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THROUGH ANALYSIS OF LOFT L2-3 BY
THYDE-P CODE

(SAMPLE CALCULATION RUN 40)

October 1981

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Through Analysis of LOFT L2-3 by THYDE-P Code

(Sample Calculation Run 40)

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A through calculation of Experiment L2-3 of the Loss-of-Fluid Test (LOFT) Facility Power Ascension Series (Experiment Series L2) was performed with the THYDE-P code. The specific objectives of Experiment L2-3 were to determine the thermal-hydraulic behavior of the nuclear core and the thermal-mechanical response of the fuel rod cladding with a maximum linear heat generation rate of 39.4 kW/m. The THYDE-P code is a computer code to analyze both the blowdown and refill-reflood phases of loss-of-coolant accidents (LOCAs) of pressurized water reactors (PWRs) without a change in the methods and the models and is now under verification study and modification. The present calculation was performed by best estimate (BE) options as Sample Calculation Run 40, which is a portion of a series of THYDE-P sample calculations. The calculation was carried out from test initiation until complete submersion of the core volume with subcooled water, i.e. about 60 sec. The trend of the calculated cladding surface temperature was in good agreement with that of the experimental results.

Keywords : LOFT, LOCA, PWR, THYDE-P Code, Verification Study,
Sample Calculation, Fuel Rod Cladding, Blowdown,
Reflood

THYDE-PコードによるLOFT L2-3の一貫解析
(サンプル計算 Run 40)

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LOFT計画における出力上昇実験シリーズ(シリーズL2)中の実験L2-3の一貫解析を、THYDE-Pコードを用いて行った。L2-3実験の目的は、最大線出力密度39.4 kW/mにおける炉心の熱水力学的挙動、および燃料被覆管の熱機械学的挙動を同定することにあつた。THYDE-Pコードは、加圧水型軽水炉の冷却材喪失事故のプロードダウン、および再冠水過程を、手法やモデルの変更なしに一貫して解析する計算コードであり、現在、検証計算、および修正を行っている。本解析は最適評価オプションを用い、サンプル計算 Run 40 として行ったものであり、一連のTHYDE-Pサンプル計算の一部を成すものである。計算は、実験開始後炉心が完全に未飽和水中に没するまで(約60秒)行った。計算された燃料被覆管表面温のふるまいは、実験値との良い一致を示した。

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1. Introduction

A through calculation of LOFT L2-3⁽¹⁾⁽²⁾ was performed with the THYDE-P code⁽³⁾⁽⁴⁾⁽⁵⁾ not only to verify the system performance of THYDE-P but also to obtain better understanding of the experiment.

Experiment L2-3 was the second test in the Power Ascension Series (Experiment Series L2) of nuclear double-ended cold leg break tests and conducted at a maximum linear heat generation rate of 39.4 kW/m (36.7 MW). This power level is about 75% of the LOFT rated thermal power level of 50 MW and corresponds to the nominal full power operation of a commercial PWR. The LOFT ECCS simulates the ECCS of a commercial PWR. The accumulator (ACC), the high-pressure injection system (HPIS), and the low-pressure injection system (LPIS) were used during the experiment. Each system was arranged to inject scaled flow rates into the primary coolant system cold leg. Electrical power to the primary system motor generator sets was terminated 200 sec. after blowdown initiation and the primary coolant pumps began to coast down. The core volume reflood time was about 55 sec. after rupture⁽¹⁾.

In the present analysis, the LOFT system was nodalized into 43 nodes and 37 junctions. The active core was simulated by 4 nodes. A hot channel analysis was not performed but only an average channel analysis was done. The discharge coefficient for the Moody correlation⁽⁷⁾ was set to be 0.8. The ACC water temperature was given by an input as 307 °K, which was the same as the experimental data. In order to avoid unrealistically large pressure decrease due to low enthalpy ECC water, a time delay model⁽⁴⁾ for density change, which takes non-equilibrium effects into consideration, was applied.

The calculation proceeded until the core nodes were completely submerged with subcooled water, i.e. about 60 sec. after rupture, without any calculation mode change during the entire process. At the early stage of the blowdown phase, one or two peaks of the cladding surface temperature were also calculated as were observed in the experiment.

2. Description of LOFT L2-3

2.1 Primary Objectives

The specific objectives of Experiment L2-3 were to determine the thermal-hydraulic behavior of the nuclear core and the thermal-mechanical response of the fuel rod cladding with a maximum linear heat generation rate of 39.4 kW/m. The LOFT facility was configured to simulate a postulated loss-of-coolant accident in a commercial pressurized water reactor (~1000 MWe) resulting from a 200% double-ended offset shear break in the cold leg of the primary coolant system. During system depressurization into a simulated containment, emergency core cooling water was injected into the primary coolant system cold leg to provide data on the effects of emergency core cooling on system thermal-hydraulic response.

2.2 System configuration and Experiment Procedures

The LOFT major components are shown in Fig. 2.1. The core contains 1300 nuclear fuel rods arranged in five square and four triangular (corner) fuel modules, shown in Figure 2.2. On the detailed information on the LOFT system configuration, reference should be made to Ref. (1) and (2).

Immediately prior to blowdown, the pressurizer heaters were turned off. The quick-opening blowdown valve-2 (QOBV-2) commenced opening 1.9 msec before QOBV-1 and opened to the flow area of a 12-inch Schedule 60 (0.3 mm OD) pipe in 19.1 msec; QOBV-1 opened to the same flow area in 17.2 msec. Electrical power to the primary system motor generator sets was terminated at 200 sec after blowdown initiation. Emergency coolant injection was directed to the intact loop cold leg during blowdown. Injection from accumulator ACC-A at a system pressure of 4.18 MPa began approximately 17 sec after initiation of blowdown and continued for 32 sec. The HPIS flow was initiated by LOCE control 14 sec after the initiation of blowdown and was injected 1.3 l/sec. The LPIS flow was initiated by LOCE control 29 sec after the initiation of blowdown. Nitrogen gas from the accumulator entered the system at 49 sec and continued to flow for about 11 sec.

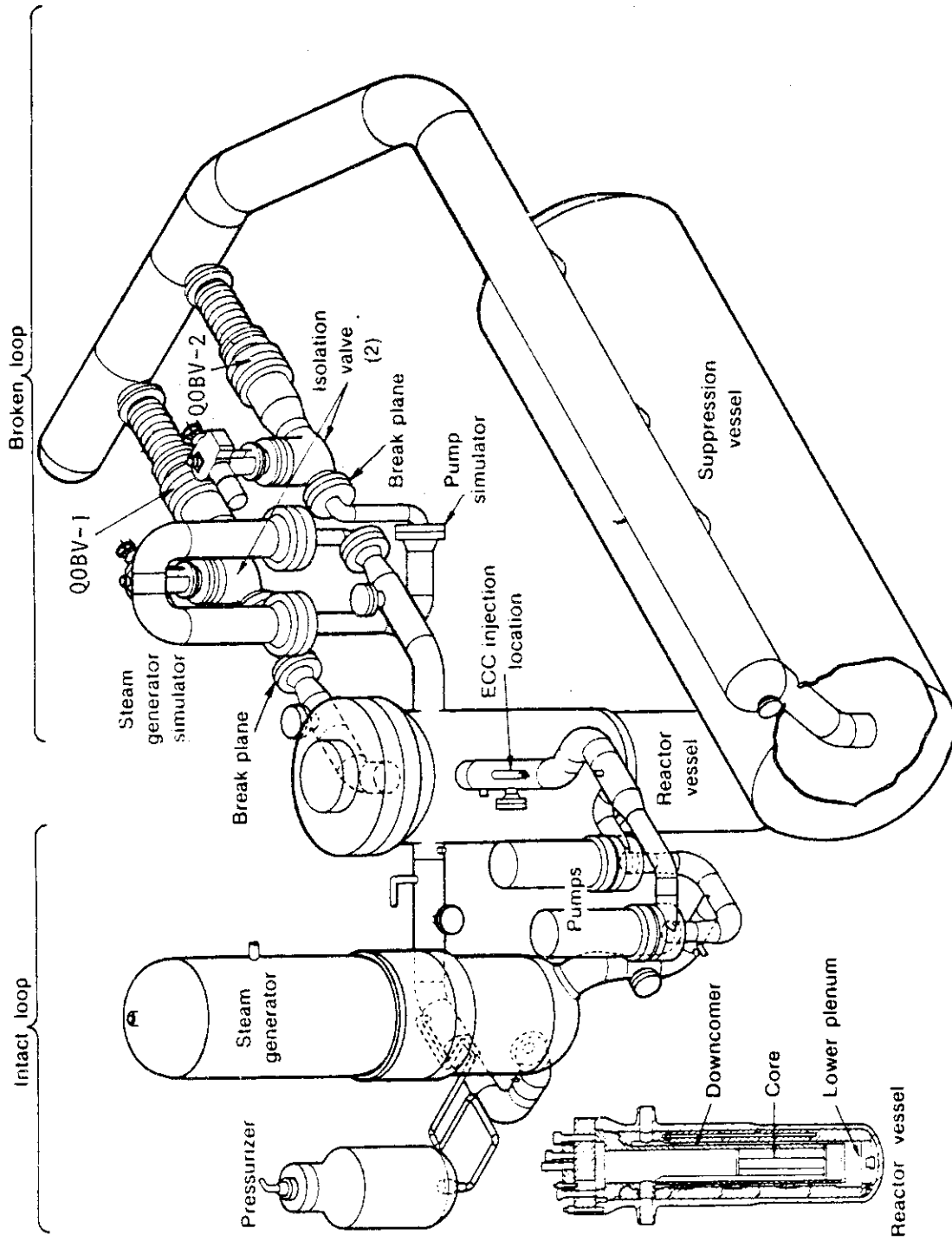


Fig. 2.1 LOFT Major Components

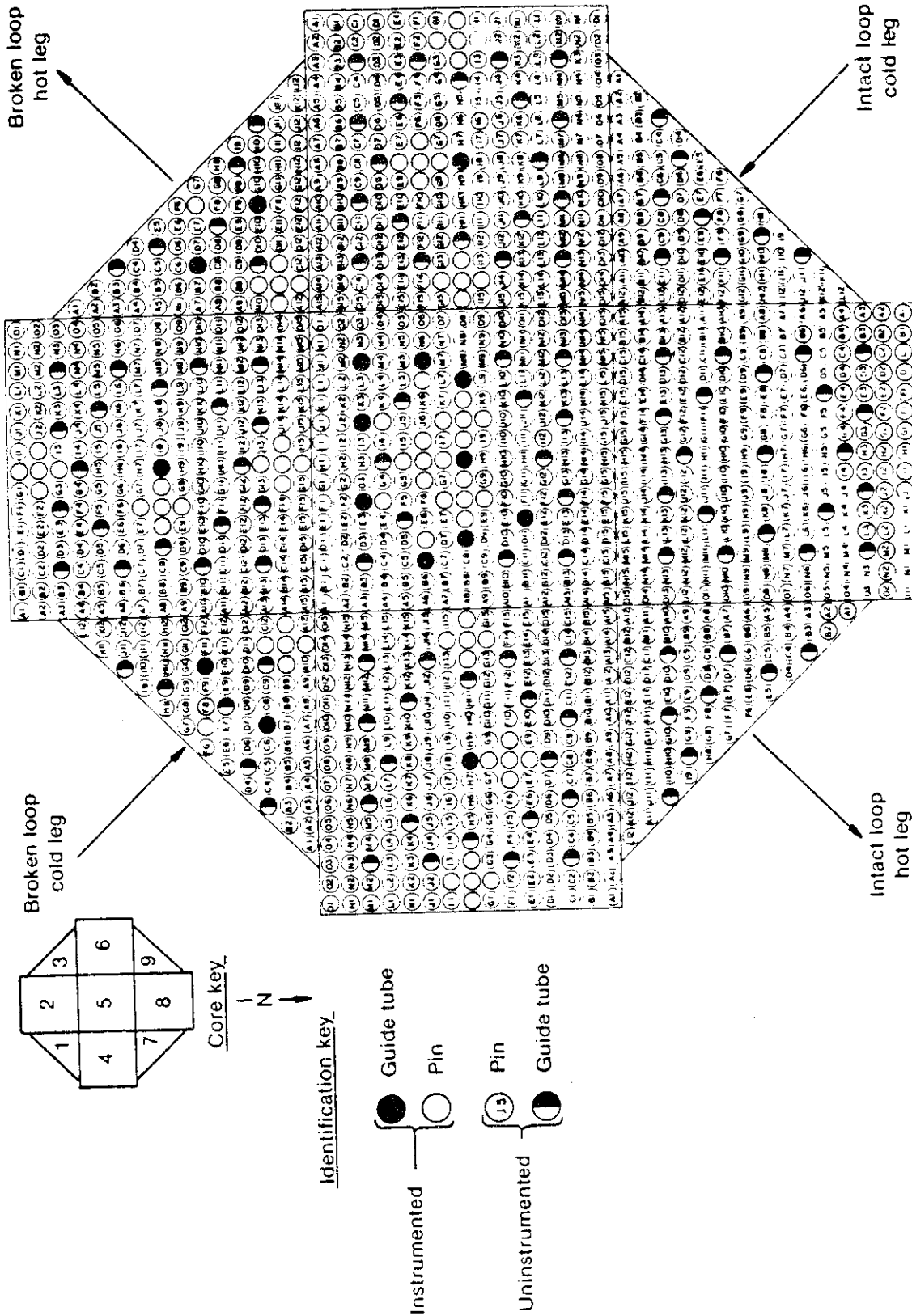


Fig. 2.2 LOFT Core 1 Configuration Showing Rod Designation

3. Analytical Models in Present Calculation

The models and the methods of the THYDE-P code are presented in detail in Ref. (3), some of which have been revised⁽⁴⁾⁽⁵⁾. Several models which may be most relevant to the present analysis are briefly described in this section.

3.1 CHF Correlations

In the present calculation, the Biasi correlation⁽¹³⁾ and the modified Zuber correlation⁽¹⁶⁾⁽¹⁷⁾ were adopted to predict CHF values for $G > G_{\min}$ and $G \leq G_{\min}$, respectively, where $G_{\min} = 273 \text{ kg/m}^2\text{s}$.

3.2 Heat Transfer Correlations

The heat transfer correlations tentatively applied in the present calculation are listed in Table 3.1.1 and 3.1.2. In heat transfer mode 4-5 (pool transition boiling), it was assumed that the Berenson correlation⁽¹⁹⁾ was not applicable when coolant quality was small enough, i.e. less than x_c . For simplicity in the present calculation, the heat flux value was set to be a constant ϕ_c . Namely,

$$\phi = \phi_c \quad \text{when} \quad x < x_c$$

where

$$\begin{aligned} x_c &= 0.1 \\ \phi_c &= 50 \text{ kcal/m}^2\text{s} \text{ (64,000 Btu/ft}^2\text{s)} . \end{aligned}$$

This heat transfer mode 4-5 played an important role in the reflooding calculation as will be shown in Sec. 5.

3.3 Break Flow Calculation

The slightly modified⁽³⁾ Zaloudek correlation⁽⁶⁾ and the Moody correlation⁽⁷⁾ are implemented for a subcooled and a saturated condition, respectively, in the present version of THYDE-P. The discharge coefficient for the Moody correlation was assumed to be 0.8, which was the same as that in the analysis of LOFT L2-2⁽⁴⁾.

Table 3.1.1 Heat Transfer Correlations

Mode		Conditions		Correlations
Core	SG	Coolant Condition	Other conditions	
1	1	Subcooled water	$T_{wall} < T_{sat}$	Dittus-Boelter ⁽⁹⁾
2	2	Subcooled water	$T_{wall} > T_{sat}$	Interpolation between D-B and J-L
3	3	Saturated state	$\phi < \phi_{CHF}$	Jens and Lottes ⁽¹⁰⁾
4	/	Saturated state	$\phi > \phi_{CHF}$	(see Table 3.1.2)
5	5	Superheated steam	$Re < 3000$	McEligot ⁽¹²⁾
6	6	Superheated steam	$3000 < Re < 5000$	McEligot ⁽¹²⁾
7	7	Superheated steam	$Re > 5000$	McEligot ⁽¹²⁾
/	8	Saturated state	$T_{coolant} > T_{wall}$	Condensation ⁽¹⁴⁾

Table 3.1.2 Heat Transfer Correlations in Mode 4

Mode	Conditions	Correlations
4-1	$G > G_{min}, \phi_{4-1} > \phi_{4-2}$	McDonough, Milich and King ⁽¹⁵⁾
4-2	$G > G_{min}, \phi_{4-1} < \phi_{4-2}$	Groenevelt ⁽¹¹⁾
4-3	$G < G_{min}, \Delta T_s < \Delta T_{min}$	Pool transition boiling correlation ⁽⁸⁾
4-4	$G < G_{min}, \Delta T_s > \Delta T_{min}$	Berenson ⁽¹⁹⁾
4-5	$G < G_{min}, x < x_c$	Pool transition boiling

3.4 Time Delay Model for Density Change

It is well known that thermal non-equilibrium effects due to low enthalpy ECC water injection is considerably large. In general in analyses by thermal equilibrium models, calculations may fail because of unrealistically large pressure drop due to an overestimated condensation rate. In THYDE-P, to avoid the difficulty, a time delay model for density change⁽⁴⁾ which takes into account phenomenologically non-equilibrium effects is implemented as follows:

$$\frac{\partial \rho^*}{\partial t} = \frac{\rho - \rho^*}{\tau_D} \quad (3.4.1)$$

where

$$\rho^* = \alpha^* \rho_{gs} + (1 - \alpha^*) \rho_{fs}$$

$$\rho = \alpha \rho_{gs} + (1 - \alpha) \rho_{fs}$$

and

- ρ equilibrium node average density
- ρ^* non-equilibrium node average density
- α equilibrium void fraction
- α^* non-equilibrium void fraction.

The parameter τ_D in Eq. (3.4.1) is called a delay parameter which specifies the time delay of the average density. It should be noted that when τ_D asymptotically approaches to zero, the model reduces to the equilibrium model, i.e. $\rho^* = \rho$. In the present analysis, this model was applied after ACC injection initiated. In the model, what is the most difficult is to determine the delay parameter, which may be dependent on flow regimes, node geometries, pressure, etc. In the present analysis, a simple formulation, which is the same as that in the analysis of LOFT L2-2⁽⁴⁾, was assumed as follows:

$$\tau_D = \begin{cases} 0 & x > x_0 \\ c_n \{ \cos(x/x_0) + 1 \} / 2 & 0 < x < x_0 \\ c_n & x < 0 \end{cases} \quad (3.4.2)$$

where

$$x = (h - h_{fs}) / h_{gs}, \text{ and}$$

$$x_0 = 0.2$$

and the constant c_n is so given as to be proportional to the node volume with $c_n = 1$ sec for the core nodes. This formulation for τ_D is the same as that tentatively applied in the analysis of LOFT L2-2⁽⁴⁾. A physical model to evaluate the parameter is yet to be developed.

4. Input Data and Results of Steady State Adjustment

The input data in the present analysis are listed in App. A. The initial conditions are compared with the experimental data in Table 4.1. The input data and the results of steady state adjustment⁽³⁾ are summarized in this section.

(1) Nodalization

The nodalization scheme in the present analysis is shown in Figs. 4.1(a) and (b) and the node geometrical data are shown in Table 4.2. The pressure vessel is expressed by nodes from 22 to 33. The downcomer was simulated by a single node whose number was 22. The active core was nodalized into 4 nodes, i.e. nodes from 26 to 29. The double-ended break was assumed to occur at junction 6. ECC water was injected into mixing junction 26.

The loss coefficients of nodes are listed in Table 4.3.

(2) Trip Data

The following trip actions were taken by inputs as follows.

<u>Trip action</u>	<u>Time after rupture (s)</u>
SG secondary feed water stop	0.002
SCRAM	0.103
HPIS injection initiation	14.0
LPIS injection initiation	29.0

(3) Core Data

Initial power level 36 MW .

The initial heat fluxes are shown as follows.

<u>Node No.</u>	<u>Heat flux (kcal/m²s)</u>
25	106.6
26	179.7
27	137.0
28	45.4

Number of fuel rods	1300
Cladding outer diameter	1.072×10^{-2} m
Cladding thickness	6.172×10^{-4} m
Fuel pelet diameter	8.934×10^{-3} m
Rod pitch	1.430×10^{-2} m
Gap gas mole number	0.57 mole
Plenum gas volume	5.493×10^{-6} m ³

The gas molecular fractions of the gap gas are listed as follows.

Gas	Molecular fraction (-)
He	0.887
Xe	0.0355
Kr	0.0063
N ₂	0.0712

As a result of steady state adjustment, the following properties were obtained.

Steady state gap pressure 3.0×10^5 Pa

The fuel center temperatures, the cladding surface temperatures and the heat transfer coefficients are shown as follows.

Node No.	Fuel center temp.(°C)	Cladding surface temp.(°C)
24	287.9	287.9
25	782.8	325.1
26	1173.8	346.0
27	950.6	346.0
28	518.1	333.0
29	320.9	320.9

Node No.	Heat transfer coefficient (kcal/m ² s°C)	
	Cladding surface	Gap
25	3.64	0.51
26	4.76	0.56
27	4.88	0.53
28	3.77	0.48

(4) Steam Generator Data

The primary and secondary systems of the steam generator were simulated by nodes 13 to 16 and node 42, respectively. Nodes 14 and 15 simulated primary coolant in the U-tubes. The input data for the steam generator are summarized as follows.

Plenums	
Volume	0.353 m ³
Hydraulic diameter	0.908 m
Height	0.518 m
U-tubes	
Number	1845
Outer diameter	1.021×10^{-2} m
Height	2.483 m
Pitch	1.905×10^{-2} m
Secondary system	
Pressure	60.99 atm
Feed water enthalpy	213.8 kcal/kg
Feed water mass flow rate	19.5 kg/s
Flow area	1.589 m ²
Height	4.188 m
Subcooled water level	0.3 m
Void fraction of saturated region	0.3

The initial heat flux values are listed as follows.

Node No.	Heat flux ratio (-)
13	0.71
14	0.29

The results of steady state adjustment concerning the steam generator are listed as follows.

Region	Enthalpy (kcal/kg)	Bulk temperature (°c)	Mass (kg)
Saturated	298.8	277.4	3324.
Subcooled	213.8	209.4	408.5

Node No.	Wall temperature (°C)	
	Primary side	Secondary side
14	560.2	554.9
15	556.7	551.8

Node No.	Heat transfer coefficient (kcal/m ² s°C)	
	Primary side	Secondary side
14	3.90	7.87
15	3.85	4.65

(5) Pressurizer Data

The input data for the pressurizer, node 41, are summarized as follows.

Flow area	0.557 m ²
Height	1.7235 m
Subcooled water level	0.4 m
Void fraction of saturated region	0.4

The results of steady state adjustment were as follows:

Steady state pressure	15.07 MPa
Enthalpy of saturated region	408.8 kcal/kg
Enthalpy of subcooled region	346.6 kcal/kg
Total mass of saturated region	294.9 kg
Total mass of subcooled region	151.3 kg

(6) Pump Data

The primary coolant pumps were simulated by nodes 18 and 19.

Rated speed	3530 rpm
Rated flow	0.3155 m ³ /s
Rated head	108.1 m
Rated torque	500.24 J/rad
Rated density	613.73 kg/m ³

Moment of inertia	1.4382 kg m ² /rad ²
Steady state speed	1270 rpm

In the present analysis, the constant pump speed option was applied throughout the analysis. As to the single-phase and two-phase pump characteristic curves, reference should be made to Ref. (4).

(7) ECCS Data

Accumulator	
Liquid volume	1.71 m ³
Gas volume	0.96 m ³
Liquid enthalpy	34.2 kcal/kg
Initial pressure	41.25 atm

The total liquid mass was calculated to be 1.703×10^3 kg.

HPIS and LPIS

Liquid enthalpy	24 kcal/kg
-----------------	------------

The injection mass flow rates from HPIS and LPIS were given by inputs as time tables based on the experimental data.

(8) Simulated SG and Pump Data

The simulated SG and pump in the broken loop hot leg were nodalized into nodes 3 to 7. The loss coefficients in these nodes are shown in Table 4.3.

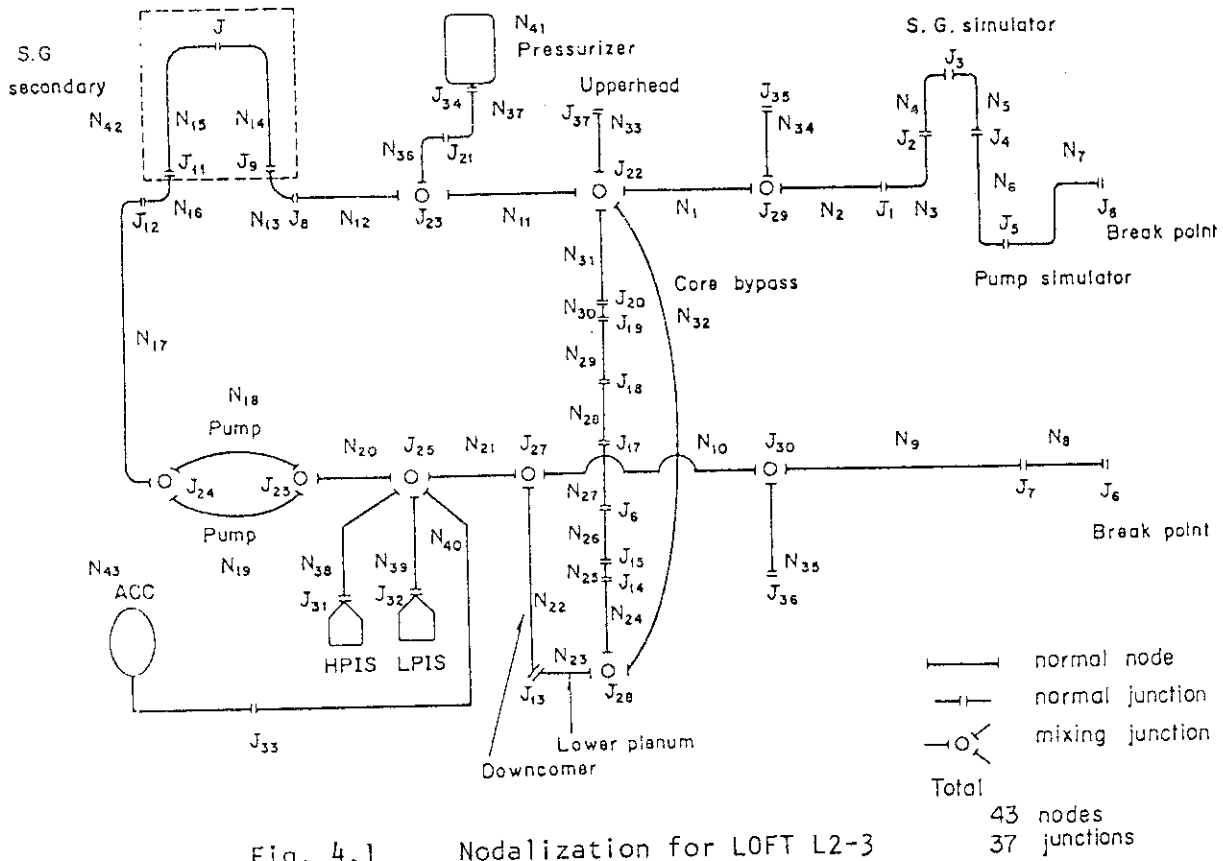


Fig. 4.1 Nodalization for LOFT L2-3

(a) Major components

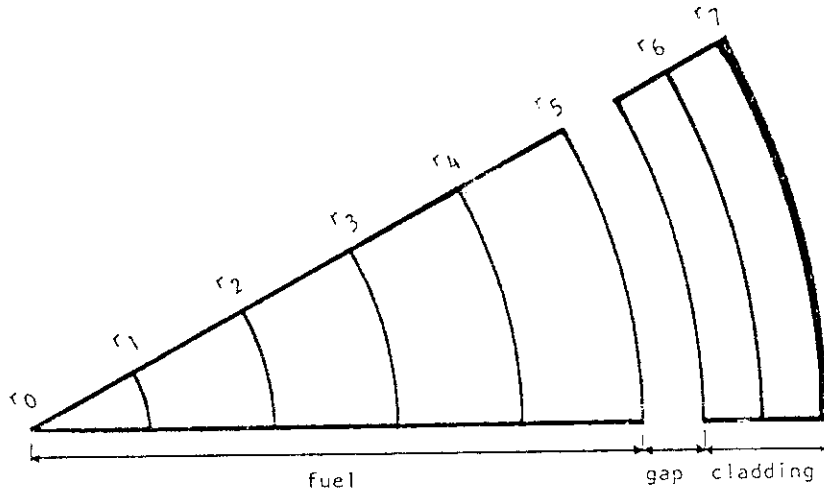


Fig. 4.1 Nodalization for LOFT L2-3

(b) Within fuel rod

Table 4.1 Initial Conditions for LOFT L2-3

Items	Measured value	Analysis
Primary coolant system		
Mass flow rate (kg/s)	199 \pm 6.3	199.0
Pressure (MPa)	15.06 \pm 0.03	15.08
Cold leg temperature (K)	560.7 \pm 1.8	561
Hot leg temperature (K)	592.9 \pm 1.8	593
Reactor vessel		
Power level (MW)	36 \pm 1	36.0
Maximum linear heat generation rate (kW/m)	39 \pm 3	22.4
Pressurizer		
Steam volume (m ³)	0.293 \pm 0.008	0.295
Water volume (m ³)	0.670 \pm 0.008	0.665
Water temperature (K)	615.3 \pm 3.0	613 ^(a) , 593 ^(b)
Pressure (MPa)	15.06 \pm 0.03	15.07
Level (m)	1.19 \pm 0.01	1.19 ^(c)
Broken loop		
Hot leg temperature (K)		
Near vessel	565.5 \pm 1.8	593
Near break	556.5 \pm 1.8	593
Cold leg temperature (K)		
Near vessel	554.3 \pm 1.8	561
Near break	550.3 \pm 1.8	561
Steam generator secondary side		
Water level (m)	3.11 \pm 0.025	3.02 ^(c)
Water temperature (K)	482.1 \pm 3	550 ^(a) , 482 ^(b)
Pressure (MPa)	6.18 \pm 0.08	6.18
Mass flow rate (kg/s)	19.5 \pm 0.4	19.5
Accumulator		
Gas volume (m ³)	0.96 \pm 0.03	0.96
Water volume injected (m ³)	1.71 \pm 0.03	1.71
Temperature (K)	307.2 \pm 3	307

(a) and (b) indicate saturated region and subcooled region, respectively.
(c) : What is called "collapsed water level".

Table 4.2 Node Geometrical Data

<u>Node No.</u>	<u>Description</u>	<u>Flow Area</u> <u>A (m²)</u>	<u>Node Length</u> <u>L (m)</u>	<u>Node Height</u> <u>H_L (m)</u>
1	Broken loop hot leg	0.06344	1.332	0.0
2	Broken loop hot leg	0.06344	0.6965	0.0
3	Broken loop hot leg	0.00836	1.517	0.7174
4	Broken loop hot leg	0.09539	3.228	2.705
5	Broken loop hot leg	0.09539	3.228	-2.705
6	Broken loop hot leg	0.01271	2.423	-2.039
7	Broken loop hot leg	0.008365	1.883	1.322
8	Broken loop cold leg	0.008365	0.4877	0.0
9	Broken loop cold leg	0.06344	0.6965	0.0
10	Broken loop cold leg	0.06344	0.9510	0.0
11	Intact loop hot leg	0.06344	2.6160	0.0
12	Intact loop hot leg	0.06299	2.643	0.2423
13	SG inlet plenum	0.6481	0.5175	0.5175
14	SG U-tube	8.187 E-5	2.568	2.483
15	SG U-tube	8.187 E-5	2.568	-2.483
16	SG outlet plenum	0.6481	0.5175	-0.5175
17	Crossover leg	0.06793	2.429	-1.523
18	Pump	0.09446	1.867	1.281
19	Pump	0.07273	3.111	1.281
20	Intact loop cold leg	0.0597	1.399	0.0
21	Intact loop cold leg	0.06343	0.5313	0.0
22	Downcomer	0.1604	4.256	-4.256
23	Lower plenum	0.7917	0.7318	0.0
24	Mixing box	0.1532	0.4285	0.4285
25	Active core	1.143 E-4	0.09423	0.09423
26	Active core	1.143 E-4	0.4191	0.4191
27	Active core	1.143 E-4	0.4191	0.4191
28	Active core	1.143 E-4	0.4191	0.4191
29	Active core	1.143 E-4	0.4191	0.4191
30	Active core	1.143 E-4	0.01753	0.01753
31	Upper core structures	0.2387	1.668	1.668

(continued)

32	Core bypass	4.766 E-3	4.146	4.146
33	Upper head	0.2306	0.9144	0.9144
34	Reflood assist line	0.03871	4.048	0.8620
35	Reflood assist line	0.03871	4.840	0.6075
36	Pressurizer surge line	1.452 E-3	4.592	0.4255
37	Pressurizer surge line	1.452 E-3	4.767	0.7678
38	ECCS piping	6.221 E-3	5.5	0.0
39	ECCS piping	6.221 E-3	5.5	0.0
40	ECCS piping	6.221 E-3	58.0	0.0

Table 4.3 Loss Coefficients of Nodes

Node No.	k	k^{Af}	k^{Ar}	k^{Ef}	k^{Er}
1	0.022	0.4	0.8	0.0	0.0
2	0.020	0.0	0.0	0.0	0.0
3	0.019	0.39	0.75	1.52	1.09
4	0.030	0.0	0.0	189.	189.
5	0.016	0.0	0.0	142.	198.
6	0.019	0.0	0.0	20.	20.
7	0.017	0.0	0.0	-	-
8	0.019	-	-	0.754	0.391
9	0.029	0.0	0.0	0.0	0.0
10	0.017	0.0	0.0	3.58	3.58
11	0.020	0.4	0.8	0.0	0.0
12	0.027	0.0	0.0	0.815	0.815
13	0.026	0.0	0.0	0.0	0.0
14	0.0	0.345	0.588	0.0	0.0
15	0.0	0.0	0.0	0.588	0.345
16	0.029	0.0	0.0	0.0	0.0
17	0.020	0.403	0.801	0.0	0.0
18	0.117	0.0	0.0	0.0	0.0
19	0.021	0.0	0.0	0.0	0.0
20	0.017	0.0	0.0	0.0	0.0
21	0.020	0.0	0.0	3.58	3.0
22	0.013	0.62	0.62	3.5	3.5
23	0.014	0.0	0.0	0.0	0.0
24	6.58	0.0	0.0	0.0	0.0
25	3.11	0.014	0.0	0.0	0.0
26	3.12	0.0	0.0	0.0	0.0
27	3.24	0.0	0.0	0.0	0.0
28	2.92	0.0	0.0	0.0	0.0
29	3.09	0.0	0.0	0.0	0.0
30	3.15	0.0	0.0	0.143	0.170
31	6.45	0.0	0.0	0.0	0.0
32	29.3	0.0	0.0	0.0	0.0
33	0.1	0.0	0.0	0.0	0.0
34	0.1	0.4	0.8	0.0	0.0
35	0.1	0.4	0.8	0.0	0.0
36	4.0	0.4	0.8	9.0	9.0
37	4.0	0.0	0.0	0.0	0.0
38	10.	0.4	0.8	0.0	0.0
39	10.	0.4	0.8	0.0	0.0
40	10.	0.4	0.8	0.0	0.0

5. Calculated Results and Discussion

The sequence of events for the present analysis is compared with that in the experiment in Table 5.1. It is remarkable that the time of ACC injection initiation and the core reflood time were well simulated by the THYDE-P. The detailed discussion on the events in the table will be made in the following subsections.

5.1 Temporal Behavior of Pressure

The calculated pressure just above the active core (node 31) is shown in Fig. 5.1 along with the experimental data. It goes without saying that the calculated depressurization process is highly dependent on the break flow simulation model. Therefore, it could be said that the present break flow model in THYDE-P with the discharge coefficient 0.8 gave a good agreement with the experimental depressurization process. The calculated break flows will be directly compared with the experimental data in Subsec. 5.5.

End of blowdown, which is often defined as the time when the system pressure has almost decreased to the containment pressure, might be defined as about 35 sec. after rupture in both the experiment and the calculation.

5.2 Cladding Surface Temperature and Thermal-Hydraulic Behavior in Core

5.2.1 Overall Trend

The cladding surface temperatures at nodes 26, 27 and 28 are shown in Figs. 5.2.1, 5.2.2 and 5.2.3, respectively, along with the experimental data, where the heights of the measurement points from the bottom of the core are nearly equal to those in the analysis, and their horizontal locations in the core are chosen from the seemingly average bundle. The heat transfer coefficient calculated at node 27 is shown in Fig. 5.3, where the heat transfer modes (see Tables 3.1.1 and 3.1.2) are shown. The calculated mass flux and coolant qualities at core node 27 are shown in Figs. 5.4 and 5.5, respectively.

The overall trends of the calculated cladding surface temperatures are in good agreement with the experimental data in the sense that there are

peakes during the blowdown and the final quenching was calculated to occur at about 50 sec. after rupture. The reason why the peakes during the blowdown were calculated will be explained in the following subsection.

In the experiment, DNB was observed at about 20 sec. and also in the analysis DNB occurred at about 18 sec. under the pool flow condition, where the CHF value was predicted by the modified Zuber correlation (16)(17). At about 30 sec. in the calculation, the core nodes became superheated and the heat transfer coefficients suddenly decreased and the cladding surface temperature increased. After about 40sec. the effects of ECC water became apparent and the core nodes returned to be saturated. As shown in Fig. 5.5, the coolant quality at node 27 became under x_c ($=0.1$) and then the heat transfer mode changed from mode 4.4 (pool film boiling) to mode 4.5 (pool transition boiling). The sudden decrease in the calculated cladding surface temperature was brought about by the mode transition and then the final quenching, the mode transition to mode 3 (nucleate boiling), occurred.

5.2.2 Detail of Blowdown

The calculated cladding surface temperatures, heat transfer coefficients at the core nodes at the very early stage of the blowdown are shown in Figs. 5.6 and 5.7, respectively. The mass fluxes at the inlet and the outlet of node 27 are shown in Fig. 5.8, where the pool flow condition is denoted.

As shown in Fig. 5.6, two prominent peakes of the cladding surface temperatures appeared at node 27 and 28. The reason may be clarified by Figs. 5.7 and 5.8. DNB was calculated to occur twice at about 0.6 and 0.8 sec. in conjunction with flow stagnation and quenching was also calculated to occur twice at about 1.2 and 3 sec., under the forced convection condition. It could be said, therefore, the rewetting phenomena observed in the blowdown might be brought about by the large forward core flow due to the effects of the primary coolant pumps, which were running until 200 sec. after rupture.

5.2.3 Coolant Temperature at Upper Plenum

The coolant temperature calculated just above the active core, at node 31, is shown in Fig. 5.9 along with the experimental data. As observed

in the experiment, primary coolant in the upper plenum departed from the saturated state at about 30 sec. and stayed at the superheated state until about 40 sec. Also in the analysis, the superheated state was calculated to exist intermittently from 30 to 40 sec. The calculated results are well understood from the fact that coolant at the active core nodes became superheated at about 30 sec. and returned to be saturated at about 40 sec. due to the effects of ECC water as stated in Subsec. 5.2.2.

5.3 Intact Loop Cold Leg and Accumulator Injection

In Fig. 5.10, the calculated ACC pressure is compared with the experimental data, where the calculated loop pressure near the ECC water injection point, node 20, is shown. The calculated injection mass flow rate from the accumulator is shown in Fig. 5.11 along with the experimental data. Overall trend of the accumulator was well simulated by the present calculation. The calculated coolant enthalpies at the accumulator and node 40, which simulated ACC piping, are shown in Fig. 5.12. It took about 10 sec. for the coolant enthalpy at the ACC side of node 40 to decrease to the value of the accumulator enthalpy, about 30 kcal/kg.

The calculated coolant density at node 21 which is located downstream of the ECC injection point is shown in Fig. 5.13 along with the experimental data. In the calculation, the node became filled with subcooled water at about 25 sec. due to ACC injection. On the other hand in the experiment, many sharp peaks, which imply the existence of slugs or drops, were observed. It is of no use to say that thermal non-equilibrium effects due to low enthalpy ACC water were considerably large in this time period. Generally, analyses of this time period by thermal equilibrium models fail because of overestimated condensation rates. In the present analysis, the difficulty was avoided by applying the time delay model for density change (see subsec. 3.4), where the value of the delay parameter at node 20 was about 1 sec. The calculated mass fluxes at node 20 are shown in Fig. 14. It is shown in the figure that coolant in node 20 once became subcooled and again returned to be saturated.

The calculated coolant temperatures at the intact loop hot and cold legs, node 11 and node 21, are shown in Fig. 5.15 along with the experimental data.

The existence of subcooled water in the intact loop cold leg is clearly shown in both the experimental and calculated curves after the ACC injection initiated.

5.4 ECC Water Penetration through Downcomer

The calculated mass flow rates and coolant enthalpies at the inlet and the outlet of the downcomer node, node 22, are shown in Figs. 5.16 and 5.17, respectively. The curves show that ECC water penetration through the downcomer node started at about 30 sec. but it was premature. The constantly forward flow at the inlet of the downcomer was established at about 36 sec. and then coolant became subcooled at about 40 sec. The reason why the inlet mass flow rate was much larger than the outlet mass flow rate even after 40 sec. is that due to the non-equilibrium model applied, the void fraction was gradually decreasing to zero during this period.

The calculated coolant temperature at the downcomer was shown in Fig. 5.18 along with the experimental data. In the experiment, subcooled water was observed first several seconds after the ACC injection initiated, i.e. the late portion of the blowdown phase. On the other hand in the analysis, only overall trend was analysed since the downcomer was simulated by a single node.

5.5 Broken Legs and Break Flows

The mass flow rates at the broken legs are shown in Figs. 5.19 and 5.20 along with the experimental data. At the early stage of the blowdown, the break flow at the hot leg was overestimated while it was underestimated at the cold leg. The coolant densities at the broken hot and cold legs are shown in Figs. 5.21 and 5.22, respectively, along with the experimental data. The coolant density at the cold leg was overestimated throughout the calculation (see Fig. 5.22). The overestimation of the break flow at the cold leg during the period from 10 to 35 sec. (see Fig. 5.20) might be brought about by this overestimation of the coolant density, namely the underestimation of the coolant enthalpy at the broken cold leg. The major reason for the underestimation of the coolant enthalpy is thought to exist in the nodalization for the downcomer region. Two-dimensional effects in the downcomer, which could be evaluated to some extent

for example, by nodalizing the downcomer into more than two nodes azimuthally, might have to be taken into consideration. Another reason for the under-estimation of the coolant enthalpy at the broken loop cold leg was that heat transfer between coolant and structure was neglected in the present analysis. In the refill-reflooding phase, the mass flow rate at the leg considerably decreased and therefore heat input to coolant from the duct wall might have played an important role.

5.6 Steam Generator

The calculated heat inputs from the SG secondary system to primary coolant at nodes 14 and 15, which simulated U-tubes, are shown in Fig. 5.23. The SG secondary system was calculated to change from heat sink to heat source to the primary coolant at about 15 sec. after rupture. The calculated SG secondary pressure is shown in Fig. 5.24 along with the calculated primary side pressure. The figure 5.25 shows the calculated coolant temperatures at both the inlet plenum and the outlet plenum of the steam generator. The outlet plenum (node 16) was filled with superheated steam at 25 sec. in the present analysis.

5.7 Pressurizer and Intact Loop Hot Leg

The calculated pressures at the intact loop hot leg (node 2) and the pressurizer are shown in Fig. 5.26, along with the experimental data. The loop pressure was in good agreement with the experimental data but the pressurizer pressure was not. One of the reasons for the discrepancy was that the initial water temperature of the pressurizer was considerably lower than the experimental value (see Table 4.1). The code modification with respect to the problem has been done in the most update version of THYDE-P.

5.8 Primary Coolant Pumps

The calculated pump normalized speed, flow and head are shown in Figs. 5.28, 5.29 and 5.30, respectively. In the experiment, the pumps were running until 200 sec., and therefore pump speeds were assumed to be constant in the present calculation. Although the pumps might have played an important role in conjunction with the rewetting phenomena during the blowdown phase, few experimental data for the pumps were available.

Table 5.1 Sequence of Events for LOFT L2-3

<u>Event</u>	<u>Time after Blowdown Initiation (sec)</u>	
	<u>Experiment</u>	<u>Present Analysis</u>
LOCE L2-3 initiated	0.0	0.0
Reactor scram signal received at control room	0.103	0.103
Control rod completely inserted	1.683	not clear
HPIS injection initiated	14.	14. ^(a)
Pressurizer emptied	14.	not clear
Accumulator injection initiated	17.	16.3
LPIS injection initiated	29.	29. ^(a)
Lower plenum filled with liquid	35.	40.
Accumulator liquid line flow ended	49.	not clear
Core volume reflood	55.	60.

(a) These values were set by inputs.

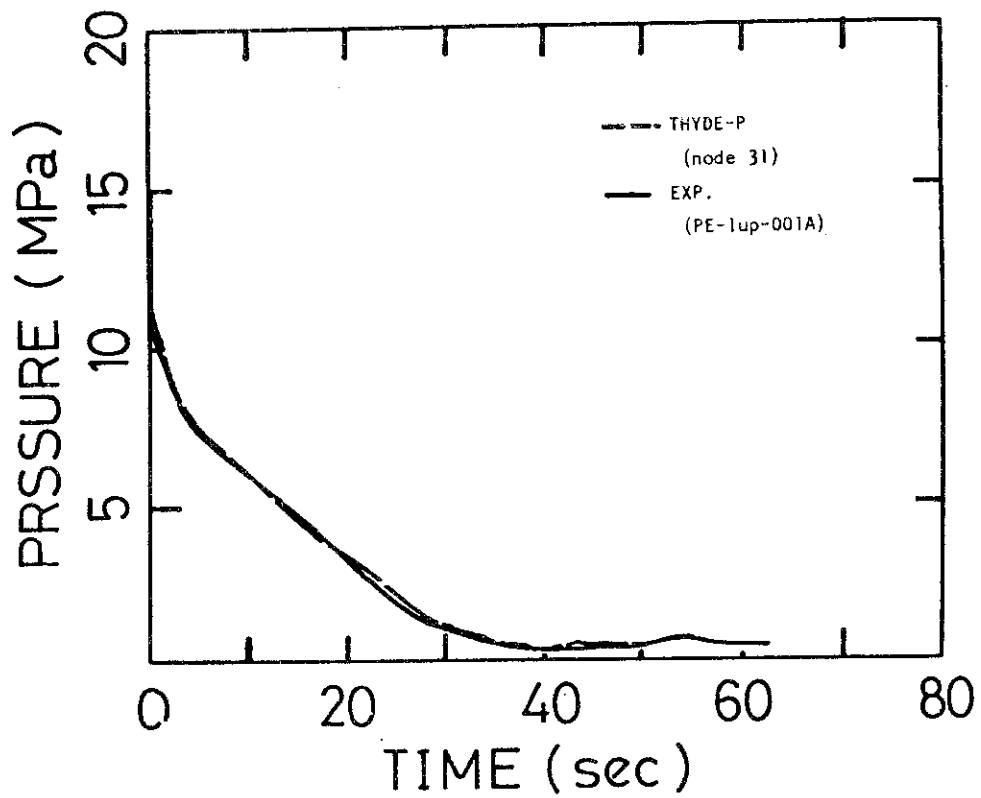


Fig.5.1 Temporal behavior of Pressure

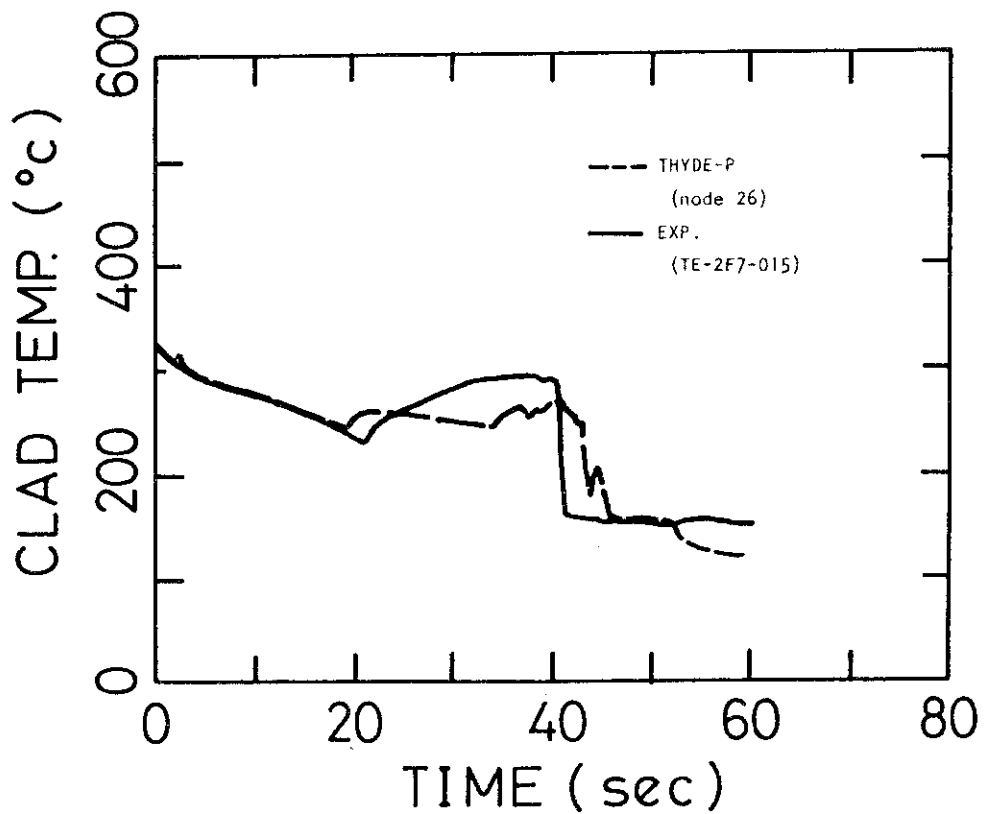


Fig.5.2.1 Cladding Surface Temperature (Node 26)

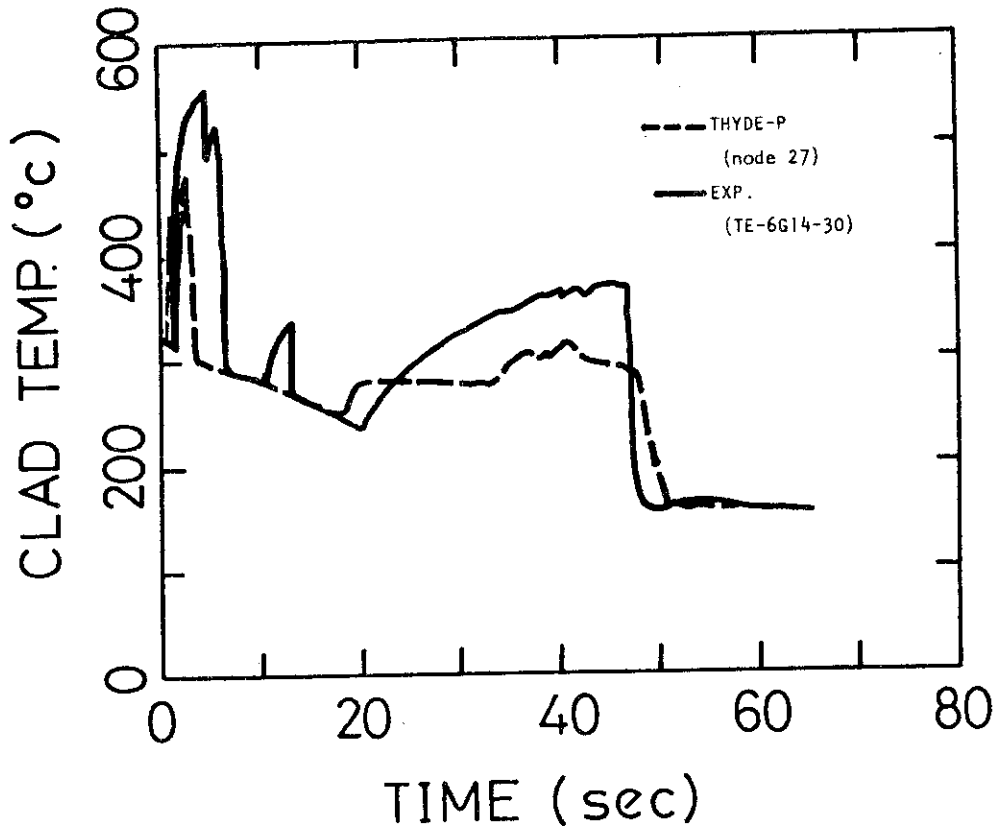


Fig.5.2.2 Cladding Surface Temperature (Node 27)

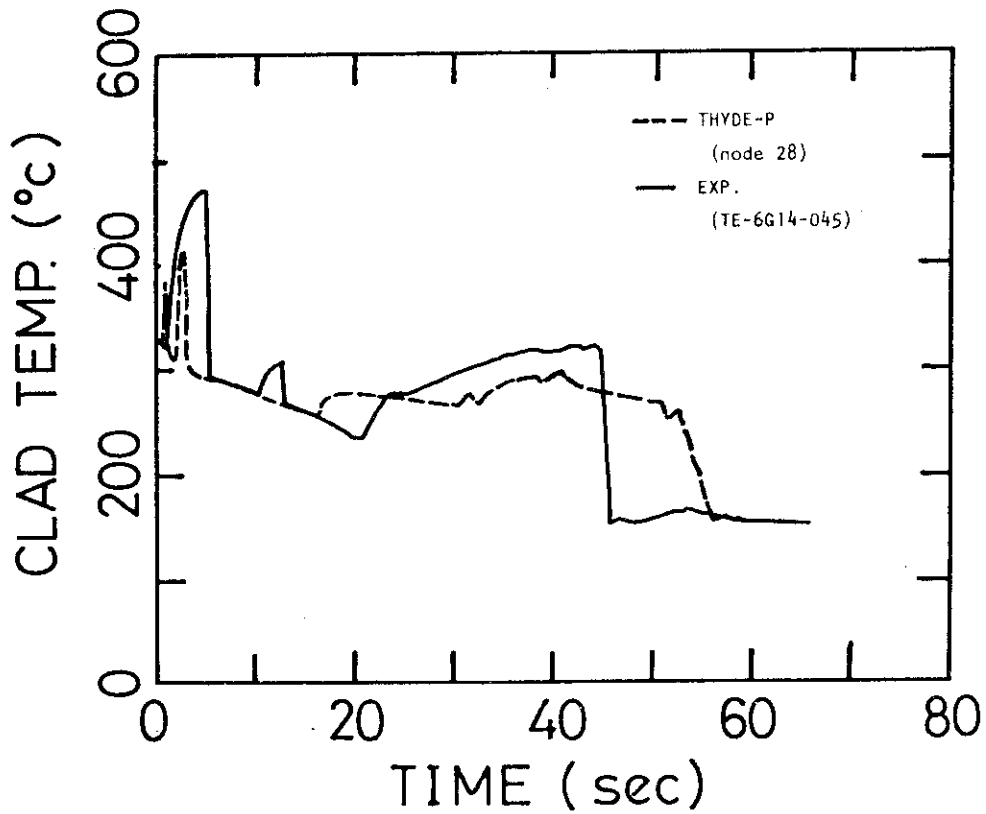


Fig.5.2.3 Cladding Surface Temperature (Node 28)

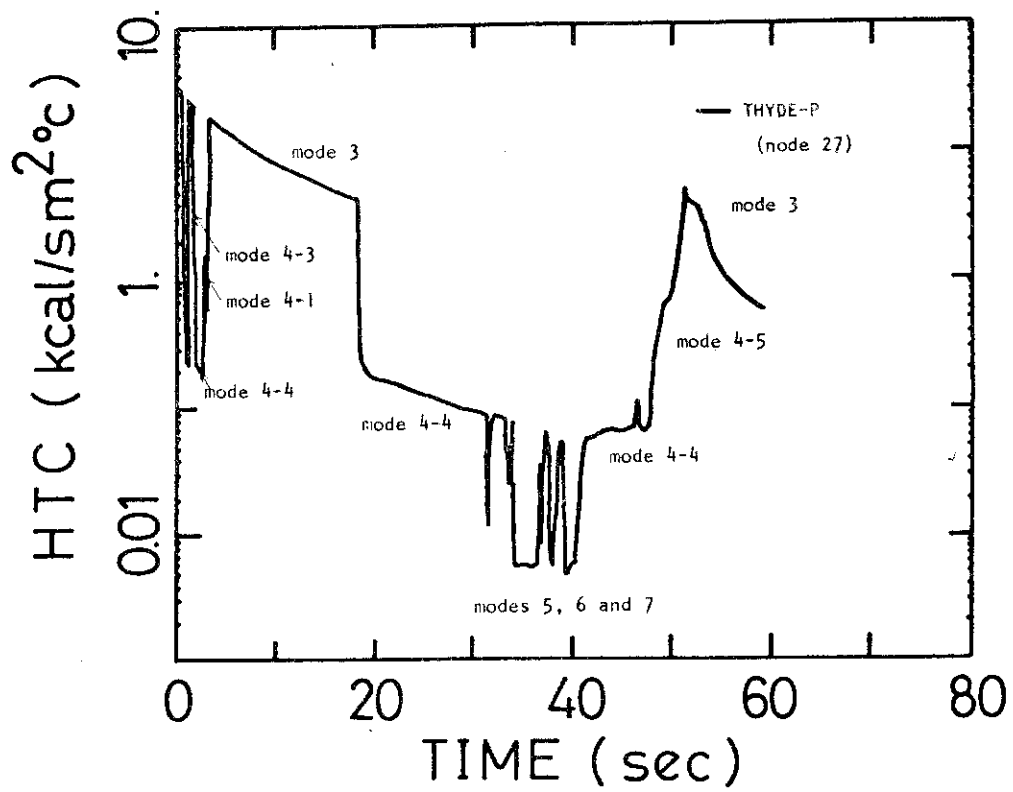


Fig.5.3 Calculated Heat Transfer Coefficient at Core Node 27

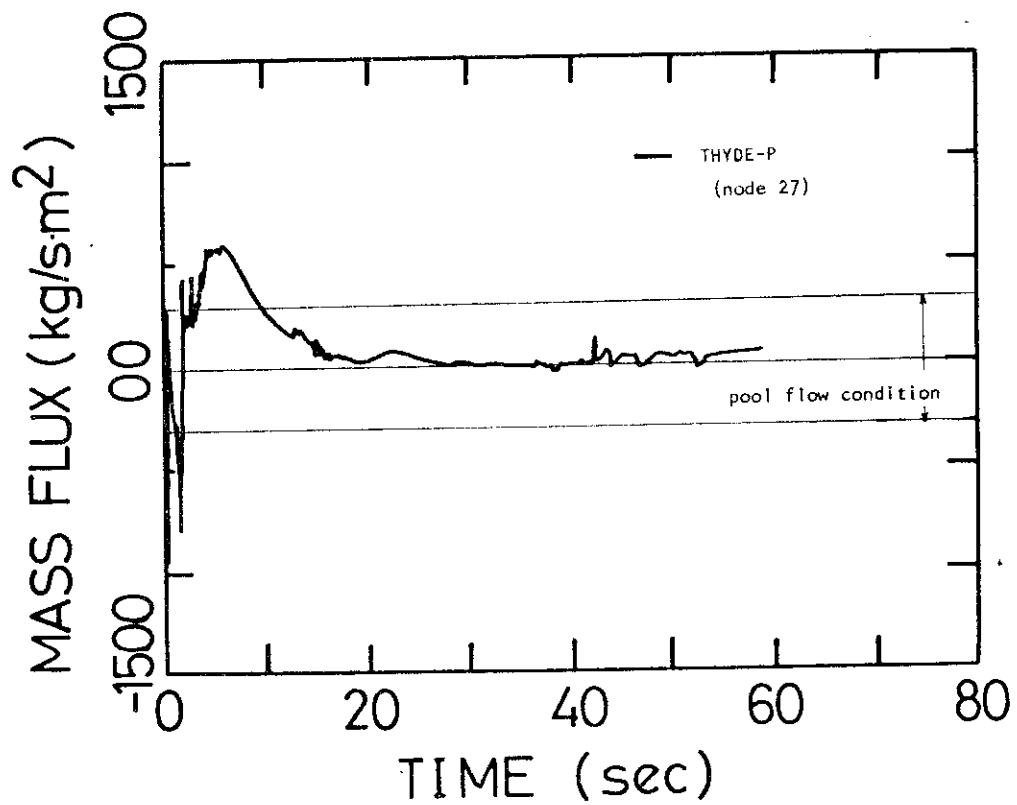


Fig.5.4 Calculated Mass Flux at Core Node 27

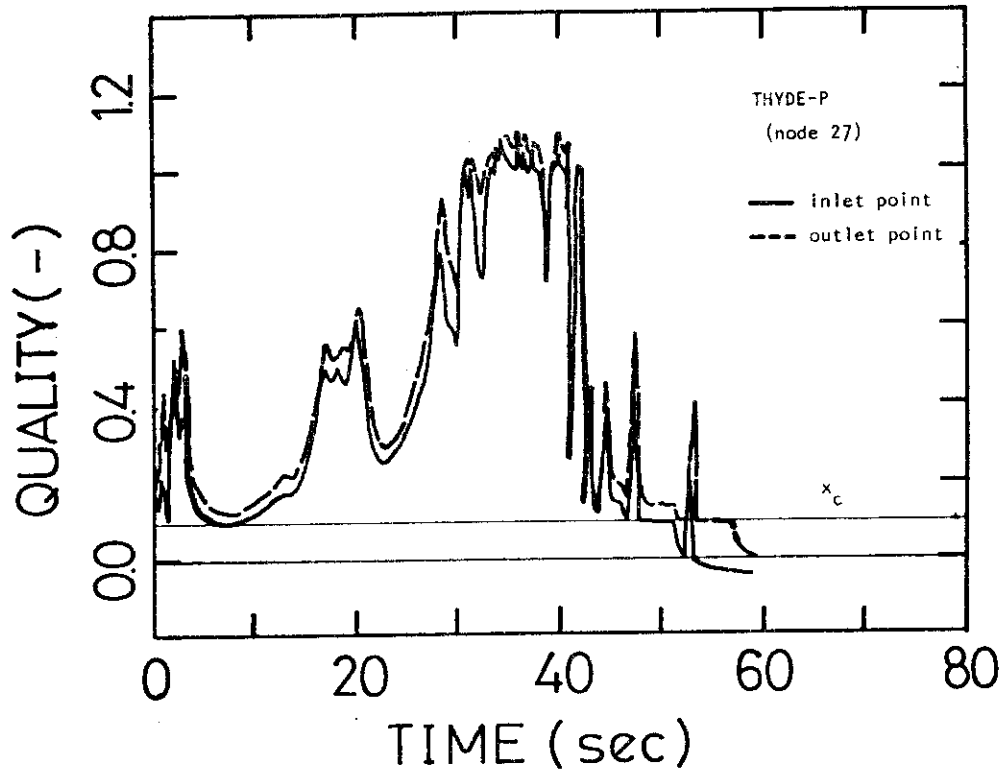


Fig.5.5 Calculated Coolant Qualities at Core Node 27

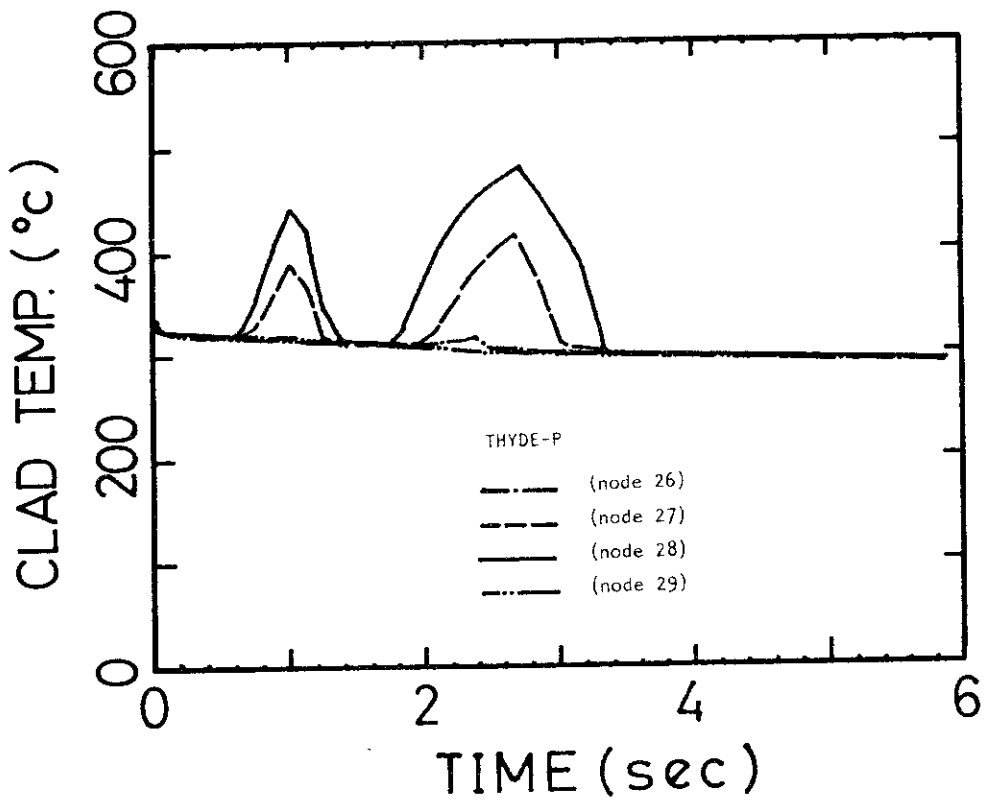


Fig.5.6 Calculated Cladding Surface Temperatures at Early Stage of Blowdown

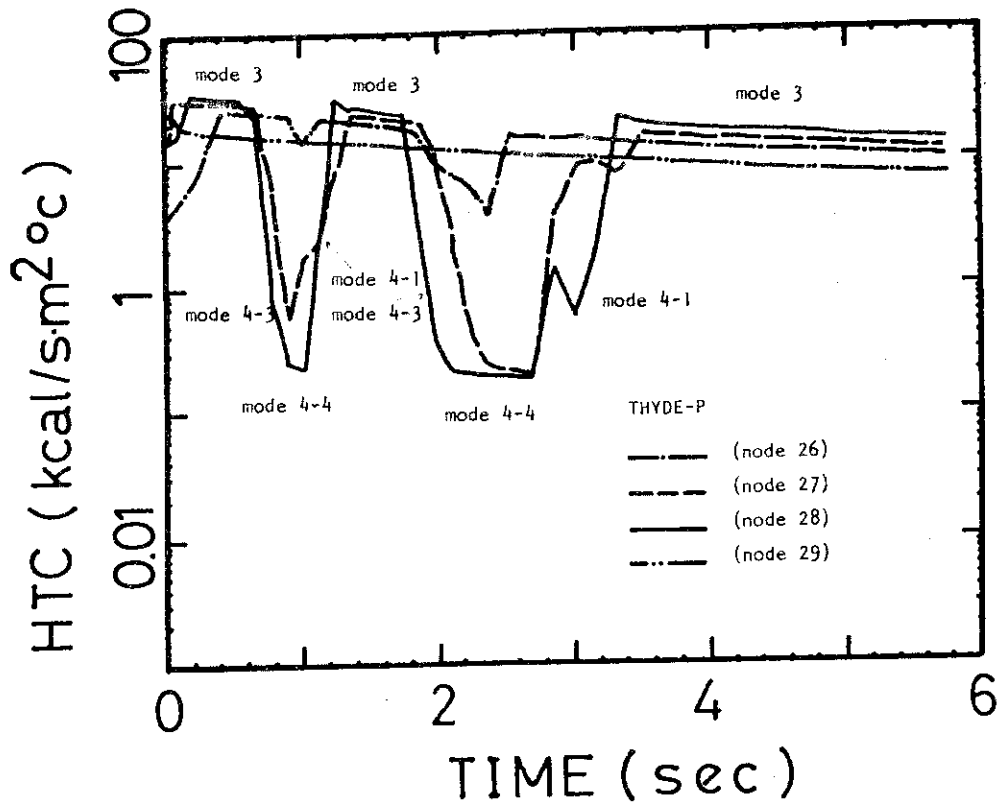


Fig.5.7 Calculated Heat Transfer Coefficients at Early Stage of Blowdown

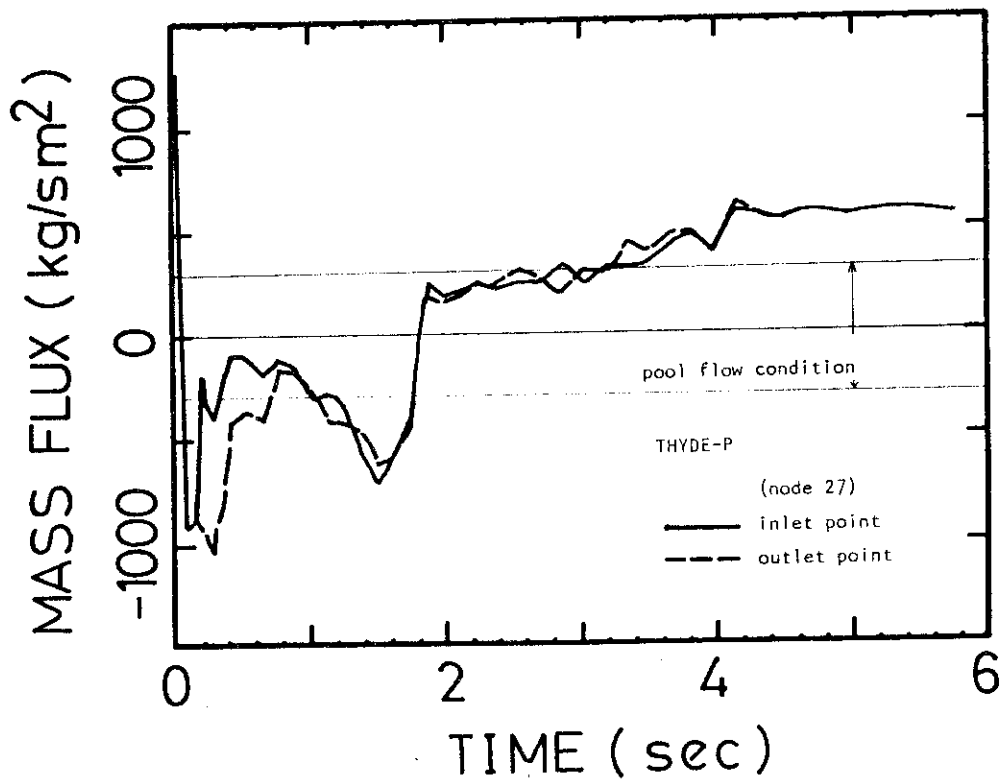


Fig.5.8 Calculated Mass Fluxes at Core Node 27 at Early Stage of Blowdown

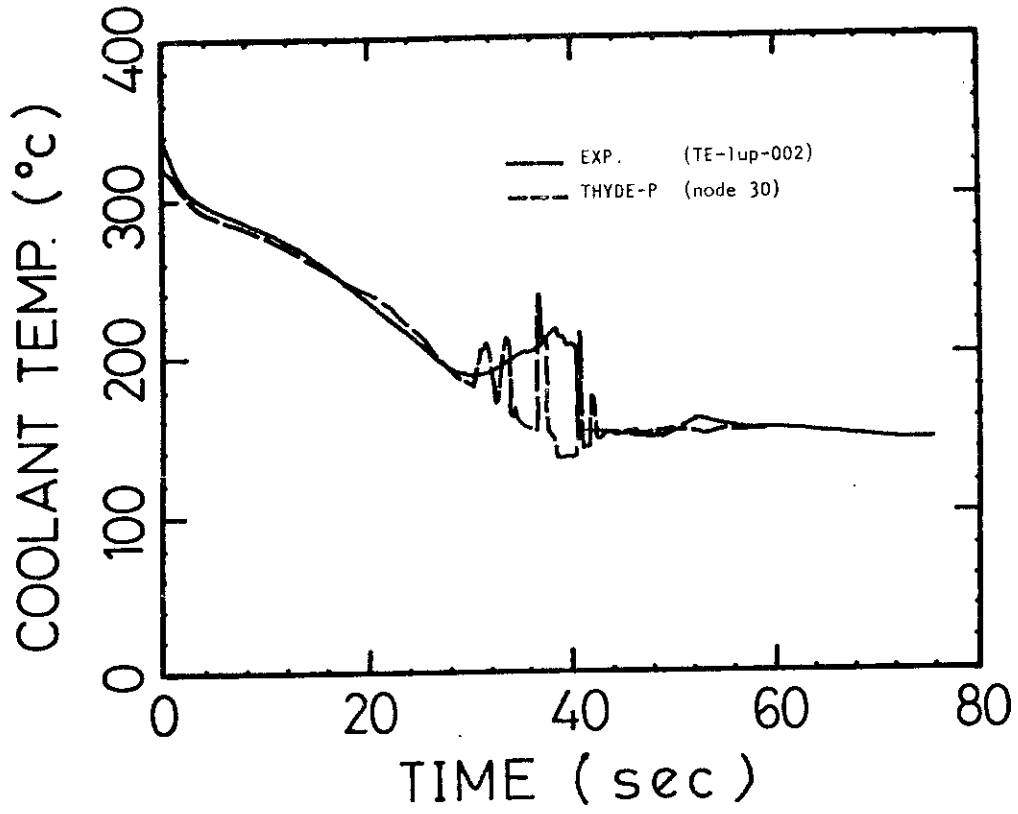


Fig.5.9 Coolant Temperature just above Active Core

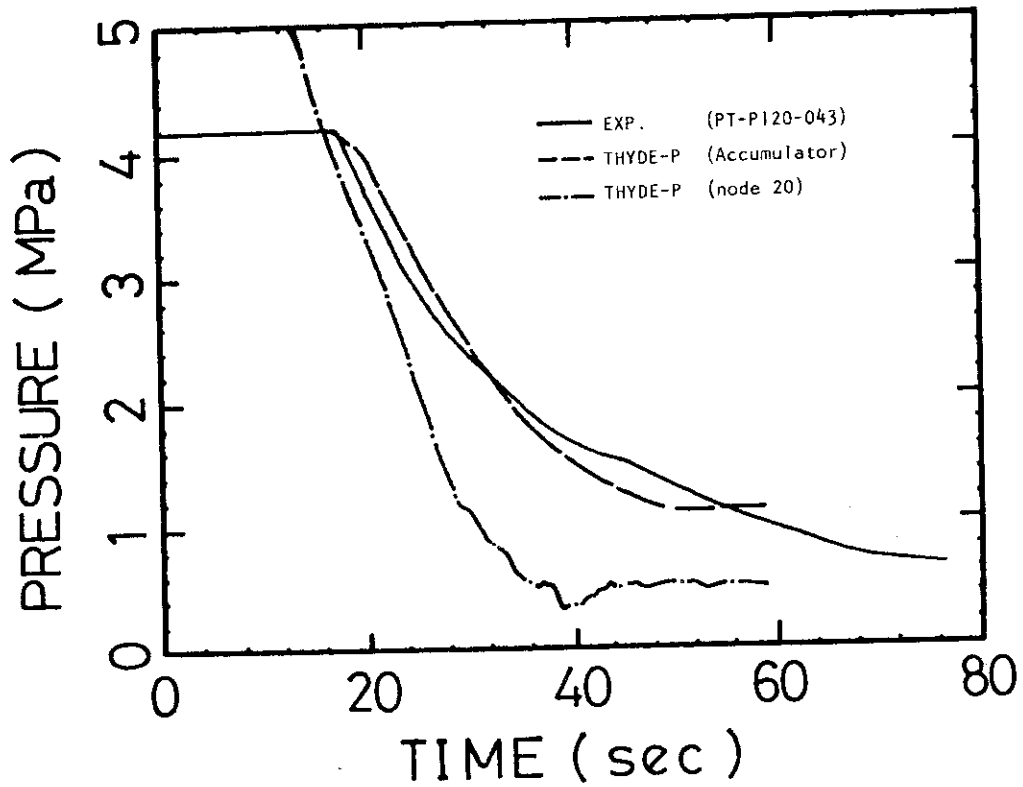


Fig.5.10 Accumulator Pressure

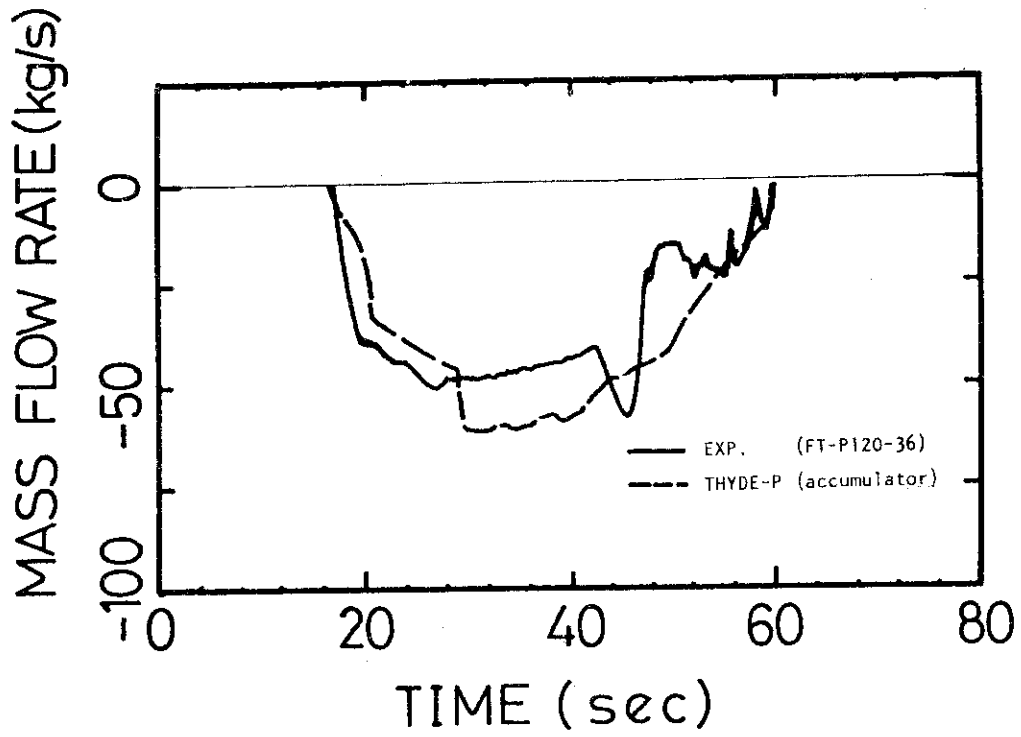


Fig.5.11 Injection Mass Flow Rate from Accumulator

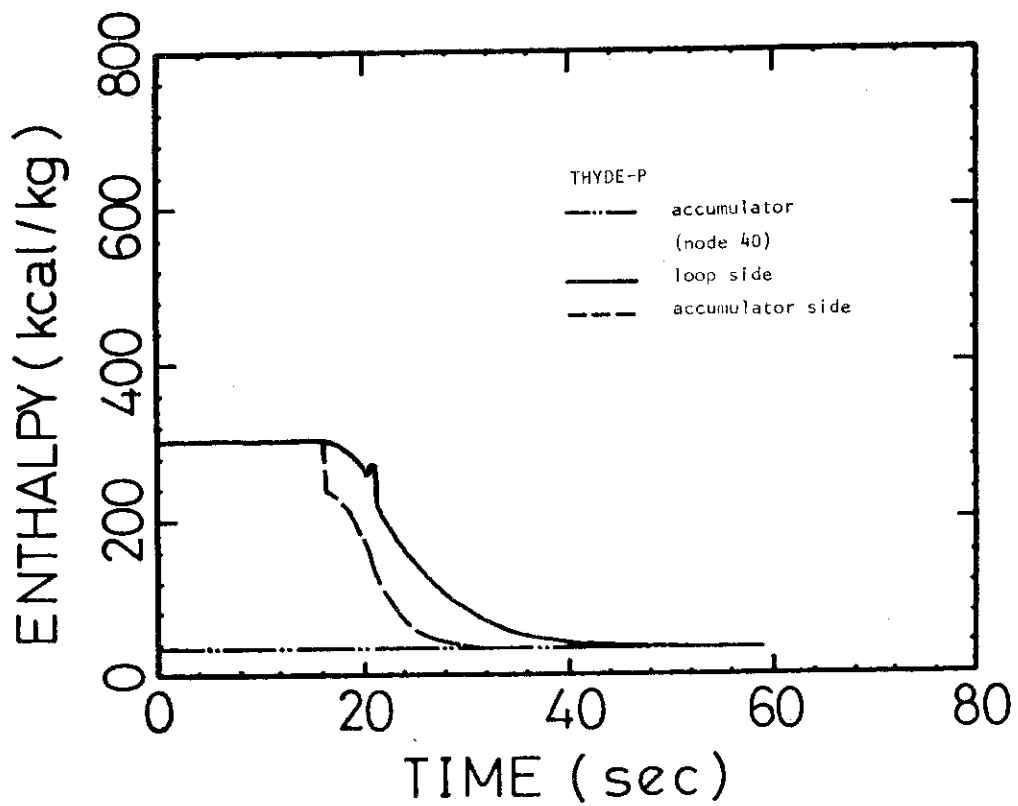


Fig.5.12 Coolant Enthalpies at Accumulator and Accumulator Piping

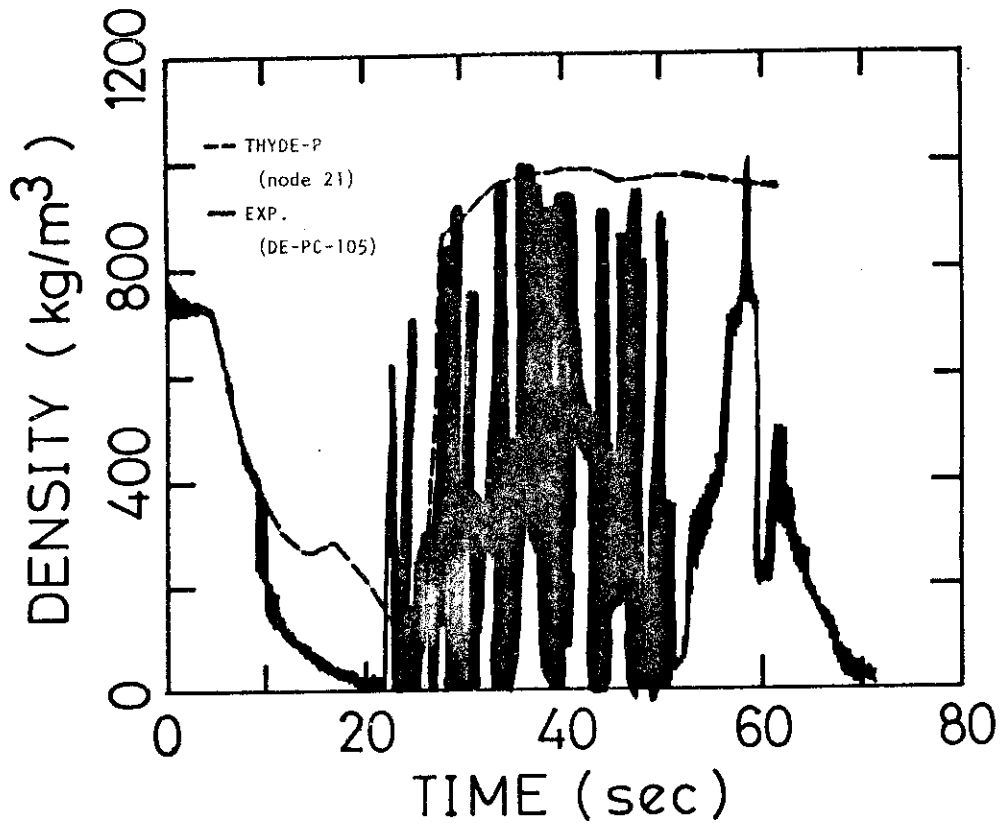


Fig.5.13 Coolant Density at Intact Loop Cold Leg

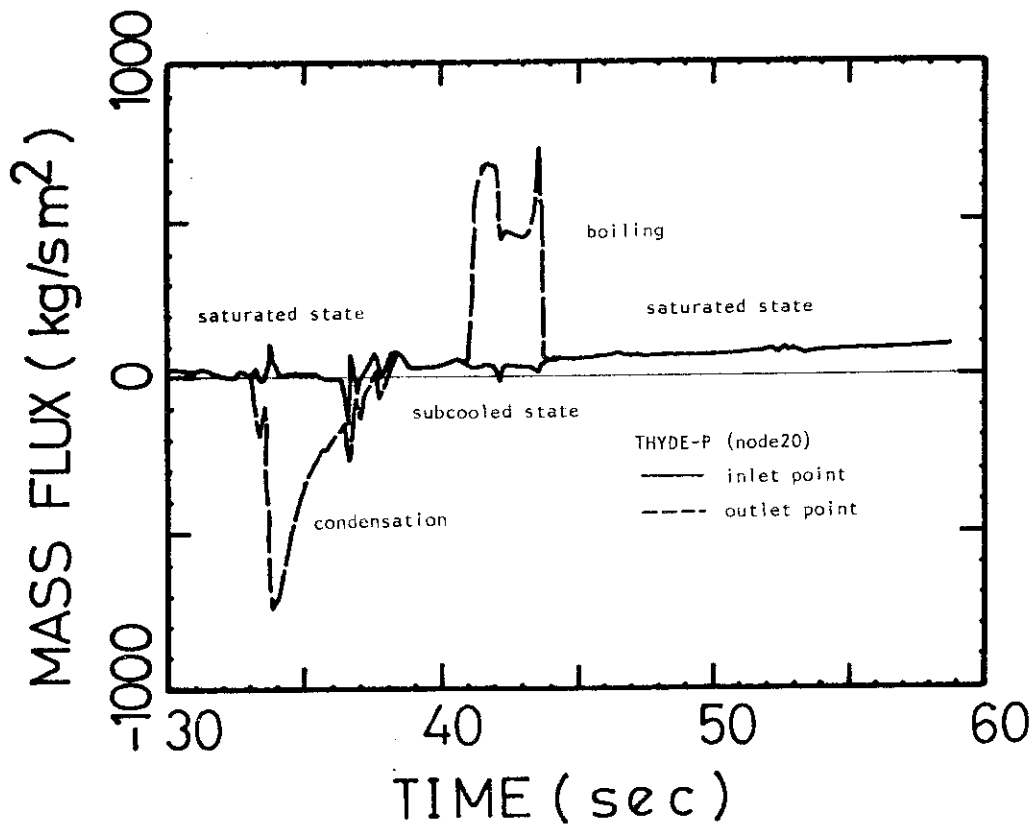


Fig.5.14 Calculated Mass Fluxes at Intact Loop Cold Leg (Node 20)

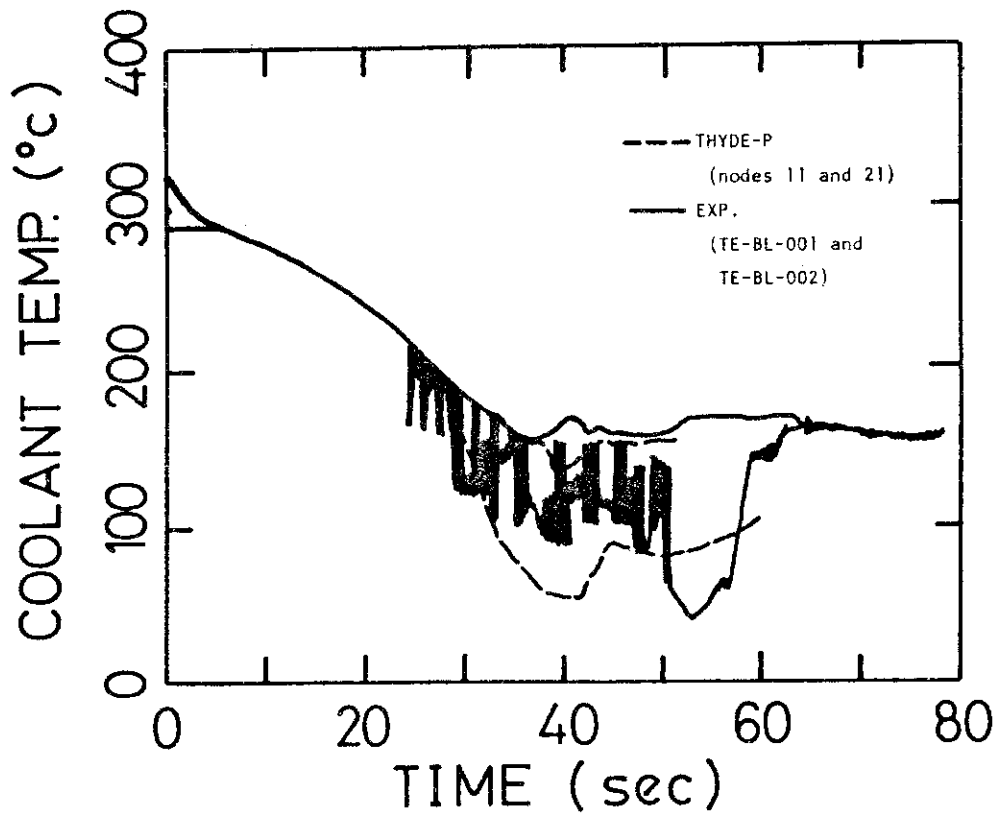


Fig.5.15 Coolant Temperatures at Intact Loop Hot and Cold Legs

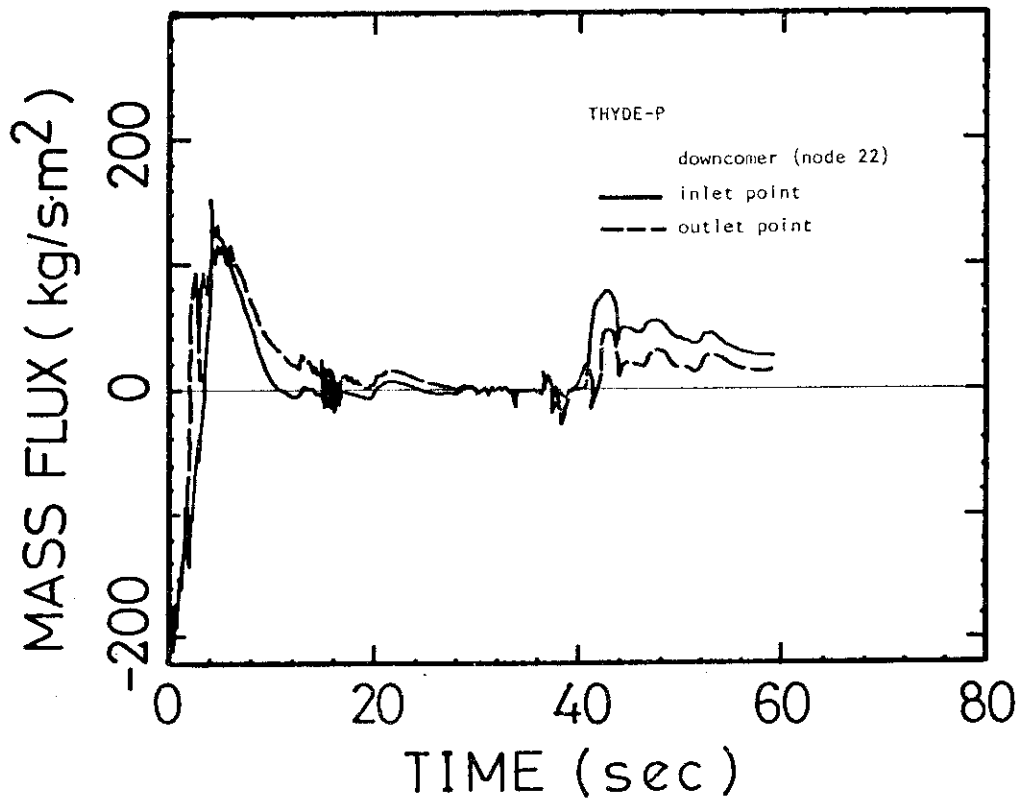


Fig.5.16 Mass Fluxes at Inlet and Outlet of Downcomer

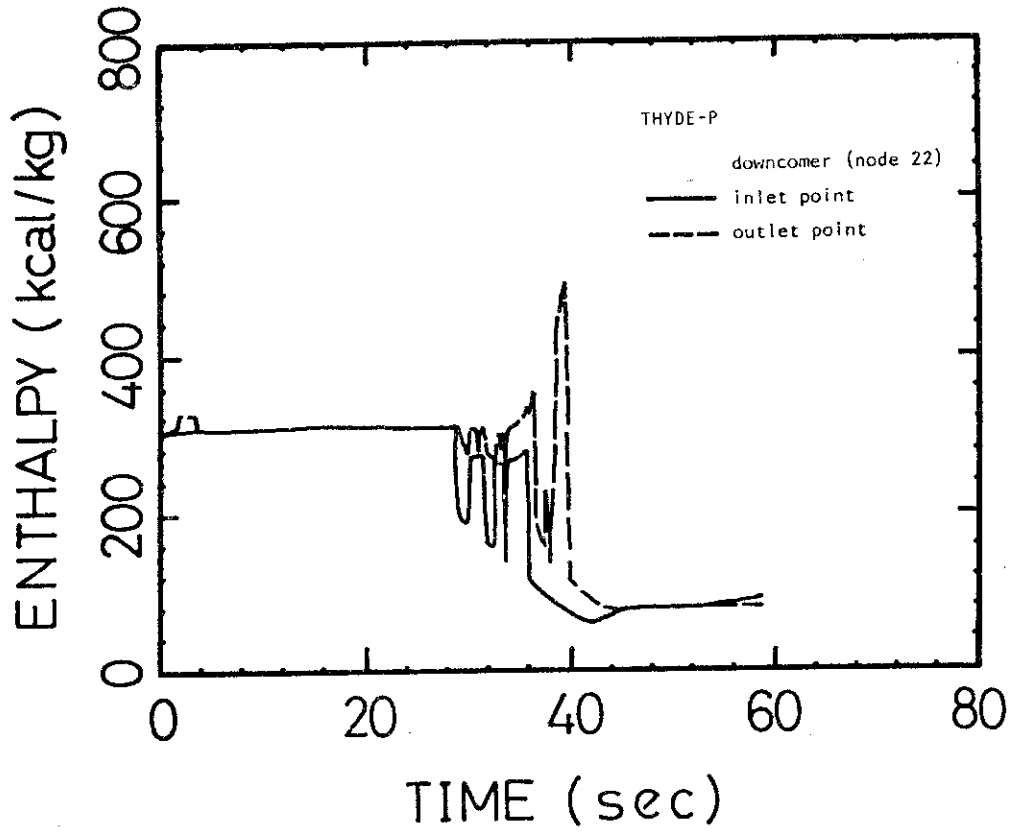


Fig.5.17 Coolant Enthalpies at Inlet and Outlet of Downcomer

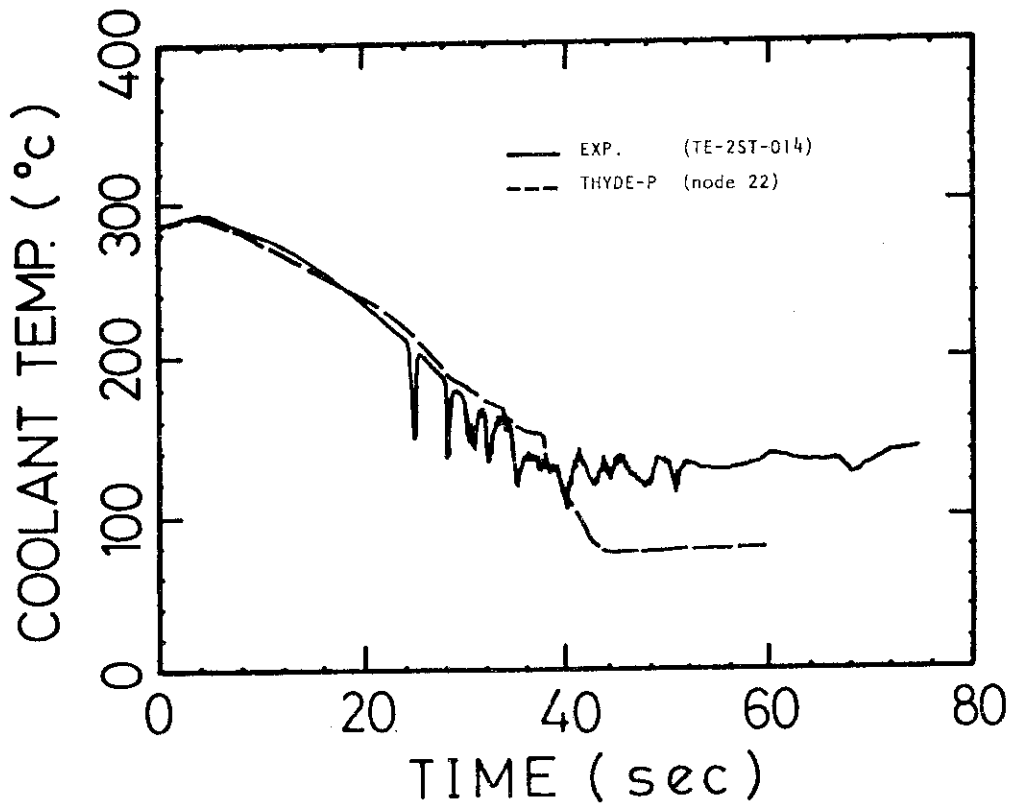


Fig.5.18 Coolant Temperature at Downcomer

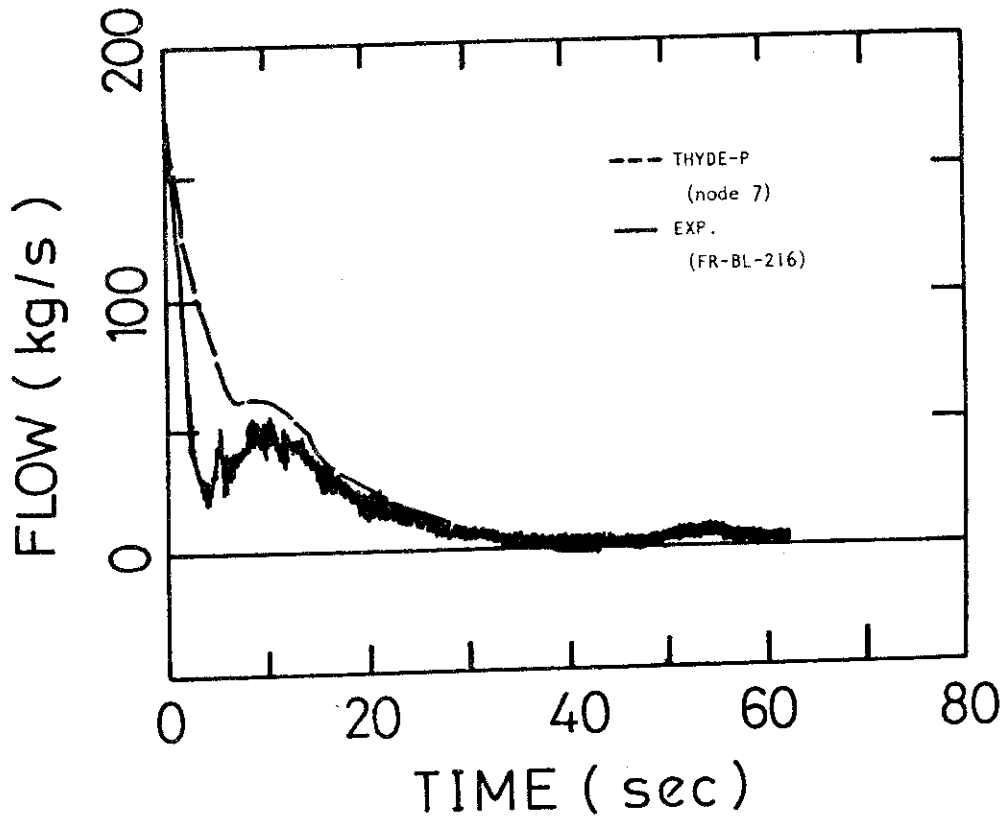


Fig.5.19 Break Flow at Hot Leg

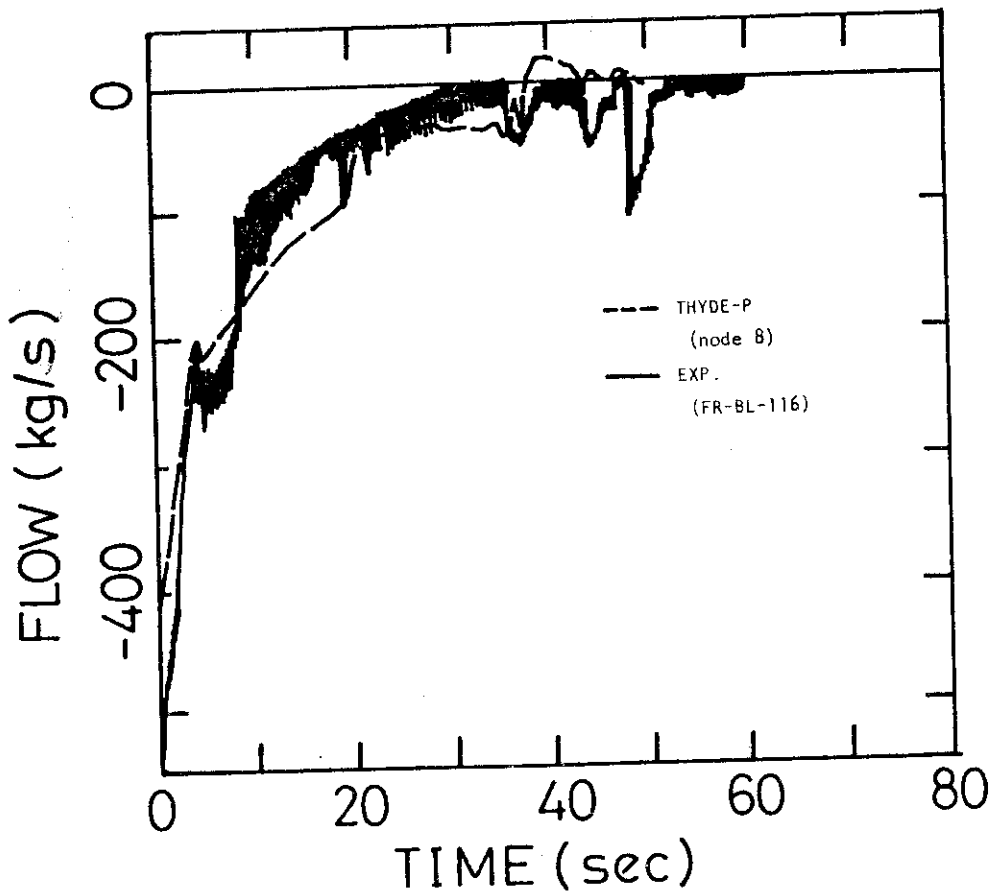


Fig.5.20 Break Flow at Cold Leg

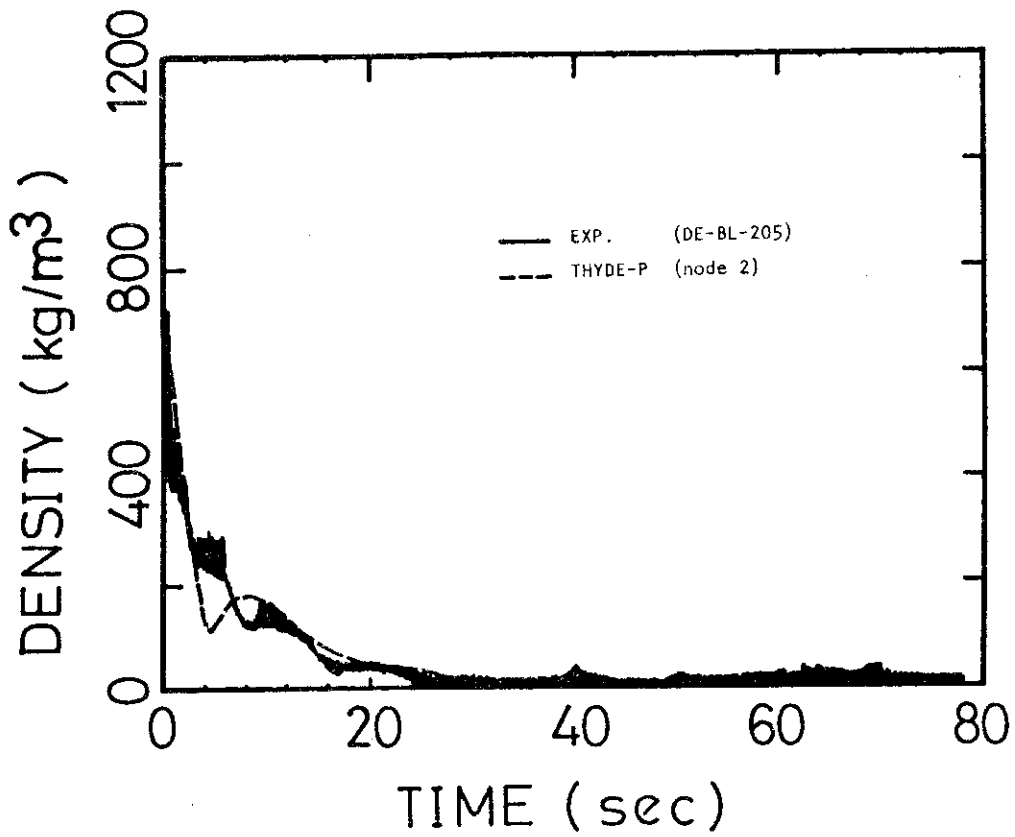


Fig.5.21 Coolant Density at Broken Loop Hot Leg

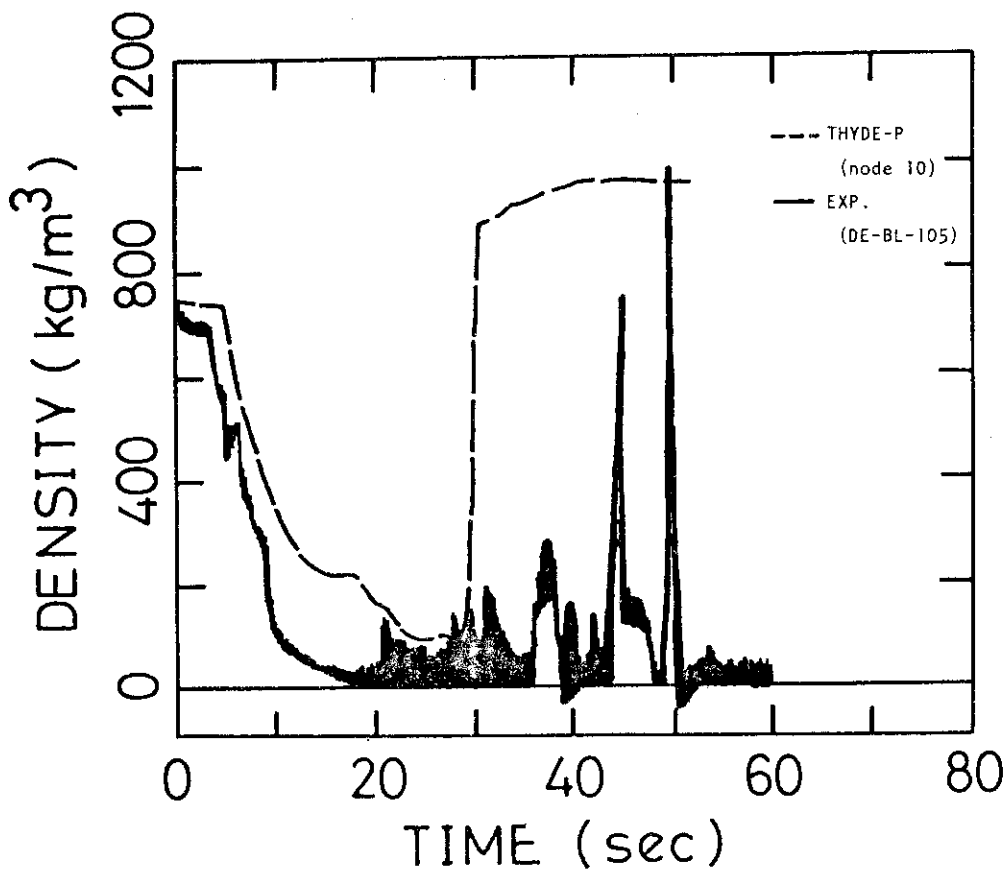


Fig.5.22 Coolant Density at Broken Loop Cold Leg

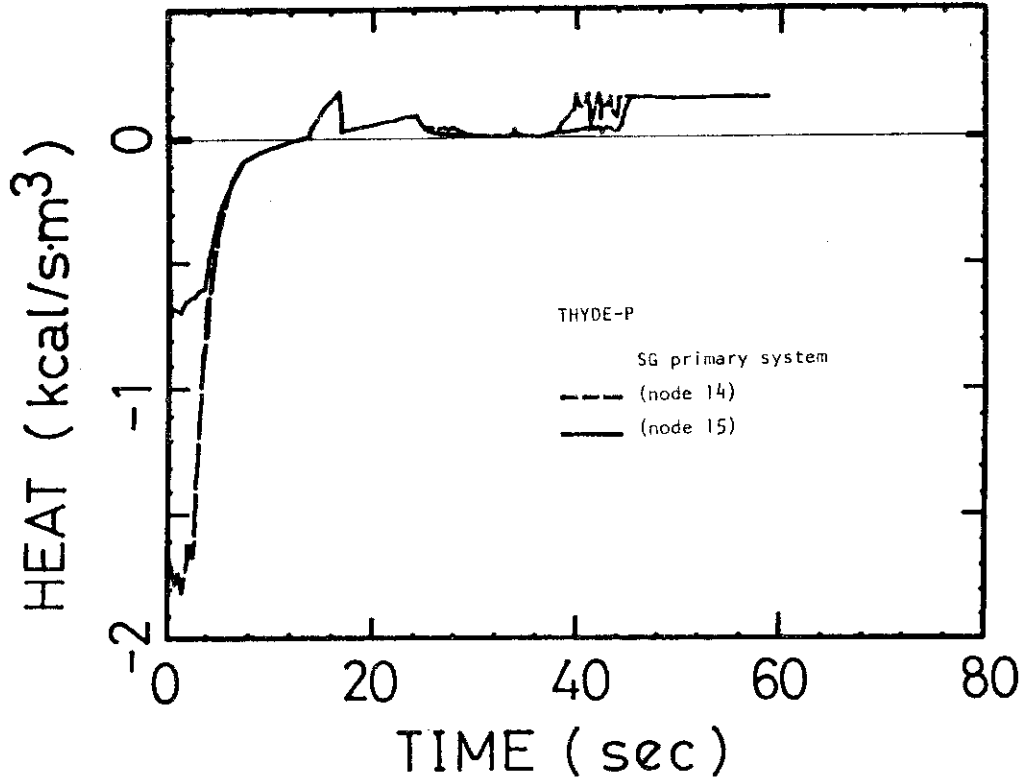


Fig.5.23 Heat Transfer from SG Secondary System to Primary System

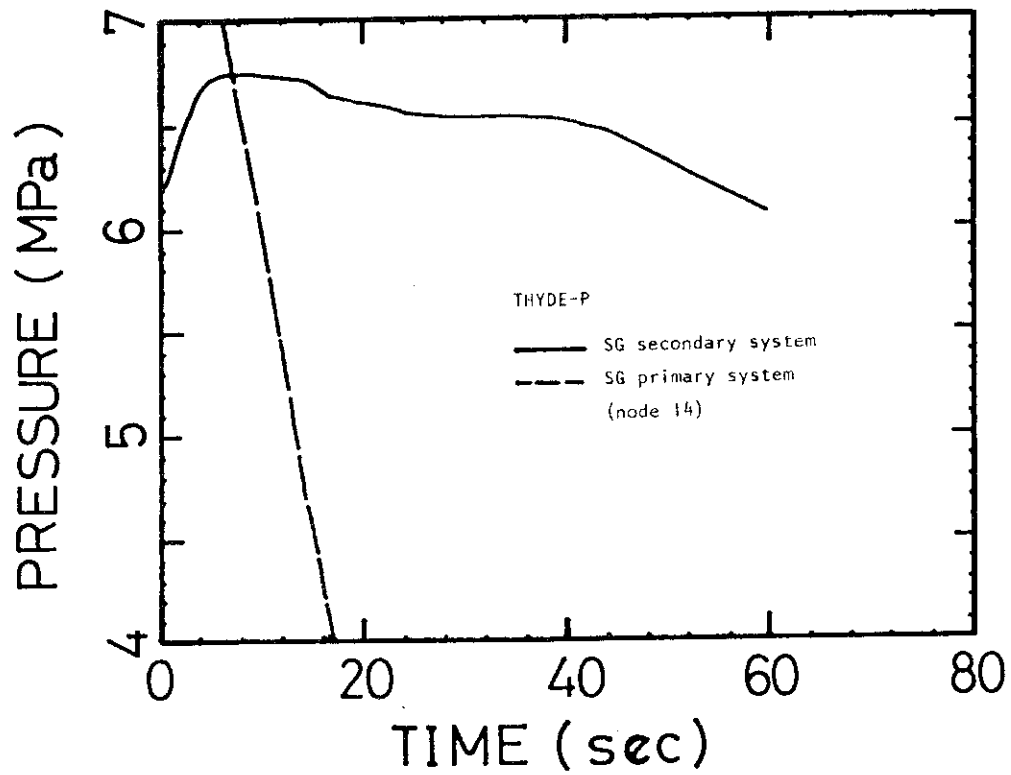


Fig.5.24 Calculated SG Secondary and Primary Pressures

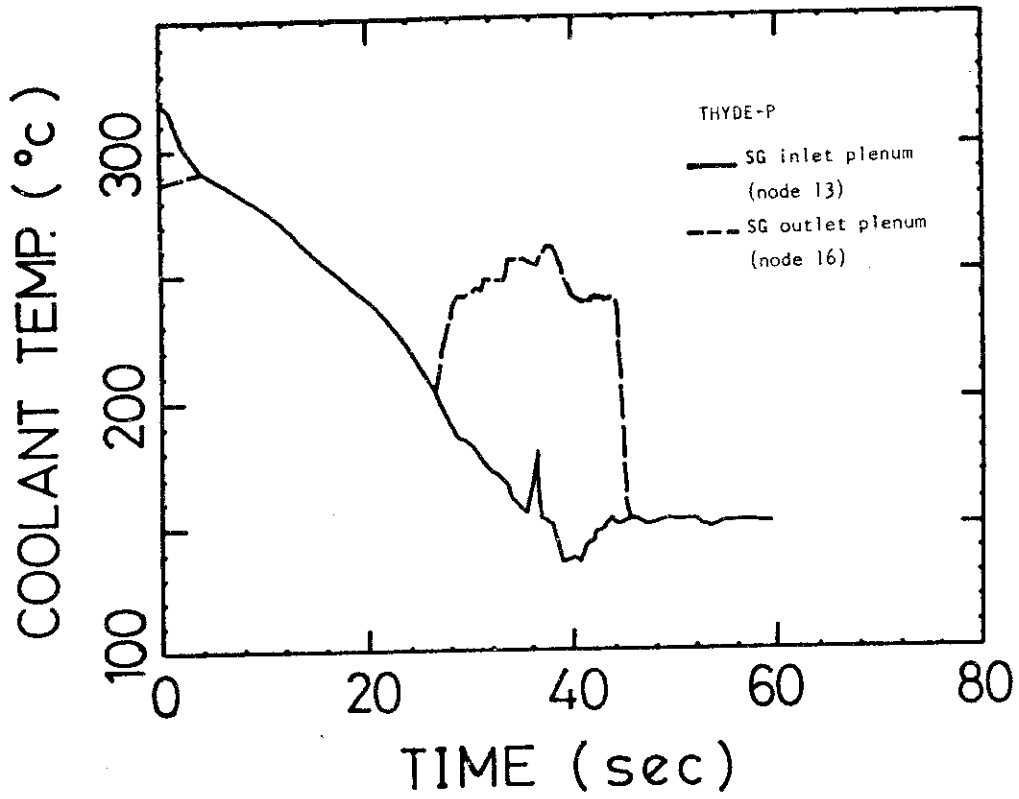


Fig.5.25 Calculated Coolant Temperatures at SG Inlet and Outlet Plenums

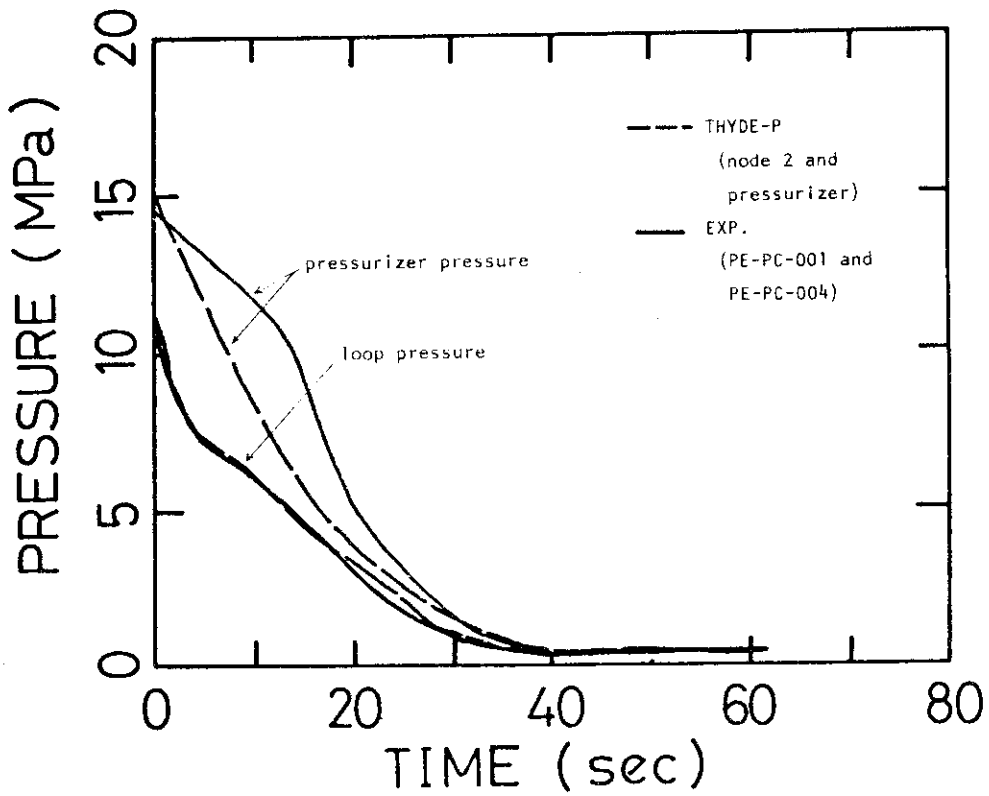


Fig.5.26 Pressurizer and Intact Loop Hot Leg Pressures

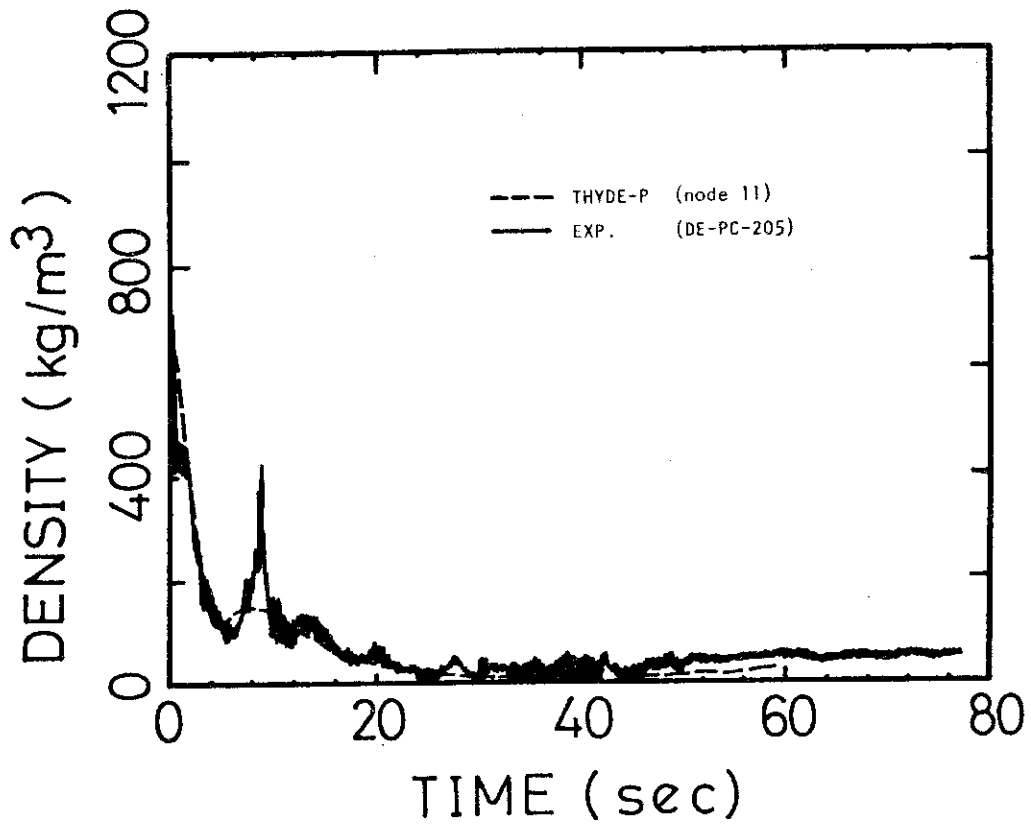


Fig.5.27 Coolant Density at Intact Loop Hot Leg

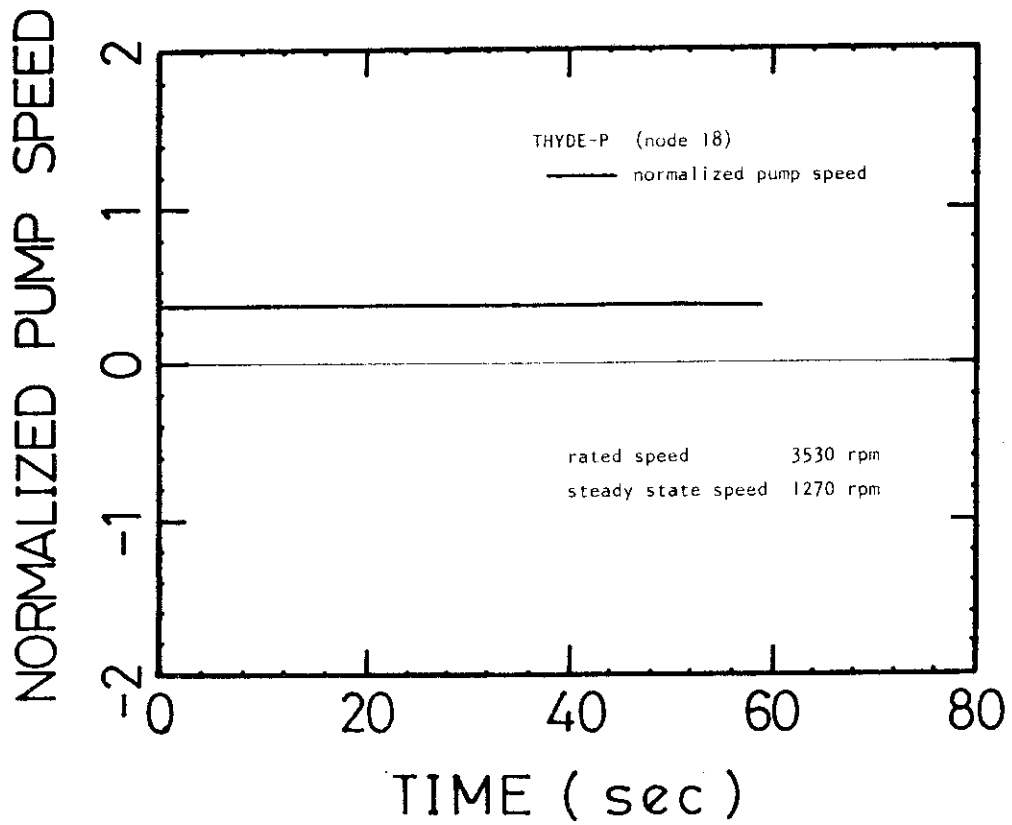


Fig.5.28 Calculated Normalized Pump Speed

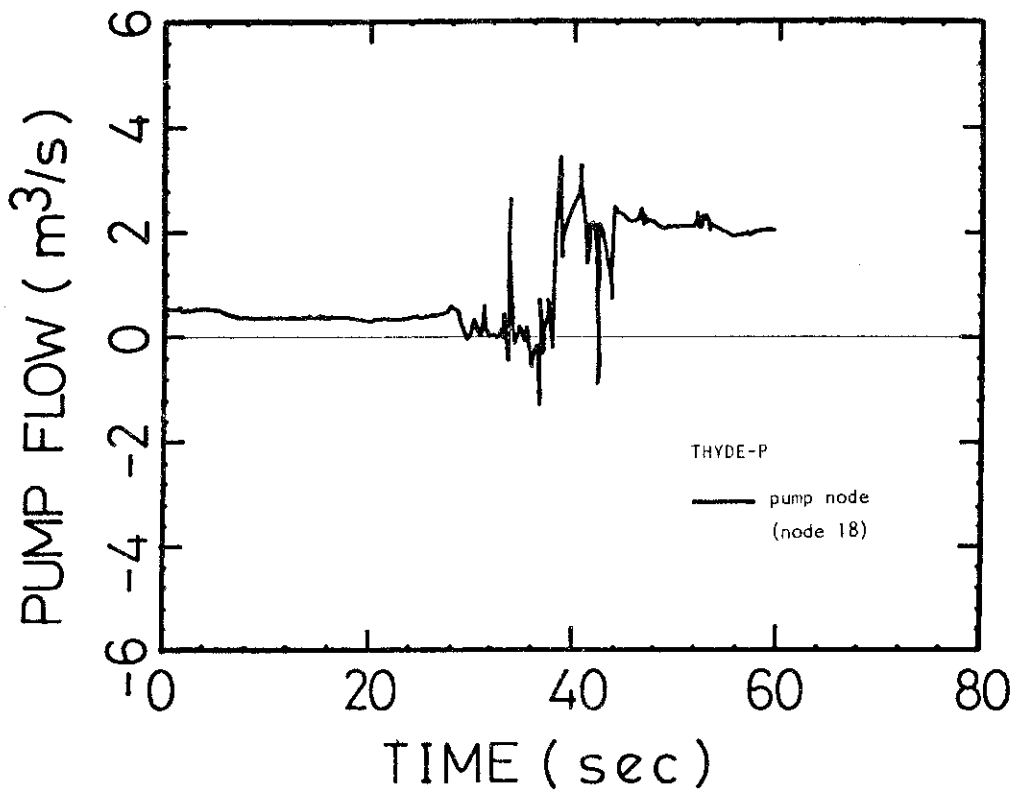


Fig.5.29 Calculated Pump Head

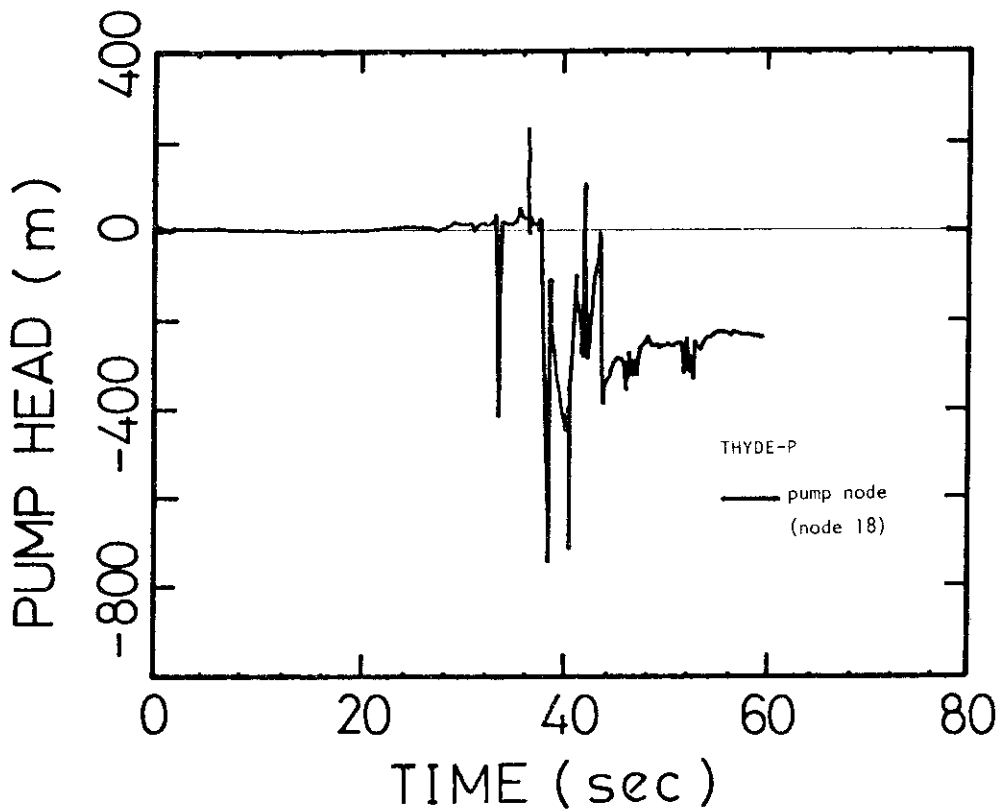


Fig.5.30 Calculated Pump Flow

6. Computing Time and Time Step Width

The CPU time required for the present calculation by a FACOM M-200 computer was about 2 hours. Therefore, the rate of the CPU time to the problem time was about 120. The computer core storage requirement was about 1.2 Mbyte without overlay structure. The maximum time step width allowed by inputs in the present calculation were:

$$t = \begin{cases} 0.001 \text{ sec.} & \text{for } 0.0 \text{ sec.} < t < 0.3 \text{ sec.} \\ 0.004 \text{ sec.} & \text{for } 0.3 \text{ sec.} < t \end{cases}$$

The whole calculation proceeded with the maximum time step width except when rapid transients were calculated.

7. Conclusion

The overall trend of the experiment was well simulated by the present calculation with the THYDE-P code. The rewetting phenomenon at the early stage of the blowdown, which was one of the most characteristic features in LOFT L2-3, was also calculated. Moreover, the calculated core reflood time was in good agreement with the experimental data. Since the present time delay model for density change had very large effects on the core reflood time, it is important to develop a model to evaluate the delay parameter realistically.

The heat transfer correlation package used in the present calculation, which should be considered to be used tentatively, was very simple and therefore refinements must be needed.

Acknowledgement

The author would like to express his thanks to Dr. Y. Asahi, who is the chief author of the THYDE-P code, for his valuable suggestions to this work. The author's thanks are also due to Mr. K. Sato, Chief of Reactor Safety Code Development Laboratory, and the members of the laboratory for their useful discussions.

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The CPU time required for the present calculation by a FACOM M-200 computer was about 2 hours. Therefore, the rate of the CPU time to the problem time was about 120. The computer core storage requirement was about 1.2 Mbyte without overlay structure. The maximum time step width allowed by inputs in the present calculation were:

$$t = \begin{cases} 0.001 \text{ sec.} & \text{for } 0.0 \text{ sec.} < t < 0.3 \text{ sec.} \\ 0.004 \text{ sec.} & \text{for } 0.3 \text{ sec.} < t \end{cases}$$

The whole calculation proceeded with the maximum time step width except when rapid transients were calculated.

7. Conclusion

The overall trend of the experiment was well simulated by the present calculation with the THYDE-P code. The rewetting phenomenon at the early stage of the blowdown, which was one of the most characteristic features in LOFT L2-3, was also calculated. Moreover, the calculated core reflood time was in good agreement with the experimental data. Since the present time delay model for density change had very large effects on the core reflood time, it is important to develop a model to evaluate the delay parameter realistically.

The heat transfer correlation package used in the present calculation, which should be considered to be used tentatively, was very simple and therefore refinements must be needed.

Acknowledgement

The author would like to express his thanks to Dr. Y. Asahi, who is the chief author of the THYDE-P code, for his valuable suggestions to this work. The author's thanks are also due to Mr. K. Sato, Chief of Reactor Safety Code Development Laboratory, and the members of the laboratory for their useful discussions.

6. Computing Time and Time Step Width

The CPU time required for the present calculation by a FACOM M-200 computer was about 2 hours. Therefore, the rate of the CPU time to the problem time was about 120. The computer core storage requirement was about 1.2 Mbyte without overlay structure. The maximum time step width allowed by inputs in the present calculation were:

$$t = \begin{cases} 0.001 \text{ sec.} & \text{for } 0.0 \text{ sec.} < t < 0.3 \text{ sec.} \\ 0.004 \text{ sec.} & \text{for } 0.3 \text{ sec.} < t \end{cases}$$

The whole calculation proceeded with the maximum time step width except when rapid transients were calculated.

7. Conclusion

The overall trend of the experiment was well simulated by the present calculation with the THYDE-P code. The rewetting phenomenon at the early stage of the blowdown, which was one of the most characteristic features in LOFT L2-3, was also calculated. Moreover, the calculated core reflood time was in good agreement with the experimental data. Since the present time delay model for density change had very large effects on the core reflood time, it is important to develop a model to evaluate the delay parameter realistically.

The heat transfer correlation package used in the present calculation, which should be considered to be used tentatively, was very simple and therefore refinements must be needed.

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References

- (1) Prassinos, P. G., "Experimental Data Report for LOFT Power Ascension Test L2-3", NUREG/CR-0792 TREE-1326, July 1979.
- (2) Reeder, D. L., "LOFT SYSTEM AND TEST DESCRIPTION(5.5 FT CORE1 LOCES)", NUREG/CR-0247 , July 1978.
- (3) Asahi, Y., "Description of THYDE-P Code (Preliminary Report of Methods and Models)", JAERI-M 7751, 1978.
- (4) Hirano, M and Asahi, Y., "Through Analysis of LOFT L2-2 by THYDE-P Code (1) (Sample Calculation Run 30)", JAERI-M 9535, 1981
- (5) Asahi, Y. and Hirano, M., "Verification Study of LOCA Analysis Code THYDE-P (Sample Calculation Run 10)", JAERI-M 8560, 1979.
- (6) Zaloudek, F. R., "Steam-Water Critical Flow from High Pressure System", HW-68936, Hanford Works, 1963.
- (7) Moody, F. J., "Maximum Floe rate of Single Component, Two-phase Mixture", Heat Trans.-Trans. ASME, 87 n1, pp 134-142, 1965.
- (8) Moore, K. V. and Retting, W. H, "RELAP4-A COMPUTER PROGRAM FOR TRANSIENT THERMAL-HYDRAULIC ANALYSIS", ANCR-1127, Dec. 1973.
- (9) Dittus, F. W. and Boelter, L. M. K., "Heat Transfer in Automobile Radiators of The Tubular Tube", 2, No. 13, pp 443-461, 1930.
- (10) Jens, W. H. and Lottes, P. A., "Analysis of Heat Transfer, Burnout, Pressure Drop and Density Data for High-Pressure Water", ANL-4627, 1951.
- (11) Groenevelt, D. C., "An Investigation of Heat Transfer in The Liquid Deficient Regime", Report AECL-3281, Chalk River, Ontatio, Dec. 1968.
- (12) McEligot, D. M., Ormand, L. W. and Perkins, H. C., J. Trans. Amer. Soc. Mech. Engrs., 88, Series C, pp 239-245, May 1966.
- (13) Biasi, L., et. al, "Studies on Burnout : Part 3", Energia Nucleare, pp 550-536, 1967.
- (14) McAdams, W. H., "Heat Transmission", 3rd Ed., pp 337, McGrow-Hill, 1954.
- (15) McDonough, J. B., Milich, W. and King, E. C., "Partial Film Boiling with Water at 2000 psig in a Round Vertical Tube", MSA Research Corrp., Technical Report 62(NP-6976), 1958.

- (16) Zuber, N., Tribus, M. and Westwater, J. W., "The Hydrodynamic Crisis in Pool Boiling of Saturated and Subcooled Liquids", International Developments in Heat Transfer, Part II, pp 230-236, 1961.
- (17) Griffith, p., Auedisian, C. T. and Walkush, J. F., "Countercurrent Flow Critical Heat Flux", presented at National Heat Transfer Conference, San Francisco, Aug. 1975.
- (18) Thom, J. R. S., et. al, "Boiling in Subcooled Water During Flow Up Heated Tubes or Annuli", Proc. Instn. Mech. Engrs., Vol. 180, Part 3c, pp 226-246, 1966.
- (19) Berenson, P. J., "Film-Boiling Heat Transfer from a Horizontal Surface", J. of Heat Transfer, Vol. 83, pp 351-358, Aug. 1961.

Appendix A Input Data List

```

-- LOFT L2-3 ANALYSIS BY THYDE-P CODE --                80.04.01      00000100
/                                                         00000200
/ **** DIMENSION DATA ****                             00000300
BB01                                                      00000400
  0  0  9  3  17  43  37  9  2  2  1  1  2  6  5  3      00000500
/                                                         00000600
/ **** MINOR EDIT DATA ****                             00000700
BB02                                                      00000800
PRE-30 PRA-08 PRA-07 GLA-21 GLE-07 GLA-08 GLE-35 GLA-23 GLA-23 00000900
/                                                         00001000
/ **** TIME STEP CONTROL DATA ****                     00001100
BB03                                                      00001200
SB0301                                                     00001300
  0.2  0.2  100.                                         00001400
SB0304                                                     00001500
  30  3  50  0  1.0E-3  1.0E-6  0.3  0.1               00001600
SB0305                                                     00001700
  30  3  50  0  4.0E-3  1.0E-6  90.0  0.1              00001800
SB0308                                                     00001900
  40  1  1  0  4.0E-3  1.0E-6  2000.0  0.1            00002000
/                                                         00002100
/ **** TRIP CONTROL DATA ****                          00002200
BB04                                                      00002300
SB0480                                                     00002400
  1  0  1  0  1000.0  0.0                                00002500
SB0481                                                     00002600
  5  42  1  0  0.002  0.0                               00002700
SB0482                                                     00002800
  2  18  1  0  1000.0  0.0                              00002900
SB0483                                                     00003000
  2  19  1  0  1000.0  0.0                              00003100
SB0484                                                     00003200
  3  0  1  0  0.103  0.0                                00003300
SB0485                                                     00003400
  4  1  1  0  14.0  0.0                                 00003500
SB0486                                                     00003600
  4  2  1  0  29.0  0.0                                00003700
SB0487                                                     00003800
 -4  1  1  0  1000.0  0.0                              00003900
SB0488                                                     00004000
 -4  2  1  0  1000.0  0.0                              00004100
SB0489                                                     00004200
  6  1  -3  1  240.0  0.005                             00004300
SB0490                                                     00004400
  6  2  -3  1  250.0  0.0                               00004500
SB0491                                                     00004600
  6  3  -3  1  360.0  0.0                               00004700
SB0492                                                     00004800
 -6  1  3  1  350.0  0.0                               00004900
SB0493                                                     00005000

```

	1	2	3	4	5	6	7-R	8
-6 2 3 1 305.0 0.0								00005100
SB0494								00005200
-6 3 3 1 380.0 0.0								00005300
SB0495								00005400
6 2 -2 1 160.0 0.0								00005500
SB0496								00005600
-6 2 2 1 190.0 0.0								00005700
/								00005800
/ **** FLOW AJUST DATA ****								00005900
BB05								00006000
1 3.1402 347.6								00006100
/								00006200
/ **** NODE DATA ****								00006300
BB06								00006400
SB0601								00006500
1 1 22 29 0 149.026047915	0.2842	0.0	1.332	0.0				00006600
	0.4	0.8	0.0	0.0				00006700
SB0602								00006800
2 1 29 1 0 148.885342560	0.2842	0.0	0.6965	0.0				00006900
	0.0	0.0	-1.0	-1.0				00007000
SB0603								00007100
3 1 1 2 0 148.885336895	0.1032	0.0	1.517	0.7174				00007200
	-1.0	-1.0	1.52	1.09				00007300
SB0604								00007400
4 1 2 3 0 148.838207175	0.3485	0.0	3.228	2.705				00007500
	0.0	0.0	189.0	189.0				00007600
SB0605								00007700
5 1 3 4 0 148.660515706	0.3485	0.0	3.228	-2.705				00007800
	0.0	0.0	142.0	198.0				00007900
SB0606								00008000
6 1 4 5 0 148.838194913	0.1272	0.0	2.423	-2.0394				00008100
	0.0	0.0	20.0	20.0				00008200
SB0607								00008300
7 1 5 6 0 148.972125842	0.1032	0.0	1.883	1.322				00008400
	0.0	0.0	-86446.58	0.0				00008500
SB0608								00008600
8 1 6 7 0 149.241450804	0.1032	0.0	0.4877	0.0				00008700
	0.0	0.0	-1.0	-1.0				00008800
SB0609								00008900
9 1 7 30 0 149.241451145	0.2842	0.0	0.6965	0.0				00009000
	-1.0	-1.0	0.0	0.0				00009100
SB0610								00009200
10 1 30 27 0 149.241451138	0.2842	0.0	0.9510	0.0				00009300
	0.0	0.0	3.58	3.0				00009400
SB0611								00009500
11 1 22 23 0 148.64454	0.2842	0.0	2.616	0.0				00009600
	0.4	0.8	0.0	0.0				00009700
SB0612								00009800
12 1 23 8 0 148.77914	0.2832	0.0	2.643	0.2432				00009900
	0.0	0.0	-1.0	-1.0				00010000
SB0613								00010100
13 1 8 9 0 148.77014	0.9084	0.0	0.5175	0.5175				00010200
	-1.0	-1.0	-1.0	-1.0				00010300
SB0614								00010400
14 7 9 10 1 148.71985	0.01021	0.0	2.568	2.483				00010500
	-1.0	-1.0	-1.0	-1.0				00010600
SB0615								00010700
15 7 10 11 1 148.49835	0.01021	0.0	2.568	-2.483				00010800
	-1.0	-1.0	-1.0	-1.0				00010900

	1	2	3	4	5	6	7-R	8			
SB0616	16	1 11 12	0 148.63618	0.9084	0.0	0.5175	-0.5175	00011000			
				-1.0	-1.0	-1.0	-1.0	00011100			
								00011200			
								00011300			
SB0617	17	1 12 24	0 148.59503	0.2941	0.0	2.426	-1.523	00011400			
				-1.0	-1.0	0.0	0.0	00011500			
								00011600			
SB0618	18	8 24 25	0 148.7532	0.3468	0.0	1.867	1.2807	00011700			
				0.0	0.0	0.0	0.0	00011800			
								00011900			
SB0619	19	8 24 25	0 148.7434	0.3043	0.0	3.111	1.2807	00012000			
				0.0	0.0	0.0	0.0	00012100			
								00012200			
SB0620	20	1 25 26	0 149.4056	0.2757	0.0	1.399	0.0	00012300			
				0.0	0.0	0.0	0.0	00012400			
								00012500			
SB0621	21	1 26 27	0 149.4106	0.2842	0.0	0.5313	0.0	00012600			
				0.0	0.0	3.58	3.0	00012700			
								00012800			
SB0622	22	4 27 13	0 149.2250	0.45190	0.0426	4.256	-4.256	00012900			
				0.62	0.62	3.5	3.5	00013000			
								00013100			
SB0623	23	5 13 28	0 149.4958	1.004	0.0	0.7318	0.0	00013200			
				0.0	0.0	0.0	0.0	00013300			
								00013400			
SB0624	24	1 28 14	0 149.4858	0.4417	0.0	0.4285	0.4285	00013500			
				0.0	0.0	-1.0	-1.0	00013600			
								00013700			
SB0625	25	2 14 15	0 149.3849	1.0	0.0	0.09423	0.09423	00013800			
				-1.0	-1.0	0.0	0.0	00013900			
								00014000			
SB0626	26	2 15 16	1 149.3422	1.0	0.0	0.4191	0.4191	00014100			
				0.0	0.0	0.0	0.0	00014200			
								00014300			
SB0627	27	2 16 17	1 149.2712	1.0	0.0	0.4191	0.4191	00014400			
				0.0	0.0	0.0	0.0	00014500			
								00014600			
SB0628	28	2 17 18	1 149.1979	1.0	0.0	0.4191	0.4191	00014700			
				0.0	0.0	0.0	0.0	00014800			
								00014900			
SB0629	29	2 18 19	1 149.1282	1.0	0.0	0.4191	0.4191	00015000			
				0.0	0.0	0.0	0.0	00015100			
								00015200			
SB0630	30	2 19 20	0 149.0567	1.0	0.0	0.01753	0.01753	00015300			
				0.0	0.0	-1.0	-1.0	00015400			
								00015500			
SB0631	31	1 20 22	0 149.0223	0.5513	0.05486	1.668	1.668	00015600			
				-1.0	-1.0	0.0	0.0	00015700			
								00015800			
SB0632	32	1 28 22	0 149.4858	0.0779	0.0	4.164	4.164	00015900			
				0.0	0.0	0.0	0.0	00016000			
								00016100			
SB0633	33	13 22 37	0 0.1 0.5419	0.0	0.9144	0.9144	0.0	0.0	0.0	00016200	
SB0634	34	13 29 35	0 0.1 0.222	0.0	4.048	0.8620	0.4	0.8	0.0	0.0	00016300
SB0635	35	13 30 36	0 0.1 0.222	0.0	4.840	0.6075	0.4	0.8	0.0	0.0	00016400
SB0636	36	13 23 21	0 4.0 0.043	0.0	4.592	0.4255	0.4	0.8	9.0	9.0	00016500
											00016600
											00016700
											00016800

	1	2	3	4	5	6	7-R	8
SB0637								00016900
37	13	21	34	0	4.0	0.043	0.0	4.767 0.7678 0.0 0.0 0.0 0.0
SB0638								00017000
38	13	26	31	0	10.0	0.089	0.0	5.5 0.0 0.4 0.8 0.0 0.0
SB0639								00017100
39	13	26	32	0	10.0	0.089	0.0	5.5 0.0 0.4 0.8 0.0 0.0
SB0640								00017200
40	13	26	33	0	10.0	0.089	0.0	58.0 0.0 0.4 0.8 0.0 0.0
/								00017300
/	**** JUNCTION DATA ****							00017400
BB07								00017500
1	1	0.0						00017600
2	1	0.0						00017700
3	1	0.0						00017800
4	1	0.0						00017900
5	1	0.0						00018000
6	1	0.0						00018100
7	1	0.0						00018200
8	1	0.0						00018300
9	1	0.0						00018400
10	1	0.0						00018500
11	1	0.0						00018600
12	1	0.0						00018700
13	1	0.0						00018800
14	1	0.0						00018900
15	1	0.0						00019000
16	1	0.0						00019100
17	1	0.0						00019200
18	1	0.0						00019300
19	1	0.0						00019400
20	1	0.0						00019500
21	1	0.0						00019600
22	4	0.1937						00019700
23	4	0.04149						00019800
24	4	0.05040						00019900
25	4	0.04644						00020000
26	4	0.08948						00020100
27	4	0.18						00020200
28	4	0.064						00020300
29	4	0.04474						00020400
30	4	0.04474						00020500
31	7	0.0						00020600
32	7	0.0						00020700
33	5	0.0						00020800
34	6	0.0						00020900
35	8	0.0						00021000
36	8	0.0						00021100
37	8	0.0						00021200
/								00021300
/	**** MIXING JUNCTION DATA ****							00021400
BB08								00021500
SB0801								00021600
22	3	1	11	33	0	0.001	0.999	0. 0.
SB0802								00021700
23	2	12	36	0	0	1.0	0.0	0. 0.
SB0803								00021800
24	2	18	19	0	0	0.5	0.5	0. 0.
SB0804								00021900
25	1	20	0	0	0	1.0	0.0	0. 0.

	1	2	3	4	5	6	7-R	8					
SB0805								00022800					
26	4	21	38	39	40	1.0	0.0	0.0	00022900				
SB0806									00023000				
27	1	22	0	0	0	1.0	0.0	0.0	00023100				
SB0807									00023200				
28	2	24	32	0	0	0.97	0.03	0.0	00023300				
SB0808									00023400				
29	2	2	34	0	0	1.0	0.0	0.0	00023500				
SB0809									00023600				
30	2	10	35	0	0	1.0	0.0	0.0	00023700				
/									00023800				
/ **** PUMPED INJECTION DATA ****									00023900				
BB09									00024000				
SB0901									00024100				
1	31	24.0							00024200				
10									00024300				
0.0	0.00	2.0	1.80	4.0	1.47	8.0	1.50		00024400				
28.0	1.60	64.0	1.70	72.0	1.00	120.0	1.00		00024500				
140.0	1.50	200.0	1.50						00024600				
SB0902									00024700				
2	32	24.0							00024800				
10									00024900				
0.0	0.00	3.0	3.50	7.0	4.80	11.0	5.30		00025000				
14.0	5.60	20.0	3.60	27.0	5.20	43.0	6.50		00025100				
59.0	7.00	200.0	7.40						00025200				
/									00025300				
/ **** PUMP DATA ****									00025400				
BB10									00025500				
SB1001									00025600				
18	1	1	3530.	.3155	500.24	108.1	613.73	1269.7	1.4328	.0	.0	1.	00025700
SB1002													00025800
19	1	1	3530.	.3155	500.24	108.1	613.73	1269.7	1.4328	.0	.0	1.	00025900
/													00026000
/ **** PUMP DATA TABLE ****													00026100
BB11													00026200
SB1101													00026300
1													00026400
12													00026500
-1.0	2.4722			-0.80574	2.0474								00026600
-0.6096	1.831			-0.40683	1.624								00026700
-0.200171	1.4705			0.0	1.4036								00026800
0.19061	1.3636			0.38963	1.3186								00026900
0.4118	1.3			0.59396	1.2328								00027000
0.7902	1.1336			1.0	1.0078								00027100
12													00027200
-1.0		-1.0		-0.80574		-0.6							00027300
-0.6096		-0.3		-0.40683		-0.05							00027400
-0.200171		0.13		0.0		0.25							00027500
0.19061		0.28		0.38963		0.34							00027600
0.4118		0.2768		0.59396		0.46							00027700
0.7902		0.70		1.0		0.9465							00027800
17													00027900
-1.0	-1.0			-0.82297	-0.98								00028000
-0.63332	-0.95			-0.45534	-0.90								00028100
-0.27109	-0.82			-0.17716	-0.78								00028200
-0.09073	-0.72			0.0	-0.67								00028300
0.091099	-0.60			0.186509	-0.52								00028400
0.271762	-0.42			0.45582	-0.21								00028500
0.574406	-0.02			0.740576	0.26								00028600

	1	2	3	4	5	6	7-R	8
	0.766619	0.36		0.871471	0.63			00028700
	1.0	1.0078						00028800
17								00028900
-1.0		2.4722		-0.82297		1.9968		00029000
-0.63332		1.5897		-0.45534		1.3279		00029100
-0.27109		1.1949		-0.17716		1.0605		00029200
-0.09073		1.0156		0.0		0.934279		00029300
0.091099		0.9229		0.186509		0.8963		00029400
0.271762		0.875		0.45582		0.8433		00029500
0.574406		0.8355		0.740576		0.8466		00029600
0.766619		0.8469		0.871471		0.8838		00029700
1.0		0.9465						00029800
14								00029900
-1.0	1.9843			-0.80096	1.394			00030000
-0.60638	1.0975			-0.40686	0.822			00030100
-0.30	0.71			-0.19928	0.6648			00030200
-0.10	0.61			0.0	0.6032			00030300
0.1930	0.6325			0.393	0.7369			00030400
0.50	0.79			0.59552	0.8381			00030500
0.79782	0.9229			1.0	0.9672			00030600
14								00030700
-1.0		-1.0		-0.80096		-0.98		00030800
-0.60638		-0.94		-0.40686		-0.91		00030900
-0.30		-0.90		-0.19928		-0.70		00031000
-0.10		-0.51		0.0		-0.45		00031100
0.1930		-0.37		0.393		-0.26		00031200
0.50		-0.01		0.59552		0.06		00031300
0.79782		0.21		1.0		0.3569		00031400
17								00031500
-1.0	-1.0			-0.82234	-0.98			00031600
-0.63371	-0.94			-0.45853	-0.92			00031700
-0.267023	-0.91			-0.176107	-0.85			00031800
-0.089310	-0.80			0.0	-0.67			00031900
0.090643	-0.59			0.188569	-0.50			00032000
0.27347	-0.40			0.455869	-0.05			00032100
0.57448	0.28			0.73816	0.52			00032200
0.76852	0.61			0.870057	0.74			00032300
1.0	0.9672							00032400
17								00032500
-1.0		1.9843		-0.82234		1.8308		00032600
-0.63371		1.6824		-0.45853		1.557		00032700
-0.267023		1.4362		-0.176107		1.3879		00032800
-0.089310		1.3481		0.0		0.23361		00032900
0.090643		1.1965		0.188569		1.1096		00033000
0.27347		1.0416		0.455869		0.8958		00033100
0.57448		0.7807		0.73816		0.6137		00033200
0.76852		0.5849		0.870057		0.4877		00033300
1.0		0.3569						00033400
12								00033500
-1.0	-1.15	-0.9	-1.24	-0.6	-2.8	-0.5	-2.9	00033600
-0.4	-2.7	0.0	0.0	0.12	0.85	0.2	1.1	00033700
0.5	1.02	0.7	1.0	0.9	0.95	1.0	1.0	00033800
4								00033900
-1.0	0.0	0.0	0.0	0.5	-0.8	1.0	-1.46	00034000
7								00034100
-1.0	0.0	0.0	0.0	0.1	-0.02	0.2	0.0	00034200
0.3	0.1	0.9	0.78	1.0	1.0			00034300
12								00034400
-1.0	-1.15	-0.8	-0.5	-0.6	-0.2	-0.4	0.03	00034500

	1	2	3	4	5	6	7-R	8	
	-0.2	0.04	0.0	0.1	0.2	0.15	0.4	0.12	
	0.6	0.05	0.8	-0.5	0.9	-0.9	1.0	-1.46	
0								00034600	
0								00034700	
0								00034800	
0								00034900	
0								00035000	
0								00035100	
0								00035200	
13	0.0	0.0	0.05	0.0	0.1	0.025	0.15	0.075	
	0.0	0.05	0.0	0.1	0.025	0.15	0.075	0.2	
	0.0	0.05	0.0	0.1	0.025	0.15	0.075	0.18	
	0.3	0.475	0.4	0.625	0.5	0.74	0.6	0.82	
	0.7	0.87	0.8	0.84	0.9	0.72	1.0	0.08	
								00035300	
11	0.0	0.0	0.1	0.0	0.20	0.13	0.3	0.24	
	0.0	0.0	0.1	0.0	0.20	0.13	0.3	0.24	
	0.4	0.31	0.5	0.33	0.6	0.3	0.7	0.23	
	0.8	0.16	0.9	0.08	1.0	0.0			
								00035400	
								00035500	
								00035600	
6 6	0.0	0.2	0.4	0.6	0.8	1.0			
	0.0	0.0	0.0	0.0	0.0	0.0			
	0.0	0.0	0.0	0.0	0.0	0.0			
	0.2	0.0	3.0650E-5	7.7239E-5	1.3263E-4	1.9460E-4	2.6207E-4		
	0.4	0.0	4.8660E-5	1.2261E-4	2.1053E-4	3.0996E-4	4.1602E-4		
	0.6	0.0	6.3760E-5	1.6066E-4	2.7587E-4	4.0485E-4	5.4514E-4		
	0.8	0.0	7.7239E-5	1.9463E-4	3.3419E-4	4.9044E-4	6.6037E-4		
	1.0	0.0	8.9628E-5	2.2585E-4	3.8780E-4	5.6910E-4	7.6631E-4		
								00036000	
								00036100	
								00036200	
								00036300	
								00036400	
								00036500	
								00036600	
								00036700	
								00036800	
/								00036900	
/	**** ACCUMLATOR DATA ****								00037000
BB12								00037100	
SB1201								00037200	
	43	33	1.71	0.96	34.2	41.25	0.9	0.1	
								00037300	
/								00037400	
/	**** BREAK POINT DATA ****								00037500
BB13								00037600	
	6	0.000	0.1	0.8	0.8	0.6	0.8	0.6	
								00037700	
	2							00037800	
	0.0	5.0	100.0	5.0				00037900	
/								00038000	
/	**** PRESSURIZER DATA ****								00038100
BB14								00038200	
	41	34	1	0.557	1.7235	0.4	0.4	0.01	
	1.0	1.0	1.0	1.0	1.0	0.0737	0.0737	0.0737	
	0.313	0.313	0.313	1.0	1.0	1.0			
								00038300	
	2							00038400	
	0.	1.0	1.0	1.0	1000.	1.0	1.0	1.0	
								00038500	
/								00038600	
/	**** STEAM GENERATOR DATA ****								00038700
BB15								00038800	
SB1501								00038900	
	42	1845	14	15	2	1		00039000	
	1.589	4.188	1.0	1.0	0.01905	0.005105	4.469	0.3	
	0.000	0.3	60.99				213.8	19.5	
		-20.0	-8.0						
	0.001	80.	0.5	0.5	0.5				
								00039100	
	3							00039200	
	0.0	1.0	1.0	1.0	1.0	1.0	1000.0	1.0	
								1.0	
								0.0	
/								00039300	
/	**** CORE DATA ****								00039400
BB16								00039500	
	1300	25	30	0	9000.			00039600	
	5.359E-3	6.172E-4	4.647E-3	1.43E-2	0.6	19.52E-6		00039700	
	0.0124	2.395E-4	0.0305	1.5897E-3	0.111	1.423E-3		00039800	
	0.301	2.869E-3	1.14	8.347E-4	3.01	3.048E-3		00039900	
								00040000	
								00040100	
								00040200	
								00040300	
								00040400	

```

-----1-----2-----3-----4-----5-----6-----7-R-----8
  5.0      0.6      4.91E-04  3.41E-06  1.2      1.54E03      00040500
  0.0     106.605    179.738    137.030    45.427     0.0          00040600
1.0000E-07 1.00E-07  1.00E-07  1.00E-07  1.000E-07  1.0E-7      00040700
1.0000E-07 1.00E-07  1.00E-07  1.00E-07  1.000E-07  1.0E-7      00040800
1.0000E-07 1.00E-07  1.00E-07  1.00E-07  1.000E-07  1.0E-7      00040900
1.0000E-07 1.00E-07  1.00E-07  1.00E-07  1.000E-07  1.0E-7      00041000
/
/ ***** SG RELIEF VALVE DATA *****
BB17
  6
  0.  0.  0.1 -14.  0.18 -32.  0.34 -62.  0.5 -94.  0.58 -179.
  4
50. -0.00030 380. -0.00022 1200. -0.00015 2280. -0.00008
  9
  0.0 0.0 0.2 -0.2 0.4 -0.4 0.6 -1.4 0.8 -2.6
  1.0 -5.6 1.2 -12.6 1.4 -15.4 200.0 -15.6
/
/ *****
BB18
  1.54E03      0.775E-04      2.29E04
/
/ ***** FUEL GAP DATA *****
BB19
  5.7E-4  0.0      5.493E-6  0.0  0.0
  0.0  0.0  0.9  0.75  0.0
  0.887  0.0355  0.0063  0.0  0.0712
  0.0  0.0
/
/ *****
BB21
  2  2  5.00E7  6.96E-08  2.87E4  2.86E-03  1.15E0  1.528E0
      1.49E-07  2.0E-08  1.25E-16  1.85E-01  8.0E09  3.3E-03
/
/ ***** OTHER DATA *****
BB22
  0. 1.4 1.4 0.
BEND
  6
  0 0 0 0 0 0.
  0. 1.E-5 0. 0. 0. 0.
END
00041100
00041200
00041300
00041400
00041500
00041600
00041700
00041800
00041900
00042000
00042100
00042200
00042300
00042400
00042500
00042600
00042700
00042800
00042900
00043000
00043100
00043200
00043300
00043400
00043500
00043600
00043700
00043800
00043900
00044000
00044100
00044200
00044300
00044400
00044500

```

Appendix B Nomenclature

c_n	Quantity defined in Subsec. 3.4, s
G	Mass flux, $\text{kg/m}^2\text{s}$
G_{\min}	Mass flux defined in Subsec 3.1, $\text{kg/m}^2\text{s}$
h	Coolant enthalpy, kcal/kg
h_{gs}	Saturated steam enthalpy, kcal/kg
h_{fs}	Saturated fluid enthalpy, kcal/kg
Re	Reynolds number, -
T_{coolant}	Coolant temperature, $^{\circ}\text{C}$
T_{wall}	Wall temperature, $^{\circ}\text{C}$
T_{sat}	Coolant saturation temperature, $^{\circ}\text{C}$
ΔT_s	Wall superheat, $^{\circ}\text{C}$
ΔT_{\min}	Minimum film boiling wall superheat, $^{\circ}\text{C}$
x	Coolant quality, -
x_c	Coolant quality defined in Subsec. 3.2, -
α	Equilibrium void fraction, -
α^*	Non-equilibrium void fraction, -
ρ	Equilibrium node average density, kg/m^3
ρ^*	Non-equilibrium node average density, kg/m^3
ρ_{gs}	Saturated steam density, kg/m^3
ρ_{fs}	Saturated fluid density, kg/m^3
τ_D	Delay parameter, s
ϕ	Heat flux, $\text{kcal/m}^2\text{s}$
ϕ_c	Heat flux defined in Subsec. 3.2, $\text{kcal/m}^2\text{s}$
ϕ_{CHF}	Critical heat flux, $\text{kcal/m}^2\text{s}$
ϕ_{4-1}	Heat flux calculated by using heat transfer mode 4.1, $\text{kcal/m}^2\text{s}$
ϕ_{4-2}	Heat flux calculated by using heat transfer mode 4.2, $\text{kcal/m}^2\text{s}$