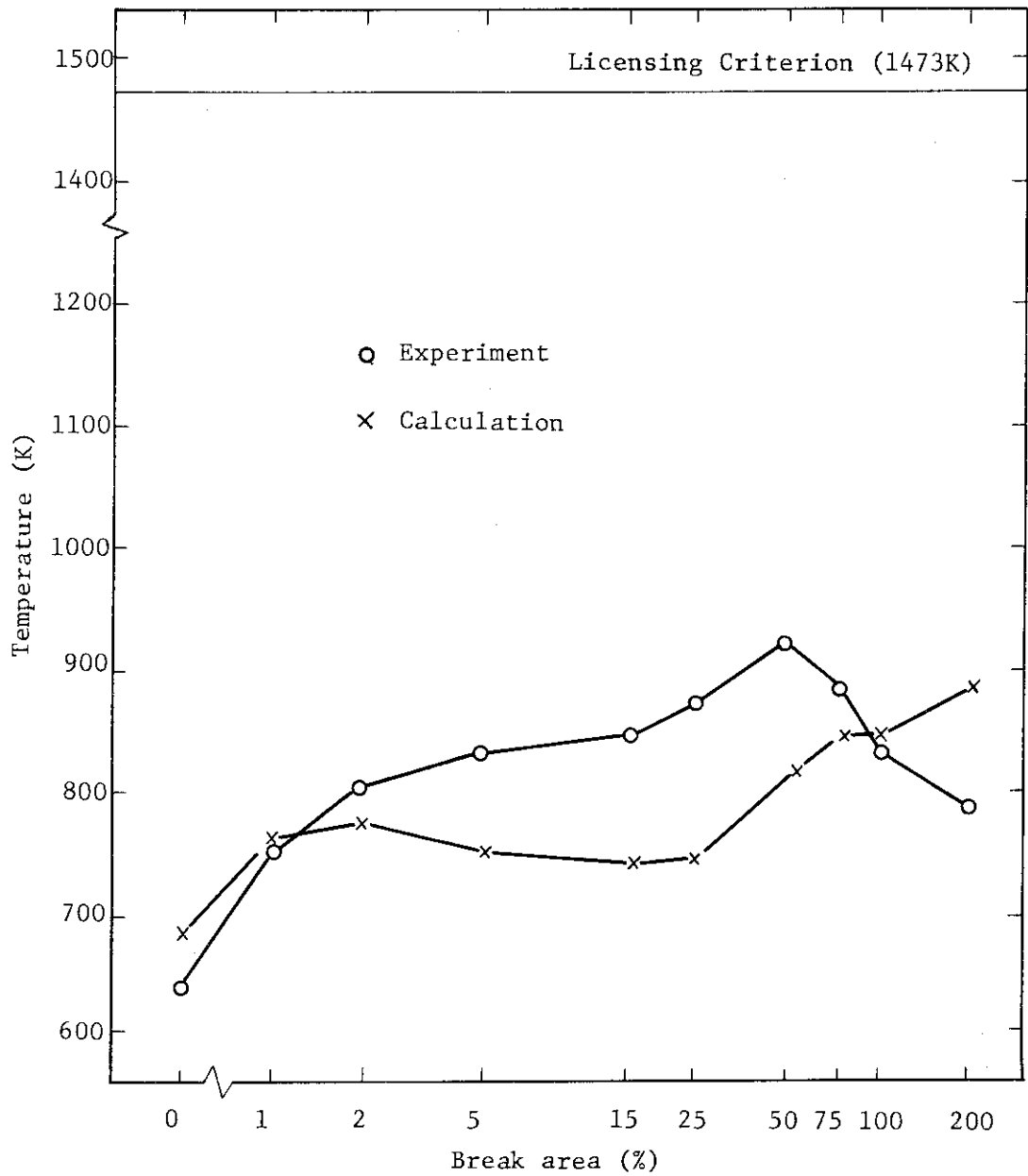


Fig. 4.14 Measured vs. calculated peak cladding temperatures for all tests

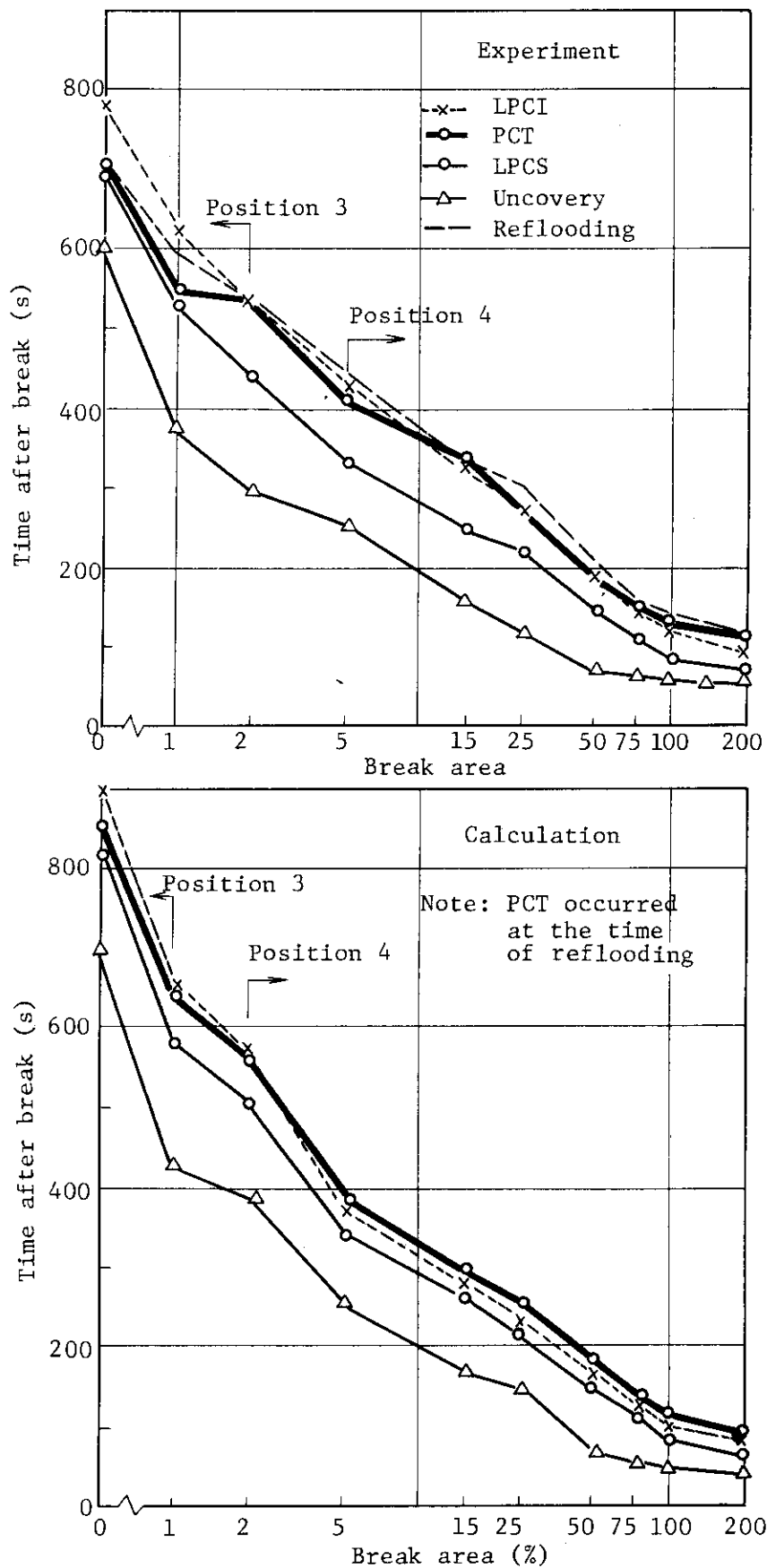


Fig 4.15 Measured vs. calculated timings of PCT and initiation of ECC flows.

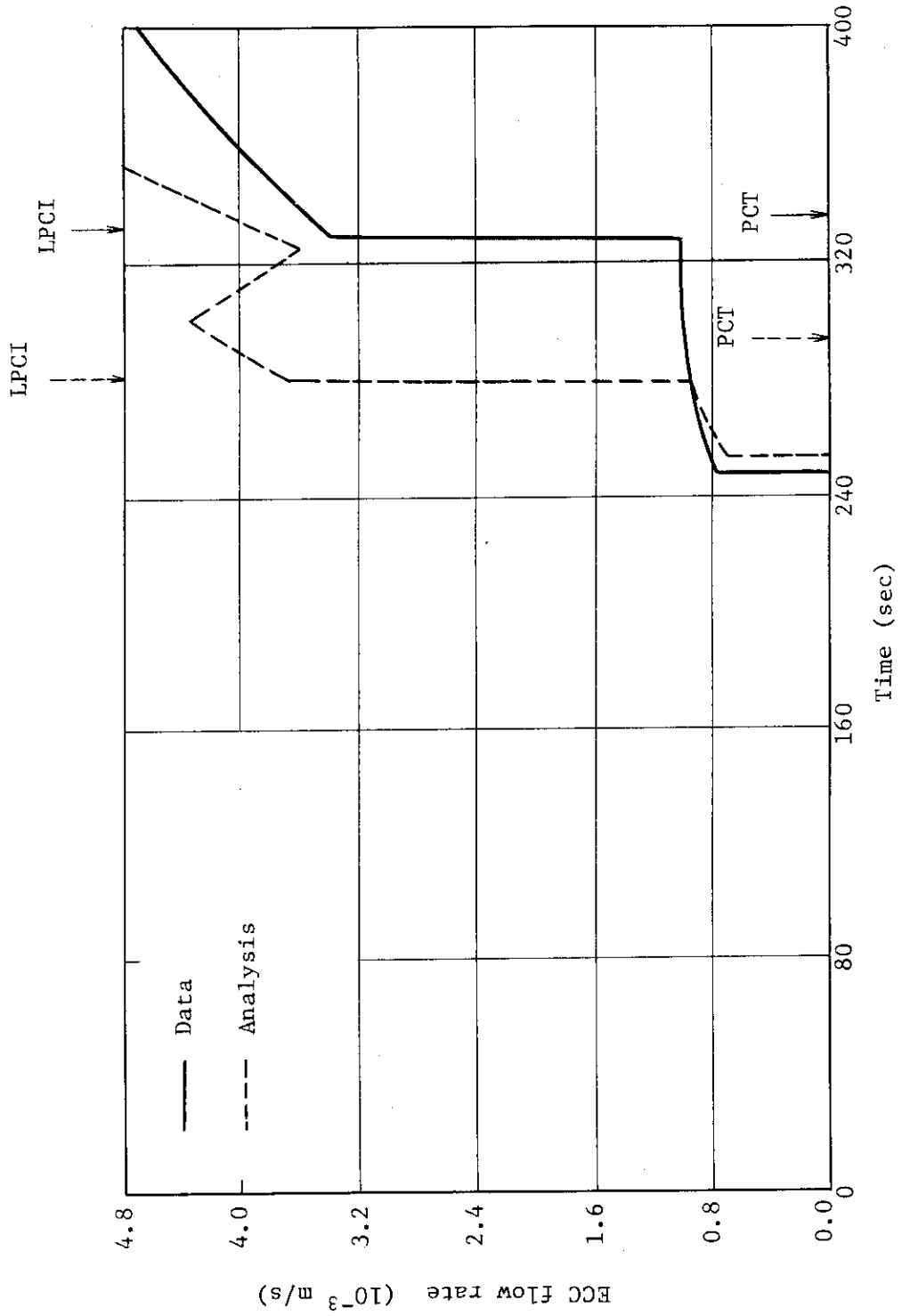


Fig. 4.16 Measured vs. calculated ECC flow rates - 15 % break test

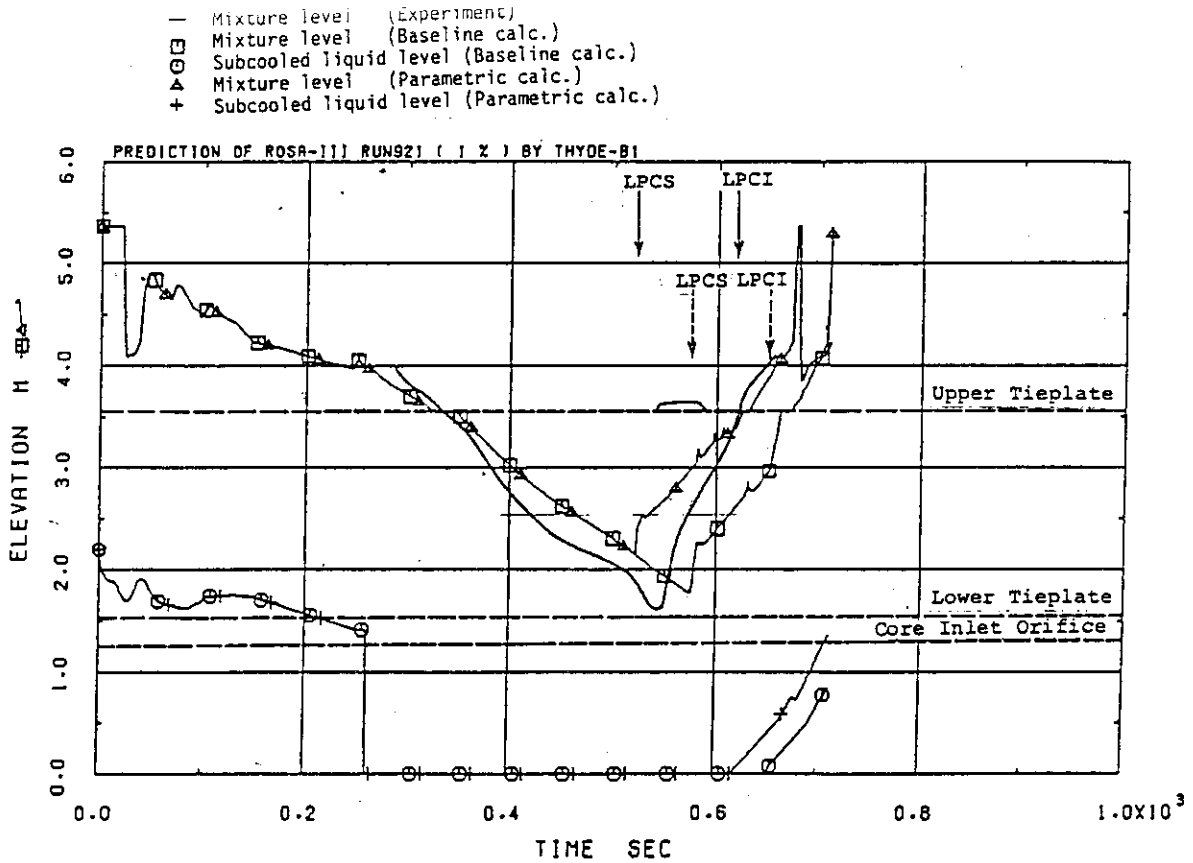


Fig. 4.17 Baseline vs. parametric calculations of core mixture level - 1 % break test

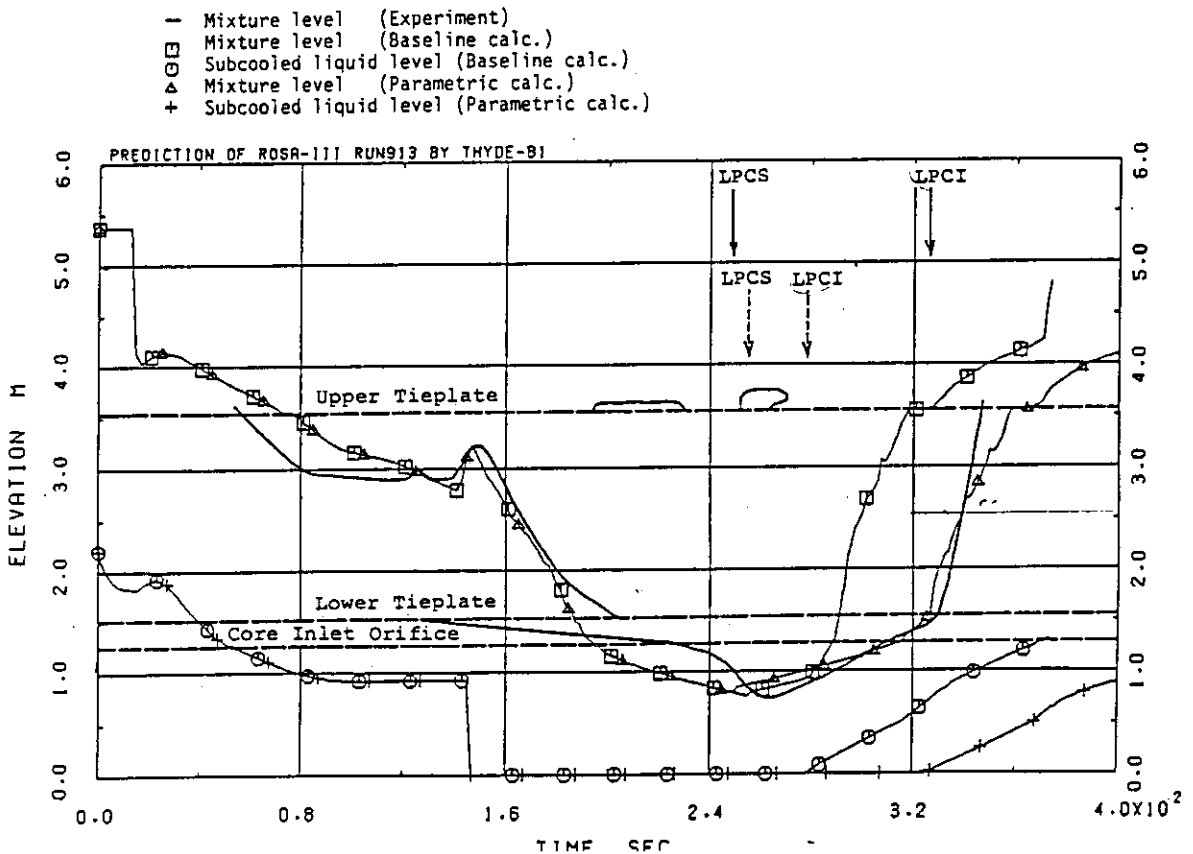


Fig. 4.18 Baseline vs. parametric calculations of core mixture level - 15 % break test

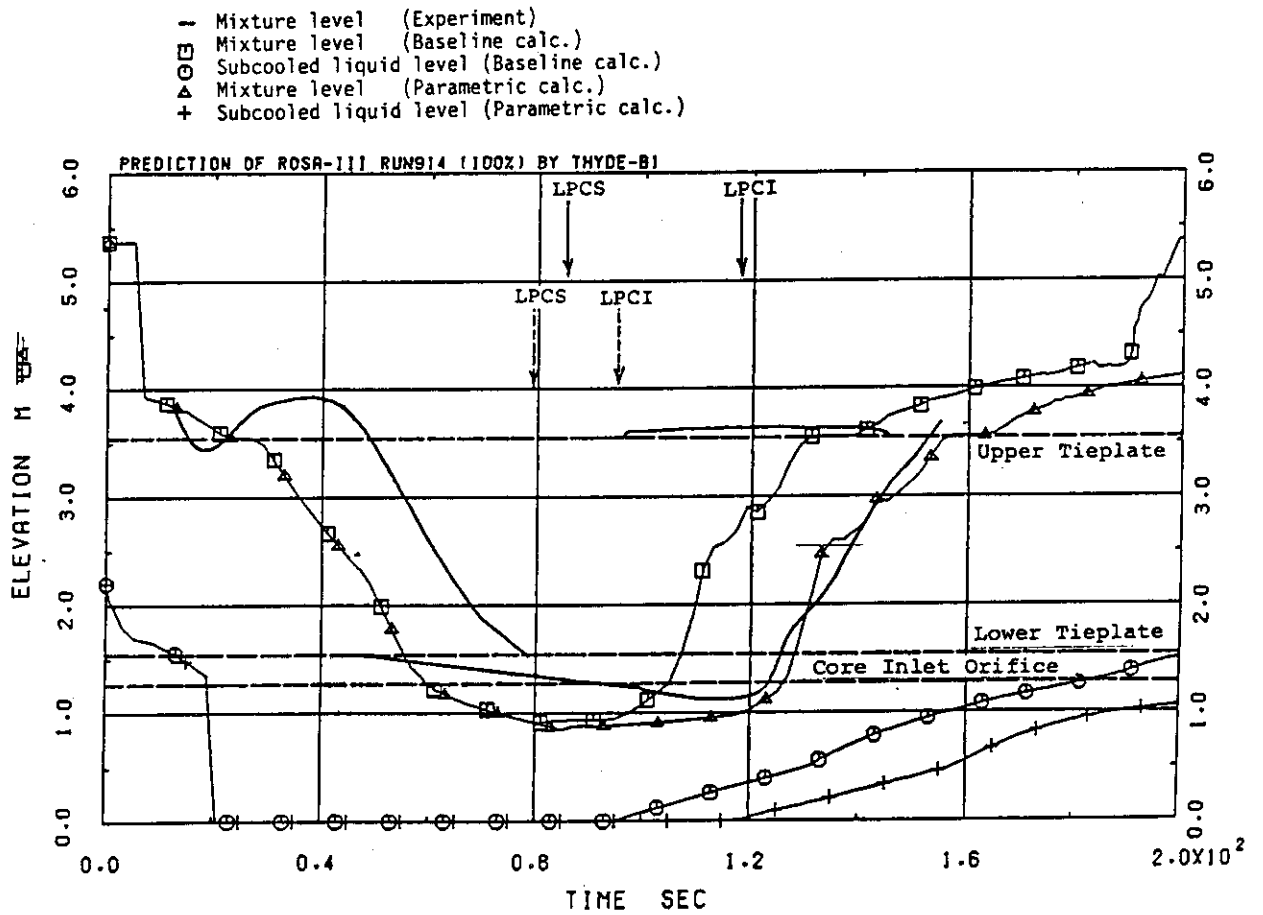


Fig. 4.19 Baseline vs. parametric calculations of core mixture level - 100 % break test

## 5. Conclusions

The calculational capability of the THYDE-B1/Mod 0 code was assessed against data from ten runs of ROSA-III recirculation line break LOCA tests. In these tests the size of break was changed parametrically from 0 to 200%, and the failure of the high pressure core spray system (HPCS) was simulated.

The THYDE-B1 code is a fast-running best-estimate code developed for prediction of BWR small- and intermediate-break LOCAs. The code's fast-running capability is obtained at the cost of modeling the potential, complicated thermal-hydraulic phenomena during a LOCA, e.g., nonuniform void distribution in the two-phase mixture, thermal nonequilibrium in the steam phase, and the counter-current flow limiting (CCFL) phenomenon at the core inlet and outlet. Thus, discrepancy was observed between the experimental and analytical results for the detailed system responses as follows:

- (1) The rate of the initial downcomer liquid level fall was underpredicted for the small break tests with break areas <5%. Since the downcomer level signal was used to trip on the automatic depressurization system (ADS), both in the experiment and calculation, the slower level decrease led to delayed operation of ADS, and hence delayed core uncovering in the calculation.
- (2) The break flow quality was underpredicted for the intermediate break tests with break areas between 5 and 50%, after the uncovering of the broken recirculation line inlet in the downcomer. This resulted in predicting slower system depressurization than the tests.
- (3) The in-vessel steam generation due to evaporation of the low pressure core spray (LPCS) water was generally underpredicted. This resulted in overpredicting the system depressurization rate after the initiation of the LPCS flow, predicting earlier initiation of the low pressure injection system (LPCI) flow, and hence predicting earlier reflooding than the experiment.
- (4) The height of core mixture level swell following the flashing in the lower plenum was generally underpredicted. This also resulted in underpredicting the in-vessel steam generation.
- (5) The CCFL phenomenon at the core inlet influenced the core fluid drainage for the large break tests. Without consideration of this phenomenon, the code predicted earlier core emptying than the experiment.



(6) The top-down quench, occurred in the tests at the core upper portion under the influence of the LPCS injection into the upper plenum, was not calculated because the code does not account for the direct contact between the falling ECCS water and the heater rods.

(7) Core temperature excursion occurred in the tests only after the dryout of the heater rod surface had occurred. However, the code predicted early DNB for the large breaks (larger than 50% in area). This resulted from underprediction of the core flow.

(8) The rod surface heat transfer after the dryout was generally over-predicted, since the code assumes that steam is always at the saturation temperature.

Despite the above-mentioned discrepancies between the experimental and analytical results for the detailed system response, the comparisons showed that the THYDE-B1 code has capability to reproduce major system response for a wide range of break size. The time-dependent behavior of the system pressure, core mixture level, and rod surface temperature were reproduced by the code qualitatively. The peak cladding temperature (PCT) was well calculated for the small break tests, whereas considerably lower PCTs than the measurements were predicted for the intermediate break tests.

Good understanding has been obtained of the capability of the THYDE-B1 code through the assessment made in this report. This provides a basis for the study of applicability of the ROSA-III test results to an actual BWR, to be made using the THYDE-B1/Mod 0 or later versions to predict the response of a BWR during a LOCA. The present results also provides basis for the future improvement of the code. It is recommended that updates be made particularly for the models for steam cooling, core flow, and in-vessel evaporation of ECC water and flashing.

## Acknowledgment

The authors are grateful to K. Muramatsu for his valuable advices in conducting THYDE-B1 calculations.

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- (9) Moore K.V. et al., "RELAP4 - a Computer Program for Transient Thermal-Hydraulic Analysis", ANCR-1127 (1973)

## Acknowledgment

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- (9) Moore K.V. et al., "RELAP4 - a Computer Program for Transient Thermal-Hydraulic Analysis", ANCR-1127 (1973)

APPENDIX

Appendix A THYDE-B1 Input Data for the 15% Break Test

```

-----1-----2-----3-----4-----5-----6-----7-R-----8
NO.1      MODULE NAME RUN913H          BLOCKS      14
          LEVEL      1          DATE      83.07.19  TIME      09.59.46
          ***** APPOINTED MODULE INFORMATION *****
          LEVEL      1          DATE      83.07.19  TIME      09.59.46

PREDICTION OF ROSA-III RUN913 BY THYDE-B1          00000100
/*****
/**      BEST ESTIMATE CALCULATION          **      00000200
/**      1983.07.08      BY IRIKO          **      00000300
/**      UPDATED      1983.07.14          **      00000400
/**      **      00000500
/**      **      00000600
/**      + CONSIDERATION OF CHANNEL BOXES HEAT CAPACITY **      00000700
/**      + CONSIDERATION OF FILLER BLOCK HEAT CAPACITY **      00000800
/**      + CONSIDERATION OF CONTROL ROD HEAT CAPACITY **      00000900
/**      + RNJUNC = 9.6E+5 ( JP-THROAT ) **      00001000
/*****
000 /*      PLOT , RESTART CONTROL OPTION          00001100
/*      NREST IDUMP IDPLOT ISPL          00001200
      0      1      1      1          00001300
      00001400
001 /PROBLEM DIMENSION          00001500
/*      NVOL NJUN NPMP NJG NJP NST NLK NFIL NHPI NLPI NCS NTRP NSEP          00001600
      6      19      2      2      1      0      4      1      0      1      2      14      1          00001700
/*      NTMAX          00001800
      6          00001900
003 / TIME STEP CONTROL DATA          00002000
/*      NRST NPRINT NPLOTT DELT TMAX          00002100
      5000      1      1      0.001      0.004          00002200
      5000      200      20      0.001      0.2          00002300
      5000      500      100      0.002      1.0          00002400
      10000      10000      1000      0.002      180.          00002500
      50000      50000      500      0.003      500.          00002600
      5000      10000      500      0.003      510.          00002700
/*          00002800
004 / VOLUME DATA ( 6 VOLUMES )          00002900
/* CARD1 IHOMO          00003000
/* CARD2 PRES ZMAX ZELEV ZPRES VMAX          00003100
/* CARD3 X AREA ( FOR HOMOGENEOUS NODE ONLY )          00003200
/* CARD4 ENTN(1) ALPHA          00003300
/* CARD5 ZLEV(1) ZLEV(2)          00003400
/* CARD6 CAS CLM          00003500
/* HP1 HP2          00003600
/* CARD8 NTV          00003700
/* CARD9 Z-VOL TABLE          00003800
/* CARD10 NTA          00003900
/* CARD11 Z-A TABLE          00004000
/* CARD12 NTD          00004100
/* CARD13 Z-DH TABLE          00004200
/*          00004300
/* NODE1 ( SHROUD INSIDE )          00004400
      2          /CARD1          00004500
      742677.      5.365      0.      0.      0.5344      /CARD2          00004600

```

```

-----*-----1-----*-----2-----*-----3-----*-----4-----*-----5-----*-----6-----*-----7-R-----*-----8
      293.6      0.46
      2.2        5.365
      0.         1.0         0.0         5.365
/* CARD 8      NUMBER OF POINTS IN ELEV-VOL TABLE
      10
/* CARD 9      ELEVATION - VOLUME TABLE
      0.         0.
      0.497      0.1168
      1.354      0.2235
      3.589      0.3795
      3.744      0.4050
      4.243      0.5031
      4.578      0.5095
      4.654      0.5109
      5.099      0.5291
      5.365      0.5344 /
/*
/*
/* CARD 10     NUMBER OF POINTS IN ELEVATION AREA TABLE
      2
/* CARD 11     ELEVATION - AREA TABLE
      0.   0.04   5.365   0.04 /
/* CARD 12     NUMBER OF POINTS IN ELEV-DH TABLE
      8 /
/* CARD 13     ELEVATION - HYDRUALIC DIAMETER TABLE
      0.         0.032      1.284   0.032
      1.294      0.0132     3.551   0.0132
      3.561      0.499      4.254   0.499
      4.264      0.1688     5.365   0.1688 /
/* NODE2      (SHROUD OUTSIDE)
      2
      737590.    5.5         0.494   0.         0.7111 /CARD1
      293.6     0.001
      3.83      4.506 /CARD2
      -10.     0.0         3.406   5.5 /CARD4
/* CARD 7     ELEVATION-VOLUME TABLE POINT NUMBER /CARD5
      13 / /CARD6
/* CARD 8     ELEVATION-VOLUME TABLE
      0.         0.
      0.89       0.0200
      1.025     0.02897
      2.861     0.0707
      3.756     0.1424
      3.919     0.1822
      4.084     0.2253
      4.16      0.2442
      4.321     0.2826
      4.421     0.3111
      4.649     0.3886
      4.871     0.4684
      5.5       0.7111
/*
/*
      10
      0.         .0235      2.861     .0235      2.862     .0783
      3.754     .0783      3.755     .2288      3.918     .2288
      3.919     .3225      5.153     .3225      5.154     .3505
      /CARD9
      00004700
      00004800
      00004900
      00005000
      00005100
      00005200
      00005300
      00005400
      00005500
      00005600
      00005700
      00005800
      00005900
      00006000
      00006100
      00006200
      00006300
      00006400
      00006500
      00006600
      00006700
      00006800
      00006900
      00007000
      00007100
      00007200
      00007300
      00007400
      00007500
      00007600
      00007700
      00007800
      00007900
      00008000
      00008100
      00008200
      00008300
      00008400
      00008500
      00008600
      00008700
      00008800
      00008900
      00009000
      00009100
      00009200
      00009300
      00009400
      00009500
      00009600
      00009700
      00009800
      00009900
      00010000
      00010100
      00010200
      00010300

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-----1-----2-----3-----4-----5-----6-----7-R-----8
      5.5      .3505      /CARD10      00010400
      10
      0.      .0283      2.861      .0283      2.862      .0920      00010500
      3.754      .0920      3.755      .4220      3.918      .4220      00010600
      3.919      .6437      5.153      .6437      5.154      .6727      00010700
      5.5      .6727      /CARD11      00010800
/* NODE3 ( BROKEN PIPE )
      1
      737525.  1.489      -0.526      0.      .01303      /CARD1      00010900
      293.6    2.1E-3      /CARD2      00011000
/* NODE4 ( PIPE FROM PUMP OUTLET TO JETPUMPS(BROKEN SIDE))
      1
      793967.  5.852      -2.526      0.      0.04050      /CARD1      00011100
      293.6    1.98E-3      /CARD2      00011200
/* NODE5 (PIPE FROM VESSEL TO PUMP (INTACT SIDE))
      1
      738765.  3.197      -2.235      0.      0.01057      /CARD1      00011300
      293.6    2.18E-3      /CARD2      00011400
/* NODE6 (PIPE FROM PUMP TO JET PUMP (INTACT SIDE))
      1
      791644.  5.851      -2.526      0.      0.03006      /CARD1      00011500
      293.6    2.03E-3      /CARD2      00011600
/*
      /CARD3      00011700
005 / JUNCTION DATA
/* CARD1 NIN      NOUT      IPUMP      IVALVE      WIJ      ZIN      00011800
/*      ZOUT      AJUNC      INERTA      RJUNC      RNJUNC      00011900
/*
/* J1 (STEAM SEPARATOR)
      1      2      -1      0      17.2      5.365      00012000
      4.871      1.496E-2  426.      0.      0.      /      00012100
/*      4.871      1.496E-2  213.      0.      0.      /      00012200
/* J2 (DOWNCOMER - BROKEN PIPE)
      2      3      0      0      3.4      0.444      00012300
      1.464      1.923E-3  3108.      0.      0.      /      00012400
/*      1.464      1.923E-3  1554.      0.      0.      /      00012500
/* J3 (BROKEN PIPE - PUMP)
      3      4      1      0      3.4      0.025      00012600
/*      2.025      1.923E-3  6673.      0.      0.      /      00012700
      2.025      1.923E-3  13346.      0.      0.      /      00012800
/* J4 (JET PUMP DRIVE FLOW (BROKEN SIDE))
      4      0      0      0      3.4      5.267      00012900
      0.      1.110E-4  6968.      0.      0.      /      00013000
/*      0.      1.110E-4  3484.      0.      0.      /      00013100
/* J5 (JET PUMP THROAT FLOW (BROKEN SIDE))
      0      1      0      0      8.6      0.      00013200
      0.4      1.785E-3  2830.      0.      9.6E+5      /      00013300
/*      0.4      1.785E-3  1415.      0.      0.      /      00013400
/* J6 (JET PUMP SUCTION FLOW (BROKEN SIDE))
      2      0      0      0      5.2      2.247      00013500
      0.      1.674E-3  1776.      0.      0.      /      00013600
/*      0.      1.674E-3  888.      0.      0.      /      00013700
/* J7 (DOWNCOMER - PIPE (INTACT SIDE))
      2      5      0      0      3.4      0.444      00013800
      3.173      1.923E-3  3312.      0.      0.      /      00013900
/*      3.173      1.923E-3  1656.      0.      0.      /      00014000
/* J8 ( PUMP SUCTION (INTACT SIDE))
      5      6      2      0      3.4      0.      00014100
      00014200
      00014300
      00014400
      00014500
      00014600
      00014700
      00014800
      00014900
      00015000
      00015100
      00015200
      00015300
      00015400
      00015500
      00015600
      00015700
      00015800
      00015900
      00016000

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-----*-----1-----*-----2-----*-----3-----*-----4-----*-----5-----*-----6-----*-----7-R-----*-----8
/* J9      0.291      1.923E-3  9000.      0.      0.      / 00016100
(JET PUMP DRIVE FLOW (INTACT SIDE))
6          0          0          0          3.4      5.267    / 00016200
0.         1.110E-4  15072.     0.         0.         / 00016300
/*         0.         1.110E-4  7536.      0.         0.         / 00016400
/* J10     (JET PUMP THROAT (INTACT SIDE))
0          1          0          0          8.6      0.       / 00016500
0.4       1.785E-3  2828.      0.         9.6E+5    / 00016600
/*         0.4       1.785E-3  1414.      0.         0.         / 00016700
/* J11     (JET PUMP SUCTION (INTACT SIDE))
2          0          0          0          5.2      2.247    / 00016800
0.         1.674E-3  1772.      0.         0.         / 00016900
/*         0.         1.674E-3  886.       0.         0.         / 00017000
/* J12     (HPCS (CS NO.1))
-4         1          1          0          0.        0.       / 00017100
4.099     0.          0.          0.         0.        0.       / 00017200
/* J13     (LPCS (CS NO.2))
-4         1          2          -2         0.        0.       / 00017300
4.099     0.          0.          0.         0.        0.       / 00017400
/* J14     (LPCI (LPCI NO.1))
-3         1          1          -3         0.        0.       / 00017500
0.1       0.          0.          0.         0.        0.       / 00017600
/* J15     (ADS (LEAK NO.1))
2          -1         1          0          0.        5.50     / 00017700
0.         1.885E-4  0.          0.         0.        0.       / 00017800
/* J16     (BREAK (LEAK NO.2))
3          -1         2          0          0.        0.025    / 00017900
0.         8.012E-5  0.          0.         0.        0.       / 00018000
/* J17     (SRV (LEAK NO.3))
2          -1         3          0          0.        5.5      / 00018100
0.         5.16E-4  0.          0.         0.        0.       / 00018200
/* J18     (FW (FILL NO.1))
-1         2          1          0          2.04     0.       / 00018300
3.839     0.          0.          0.         0.        0.       / 00018400
/* J19     (MSL (LEAK NO.4))
2          -1         4          1          2.04     5.5      / 00018500
0.         3.1416E-4  0.          0.         0.        0.       / 00018600
/*
/*
006 / JET PUMP JUNCTION GROUP
/* CARD1 JMOPT IJPUMP JETGRP(1) (2) (3) PIN /00020100
/* GROUP1 (BROKEN SIDE)
2          1          6          4          5          721219. /00020200
/* GROUP2 (INTACT SIDE)
2          1          11         9          10         721475. /00020300
/*
007 / JET PUMP GEOMETRY DATA CARD
/* CARD1 AS AD AJ ADIF DL1 DL2 /00020400
/* DL3 AJS AJD AJJ /00020500
4.743E-4  1.108E-4  5.851E-4  1. 0.1 0.285 /00020600
1.956 1. 1. 1. /00020700
008 / RECIRCULATION PUMP DATA
/* CARD1 TPCON HO QO XNO FX XKSP /00020800
/* INTACT SIDE
4.718 57670. 3.4 197. 0. 0. /00020900
/* PUMP CHARACTERISTIC CURVE /00021000

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-----1-----2-----3-----4-----5-----6-----7-R-----8
/*          2          /CARD2          00021800
          9 0.          00021900
0.0          0.92          0.222          0.94          0.443          0.97          00022000
0.665          1.0          1.109          1.0          1.583          1.019          00022100
2.772          0.75          4.434          0.          10.E20          0.          00022200
          2          0.025          00022300
0.0          0.0          1.E20          0.0          /          00022400
/* CARD1 TPCON          HO          QO          XNO          FX          XKSP          00022500
          4.718          58609.          3.4          202.          0.          0.          /          00022600
/* PUMP CHARACTERISTIC CURVE          00022700
/*          2          /CARD2          00022800
          9 0.          00022900
0.0          0.92          0.222          0.94          0.443          0.97          00023000
0.665          1.0          1.109          1.0          1.583          1.019          00023100
2.772          0.75          4.434          0.          10.E20          0.          00023200
          2          0.025          00023300
0.0          0.0          1.E20          0.0          /          00023400
/*          00023500
/*          00023600
/* PUMP 2          00023700
010 / LEAK DATA          00023800
/* CARD1 ICHOKE          SINK PR.          CONCO          ZLEAK          HLEAK          00023900
/*          ICHOKE=-3          TIME-FLOW TABLE          00024000
/*          ICHOKE=-2          00024100
/*          ICHOKE=-1          PRESSURE FLOW TABLE          00024200
/*          00024300
/*          00024400
/*          00024500
/*          00024600
/* CARD1(PS)          CONC1          TRNQL          (THIS CARD IS USED ONLY WHEN ICHOKE=2)          00024700
/* CARD2          NFAT          00024800
/* CARD3          TABA(1)          ---TABA(2*NFAT)          00024900
/*          00025000
/* LEAK 1 (ADS          JUNC.15)          00025100
/*          CHOKED FLOW LEAK DATA FOR BASE CASE          00025200
          1          1.E4          0.6          5.4          0.1          /          00025300
          3          /          00025400
          0.          0.          .1          1.          2000.          1.          /          00025500
/*          00025600
/* LEAK 2 (BREAK          JUNC.16)          00025700
          2          1.E4          0.6          0.025          0.          /          00025800
          0.61          0.02          /          00025900
          3          /          00026000
          0.          0.          0.1          1.          2000.          1.          /          00026100
/* LEAK 3 (SRV          JUNC.17)          00026200
          -1          1.E4          1.          5.4          0.1          /          00026300
          4          /          00026400
          0.          0.          810000.          0.          820000.          2.          00026500
          1406142.          6.          /          00026600
/*          0.          0.          828218.          0.          828921.          2.128          00026700
/*          843123.          2.128          843137.          4.867          857044.          4.867          00026800
/*          857184.          6.044          1406142.          6.044          /          00026900
/* LEAK 4 (MSL          JUNC.19)          00027000
/*          00027100
          1          1.E4          0.6          5.4          0.1          /          00027200
          3          /          00027300
          0.          1.          0.1          1.          2000.          1.          /          00027400

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-----1-----2-----3-----4-----5-----6-----7-R-----8
/*
011 / FILL 00027500
/* CARD1 CGL CML FEG FEM 00027600
/* CARD2 NT 00027700
/* CARD3 T DR H TABLE 00027800
/* CARD4 NW 00027900
/* CARD5 W TABLE 00028000
/* FILL 1 (FEED WATER JUNC.18) 00028100
0.1 0. 1. 1. / COMPLETE MIXING / 00028200
/* 0.1 1. 0. 0. /COMPLETE NO-MIXING 00028300
/* 0.1 0. 0. 1. /MIXING IN MIXTURE 00028400
/* NOMIXING IN VAPOR SUB NODE 00028500
0 00028600
221.4 00028700
/* TIME-FLOW TABLE FOR BASE CASE 00028800
-4 00028900
0. 2.04 2.0 2.04 4.0 0.0 00029000
2000.0 0.0 / 00029100
/* 00029200
/* LPCI (JUNC.14) 00029300
013 / LPCI 1. 0.2 0. 1. / 00029400
0 / 00029500
40. / 00029600
/* 00029700
/* PRESSURE DEPENDENT FLOW TABLE 00029800
7 00029900
0. 4.3 5.E4 4.2 10.E4 4. 00030000
15.E4 3.2 20.E4 1.4 22.E4 0. 00030100
100.E4 0. / 00030200
/* P-W TABLE END 00030300
/* 00030400
014 / CORE SPRAY 00030500
/* CS 1 (HPCS JUNC.12) 00030600
0.1 0. 1. 1. / 00030700
0 / 00030800
40. / 00030900
/* 00031000
/* P-W TABLE FOR BASE CASE 00031100
5 00031200
0. 0.82 45.E4 0.78 88.E4 0.25 / 00031300
89.E4 0. 100.E4 0. / 00031400
/* P-W TABLE END 00031500
/* 00031600
/* CS 2 (LPCS JUNC.13) 00031700
0.1 0. 1. 1. / 00031800
0 / 00031900
40. / 00032000
8 / 00032100
0. 1. 5.E4 0.98 15.E4 0.84 00032200
20.E4 0.74 30.E4 0.4 32.E4 0.3 00032300
33.E4 0. 1.E7 0. / 00032400
/* 00032500
015 / STEAM SEPARATOR EFFICIENCY 00032600
/* CARD1 NTAB 00032700
/* CARD2 TABLE 00032800
2 / 00032900
00033000
00033100

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-----1-----2-----3-----4-----5-----6-----7-R-----8
      0.      1.      10.      1.
/*
016 / TRIP CONTROL
/*CARD1 IDACT KSIG IV IPV SETP DELAY / 00033200
/* 00033300
/* 00033400
/* 00033500
/* 00033600
/* 00033700
      22      1      0      0      0.      0. /BREAK 00033800
      81      -3      2      0      4.264      1.E6 /HPCS 00033900
      82      -3      2      0      3.756      40. /LPCS 00034000
      71      -3      2      0      3.756      40. /LPCI 00034100
      21      -3      2      0      3.756      120. /ADS 00034200
      31      1      0      0      0.      0. /PUMP1 00034300
      32      1      0      0      0.      0. /PUMP2 00034400
     -101     -3      2      0      4.264      3. /MSIV 00034500
      23      1      0      0      0.      0. /SRV 00034600
      102     -2      2      0      220000.      0. /LPCS 00034700
      103     -2      2      0      160000.      0. /LPCI 00034800
/* DUMMY
     -101      1      0      0      10000.      0. 00034900
     -101      1      0      0      10000.      0. 00035000
     -101      1      0      0      10000.      0. 00035100
     -101      1      0      0      10000.      0. 00035200
/* 00035300
/* 00035400
017 /*** DIMENSION CARD FOR SLABS *** 00035500
/* NSLAB NGEOM NMATG NTVSNP NTALP 00035600
/* NOCOR NMAT MAXREG NTROD NTFUT 00035700
      22  16  9  8  0  4  45  0  0  0 00035800
/* 00035900
018 /*** HEAT SLAB DATA CARDS *** 00036000
/* NVSL NVSR IGEOM ZSLB HLSLB VOLS 00036100
/* AHTR HMDR DHER 00036200
      1      0      1      1.586      0.2350      2.894E-5      00036300
      0.009236      0.01438      0.01438 /SLAB1 CORE100036400
      1      0      1      1.821      0.2350      2.854E-5      00036500
      0.009236      0.01438      0.01438 /SLAB2 CORE200036600
      1      0      1      2.056      0.2350      2.854E-5      00036700
      0.009236      0.01438      0.01438 /SLAB3 CORE300036800
      1      0      1      2.291      0.4700      5.782E-5      00036900
      0.01847      0.01438      0.01438 /SLAB4 CORE400037000
      1      0      1      2.761      0.2350      2.894E-5      00037100
      0.009236      0.01438      0.01438 /SLAB5 CORE500037200
      1      0      1      2.996      0.2350      2.894E-5      00037300
      0.009236      0.01438      0.01438 /SLAB6 CORE600037400
      1      0      1      3.231      0.2350      2.894E-5      00037500
      0.009236      0.01438      0.01438 /SLAB7 CORE700037600
      1      0      2      0.      1.110      7.06E-5      00037700
      0.0314      0.02      0.02 /SLAB8 CABLE 1 00037800
      2      0      3      0.494      5.500      0.2920      00037900
      6.547      0.4025      0.4025 /SLAB9 00038000
      1      0      4      0.      0.517      0.3594      00038100
      1.5218      0.7000      0.7000 /SLB10 00038200
      1      0      1      1.586      0.2350      2.894E-5      00038300
      0.009256      0.01438      0.01438 /SLB11 CORE800038400
      1      0      1      1.821      0.2350      2.894E-5      00038500
      0.009236      0.01438      0.01438 /SLB12 CORE900038600
      1      0      1      2.056      0.2350      2.894E-5      00038700
      0.009236      0.01438      0.01438 /SLB13 COR1000038800
  
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-----1-----2-----3-----4-----5-----6-----7-R-----8
1      0      1      2.291  0.4700  5 .782E-5      00038900
0.01847  0.01438  0.01438  /SLB14 COR1100039000
1      0      1      2.761  0.2350  2.894E-5      00039100
0.009236  0.01438  0.01438  /SLB15 COR1200039200
1      0      1      2.996  0.2350  2.894E-5      00039300
0.009236  0.01438  0.01438  /SLB16 COR1300039400
1      0      1      3.231  0.2350  2.894E-5      00039500
0.009236  0.01438  0.01438  /SLB17 COR1400039600
1      0      6      1.11  1.587  5.64E-5      00039700
0.01839  0.02  /SLAB18 CABLE 2 00039800
1      0      5      1.159  2.391  1.555E-2      00039900
5.069  0.01227  0.01227 /SLAB19 C.B. 00040000
1      2      7      1.519  1.836  0.08329      00040100
2.9551  0.323  0.323      00040200
2.6648  0.323  0.323  /SLAB20 F.B. 00040300
1      0      8      0.0  0.2871  1.373E-2      00040400
1.7585  0.02425  0.02425 /SLAB21 L.P. 00040500
1      0      9      1.524  2.026  0.6697E-2      00040600
2.026  0.012  0.012  /SLAB22 C.R. 00040700
/*      00040800
/*      00040900
019  /*** CORE SECTION DATA CARDS ***      00041000
/* ISLB  IXSN  PSLB  X  TFCT      00041100
1  186  0.0399  1.0  0.0399  /CORE #01 00041200
2  186  0.0766  1.0  0.0766  /CORE #02 00041300
3  186  0.1039  1.0  0.1039  /CORE #03 00041400
4  186  0.2409  1.0  0.2409  /CORE #04 00041500
5  186  0.1039  1.0  0.1039  /CORE #05 00041600
6  186  0.0766  1.0  0.0766  /CORE #06 00041700
7  186  0.0399  1.0  0.0399  /CORE #07 00041800
11  62  0.0186  1.0  0.0186  /CORE #08 00041900
12  62  0.0358  1.0  0.0358  /CORE #09 00042000
13  62  0.0485  1.0  0.0485  /CORE #10 00042100
14  62  0.1125  1.0  0.1125  /CORE #11 00042200
15  62  0.0485  1.0  0.0485  /CORE #12 00042300
16  62  0.0358  1.0  0.0358  /CORE #13 00042400
17  62  0.0186  1.0  0.0186  /CORE #14 00042500
8  248  0.  1.  0.  /CABLE 1 00042600
18  248  0.  1.  0.  /CABLE 2 00042700
/*      00042800
020  /*** SLAB GEOMETRY DATA CARDS ***      00042900
/* JGOM  JREG      00043000
/* JGAP  (GAP INDEX)      00043100
/* JMAT  (MTERIAL INDEX)      00043200
/* JPNT  (NUMBER OF SPACE MESH)      00043300
/* WREG  (REGIO WIDTH)      00043400
/* DREG  (MATERIAL DENSITY)      00043500
/* PREG  (POWER FRACTION)      00043600
/* TREG  (WEIGHTING FACTOR FOR AVE. TEMP. CALC.)      00043700
/* SLAB GEOMETRY DATA SET NO. 1      00043800
2  4      00043900
0  0  0  0      00044000
3  2  3  4      00044100
3  1  1  1      00044200
0.002825  0.0007  0.00131  0.0013      00044300
1850.  8410.  1850.  8430.      00044400
0.0  1.0  0.0  0.0      00044500

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-----*-----1-----*-----2-----*-----3-----*-----4-----*-----5-----*-----6-----*-----7-R-----8
0.0          1.0          0.0          0.0          00044600
/* SLAB GEOMETRY DATA SET NO. 2          00044700
2          3          00044800
0          0          0          00044900
7          6          4          00045000
1          1          1          00045100
0.0025      0.001      0.001      00045200
8960.      2700.      8430.      00045300
1.0        0.0        0.0        00045400
1.0        0.0        0.0        00045500
/* SLAB GEOMETRY DATA SET NO. 3          00045600
1          1          00045700
0          00045800
5          00045900
4          00046000
0.03962    00046100
7910.      00046200
0.0        00046300
0.0        00046400
/* SLAB GEOMETRY DATA SET NO. 4          00046500
1          1          00046600
0          00046700
5          00046800
4          00046900
0.155      00047000
7910.      00047100
0.0        00047200
0.0        00047300
/* SLAB GEOMETRY DATA SET NO. 5 ( CHANNEL BOX ) 00047400
1          1          00047500
0          00047600
5          00047700
4          00047800
0.003      00047900
7910.      00048000
0.0        00048100
0.0        00048200
/* SLAB GEOMETRY DATA SET NO. 6          00048300
2          3          00048400
0          0          0          00048500
8          6          4          00048600
1          1          1          00048700
0.0034     0.001435    0.0013    00048800
8960.      2700.      8430.      00048900
1.0        0.0        0.0        00049000
1.0        0.0        0.0        00049100
/* SLAB GEOMETRY DATA SET NO. 7 ( FILLER BLOCK ) 00049200
1          1          00049300
0          00049400
5          00049500
4          00049600
0.0488     00049700
7910.      00049800
0.0        00049900
0.0        00050000
/* SLAB GEOMETRY DATA SET NO. 8 ( LOWER PLENUM STRUCTURE ) 00050100
1          1          00050200

```

```

-----*-----1-----*-----2-----*-----3-----*-----4-----*-----5-----*-----6-----*-----7-R-----*-----8
0 00050300
5 00050400
4 00050500
0.012 00050600
7910. 00050700
0.0 00050800
0.0 00050900
/* SLAB GEOMETRY DATA SET NO. 9 ( CONTROL ROD ) 00051000
1 1 00051100
0 00051200
5 00051300
4 00051400
0.006 00051500
7910. 00051600
0.0 00051700
0.0 00051800
/* 00051900
021 /*** MATERIAL PROPERTY DATA CARDS *** 00052000
/* (1) THERMAL CONDUCTIVITY TABLE 00052100
/* NTPK 00052200
/* TPK (TEMP. COND. ---) 00052300
7 / BORON-NITRIDE ( NOT USED ) 00052400
0. 7.213E-3 300. 6.903E-3 500. 6.696E-3 00052500
700. 6.489E-3 900. 6.283E-3 1000. 6.407E-3 00052600
2000. 7.647E-3 00052700
3 / NICHROME-5 00052800
20. 4.175E-3 100. 3.307E-3 2605. 2.778E-3 00052900
5 / BORON-NITRIDE 00053000
100. 1.500E-3 200. 1.639E-3 400. 1.833E-3 00053100
600. 1.944E-4 800. 2.000E-3 00053200
11 / INCONEL-600 00053300
0.0 3.486E-3 21.1 3.548E-3 93.3 3.754E-3 00053400
204.4 4.168E-3 315.6 4.581E-3 426.7 4.994E-3 00053500
537.8 5.442E-3 648.9 5.924E-3 760.0 6.407E-3 00053600
871.1 6.889E-3 2000.0 1.194E-3 00053700
2 / SUS 00053800
0. 3.889E-3 500. 5.000E-3 00053900
/* 12 / MGO 00054000
/* 0. 9.259E-3 200. 6.365E-3 300. 4.919E-3 00054100
/* 400. 4.100E-3 500. 3.360E-3 600. 2.798E-3 00054200
/* 700. 2.401E-3 800. 2.100E-3 1000. 1.649E-3 00054300
/* 1200. 1.500E-3 1233. 1.600E-3 1600. 1.748E-3 00054400
2 / MGO 00054500
200. 2.222E-4 800. 2.222E-4 00054600
2 / CU 00054700
0. 9.22E-2 100. 8.75E-2 00054800
2 / CU 00054900
0. 9.22E-2 100. 8.75E-2 00055000
/* (2) SPECIFIC HEAT CAPACITY TABLE 00055100
/* NTPC 00055200
/* TPC (TEMP. SPECIFIC HEAT ---) 00055300
/* 6 / BORON-NITRIDE 00055400
/* 0. 57.67 360. 84.59 510. 95.80 00055500
/* 683. 121.0 1260. 151.7 2000. 191.2 00055600
4 / BORON-NITRIDE UPDATE 80.04.20 00055700
0. 497. 100. 497. 1000. 698. 3000. 1195. / 00055800
2 / NICHROME-5 00055900

```

```

-----1-----2-----3-----4-----5-----6-----7-R-----8
0. 0.104 2000. 0.104 00056000
/* 6 / BORON-NITRIDE 00056100
/* 0. 57.29 360. 84.59 510. 95.96 00056200
/* 850. 121.1 1260. 151.7 2000. 206.9 00056300
3 / BORON-NITRIDE UPDATE 82.09.20 00056400
298. 0.1925 1000. 0.4418 2000. 0.5015 00056500
10 / INCONEL-600 00056600
0.0 0.106 21.1 0.106 93.3 0.111 00056700
204.4 0.116 315.6 0.121 426.7 0.126 00056800
537.8 0.132 648.9 0.140 760.0 0.145 00056900
871.1 0.149 00057000
2 / SUS 00057100
0. 0.120 2000. 0.120 00057200
3 / MGO 00057300
177. 0.25 527. 0.30 847. 0.33 00057400
3 / CU 00057500
20. 9.22E-2 100. 9.00E-2 300. 8.75E-2 00057600
3 /CU 00057700
20. 9.22E-2 100. 9.00E-2 300. 8.75E-2 00057800
/* 00057900
022 /*** OTHER HEAT SLAB DATA CARDS *** 00058000
/* IVOLC QINIT BETABL 00058100
1 946.8 0.0 00058200
/* PTABL (TIME NORMALIZED POWER ---) 00058300
/* NEW P(T) CURVE MAY BE USED IN THE FUTURE 00058400
/* 0.0 1.0 11.4 1.0 20.0 0.597 00058500
/* 30.0 0.362 40.0 0.304 50.0 0.254 00058600
/* 70.0 0.195 100.0 0.172 200.0 0.108 00058700
/* 400.0 0.0813 800.0 0.0659 2000.0 0.0555 00058800
/*4000.0 0.0478 00058900
/* POWER CURVE NOW USED (UNTIL JUNE OF 1980) 00059000
/* 0.0 1.0 11.208 1. 11.352 0.987 00059100
/* 11.5 0.971 12.0 0.938 12.5 0.905 00059200
/* 13. 0.874 14. 0.819 15. 0.766 00059300
/* 16. 0.715 17. 0.664 18. 0.615 00059400
/* 20. 0.523 25. 0.349 28. 0.261 00059500
/* 30. 0.218 35. 0.134 36. 0.121 00059600
/* 37. 0.119 50. 0.111 70. 0.104 00059700
/* 100. 0.097 200. 0.085 300. 0.079 00059800
/* 500. 0.071 700. 0.066 1000. 0.061 00059900
/*2000. 0.051 3000. 0.046 4000. 0.042 00060000
/* POWER CURVE FOR RUN 901 00060100
0. 1. 7.5 1. 8.0 0.951 9. 0.885 00060200
10. 0.824 12. 0.707 14. 0.614 16. 0.545 00060300
18. 0.496 20. 0.429 22. 0.386 24. 0.348 00060400
26. 0.309 28. 0.274 30. 0.262 32. 0.253 00060500
34. 0.244 36. 0.236 38. 0.227 40. 0.219 00060600
42. 0.212 44. 0.205 46. 0.198 48. 0.191 00060700
50. 0.184 60. 0.163 70. 0.151 80. 0.141 00060800
90. 0.132 100. 0.125 110. 0.12 120. 0.115 00060900
150. 0.102 180. 0.088 210. 0.077 240. 0.072 00061000
270. 0.067 300. 0.062 360. 0.06 420. 0.058 00061100
480. 0.056 540. 0.054 600. 0.053 1200. 0.042 00061200
1800. 0.041 / 00061300
/* 00061400
999 00061500
/* END OF DATA 00061600

```

Appendix B    Computational Results for 0, 2, 5, 25, 50, 75, and 200%  
Break Tests



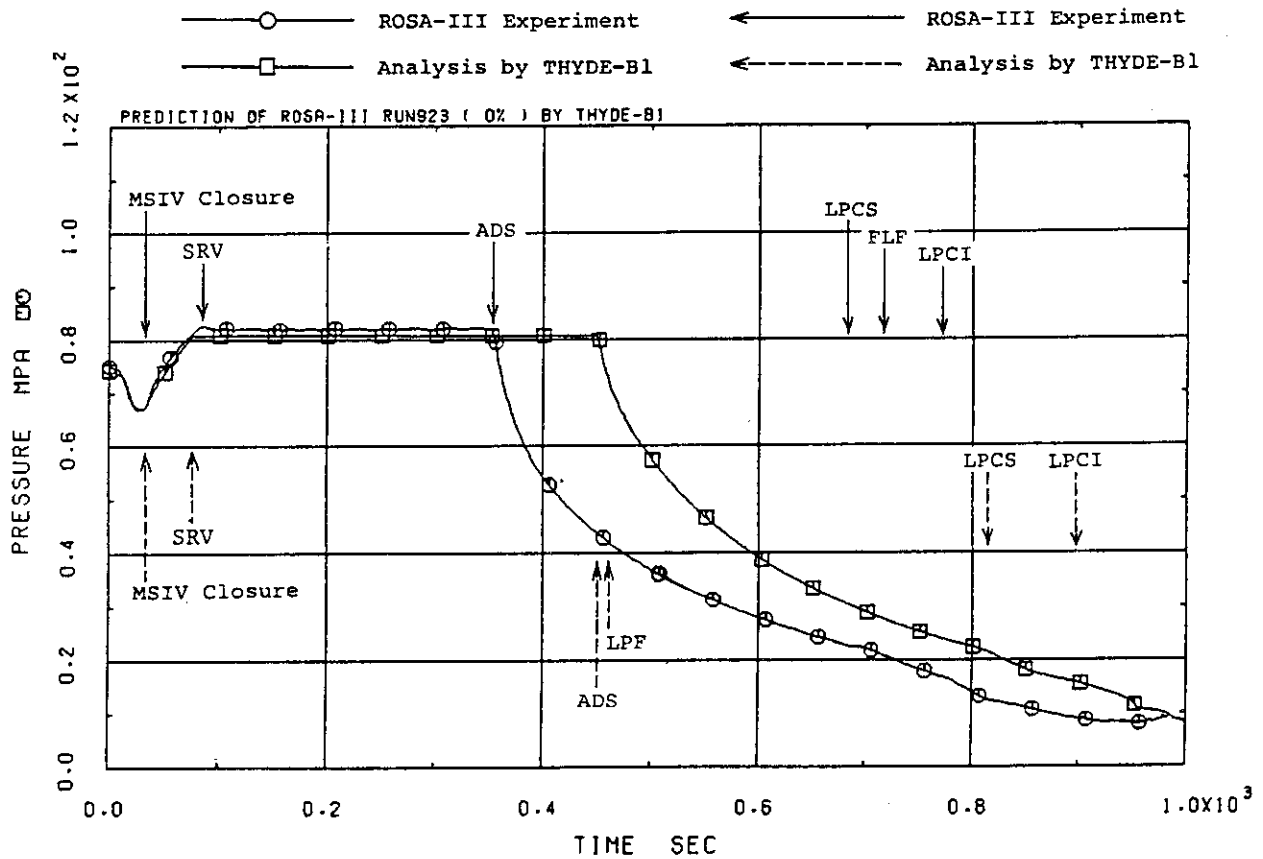


Fig. B.1 Measured vs. calculated system pressures - 0 % break test

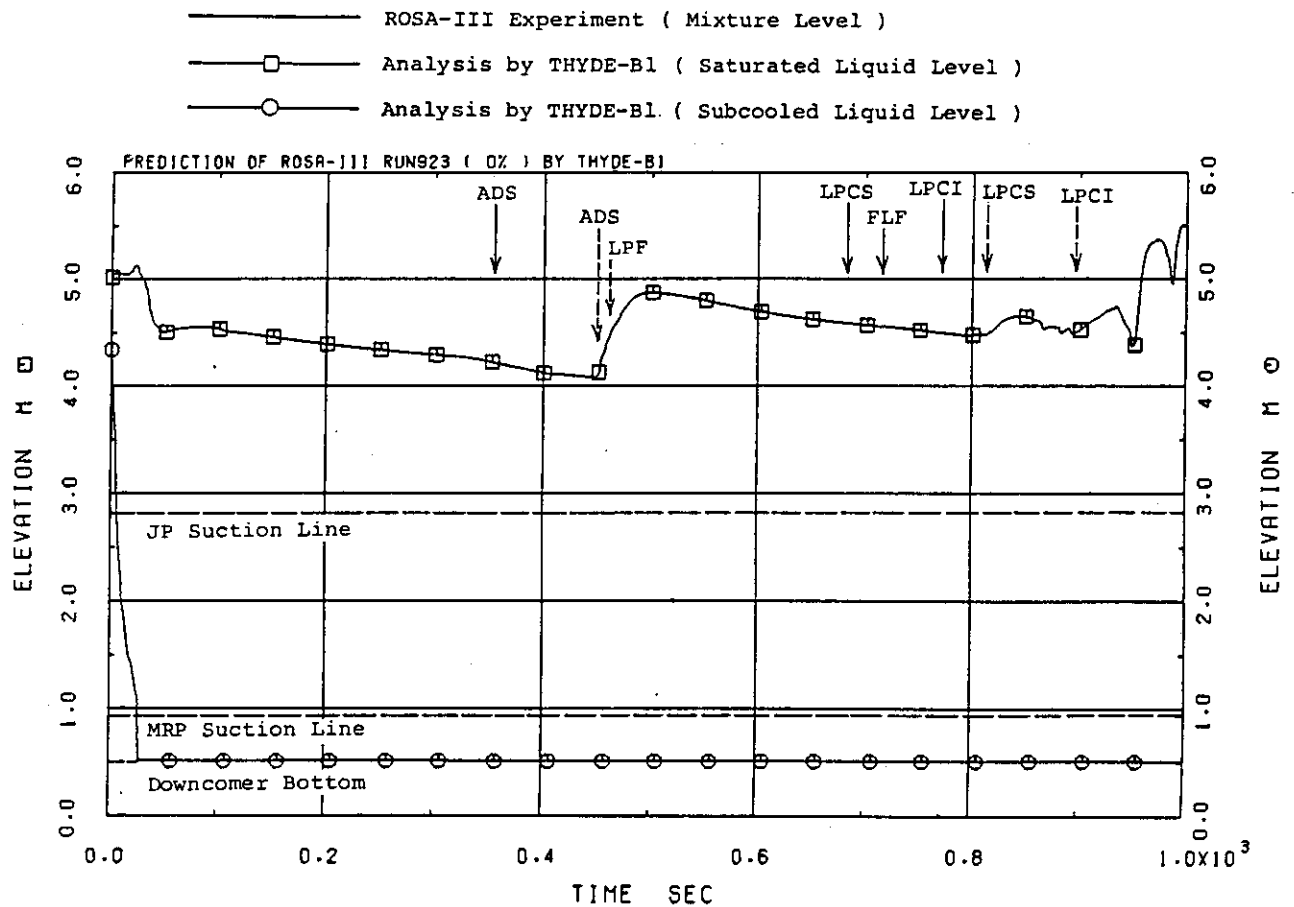


Fig. B.2 Measured vs. calculated downcomer mixture levels - 0 % break test

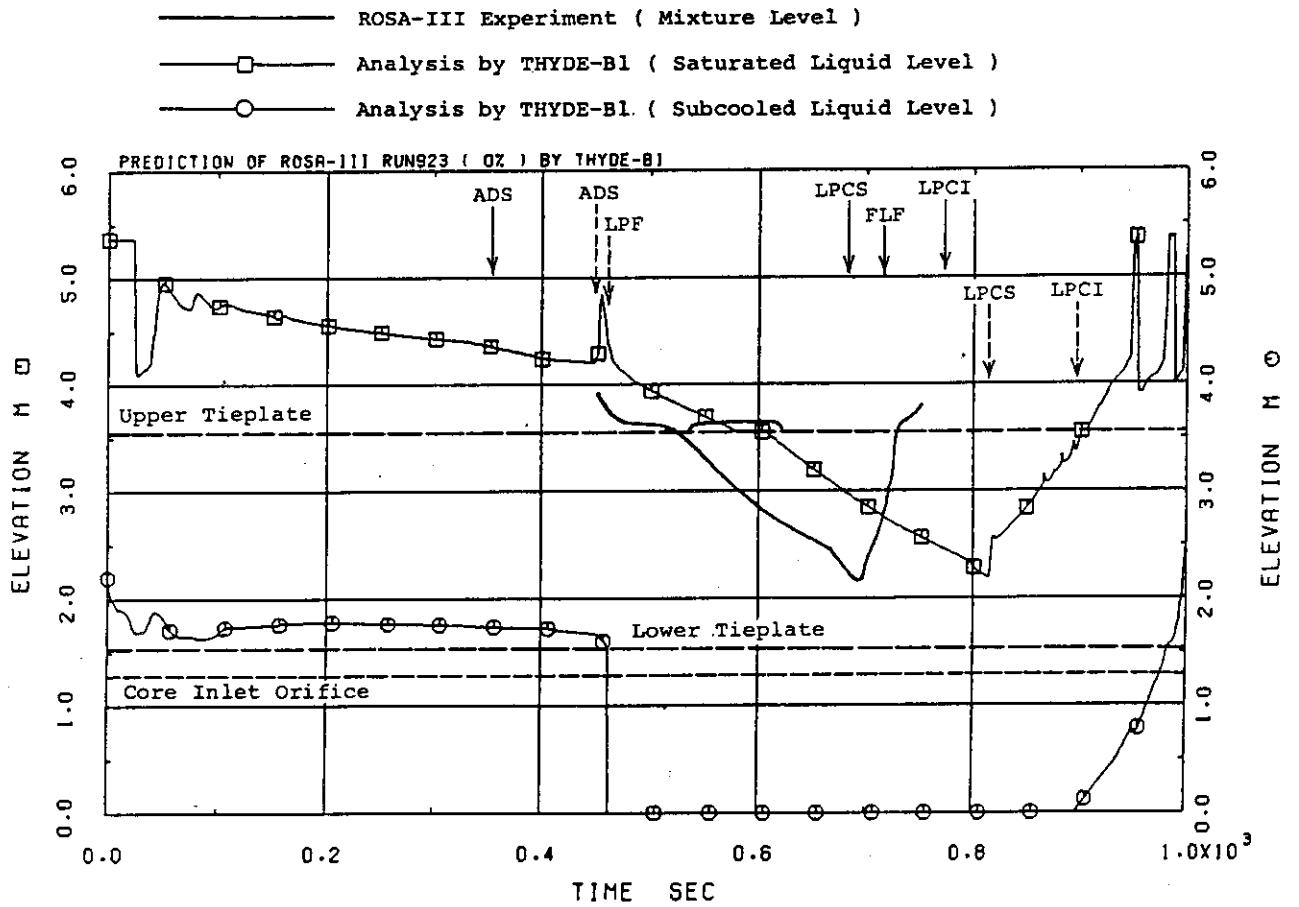


Fig. B.3 Measured vs. calculated core mixture levels - 0 % break test

× ◇ ↑ × ROSA-III Experiment  
 □ ○ △ + Analysis by THYDE-B1

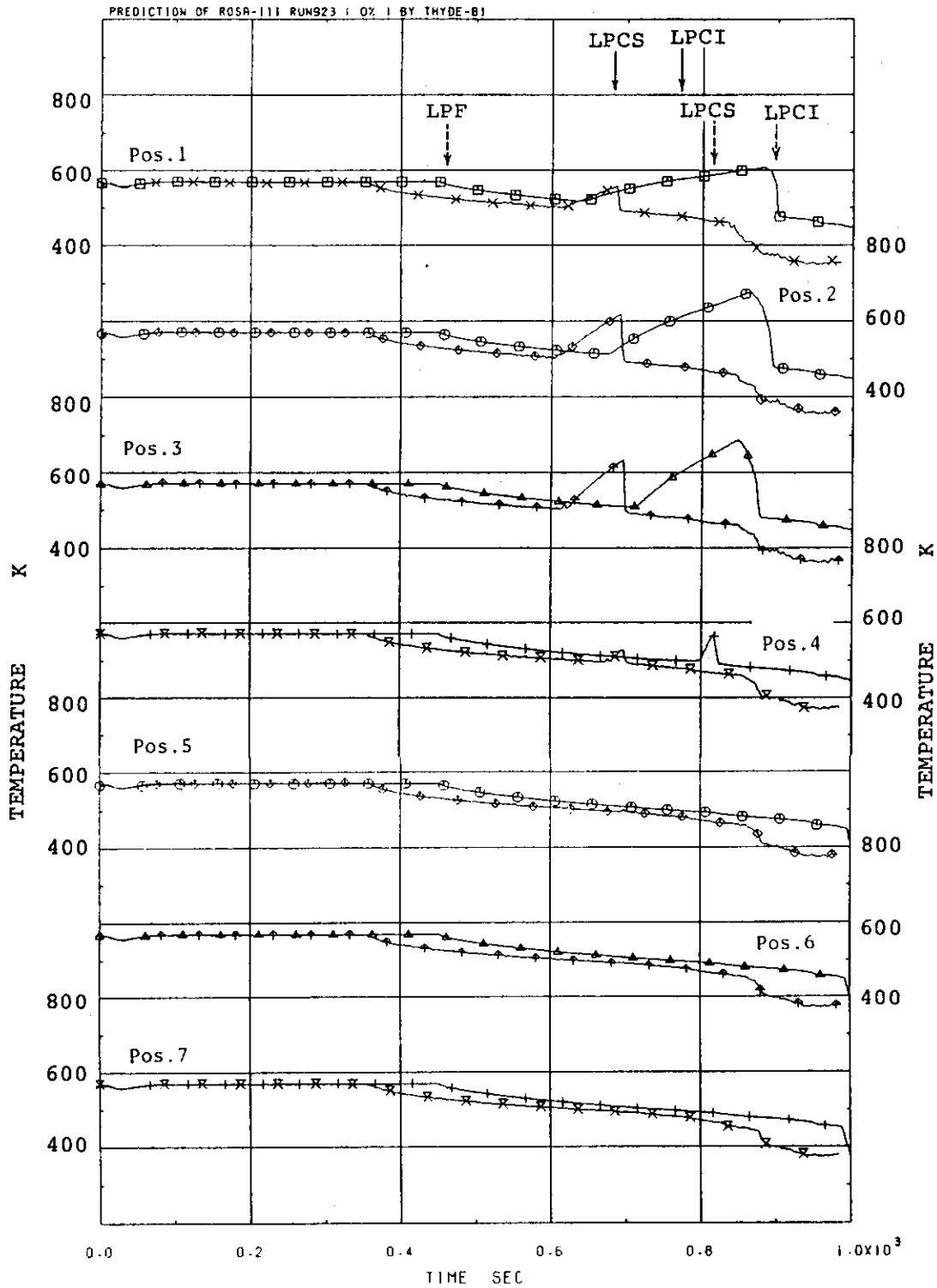


Fig. B.4 Measured vs. calculated peak-power rod temperatures - 0 % break

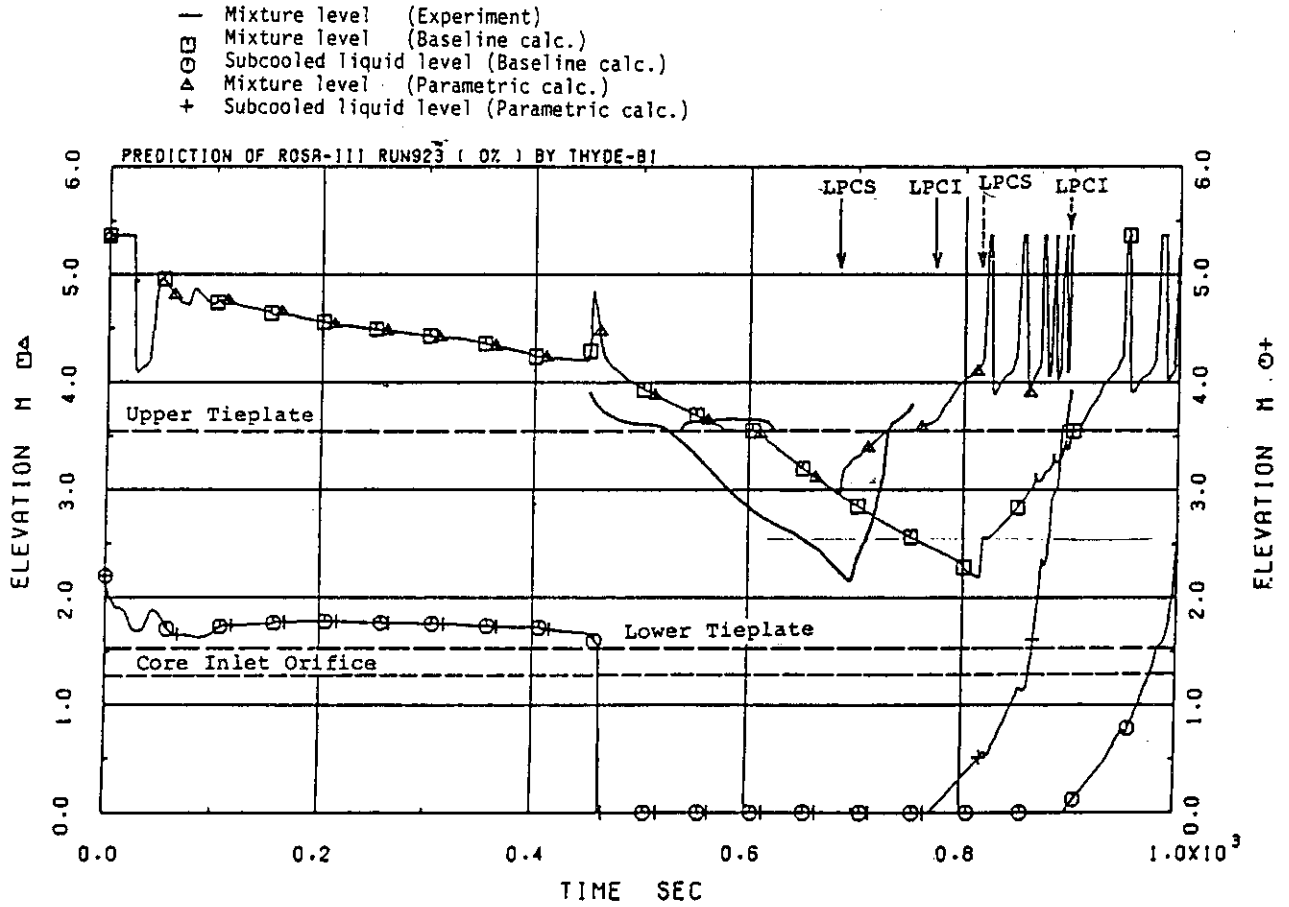


Fig. B.5 Core mixture level: baseline vs. parametric calculations - 0 % break test

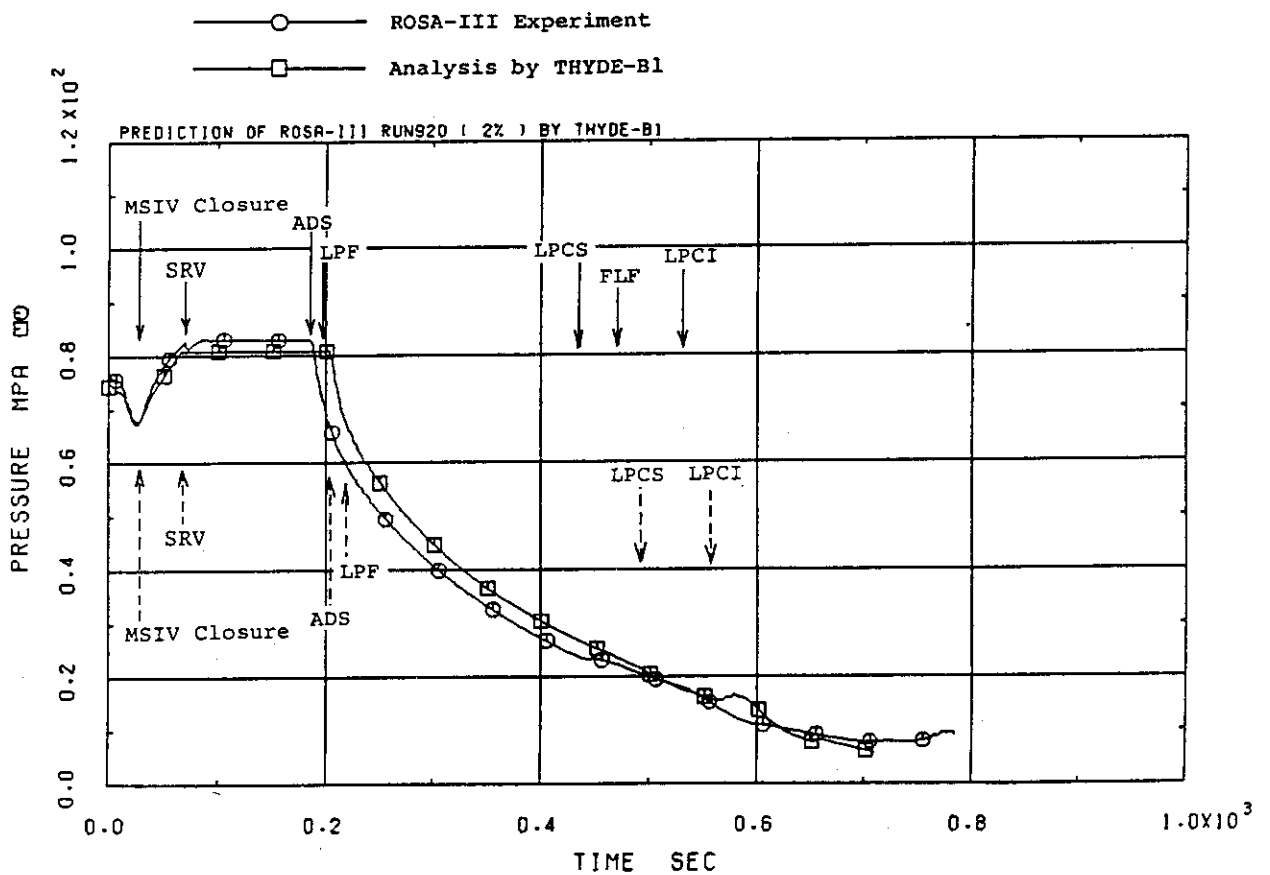


Fig. B.6 Measured vs. calculated system pressures - 2 % break test

- ROSA-III Experiment ( Low Range )
- △— ROSA-III Experiment ( High Range )
- Analysis by THYDE-B1

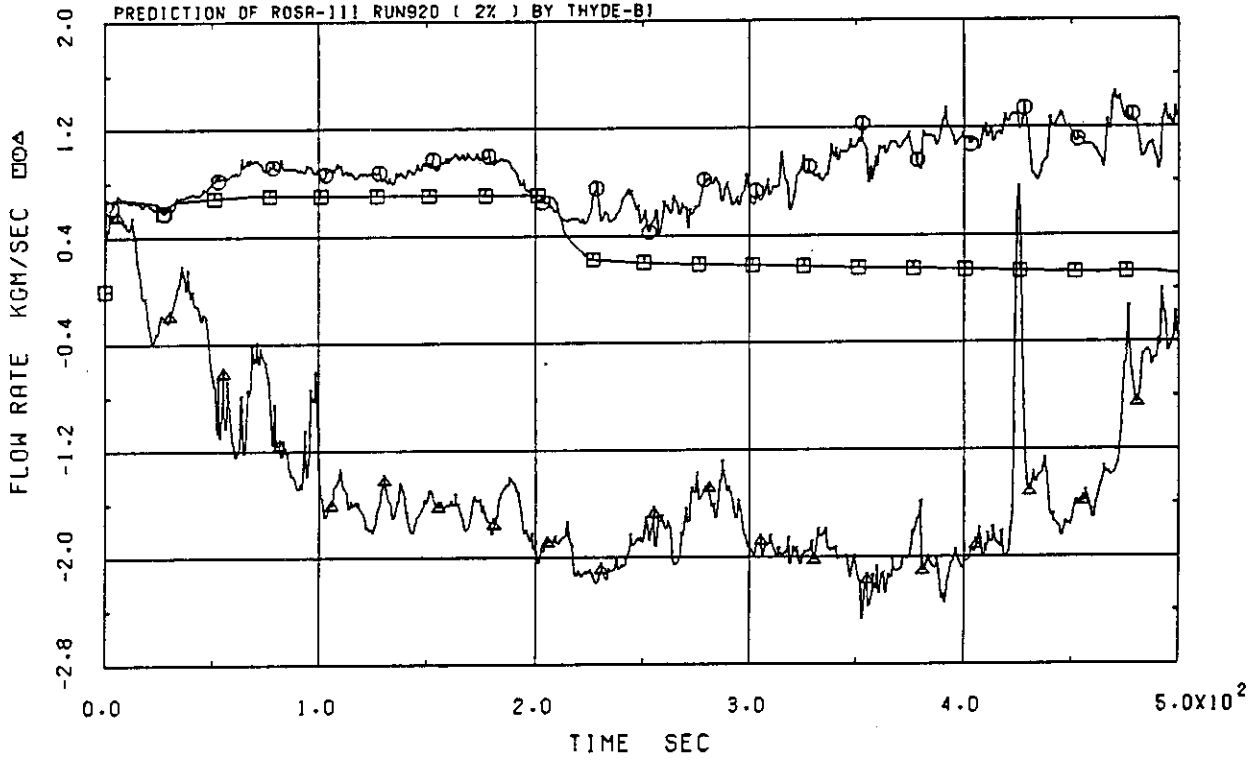


Fig. B.7 Measured vs. calculated break flow rates - 2 % break test

- ROSA-III Experiment ( Mixture Level )
- Analysis by THYDE-B1 ( Saturated Liquid Level )
- Analysis by THYDE-B1 ( Subcooled Liquid Level )

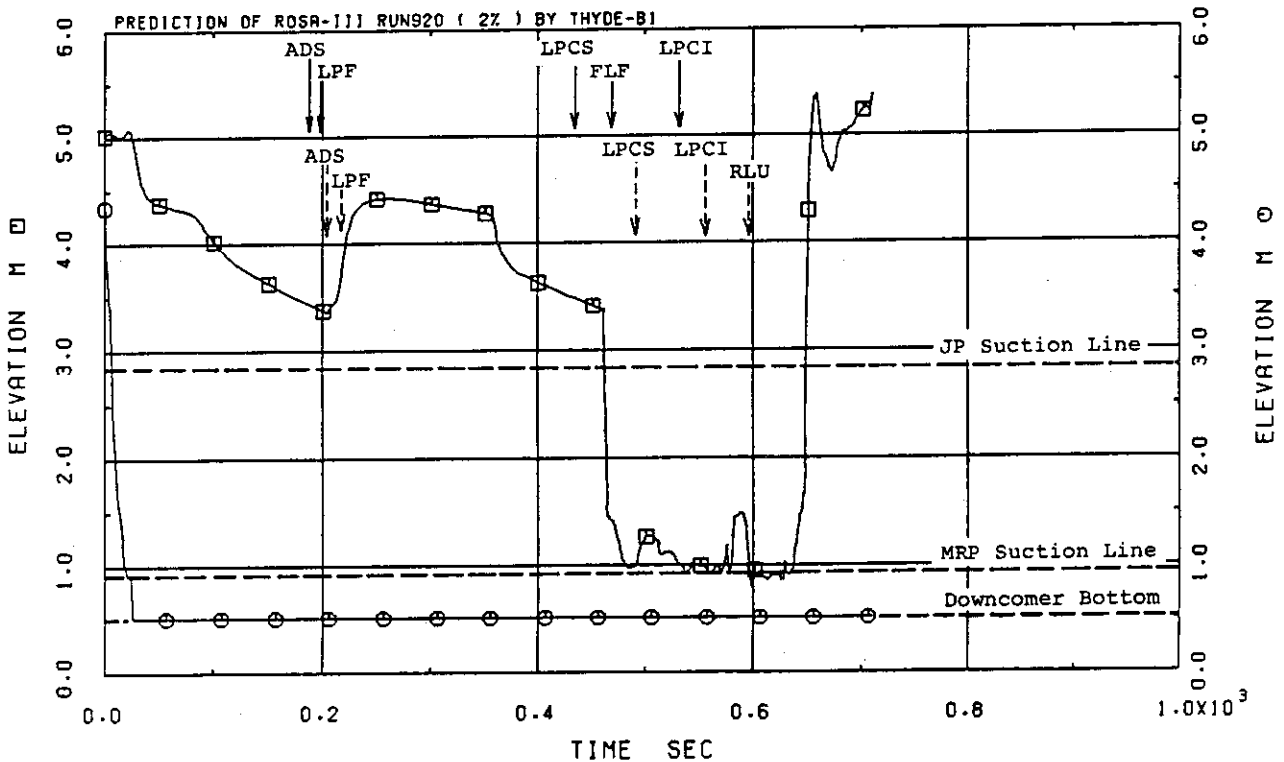


Fig. B.8 Measured vs. calculated downcomer mixture levels - 2 % break test

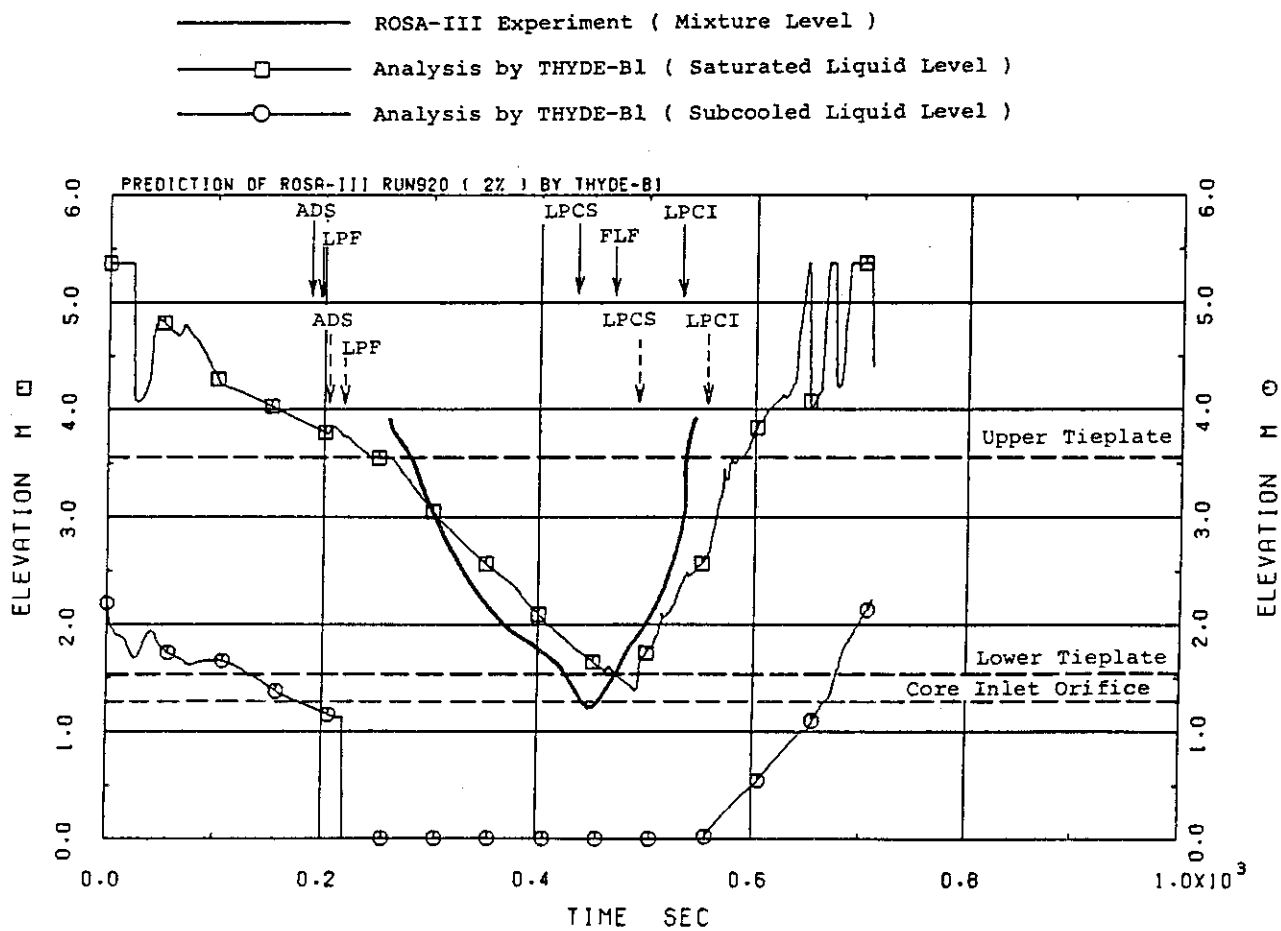


Fig. B.9 Measured vs. calculated core mixture levels - 2 % break test

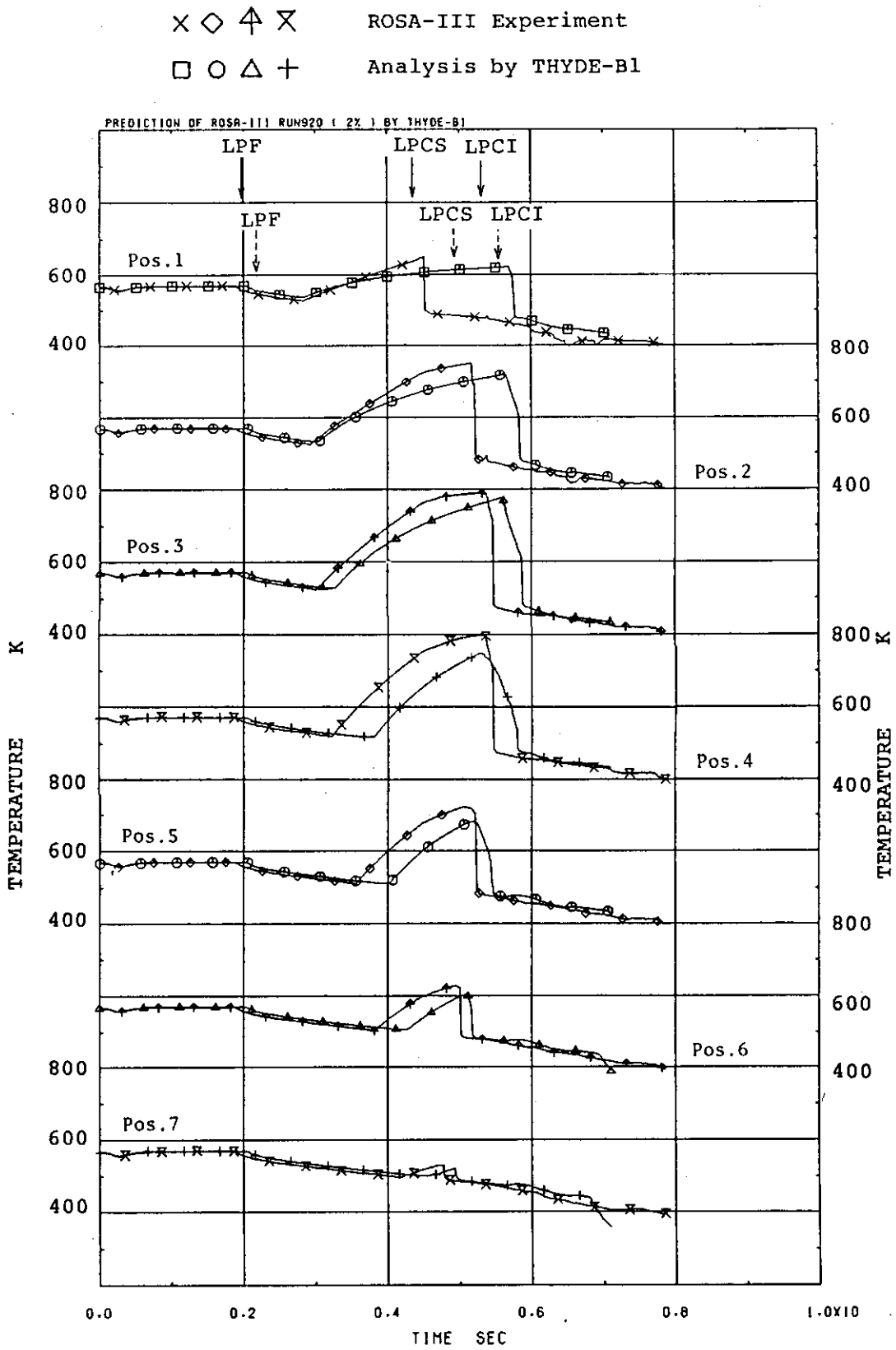


Fig. B.10 Measured vs. calculated peak-power rod temperatures - 2 % break test

- Mixture level (Experiment)
- Mixture level (Baseline calc.)
- △— Subcooled liquid level (Baseline calc.)
- ◇— Mixture level (Parametric calc.)
- +— Subcooled liquid level (Parametric calc.)

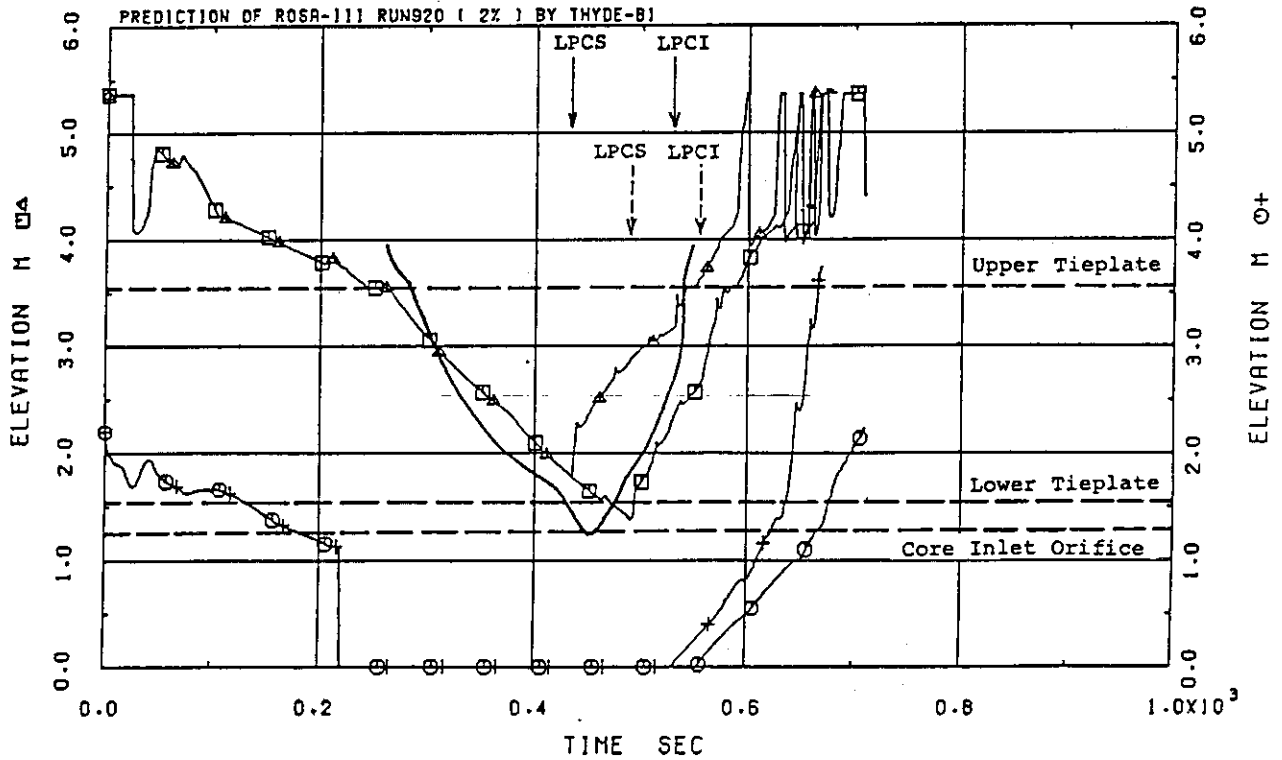


Fig. B.11 Core mixture level: baseline vs. parametric calculations - 2 % break test

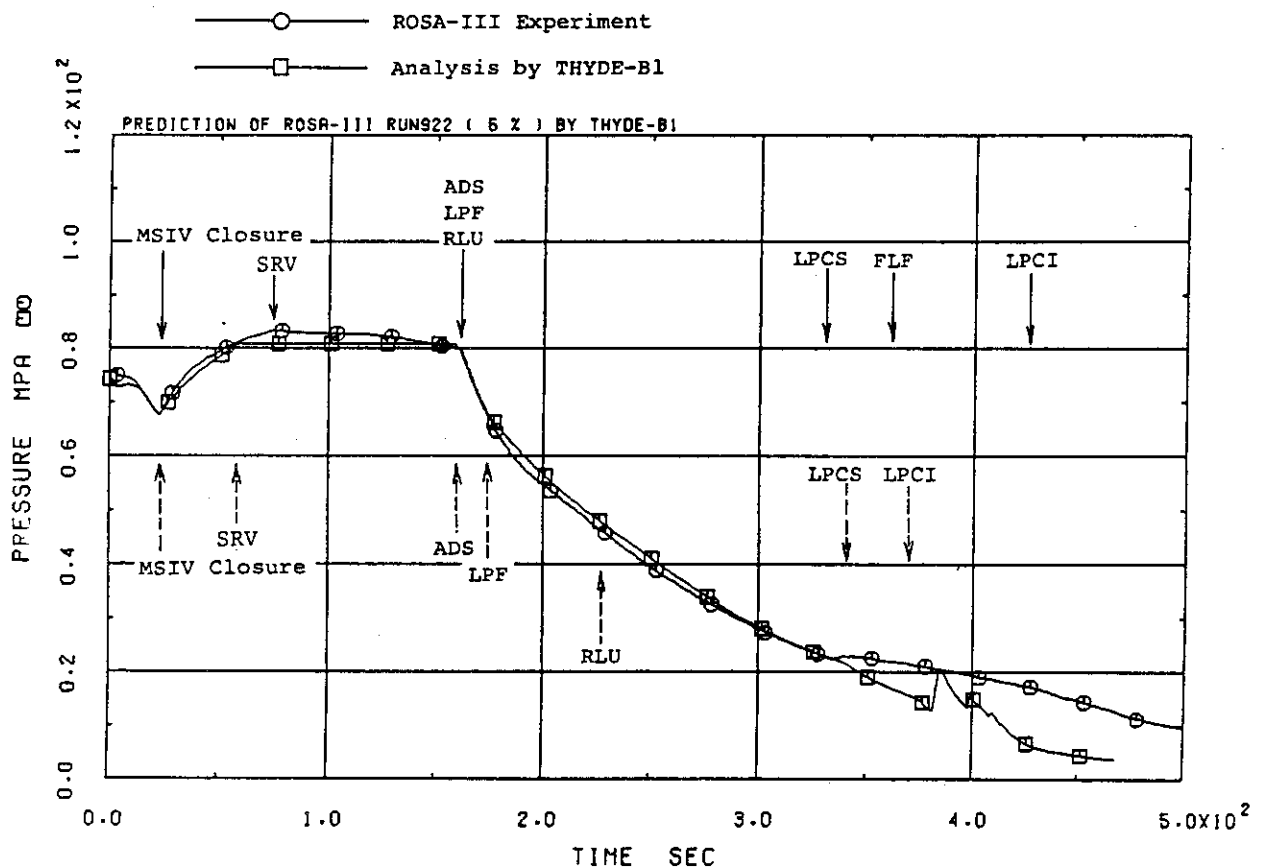


Fig. B.12 Measured vs. calculated system pressures - 5 % break test



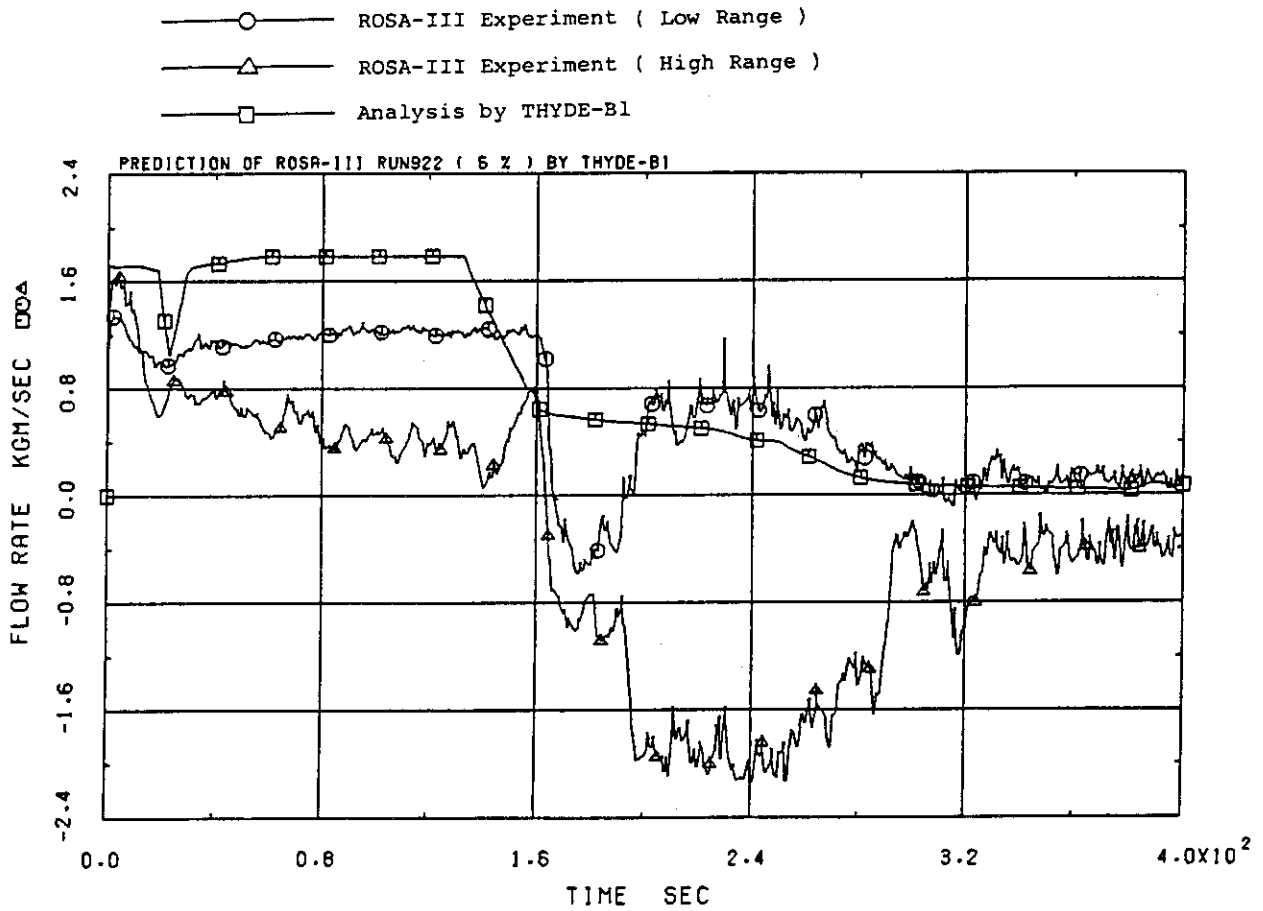


Fig. B.13 Measured vs. calculated break flow rates - 5 % break test

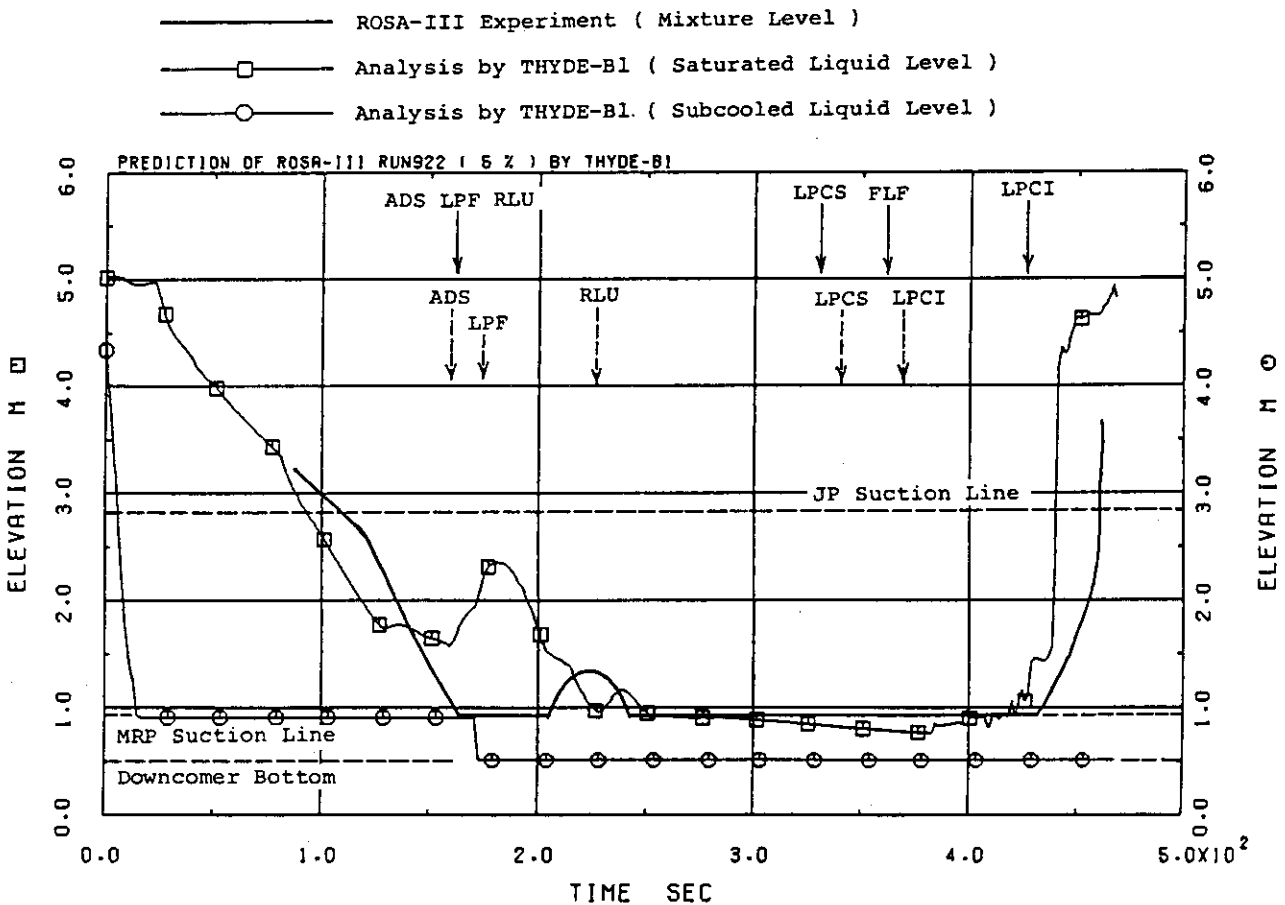


Fig. B.14 Measured vs. calculated downcomer mixture levels - 5 % break test

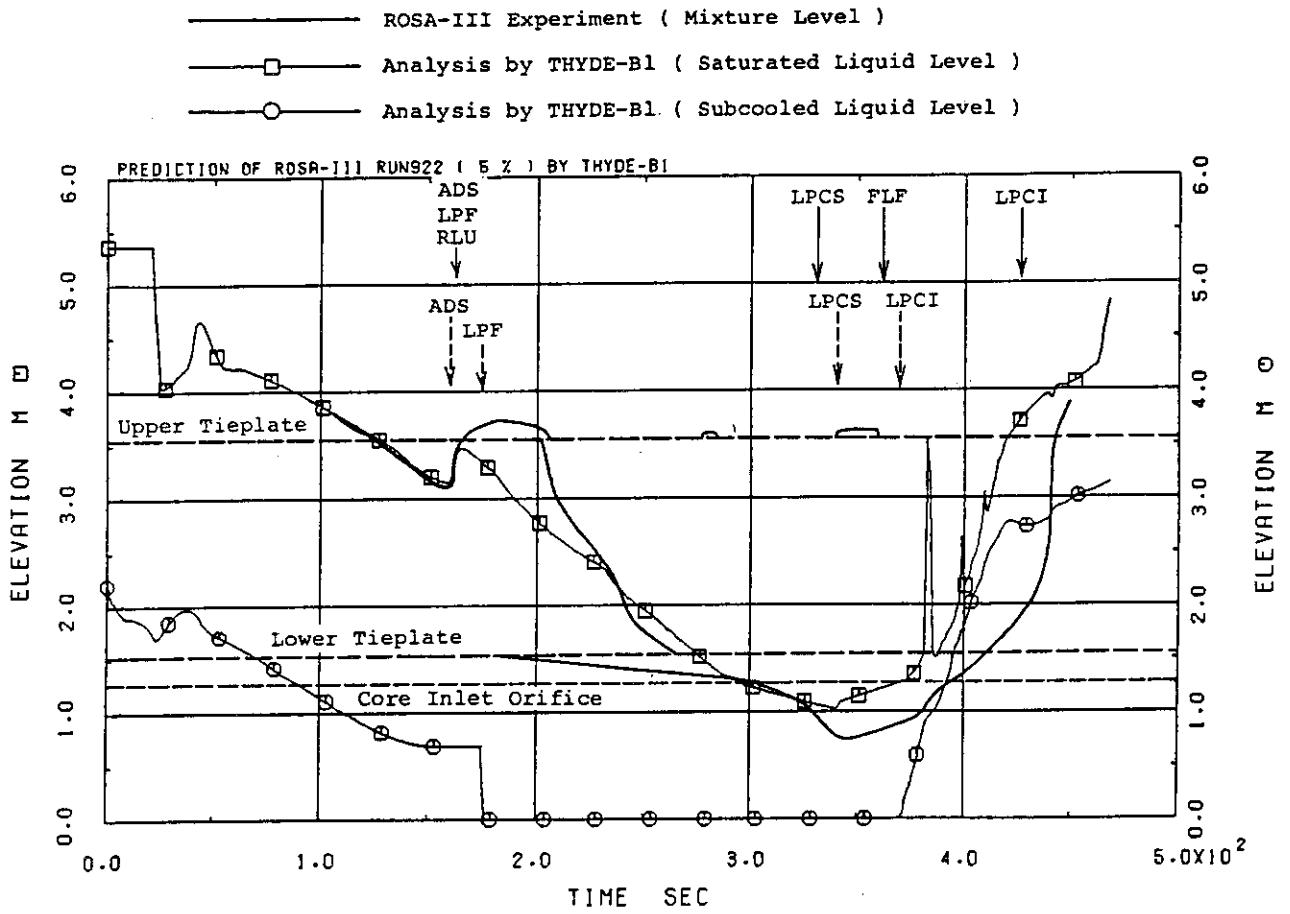


Fig. B.15 Measured vs. calculated core mixture levels - 5 % break test

× ◊ ⋈ ✕      ROSA-III Experiment  
 □ ○ △ +      Analysis by THYDE-B1

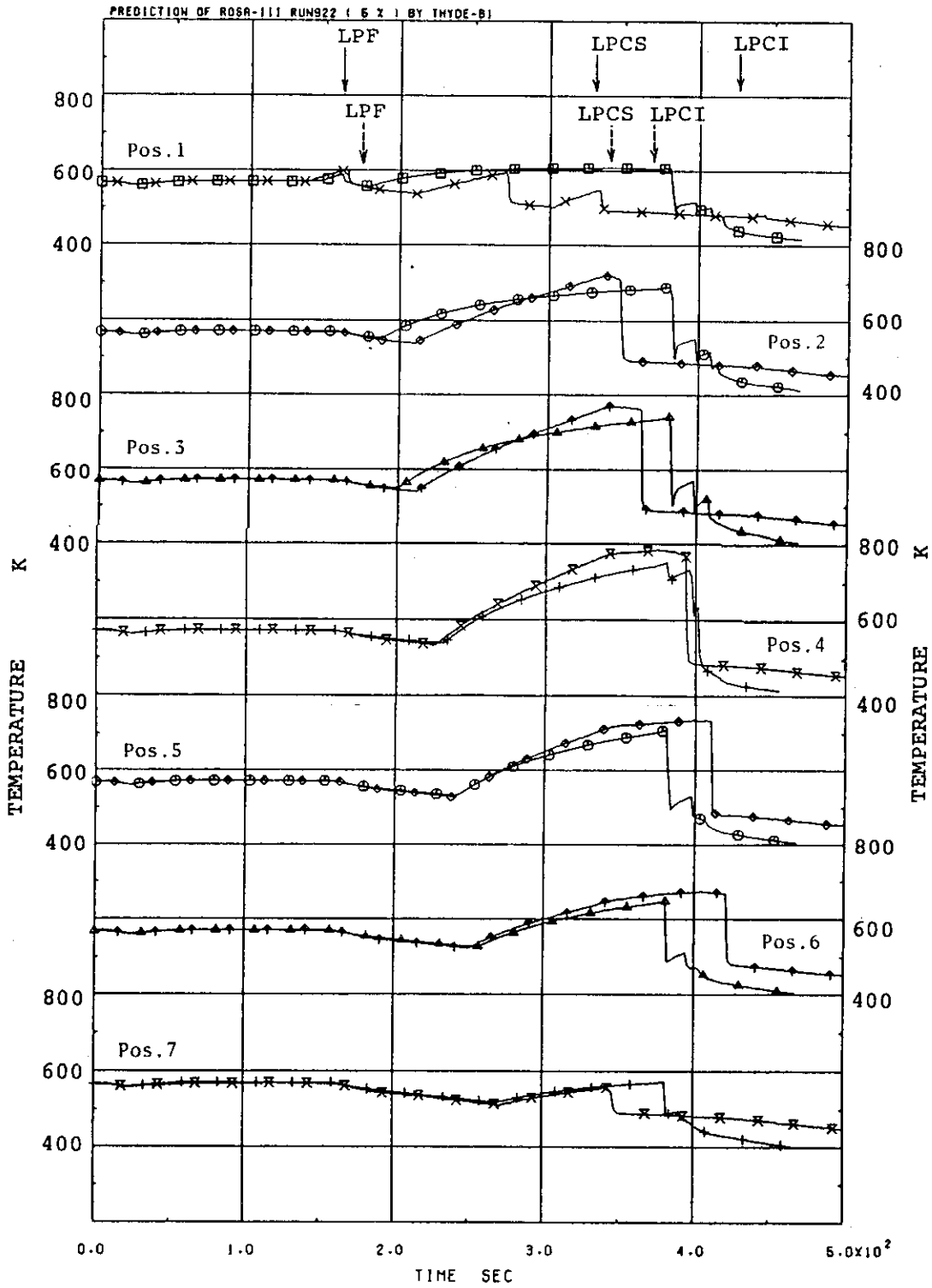


Fig. B.16 Measured vs. calculated peak-power rod temperatures - 5 % break test

- Mixture level (Experiment)
- Mixture level (Baseline calc.)
- Subcooled liquid level (Baseline calc.)
- ▲ Mixture level (Parametric calc.)
- + Subcooled liquid level (Parametric calc.)

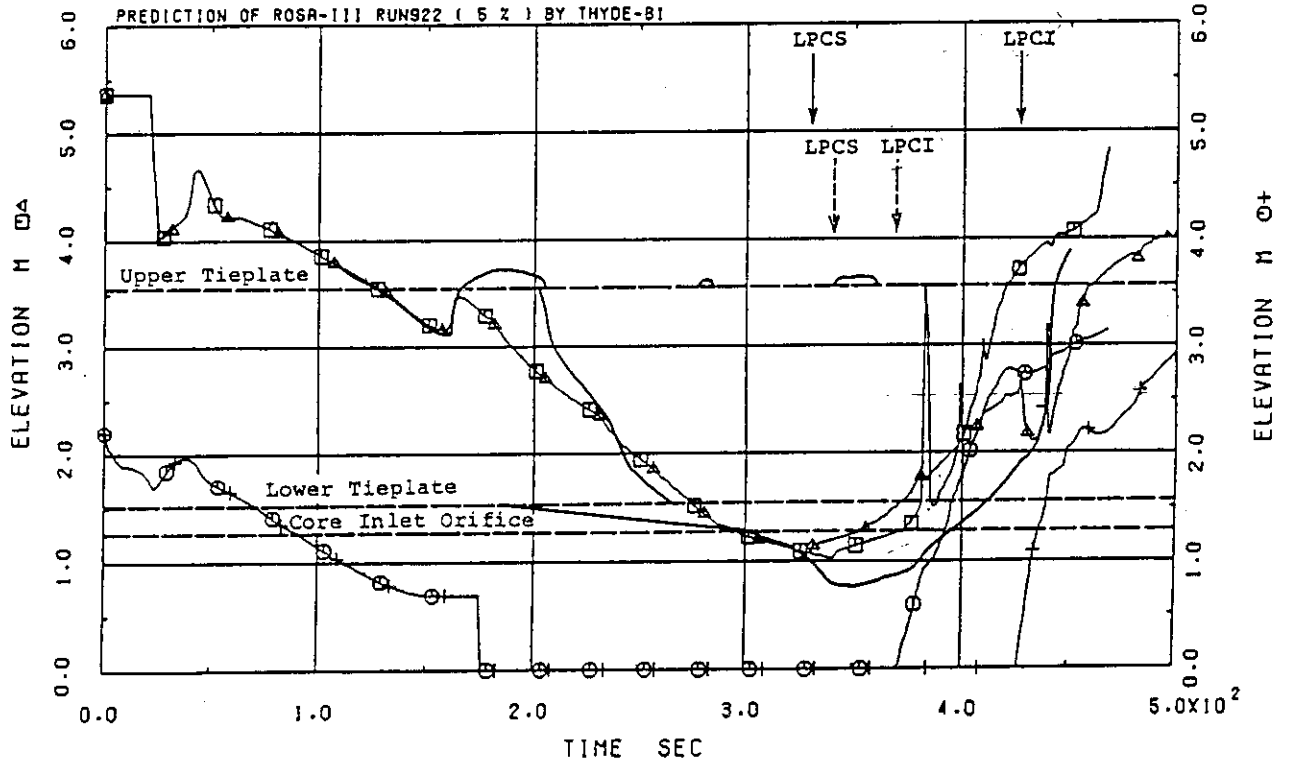


Fig. B.17 Core mixture level: baseline vs. parametric calculations - 5 % break test

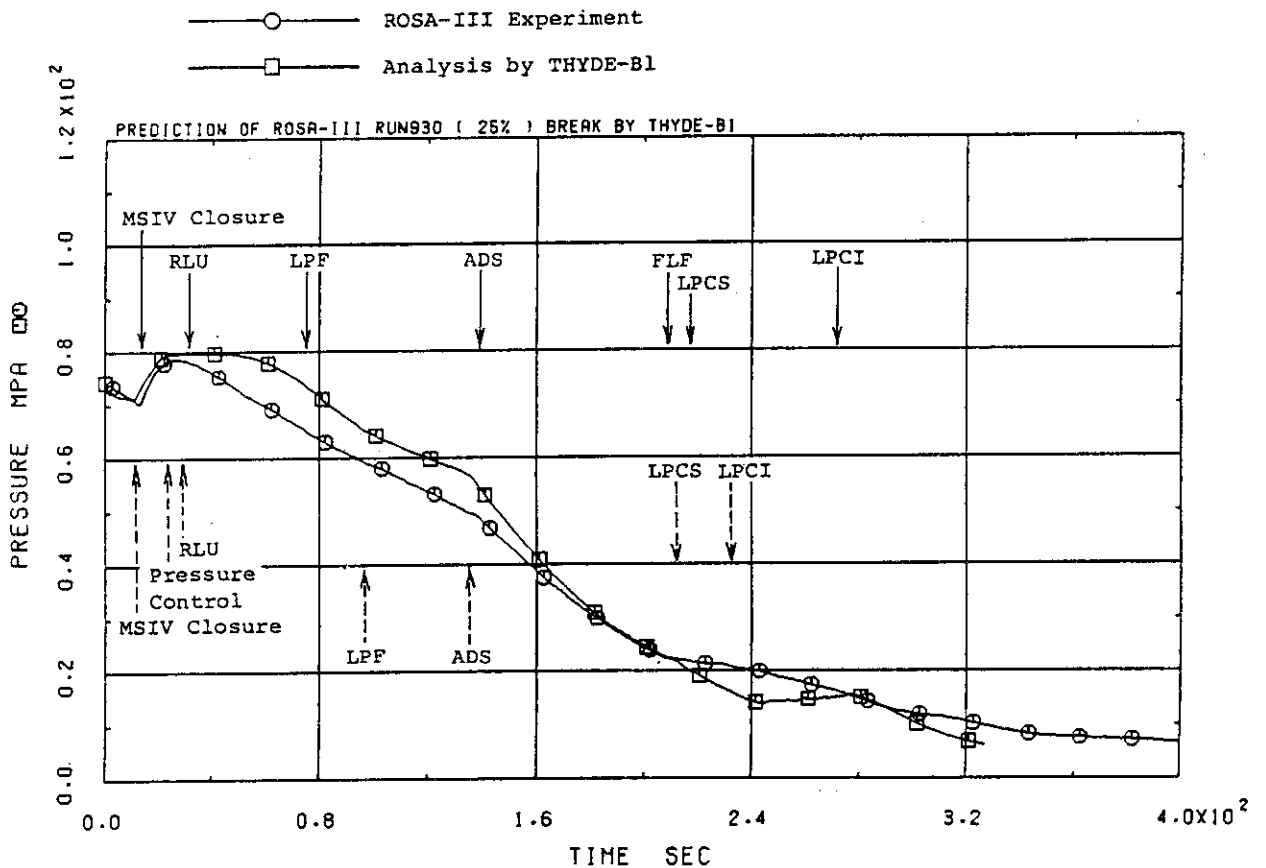


Fig. B.18 Measured vs. calculated system pressures - 25 % break test

- ROSA-III Experiment ( Mixture Level )
- □ — Analysis by THYDE-B1 ( Saturated Liquid Level )
- ○ — Analysis by THYDE-B1 ( Subcooled Liquid Level )

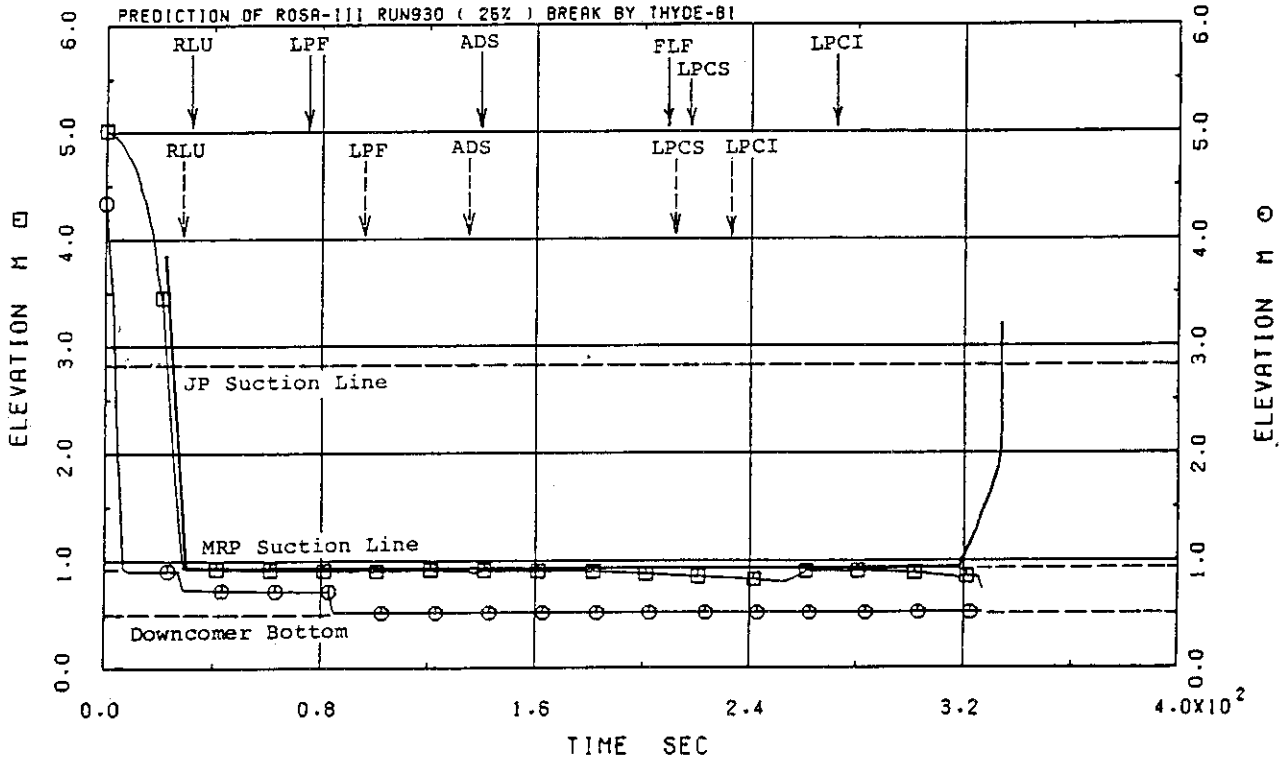


Fig. B.19 Measured vs. calculated downcomer mixture levels - 25 % break test

- □ — Analysis by THYDE-B1 ( Saturated Liquid Level )
- ○ — Analysis by THYDE-B1 ( Subcooled Liquid Level )

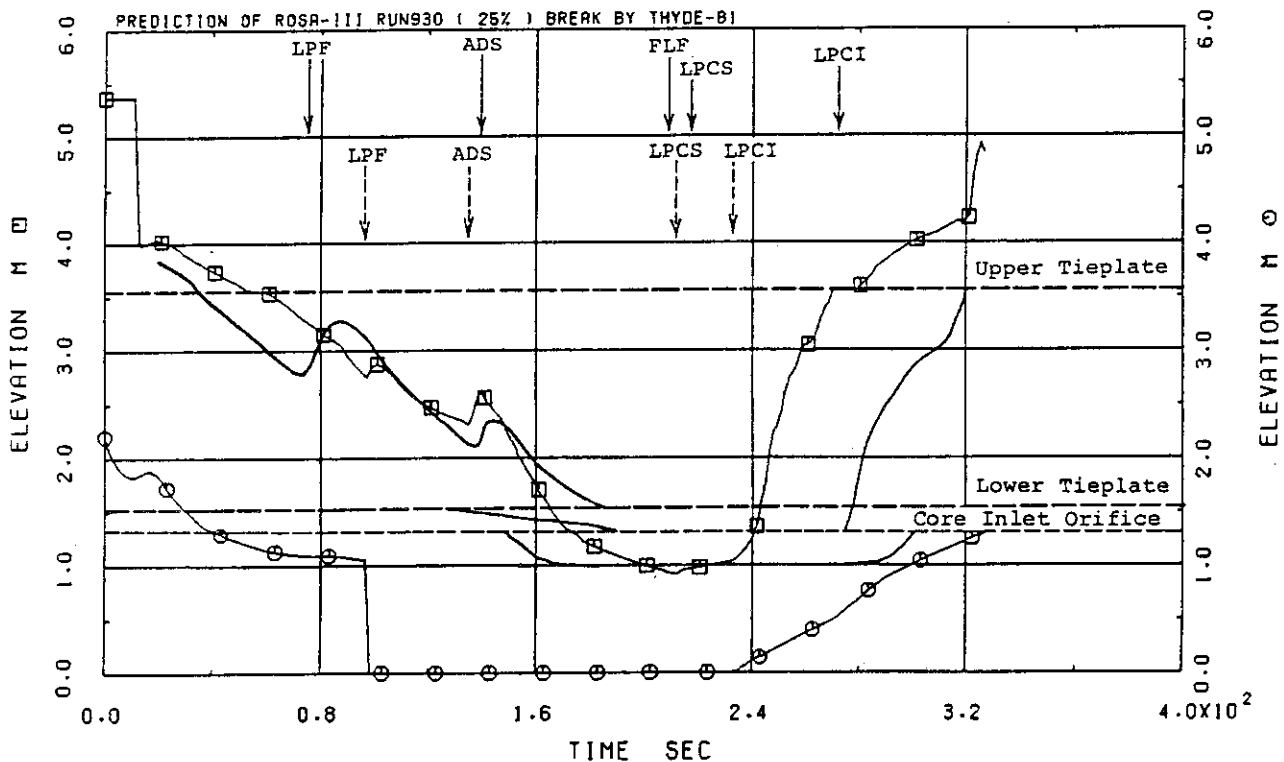


Fig. B.20 Measured vs. calculated core mixture levels - 25 % break test

× ◇ ↑ × ROSA-III Experiment  
 □ ○ △ + Analysis by THYDE-B1

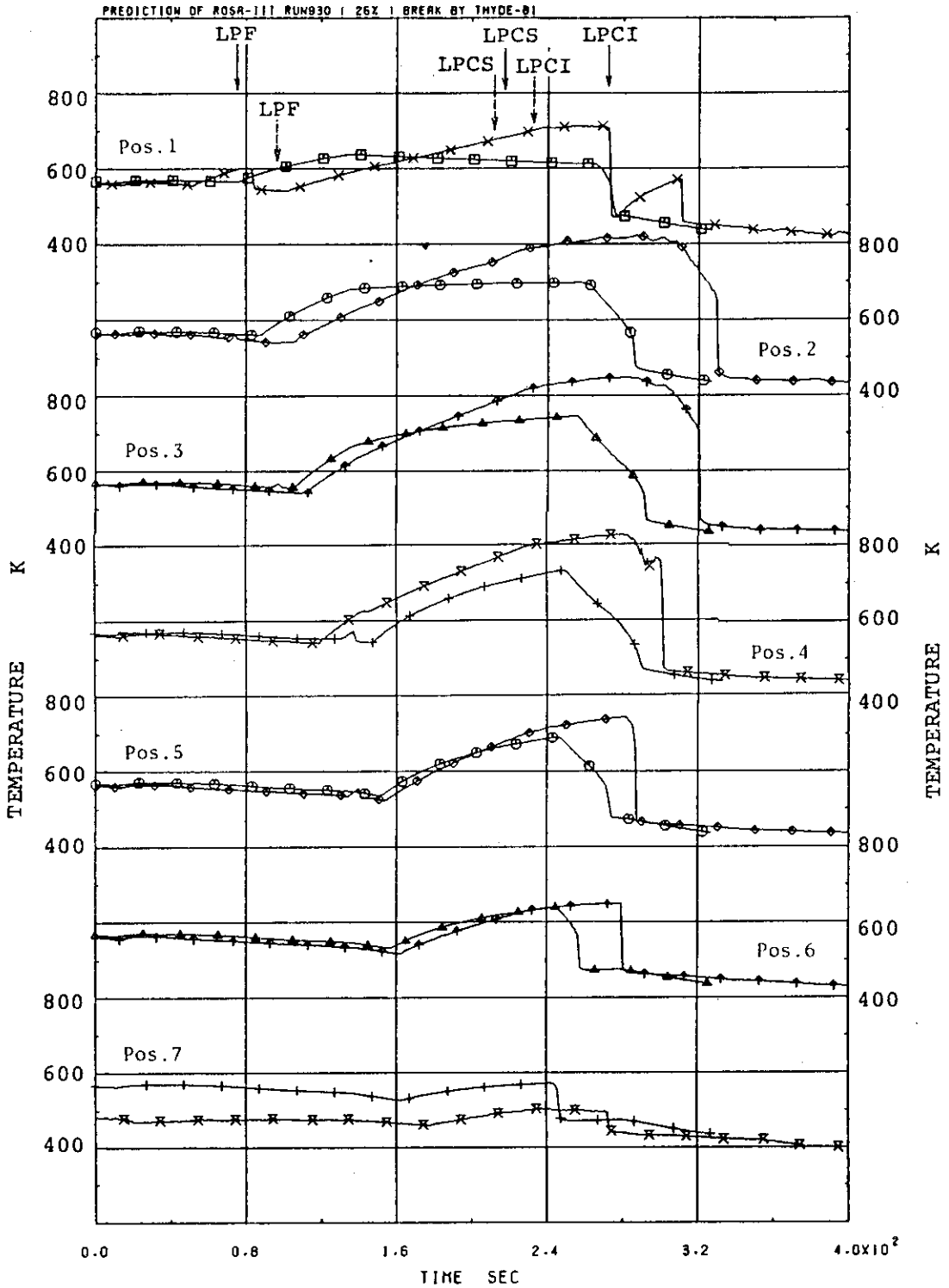


Fig. B.21 Measured vs. calculated peak-power rod temperature - 25 % break test

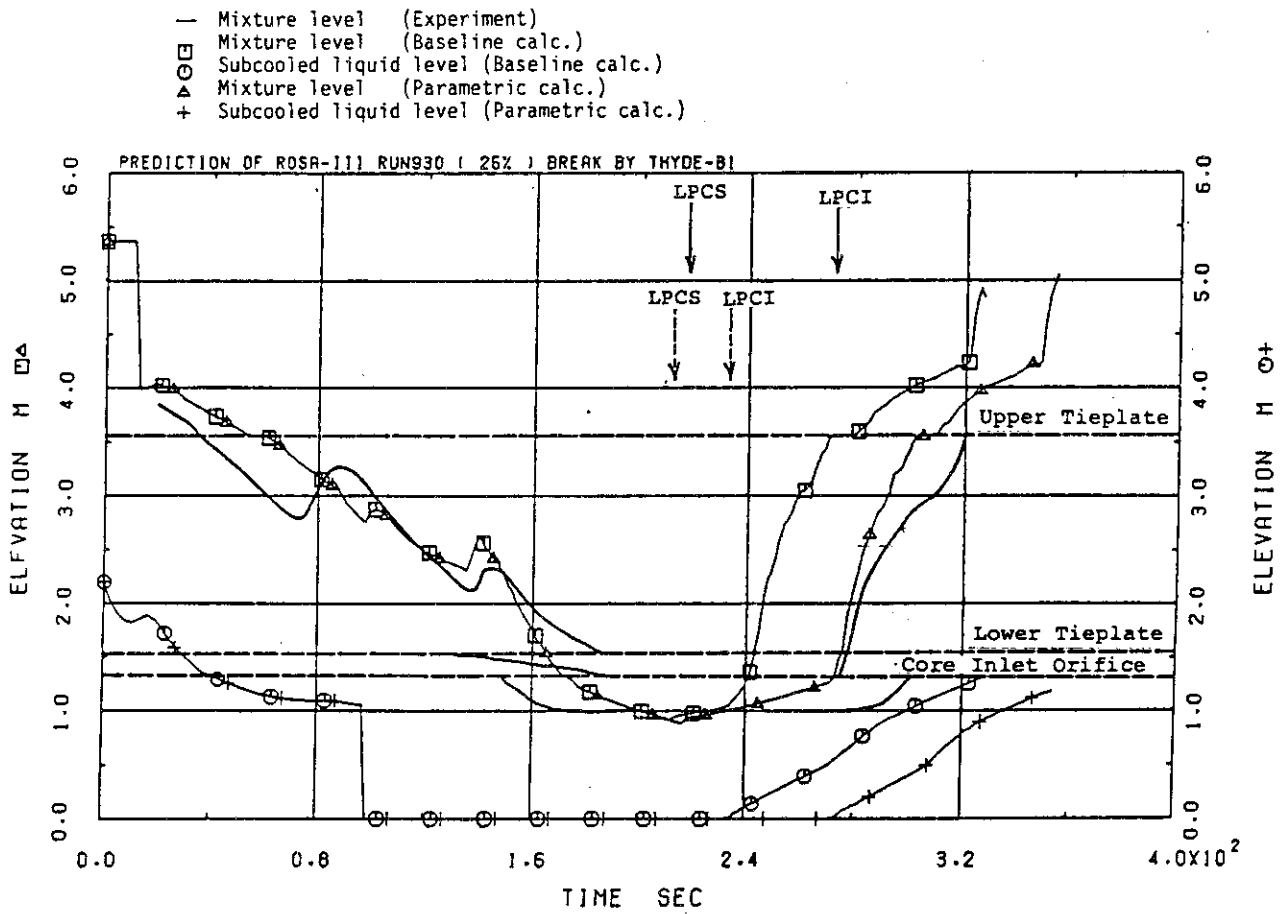


Fig. B.22 Core mixture level: baseline vs. parametric calculations  
 - 25 % break test

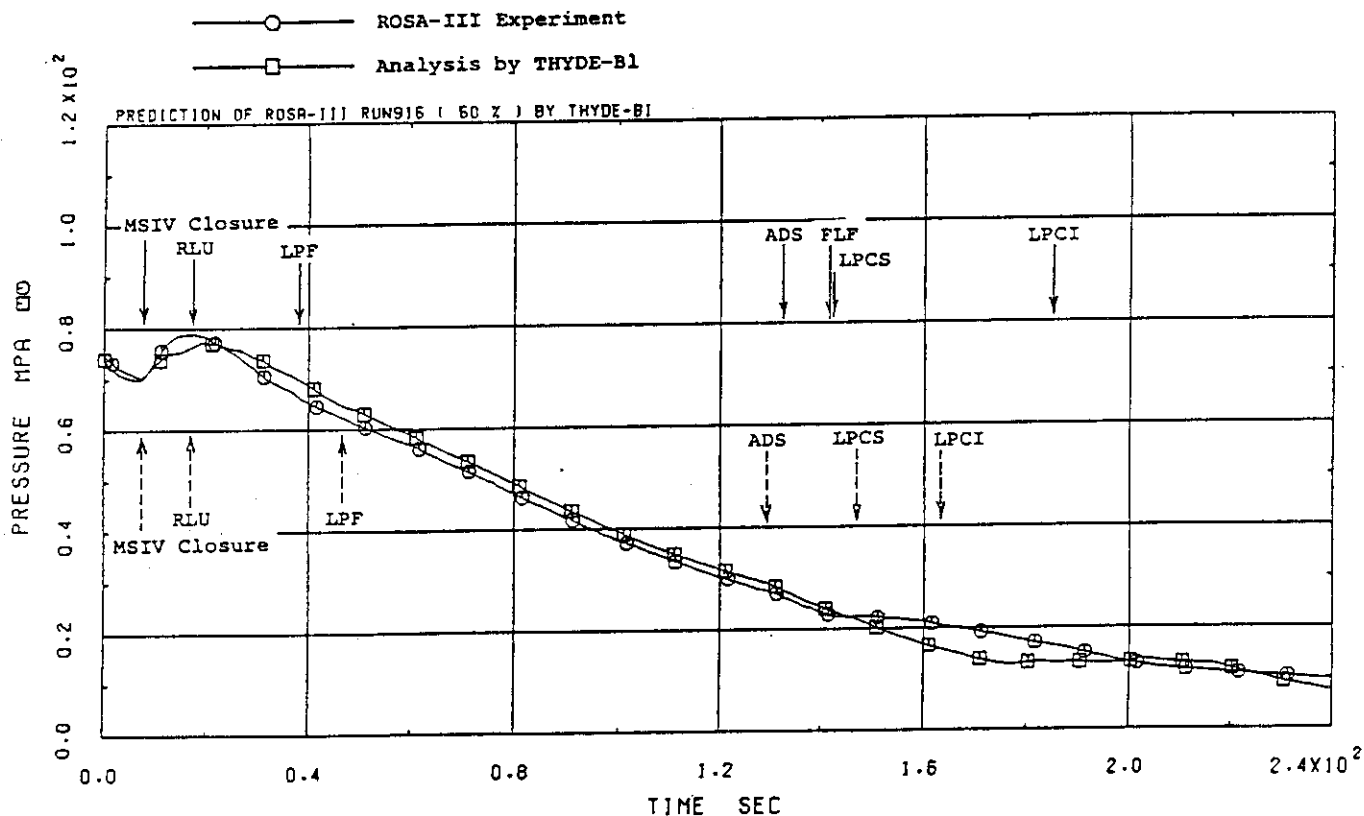


Fig. B.23 Measured vs. calculated system pressures - 50 % break test

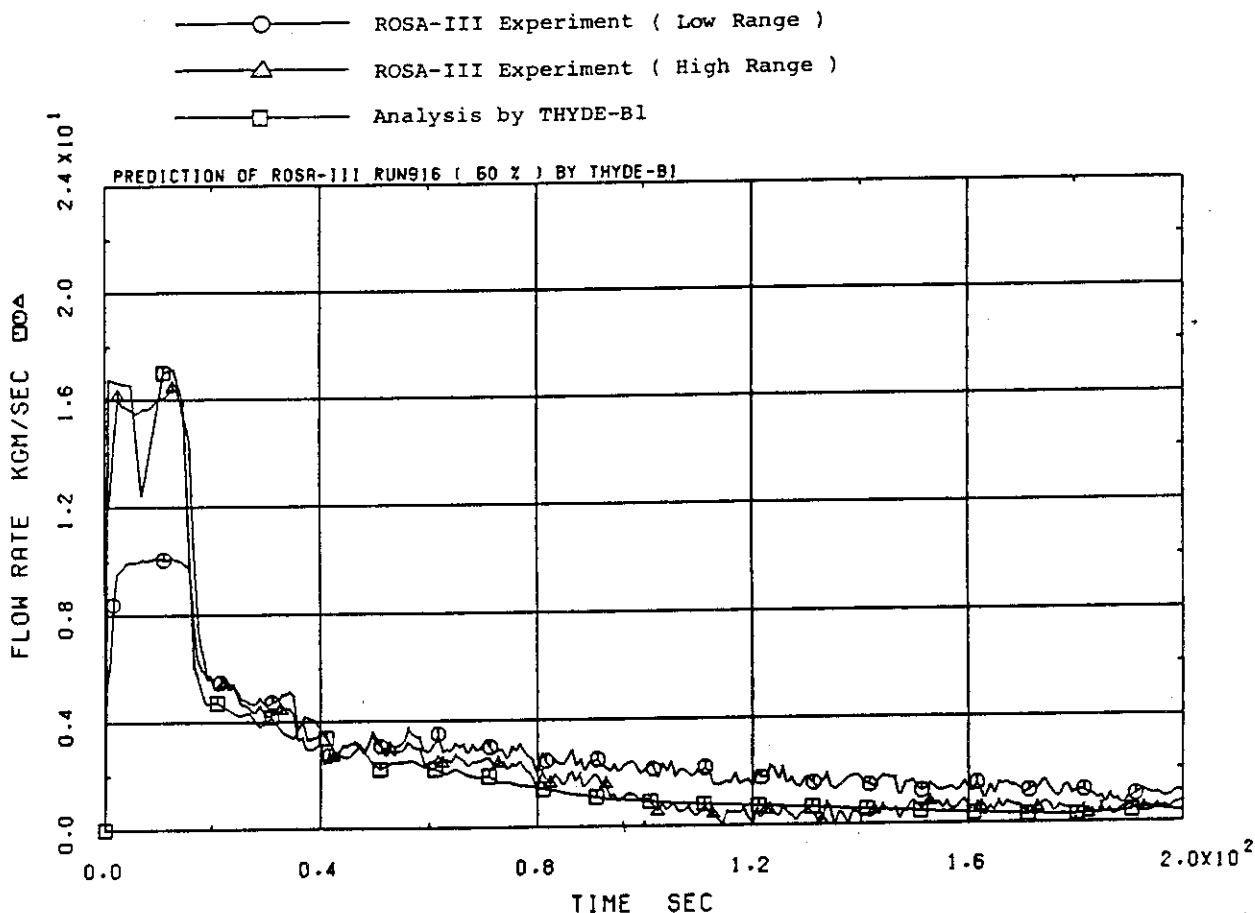


Fig. B.24 Measured vs. calculated break flow rates - 50 % break test



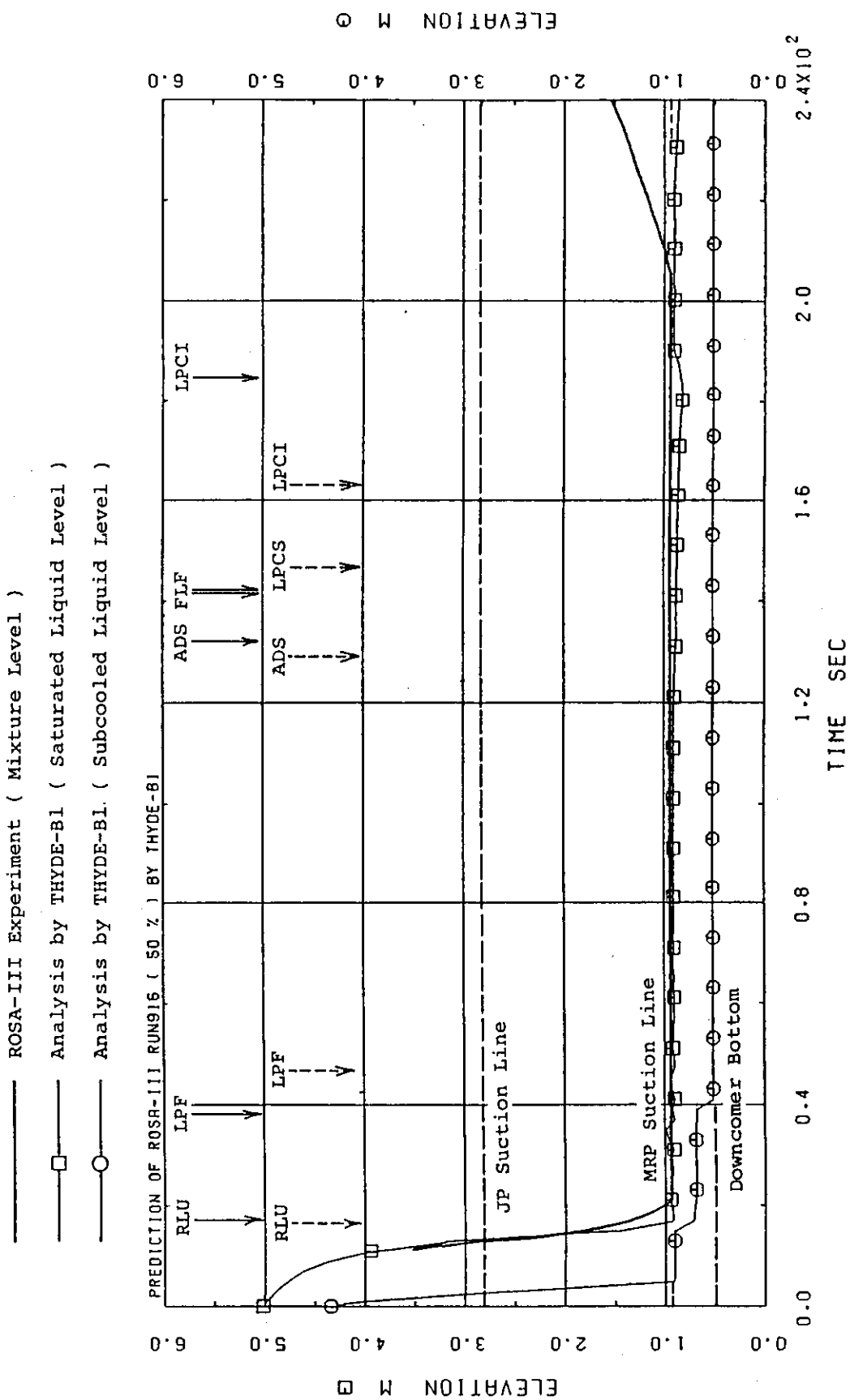


Fig. B.25 Measured vs. calculated downcomer mixture levels - 50 % break test

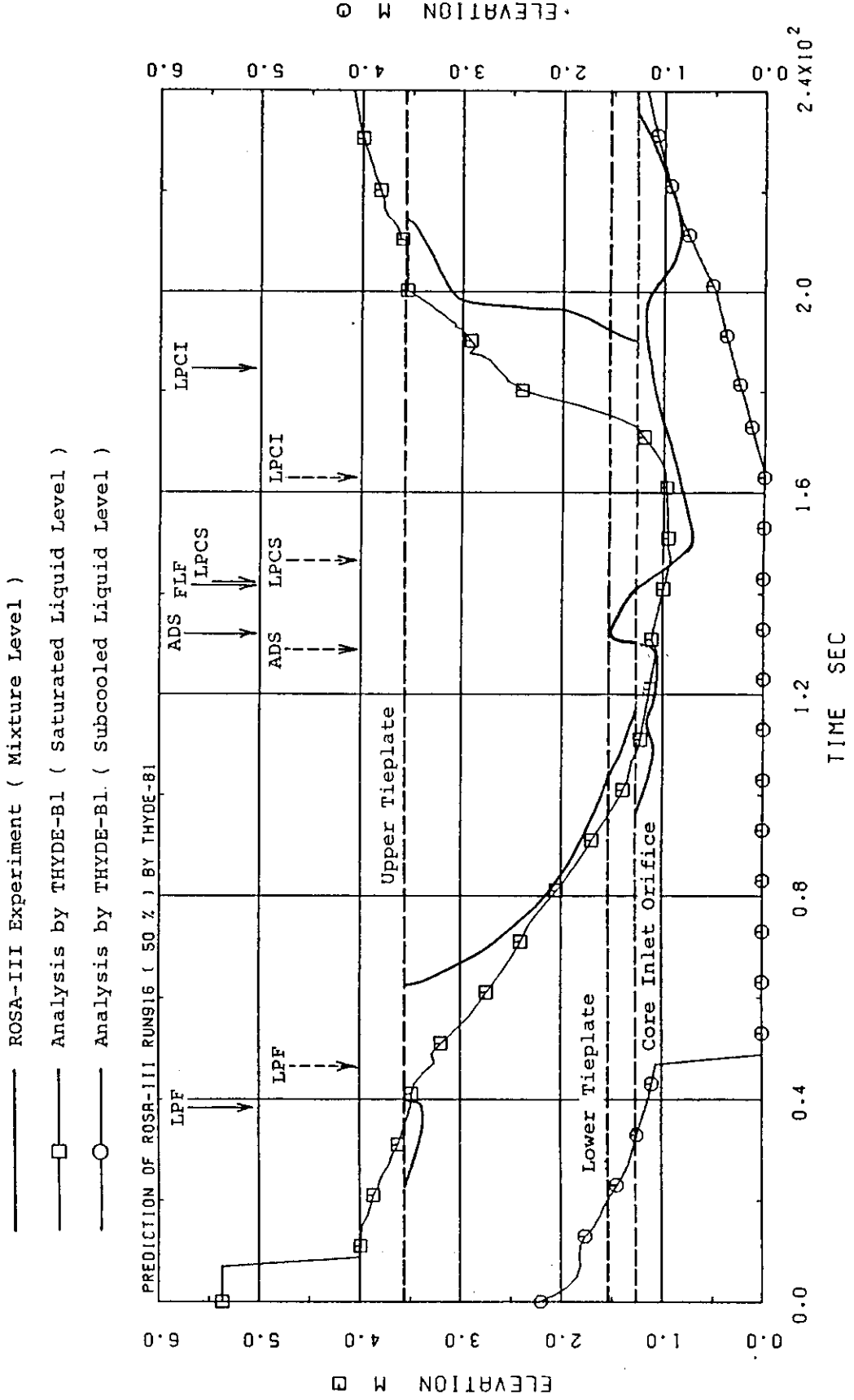


Fig. B.26 Measured vs. calculated core mixture levels - 50 % break test

× ◇ ↑ × ROSA-III Experiment  
 □ ○ △ + Analysis by THYDE-B1

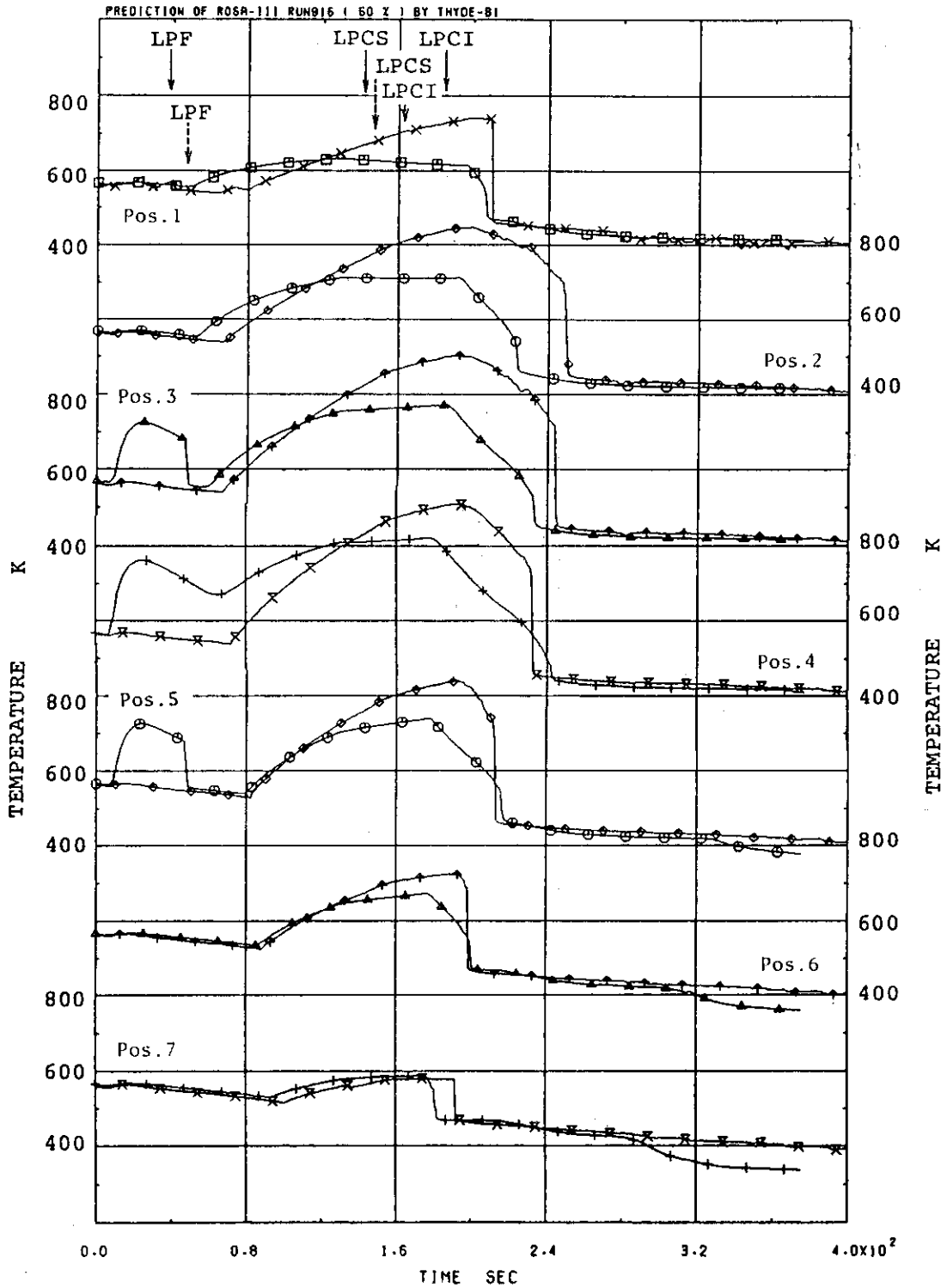


Fig. B.27 Measured vs. calculated peak-power rod temperatures - 50 % break test

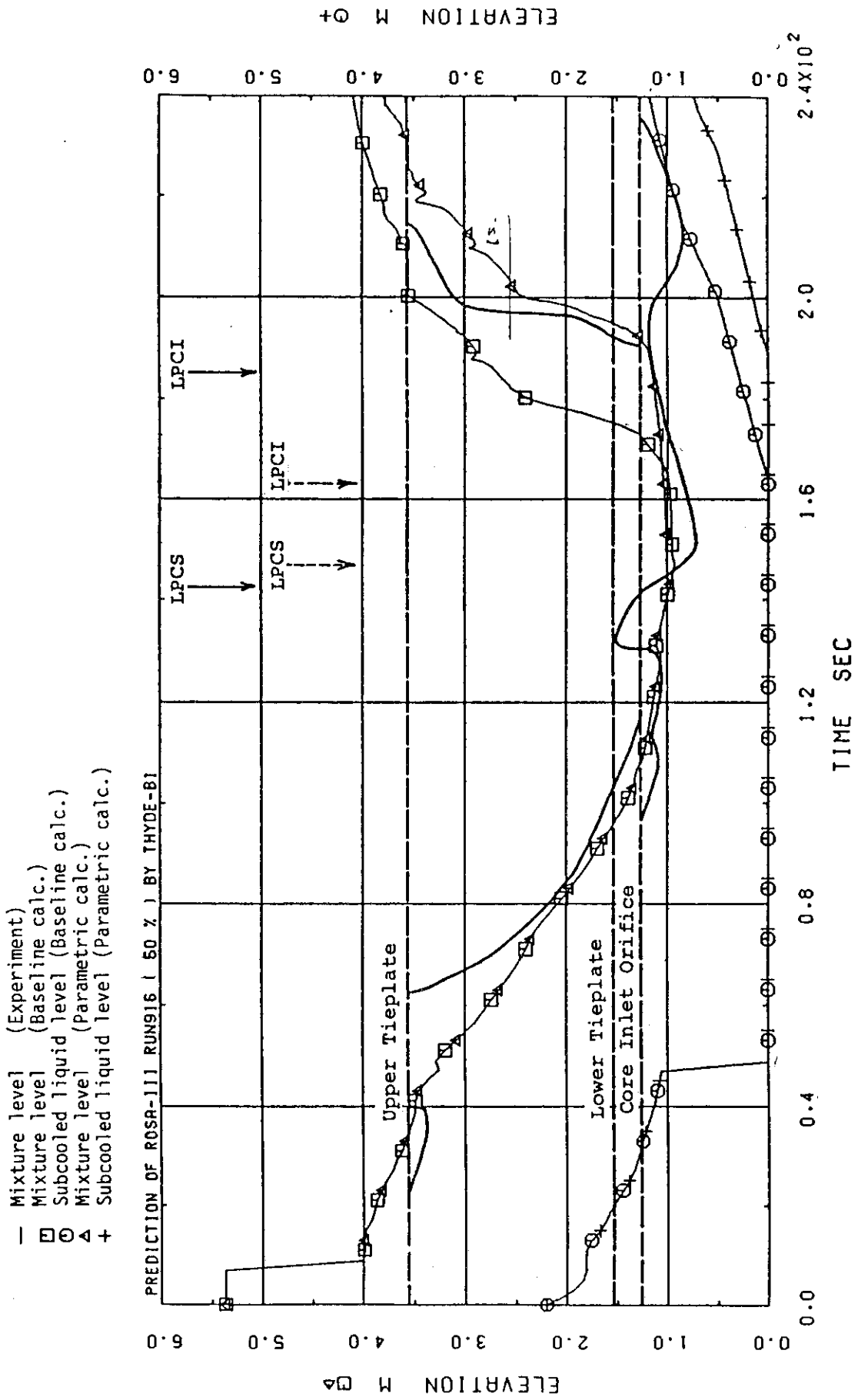


Fig. B.28 Core mixture level: baseline vs. parametric calculations  
 - 50 % break test

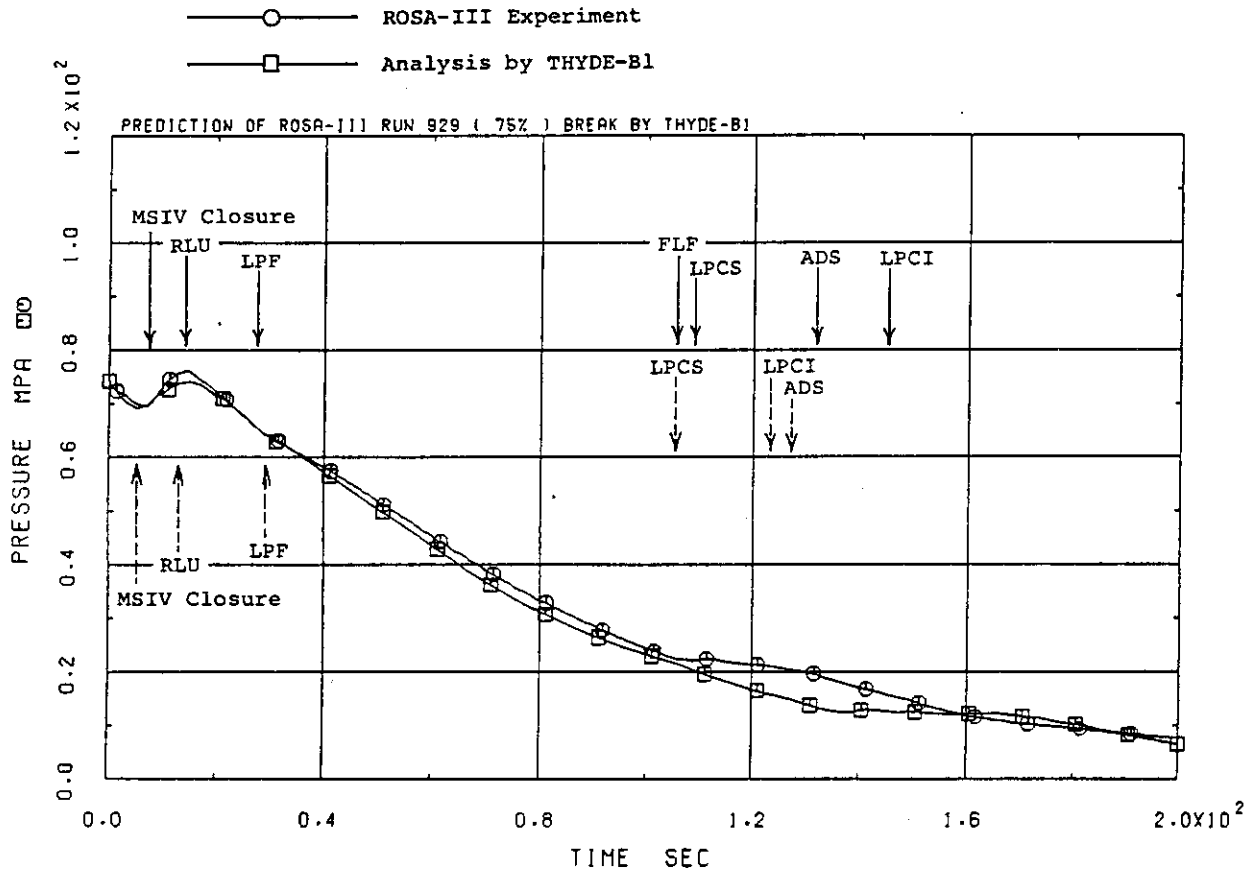


Fig. B.29 Measured vs. calculated system pressures - 75 % break test

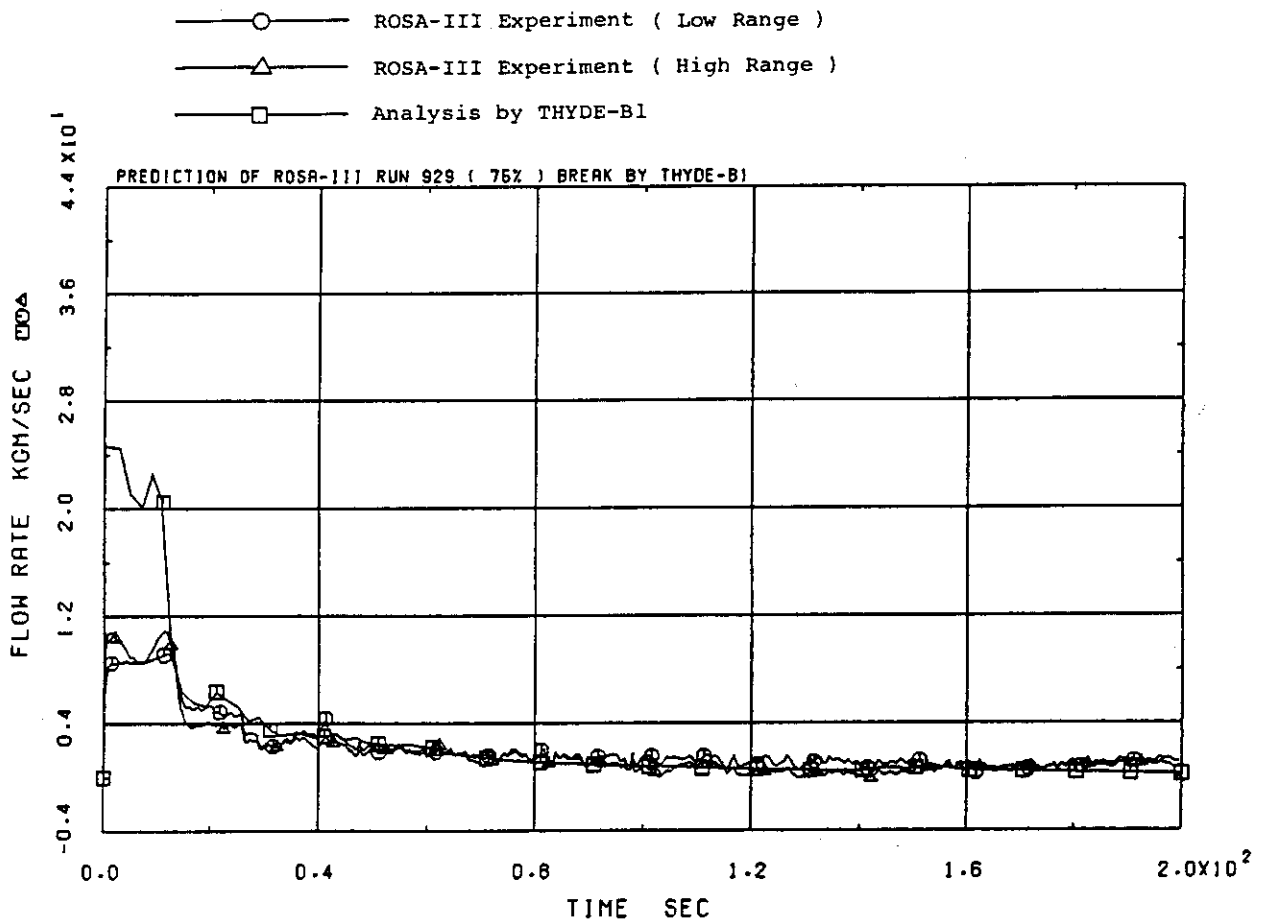


Fig. B.30 Measured vs. calculated break flow rates - 75 % break test

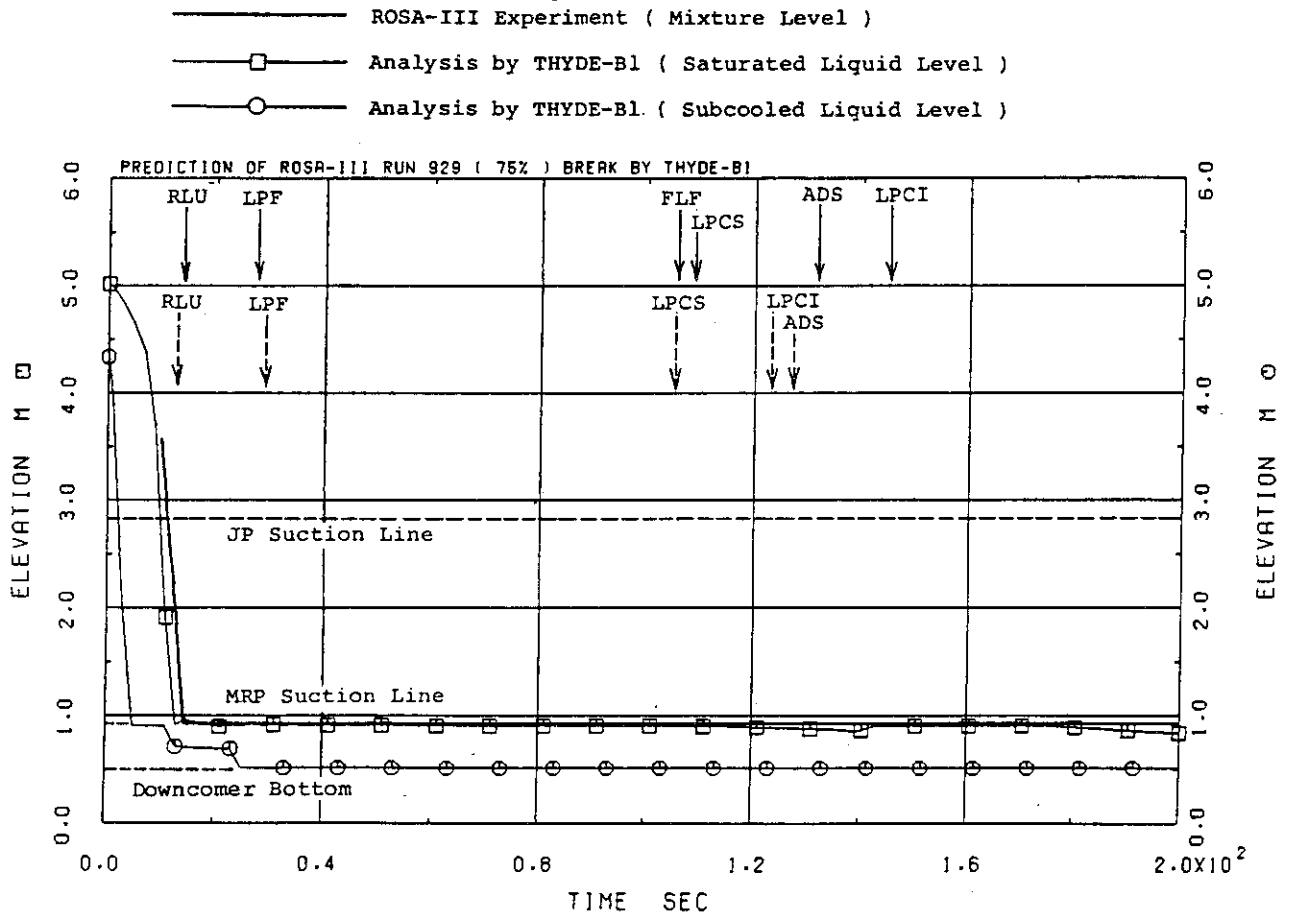


Fig. B.31 Measured vs. calculated downcomer mixture levels - 75 % break test

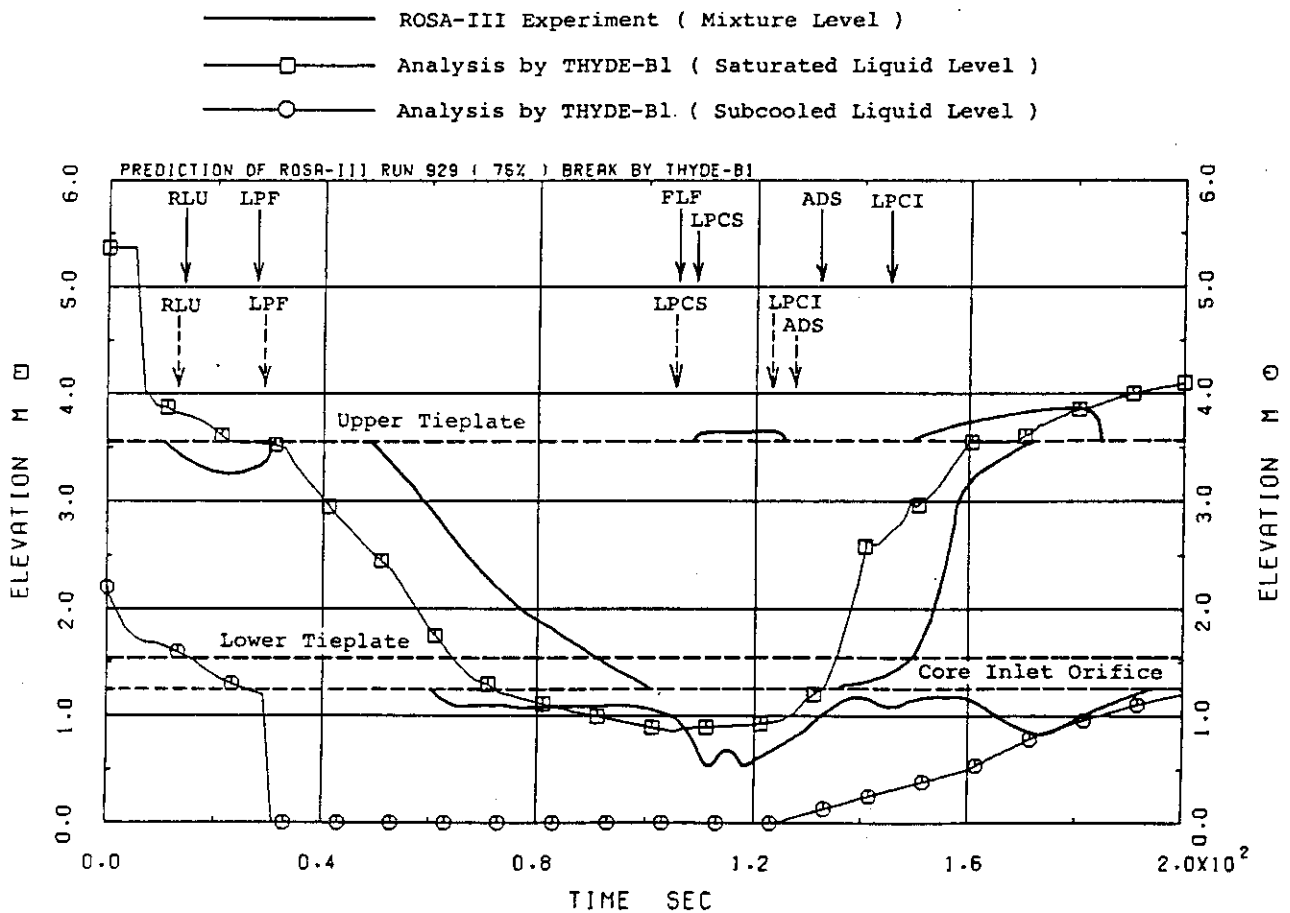


Fig. B.32 Measured vs. calculated core mixture levels - 75 % break test

× ◇ ↑ ×      ROSA-III Experiment  
 □ ○ △ +      Analysis by THYDE-B1

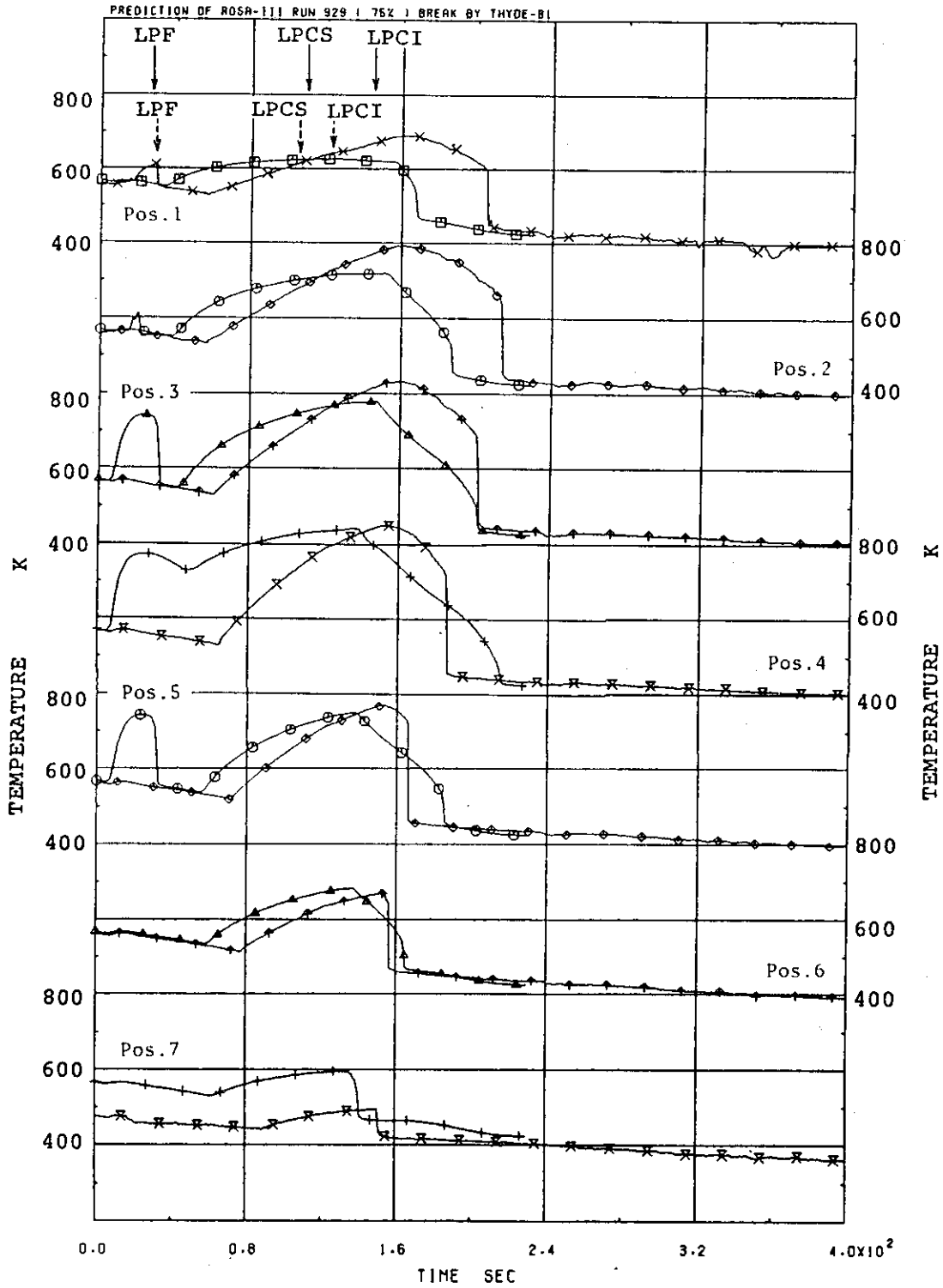


Fig. B.33 Measured vs. calculated peak-power rod temperatures - 75 % break test

- Mixture level (Experiment)
- Mixture level (Baseline calc.)
- Subcooled liquid level (Baseline calc.)
- + Mixture level (Parametric calc.)
- + Subcooled liquid level (Parametric calc.)

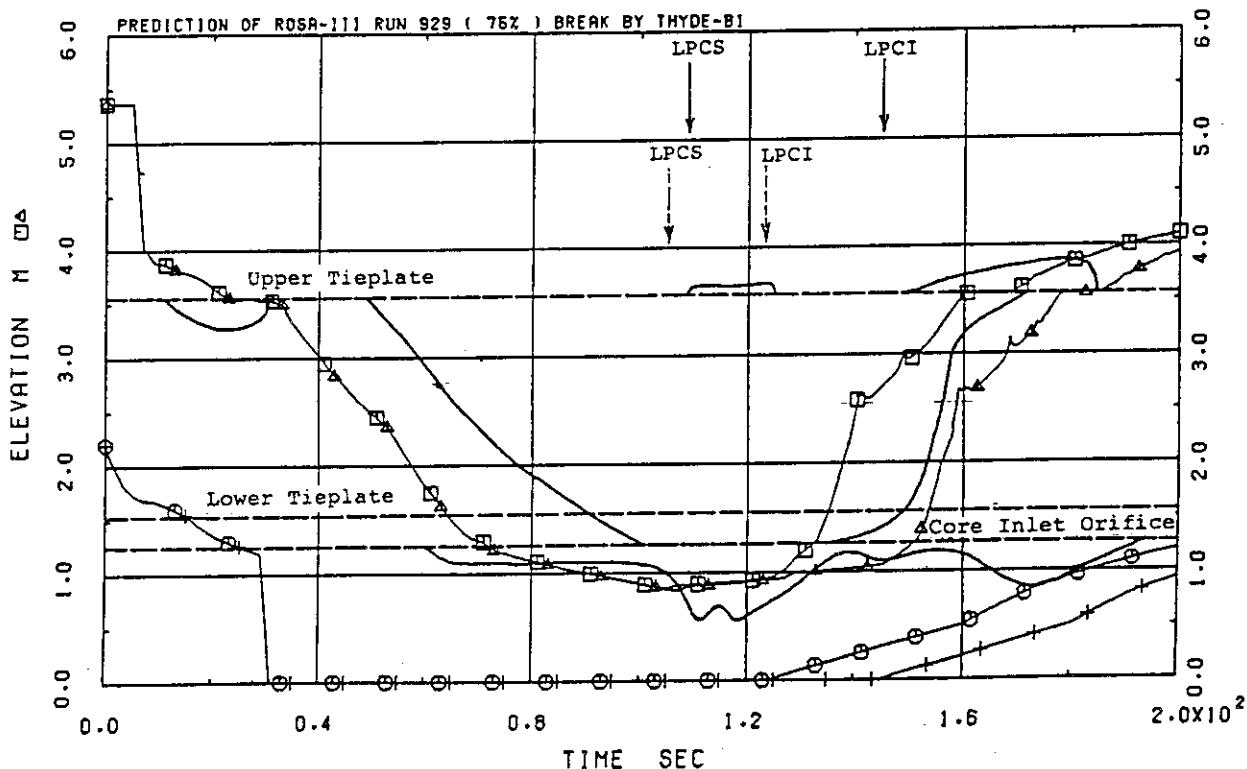


Fig. B.34 Core mixture level: baseline and parametric calculations - 100 % break test

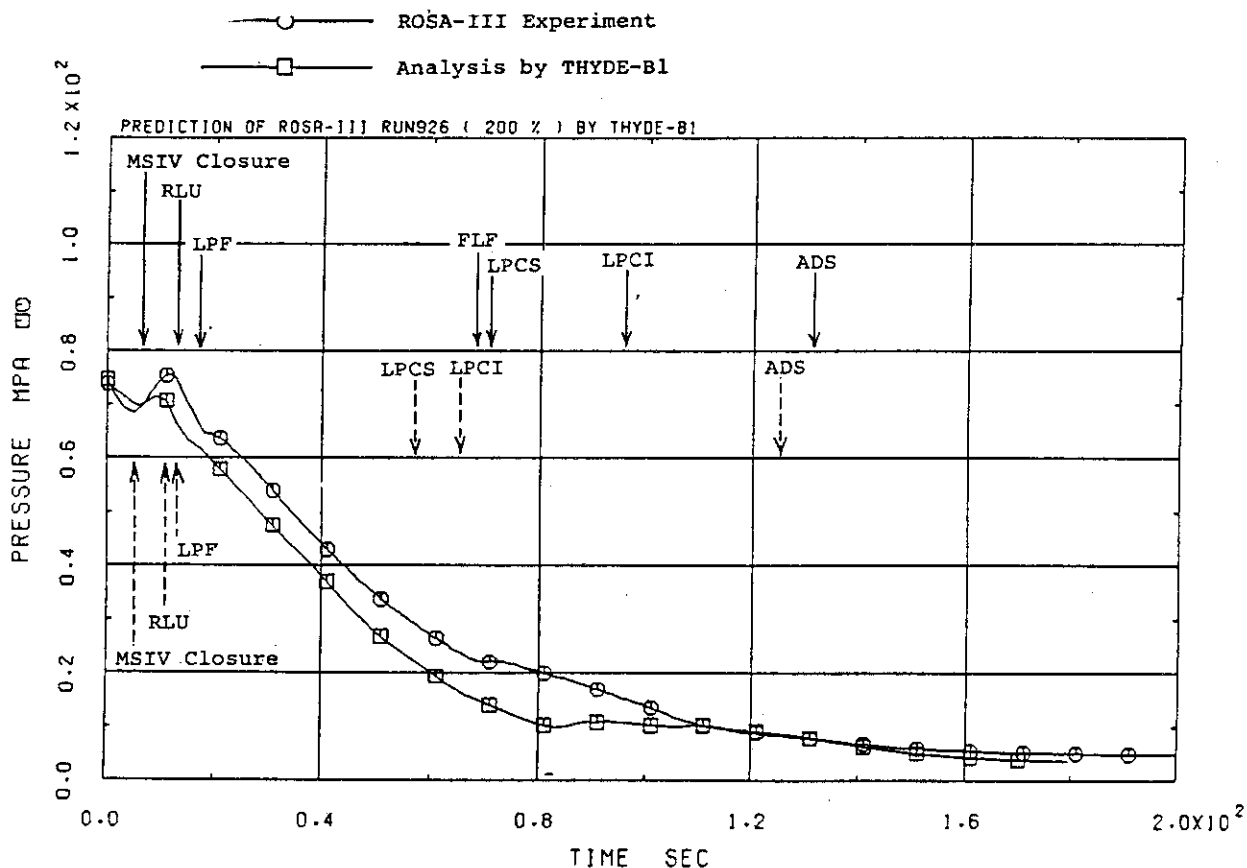


Fig. B.35 Measured vs. calculated system pressures - 200 % break test



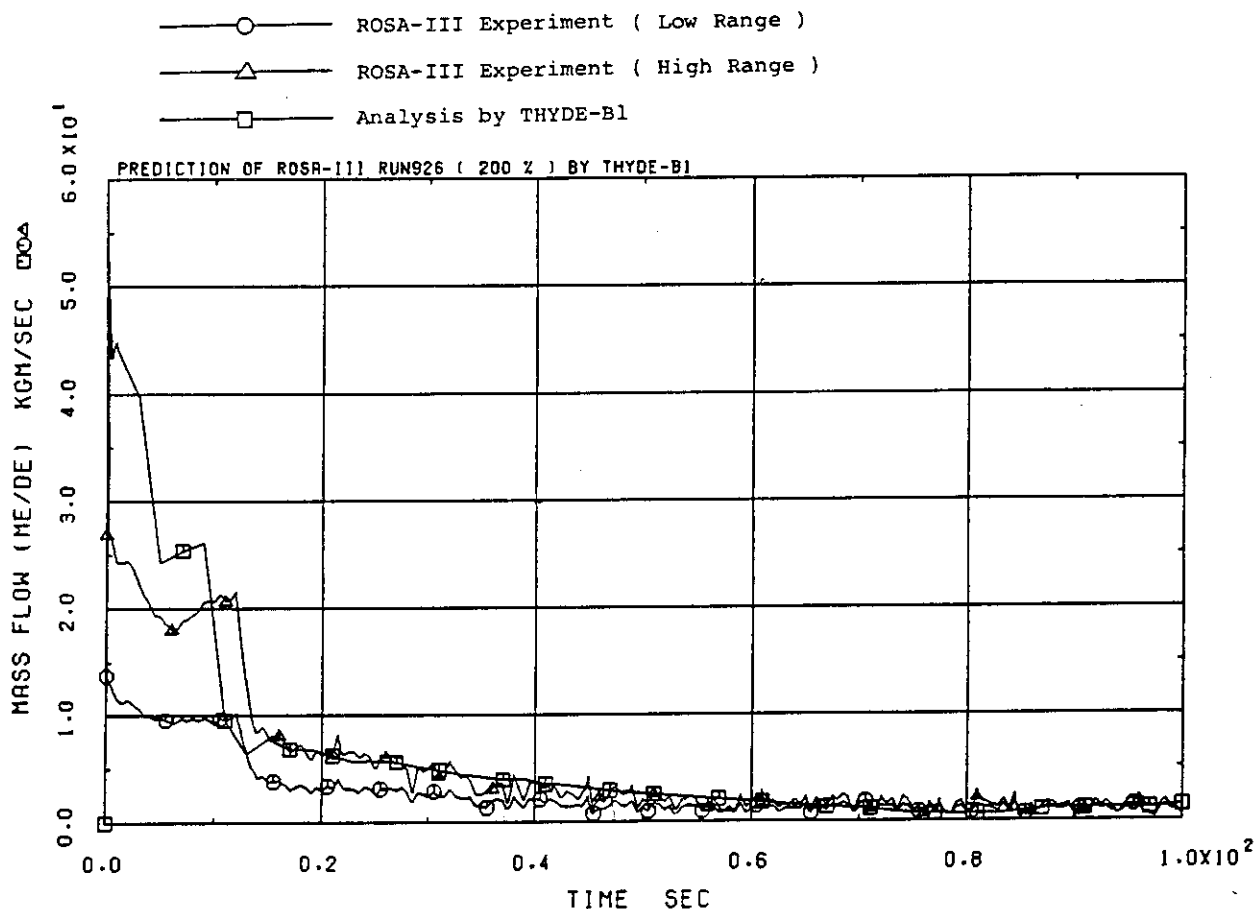


Fig. B.36 Measured vs. calculated break flow rates - 200 % break test

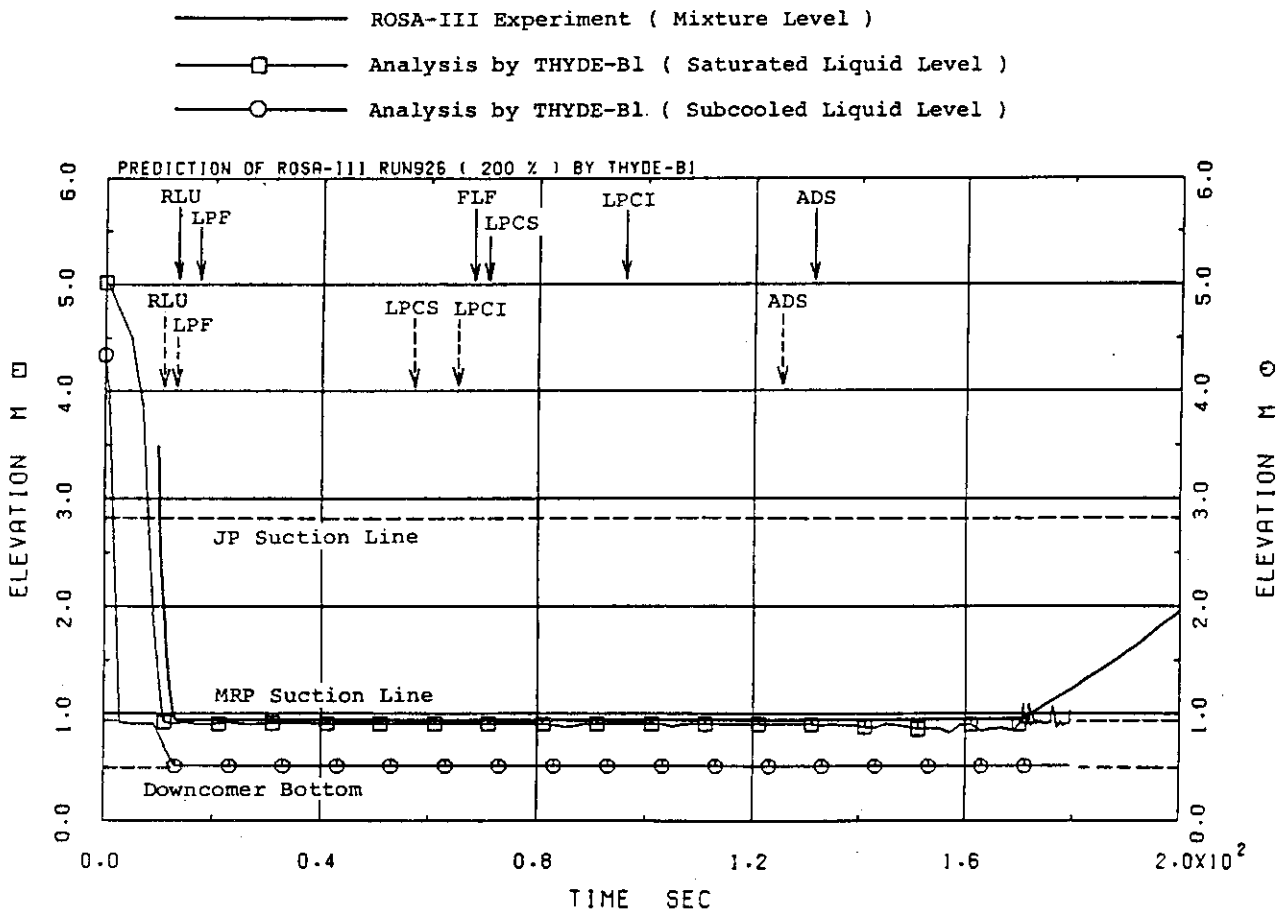


Fig. B.37 Measured vs. calculated downcomer mixture levels - 200 % break test

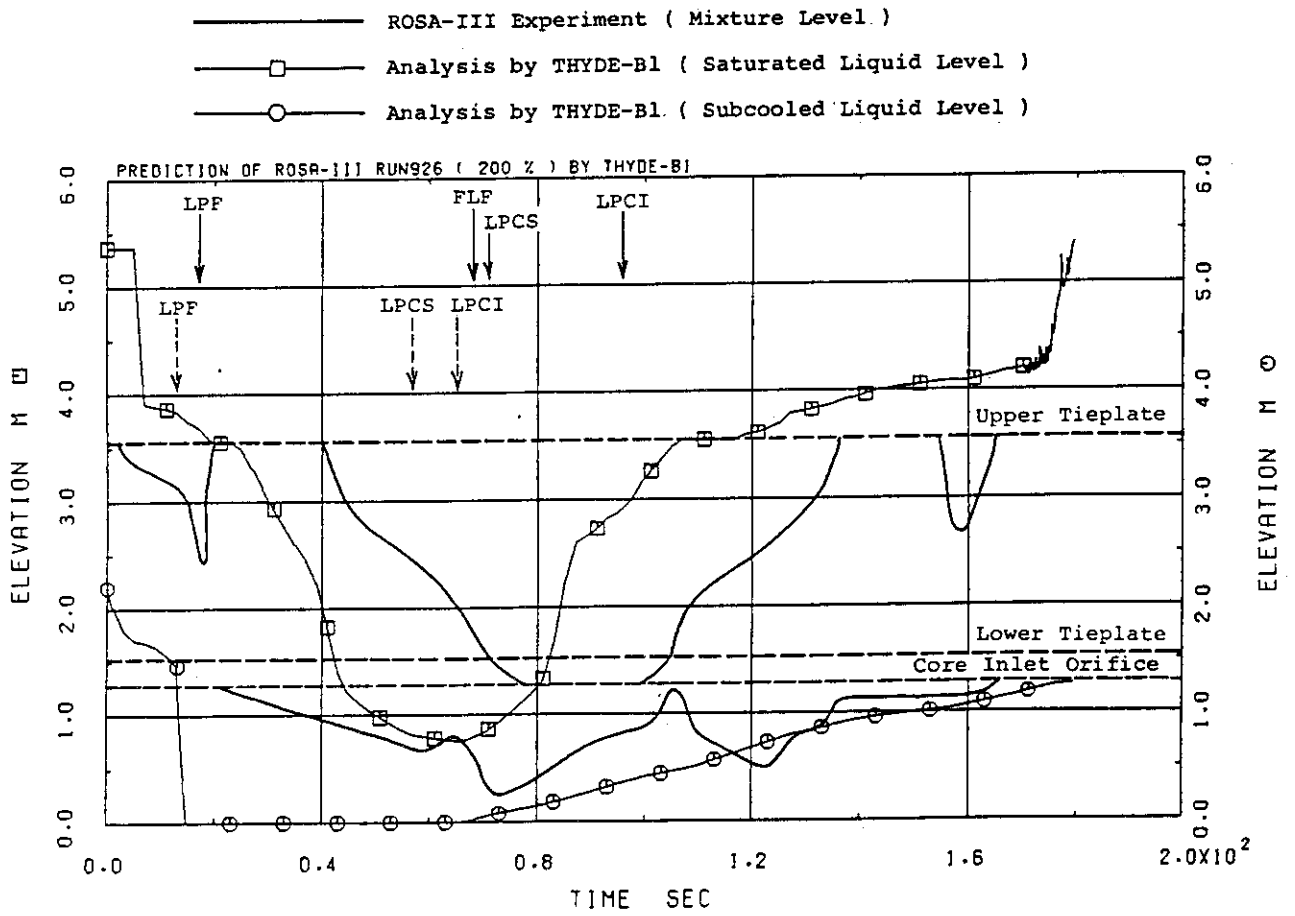


Fig. B.38 Measured vs. calculated core mixture levels - 200 % break test

× ◊ ↗ ✕      ROSA-III Experiment  
 □ ○ △ +      Analysis by THYDE-B1

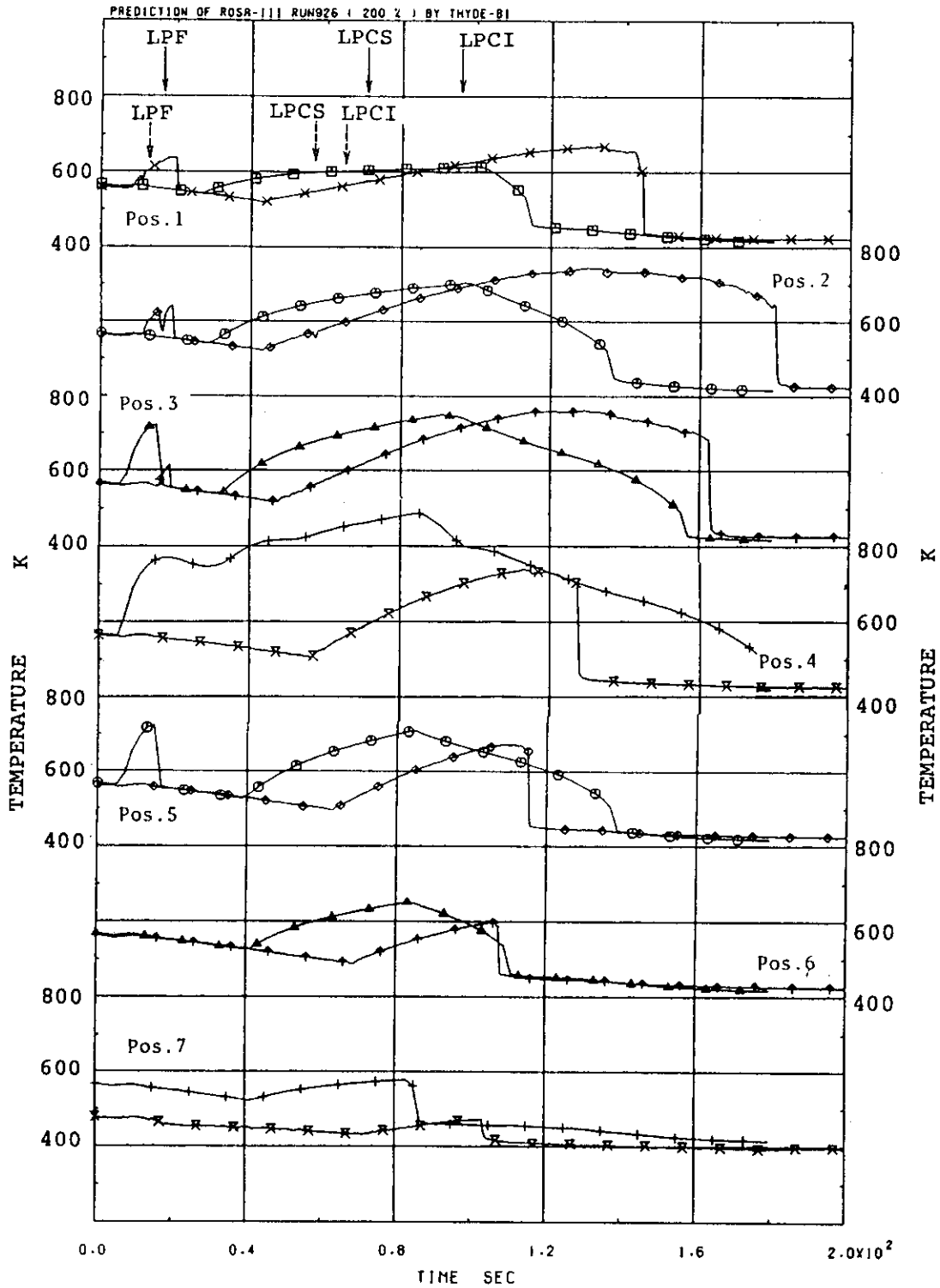


Fig. B.39 Measured vs. calculated peak-power rod temperatures - 200 % break test

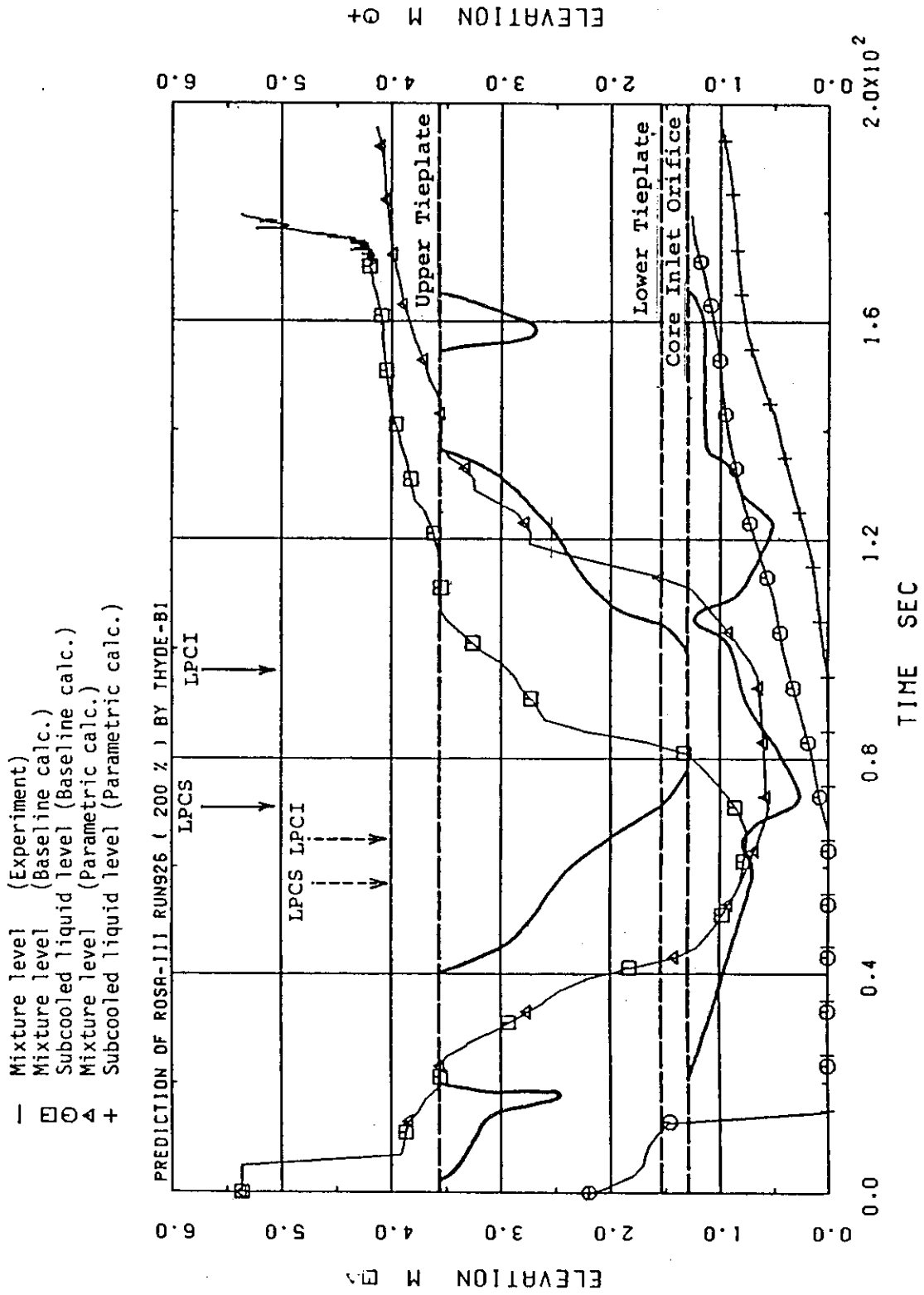


Fig. B.40 Core mixture level: baseline vs. parametric calculations  
 - 200 % break test